

# Beneficial Biogas – Lakewood's Design-Build Digester Upgrades



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# Presenters

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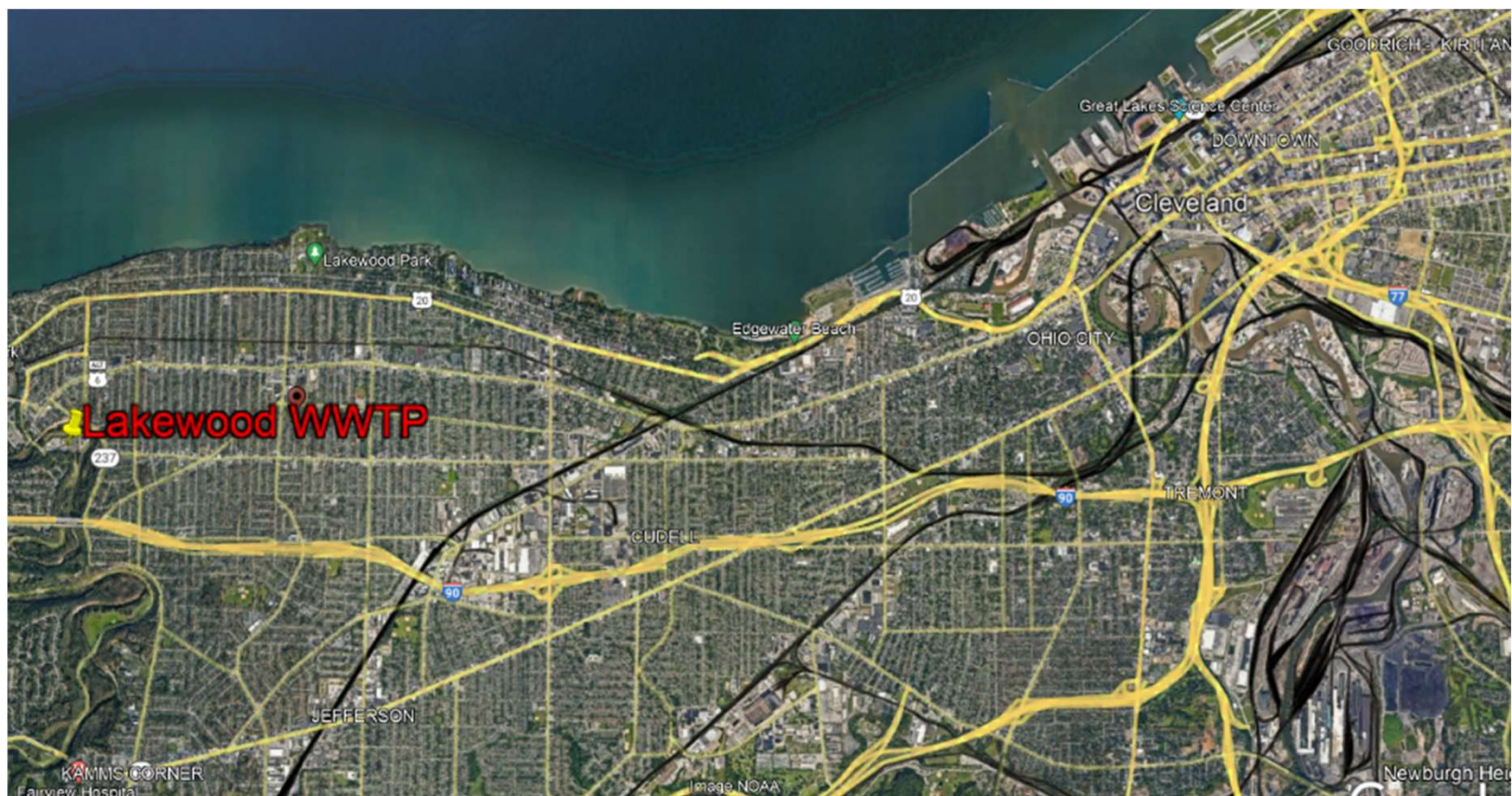


# Agenda

- Introduction
- Lakewood WWTP Background
- Project Background
- Design Build Approach and Solutions
- Construction of the Improvements
- Operational Information
- General Discussion / Q&A



