# Global Apollo KleanGas Joint Venture

GLOBAL APOLLO KLEANGAS LTD

"Solutions for Tomorrow's Problems Today"



# THE GLOBAL APOLLO KLEANGAS POWER PLANT

- The Power Plant operates as a Parallel System in a house, farm or commercial establishment with the Lead Cobalt Battery supplying power directly to the <u>DCto ACInverter</u> 24-hours a day and the Fuel Cell charging the battery. The battery can supply excess power to the grid during peak hours at the command of the electric utility company which controls this function.
- A Photovoltaic Cell operates in daylight hours and supplies power to a Battery Conditioner or an Electrolysis Unit for generating hydrogen. This is an optional device which may be used to enhance the system operation.
- The Fuel Cell charges the battery at various rates of charge throughout the day and night, but may be shut down part of the day and all night, as controlled by the Microprocessor. It can also supply power to the grid during peak hours, by-passing the battery. It can supply heat for a continuous flow of hot water at 800C.
- A Silver Volt Electric Vehicle contains a Power Plant which may also supply power to the grid during peak hours by plugging into a special receptade.
- The Power Plant can be utilised in an infinite number of ways, depending on its size. Six sizes, Models 101-B, 102-C, 104-C, 115-C, 120.5-A and 127-C, have been designed so far to handle different situations for various customers. Other combinations of fuel cell and battery can be designed for other applications.

One operating scenario for Model 101-B is shown below. It supplies 51.6 kWh per day to a large house and 48 kWh a day to the grid, for a total supply of 99.6 kWh. (Its maximum capacity is 276 kWh per day).

#### Supply to large house:

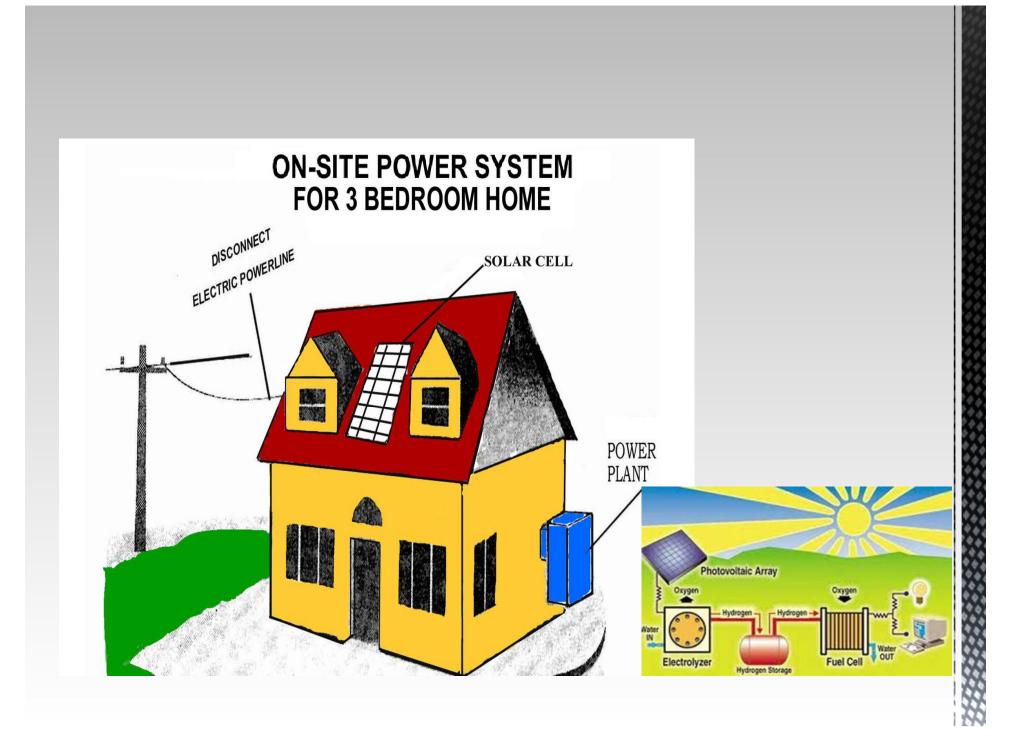
100-amps x 1-hour	=	100 ampere hours	
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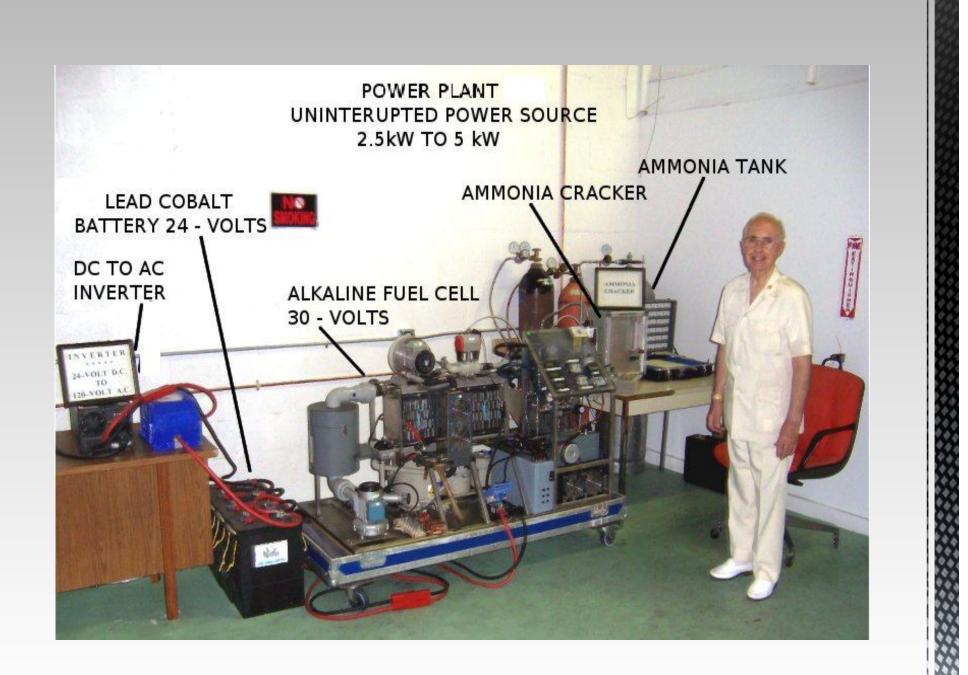
- 5-amps x 23 hours =  $\underline{115}$  ampere hours
- Total 215 ampere hours x 240 volts = 51.6 kWh

#### Additional supply to the grid:

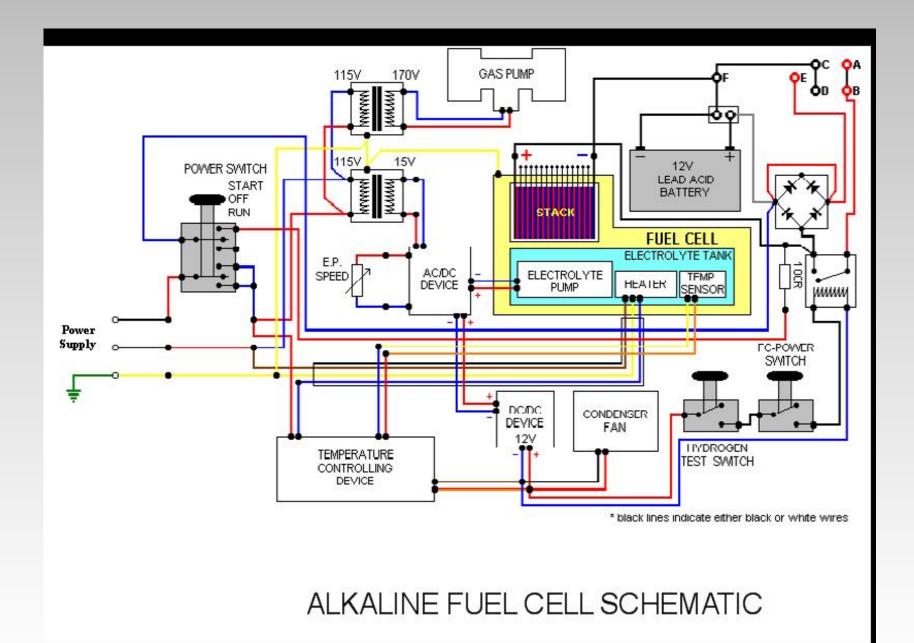
- 40-amps x 5 hours = <u>200</u> ampere hours x 240 volts = <u>48.0 kWh</u>
  - 415 ampere hours = 99.6 kWh
- Average charging rate for Fuel Cell when charging battery:
- 19-amps x 24 hours x 288-volts (on-charge battery voltage) = 131.33 kWh
- To replace 415 ampere hours: 415 + 41 = 456 a.h. [456 a.h. x 288-volts= 131.33 kWh]
- DAILY FUELCONSUMPTION FOR FUELCELLIS 131.33 kWh IN THIS EXAMPLE AND CAN BE SUPPLIED BY VARIOUS FUELS AS SHOWN ON THE FOLLOWING PAGES.

• MODEL 101-B COULD SUPPLY UP TO 276 kWh OF POWER PER DAY.









#### 72 kWh POWER PLANT

 Application: 24-Hour Power Supply for Home, Farm or Commercial Establishment for Heating, Lighting and operation of Appliances independent of outside power line (utility grid) supplied by electric utility company. Will operate an 8-HP AC Electric Motor on a continuous 24-hour basis.

Specification of Power Plant

- Lead Cobalt Battery. 240-volt @ 300-amps 1/C -- 72 kWh Battery supplies power to Inverter.
- Fuel Cell. 342-volts open circuit (360 cells @ 0.95 volts/cell). 288-volts (@ 0.8 volts per cell) under 19-amp load = 5.47 kW. Fuel cell charges battery at 288-volts @ 19-amps.

• Maximum Heating & Lighting Energy: 5.47 kW x 24-hours = <u>131 kWh</u> x 30 days = 3,930 kWh.

	DCto ACInverter for supplying		72.00 kW	
	Overload protection for one m	inute 600 amps @240 volts	144 kW	
	Input from battery:	288 VDC, 19-amps	5.47 kW	1
	···•••••••••••••••••••••••••••••••••••	, , , , , , , , , , , , , , , , , ,	•••••	
-	<b>-</b> · · · · · · · · · · · · · · · · · · ·			
	Output: 240	VAC, 50/60 Hertz, 21.6-amps	s <b>5.200 kW</b>	
	230 /	VAC, 50/60 Hertz, 22.6-amps	s <b>5.200 kW</b>	,
_	200	vAQ, 50/00 Tiertz, 22.0-amps	J.200 KW	
				HOME HEATING & HOUTING
	120 \	VAC, 50/60 Hertz, 43.3-amps	5 5.200 kW	HOME HEATING & LIGHTING
		, , , ,		COMMERCIAL. 5.47 kW FUEL CELL
	Microprocessor for control of e	entire system.		<u>&amp;</u>

Cable, conduit, plumbing, sensors, cabinets for system integration

• FOB Factory

Hydrogen Generation Equipment

**OVERLOAD PROTECTION** 

72 kWh BATTERY with 144 kW



# For Model 106 - B

FUEL >	Hydrogen (Liquid)	Hydrogen (Liquid)	n-Butane	Methanol	Ammonia Anhyd.	Ammonia 29.0%	Methane	Natural Gas	LPG (Propane)
Chemical \$ ymbol	Н	Н	C4H30	CH3OH	NH3		CH4	96%CH4	96%C3H
Power consumption	131.3	131.3	131.3	131.3	131.3	131.3	131.3	131.3	131.3
(kWh/day)									
System efficiency	66.0	66.0	40.0	420	50.0	45D	40.0	40.0	40.0
(%)					-				
Fuel consumption (kWh/day)	199.0	1990	328.3	312.7	262.7	291.8	328.3	328.3	328.3
Fuel consumption	7163	7163	11820	1125.7	945.6	1050.6	11820	1182.0	11820
(MJ/dav)									
(1 kWh = 3.6 x 10 <sup>s</sup> J)									
High Heat Value (HHV)	143.4	143.4	49.5	21.8	209	58	561	56.1	48.0
(MJ/log)						+ +		+	
Fuel (kg)	50	5.0	239	51.6	452	181.0	21.1	21.1	24.6
Fuel (ft <sup>3</sup> as gas)	2114.2	2114.2	338.0		2075.0		1096.6	1096.6	468.0
Fuel (liters as liquid)	728	728	41.5	653	743		49.5	49.5	49.5
								Values =	Value =
			_			+ +	_	Methane	Propane
Fuel Cost Information	\$0.320	\$1.00-\$1.40		\$0.185	\$0.09-\$0.10	\$0.04-\$0.06	_	\$5-\$10	\$0.90-\$0.93
	per lb.	per lb.		per liter	per lb.	per lb.		per 1000 ft <sup>i</sup>	Pergal
				(\$.70/gal)		1 1			
	H2 Info Net as Liquid at producer site	H2 Info Net as Liquid delivered and stored		Methanex Bage Pice FOB port	CF Ind. In 40,000 Ib. Tanker FOB dist	LaRoche In 44,000 Ib. Tanker FOB dist		EIA Chart Ave. Resid. 96% CH4	Teco Bulk undelivered 96% C3H3
Calculation	\$0.32	\$1.20		\$0.185	\$0.095	\$0.05		\$7.50	\$925
Celturation	40.32	41.20	-		40.000	<i>20.05</i>	-	41_0	
Cost Per Day	\$3.52	\$13.20		\$12.08	\$9.45	\$19.95		\$8.23	\$12.10
Cost Per 30-Day Month	\$105.60	\$396.00		\$362.42	\$283.50	\$597.30	_	\$246.74	\$363.00

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#### FUEL CELL OPERATING COST - PRELIMINARY for Power Plant Hybrid Model 106-B

# GLOBAL APOLLO KLEANGAS J.V. Fuel Consumption Ia

	Hydrogen	Butane	Propane	Methanol	Ammonia
Power consumption [kWh/day]	131.3	131.3	131.3	131.3	131.3
System eff. [%]	66	40	40	42	50
Fuel consumption [kWh/day]	199.0	328.3	328.3	312.7	262.7
Fuel consumption [MJ/day]	716.3	1,182.0	1,182.0	1,125.7	945.6

# GLOBAL APOLLO KLEANGAS J.V. Fuel Consumption Iia

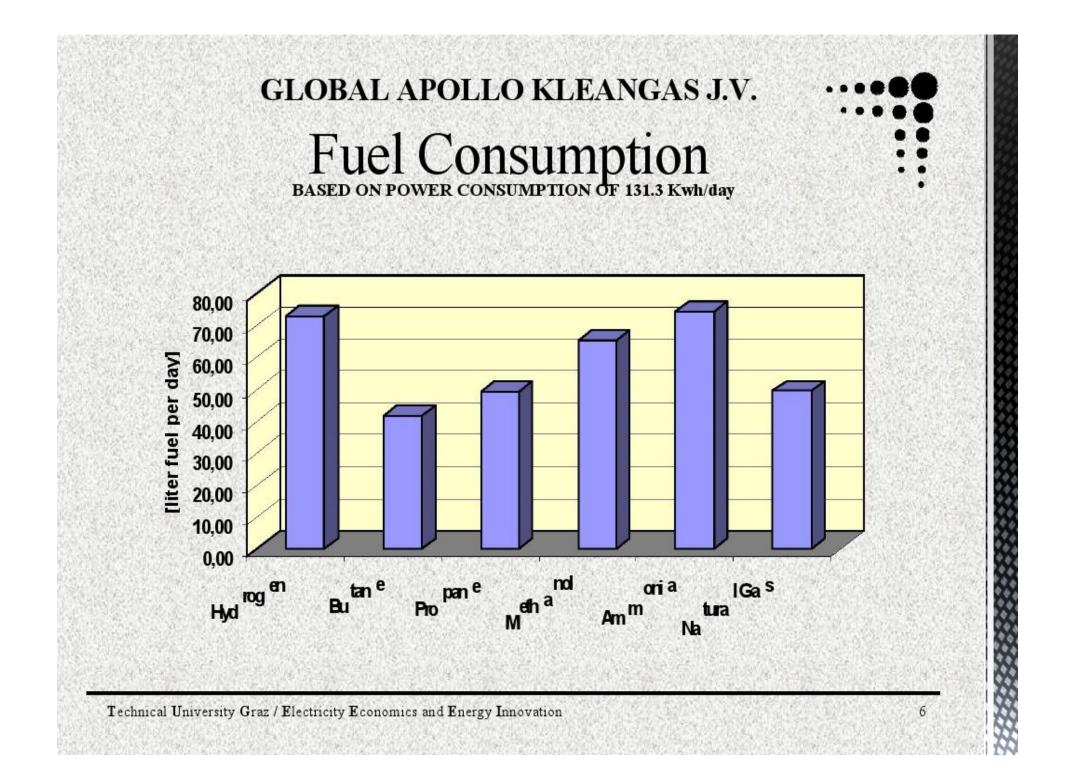
	Natural Gas	Ammonia 25%	Ammonia 40%	Ammonia anhydr.
Power consumption [kWh/day]	131.3	131.3	131.3	131.3
System eff. [%]	40	45	45	50
Fuel consumption [kWh/day]	328.3	291.8	291.8	267.7
Fuel consumption [MJ/day]	1,182.0	1,050.6	1,050.6	945.6

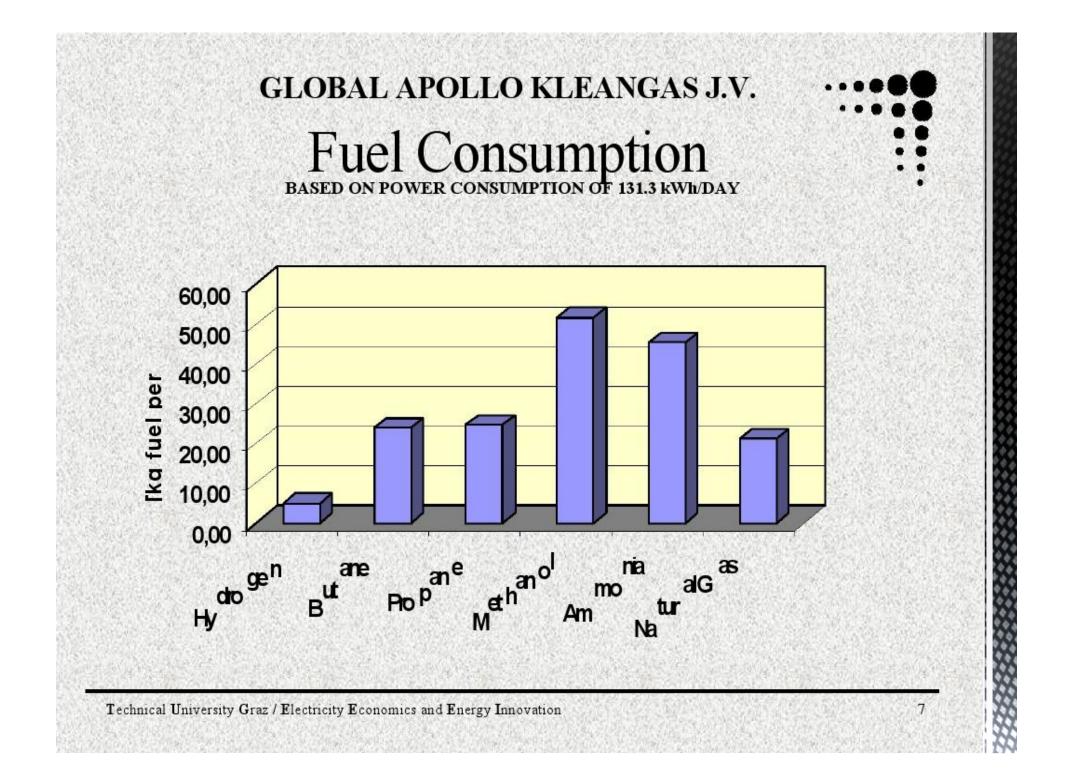
# GLOBAL APOLLO KLEANGAS J.V. Fuel Consumption Ib

	Hydrogen	Butane	Propane	Methanol	Ammonia anhydr.
Power consumption [kWh/day]	131.3	131.3	131.3	131.3	131.3
Fuel consumption [MJ/day]	716.3	1,182.0	1,182.0	1,125.7	945.6
HHV [MJ/kg]	143.4	49.5	48.0	21.8	20.9
Fuel [kg]	5.0	23.9	24.6	51.6	45.2
Fuel [ft <sup>3</sup> ]	2,114.2	338.8	468.0		2,075.0
Fuel [liter]	72.8	41.5	49.3	65.3	74.3

# GLOBAL APOLLO KLEANGAS J.V. Fuel Consumption Iib

	Natural Gas	Ammonia 25%	Ammonia 40%	Ammonia anhydr.
Power consumption [kWh/day]	131.3	131.3	131.3	131.3
Fuel consumption [MJ/day]	1,182.0	1,050.6	1,050.6	945.6
HHV [MJ/kg]	56.1	5.2	8.4	20.9
Fuel [kg]	21.1	201.1	125.7	45.2
Fuel [ft <sup>3</sup> ]	1,096.6	-	-	2,075.0
Fuel [liter]	49.5	220.9	147.0	74.3







Cabinet on left will house 26.4 kWh Lead Cobalt Battery (240-volts @ 110-amps I/ C) Cabinet in center will house 15.8 kW Fuel Cell (288-volts @ 0.8 volts' cell under 55-amp load) Cabinet on right will house DCto ACInverter,

Microprocessor and Miscellaneous Equipment Output: 240 VAC, 50/60 Hertz, 62.7amps 230 VAC, 50/60 Hertz, 65.4amps 120 VAC, 50/60 Hertz, 125.4amps Oneminute power surge: 330.0-amps @ 288-volts

Fuel Cell can be shut down at night while battery continues to operate the system

### POWER PLANT MODEL 115-C for Residential / Commercial Use

#### **POWER PLANT MODEL 5200**

#### 51.8 kW FUEL CELL & 86 kWh BATTERY with 891 kW OVERLOAD PROTECTION

APPLICATION: 24-Hour Power Supply for Homes

#### Required equipment for back-up Power Plant:

- Lead Cobalt Battery. 240 volts @360 amps 20/C-86.40 kWh
- One-minute power surge: 1,440 amps. Battery supplies power directly to Inverter.
- -

Fuel Cell. 288 volts (303 cells @ 0.95 volts/cell) @180-amps-51.84 kW

#### DCto ACInverter, Grid-Tie, for supplying power to load.

Input from battery (continuous): 360 VDC, 360 amps	86.400 kW
One minute surge power: 1,440-amps @ 240 volts	345.600 kW

Output:	240 VAC, 50/60 Hertz,	216 amps	51.840 kW
	230 VAC, 50/60 Hertz,	225.39 amps	51.840 kW
	120 VAC, 50/60 Hertz,	432 amps	51.840 kW

- Microprocessor for control of entire system. Grid feedback controlled by utility company.
- Cable, conduit, plumbing, hydrogen sensors, cabinets for system integration.

		Per Power Plant
Price FOB Factor	y For 4 Power Plants	US\$147,531
	For 300 Power Plants	US\$ 118,519
	For 5,000 Power Plants	US\$ 94,258
	For 200,000 Power Plants	US\$ 67,600

Water Bectrolyser

Size of Power Plant	Gallons NH3	Square Feet	Cubic Feet	Replacement	Annual	Replacement	Selling Price
	per 24 hours	Installation	Fuel Tank	of F.C. Stacks**	Maintenance	of Batteries#**	Sennig Thee
100 kW	39	16	7	\$24,502	See note ##	\$9,620	\$129,012
1,000 kW (1 MW)	393	1,600	70	\$245,024	See note ##	\$96,720	\$1,289,600
10 MW	3,936	16,000	700	\$2,450,240	See note ##	\$967,200	\$12,896,000
20 MW	7,872	32,000	1,400	\$4,900,480	See note ##	\$1,934,400	\$25,792,000
25 MW	9,840	40,000	1,750	\$6,110,000	See note ##	\$2,418,000	\$32,240,000
40 MW	15,744	64,000	2,800	\$9,800,960	See note ##	\$3,868,800	\$51,584,000
50 MW	19,680	80,000	3,500	\$12,220,000	See note ##	\$4,836,000	\$64,480,000
100 MW	39,360	160,000	7,000	\$24,440,000	See note ##	\$9,672,000	\$128,960,000
**Replacement of							
Fuel Cell Stacks							
every 7-1/2 years							
## One day per week							
inspection by an							
engineer + worker							
plus \$1,000 per week							
for spare parts.							
#**Replacement of							
Batteries every 5-years							

1.2.5

#### Fuel Cell Chart

	Phosphoric Acid Fuel Cell	Proton Exchange Membrane Fuel Cell	Liquid Molten Carbonate Fuel Cell	Solid Oxide Fuel Cell	Alkaline GAK Fuel Cell (1)	GAK Direct Methanol 'MARS'' Fuel Cell (2)
	PAFC	PEM	MCFC	SOFC	AFC	DMFC
Electrolyte	Liquid Phosphoric Acid r	Ion Exchange nembrane (solid polymer)	Liquid Molten Carbonate	Ceramic	Potassium Hydroxide	Potassium Hydroxide-
Catalyst	Platinum	Platinum	Nickel	Perovskites	Silver Alloy	Silver Alloy
Cell Operating Temperature (degreesC)	205 C	Room temperature to 80?C	550 C	800-1000 C	Room temp. to307C	Room temp- To 709C (3)
Electrical System Efficiency (% LHV)	36-45	32-40	43-55	43-55	50-60	>50
Some Applications Cogeneration	۲.	4	4	4	4	
Utility Power	4		4	4	4	
Distributed Power	*	*	4	4	*	
Utility Repowering	4		4	4	×	
Passenger Vehicles		*			4	4
HeavyDuty Vehicles	4	4		4	4	4
Portable Power		4			4	4
Specialty Power		*			×	4

- - -

#### 1. The GAK FUEL CELL

Alkaline Fuel Cell with circulating electrolyte, which can be shut down when not in use. This extends life of the electrodes and allows for maintenance. It has a higher voltage than the other types of Fuel Cells. Patents have been applied for by AES on this fuel cell and a working model is in operation at AES's laboratory in Fort Lauderdale florida.

2. The GAK MARS FUEL CELL

Direct Methanol Alkaline Fuel Cell with circulating electrolyte and a polyethylene separator (proton exchange membrane separator not needed). The anode catalyst draws hydrogen from the liquid methanol, eliminating the need for a reformer. The carbon dioxide produced stays in the electrolyte as a liquid carbonate (K<sup>2</sup> CO [or Na<sup>2</sup>CO<sup>3</sup> if sodium hydroxide is used instead of potassium hydroxide], which can be pumped out periodically and exchanged for fresh potassium hydroxide (or sodium hydroxide). There are no CO<sup>2</sup> or, other emissions from the alkaline DMFC (there are CO2 emissions from the acidic [H<sup>2</sup>SO ] DMFC). Cell voltage of the alkaline DMFC is higher than the acidic DMFC. Patents have been applied for by Apollo<sup>TM</sup> Energy Systems, Inc. on the Direct Methanol And Alkaline Fuel Cell.

3. Or higher temperature if methanol vapor is used.

### Ammonia Consumption of a 5 kW Fuel Cell System

### Premises

Nominal rated power	5 kW
Cell voltage	0.65 V
Cell current	40 A
Hydrogen use efficiency	66%

### Results

Mass related ammonia demand	$0.71~{ m g~s}^{-1}$
	2.5 <sup>-1</sup>
	5.5 lb/h
Volumetric ammonia demand	$3.1  \mathrm{l}  \mathrm{h}^{-1}$
	0.82 gal/h

- Summary of technical possibilities, Global Projections, Ammonia Fuel
- The use of ammonia as hydrogen source for alkaline fuel cells with circulating liquid electrolyte was already
- demonstrated with low-cost crackers built in 2000. Figure 1 shows the diagram of an AFC system with an
- ammonia cracker. Figure 2 shows a picture of an operating system. We discuss and model the use of ammonia
- and crackers together with alkaline fuel cells, analyzing the gains in efficiencies and in savings by using lowcost
- accessories and offering green house environmental advantages. The immediate commercial global
- availability is emphasized. Several companies in USA and the European Union continue to develop alkaline
- fuel cells (AFCs) with liquid electrolyte for mobile and stationary applications. At the University of Technology
- Graz, Austria, the Union Carbide Corp. Fuel Cell System has been improved in power output and life in on-off

Alkaline Fuel Cell–Hybrid Systems with NH3 Cracker as H2-Producer

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- In recent Automobile-Hybrid Systems, the combined operation with batteries has been emphasized in order to
- reduce the size and cost of fuel cells and improve their peak performance. The key questions still remains:
- Where should the hydrogen come from and how should it be stored and transported. To solve this urgent
- question of the fuel supply, the use of ammonia as hydrogen source for alkaline fuel cells was demonstrated at
- the University of Technology Graz in cooperation with Apollo Energy Systems, Inc. (AES Inc.) in Horida.
- The AFC's of AESInc. optimally operate at a temperature around 70 deg C, with a liquid circulating alkaline
- electrolyte which also serves as heat- and water management system. The operation is essentially at
   etmospheric pressure of budgegep and size. As preseded, the budgegep is preduced by an Ammonia Cred
- atmospheric pressure of hydrogen and air. As needed, the hydrogen is produced by an Ammonia Oracker
- System on demand. Important for this fuel cell set-up which avoids any amount of hydrogen in storage or
- transportation, is also the operation as a hybrid with a rechargeable battery in parallel. It takes care of peak
- performance requirements and delays after shut down and restarting. A new ammonia cracker (Pat. appl. for)
- operates very efficiently at temperatures which make it possible to build it from low cost steel components.
- Commercial liquid ammonia, which is stored in low pressure tanks, can be delivered by existing international

- and national ammonia networks and therefore, a global hydrogen carrier infrastructure is already well
- established. The safety aspects of ammonia are commercially established (ice-rinks, refrigerator industry,
- fertilizer). The global production of ammonia steadily increases with the world population.

- A global distribution for H2-fuel can be guaranteed by using ammonia which is produced in quantities of
- hundreds of million tons per year and is distributed by boats, tank cars and even pipelines. There is no
  problem
- with gas stations if ammonia will be distributed to the customers in liquefied form like propane, in low-pressure
- exchangeable tanks, for heating or for farm and recreation vehicles.
- distribution station. The distribution at "gas stations", like e.g. propane, can be proposed without building
- costly electrolyzing stations, supplying liquefied hydrogen or using highly pressurized hydrogen. Investigations
- have been started in Florida and California, they may lead to factual demonstrations by auto companies (e.g.
- SMART). At AESInc., preparations for a production of different types of ammonia crackers have been started.
- System studies, modelling of cell stack configurations and designs of Balance of Plant (BOP) accessories are
- made. The goal is a high speed mass production at a reasonable cost, getting down to a few \$ 100 per kW, for
- electric vehicles even lower. To use low-cost ammonia crackers with PEM-FC's, an additional NH3 trace
- cleaner is required. However, the high temperature SOFC Systems need no cracker, they can operate on NH3
- directly. Cracker systems can be completely electrically heated for simplicity reasons. However, for fuel cell
- system-cracker combinations it is desired to use the exhaust from the fuel cell to participate in heating the
- cracker. For such a more efficient combination a hydrogen enrichment step is required.

#### Ammonia - A high energy density, inexpensive fuel

- Ammonia tends to follow natural gas prices (which are approaching record levels now). Ammonia is a zero
- carbon fuel that can generate hydrogen in a simple, cheap reactor. Ammonia is 17.5% by weight hydrogen.
- It has a higher hydrogen density (~6.56 lb/ft3) than liquid hydrogen (~4 lb/ft3). Domestic production is about 20
- million tons per year. Presently in the USA, the cost of ammonia is higher than natural gas, but considering
- different shipping ports and larger quantities it can become competitive, considering its use in fuel cell cracker
- systems offering a higher energy conversion efficiency than combustion engines.
- About 140 MM Tons are produced annually, and farmers, both in the US and in third world countries, routinely apply it directly to the
- soil as a fertilizer. Its range of flammability is so narrow that it is classified as non-flammable by the DOT.
- It was used as a fuel in the X15 rocket plane. Ammonia is also catalytically decomposed to produce a reducing
- gas for treating metals and it is the most widely used industrial refrigerant..

#### Internal combustion engines

- can operate on cracked ammonia with no reduction in power, ideal for telecommunications, emergency and
- remote site applications. Several AES fuel cell stacks have operated on ammonia cracker effluent. Ammonia is
- a severe poison to PEM cells and great care must be taken to eliminate all traces of ammonia from the cracker
- effluent. A fuel cell system operating at 80 % hydrogen utilization could supply the effluent low hydrogen nitrogen
- mix to the burner of the ammonia cracker, preferably using a low-cost membrane type diffusion based
- H2-enrichment step (a low-cost simple method is under development at the TU-Graz).

#### Ammonia as competitive Hydrogen Carrier and Fuel Source

- Ammonia has been identified as a suitable hydrogen carrier. Ammonia is essentially non flammable and is
- readily obtained and handled in liquid form. It contains 1.7 times more hydrogen than liquid hydrogen for a
- given volume. Ammonia therefore offers significant advantages in cost and convenience as a vehicular fuel.
- Procedures for safe handling have been developed in every country. Facilities for storage and transport by
- barges, trucks and pipelines from producer to ultimate consumer are available throughout the world. Therefore
- liquid anhydrous ammonia is an excellent storage medium for hydrogen. Compared with methanol/water mixes,
- the fuel capacity per weight of ammonia is higher and the price per kW/hr is far lower.

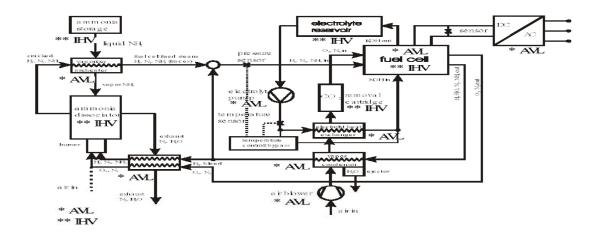
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Figure 1. Combination of an AFC-System and an Ammonia Cracker

HV: Cracker Design by High Voltage Institute, TU - Graz,

AVL: System Simulation by AVL-List GmbH, Graz, Austria





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