# Lakewood WWTP Background



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# Lakewood WWTP Background

- Current Plant built in 1965
- Activated Sludge Treatment
- WWTP and CEHRT sit on 11 AC along the Rocky River
- Effluent discharge to Lake Erie
- Treats 18 MGD (Avg)
- Capacity – 30 MGD wet weather
- Capacity – 40 MGD max hydraulic

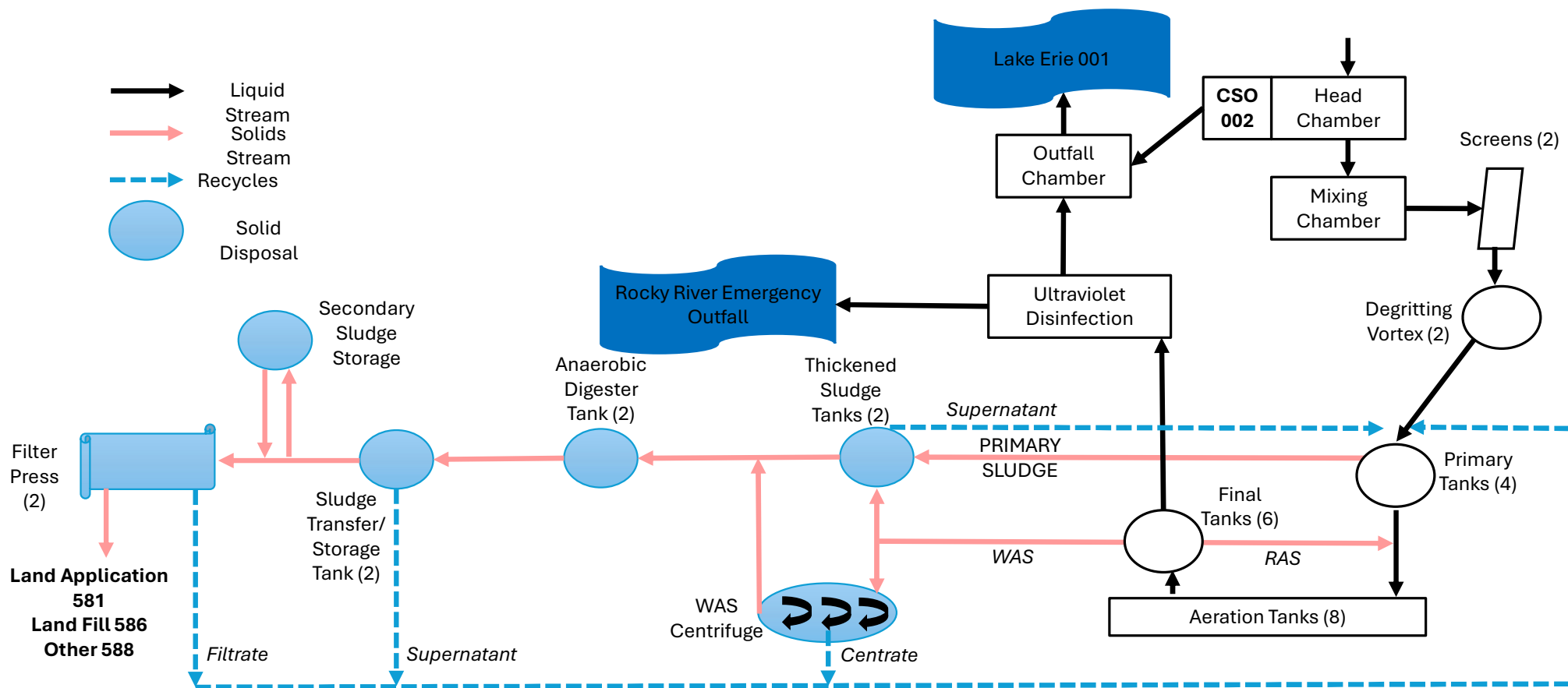


# Lakewood WWTP Treatment Processes

- Screening, De-Gritting, and CEHRT
- Primary Settling
- Gravity Sludge Thickening
- Biological Treatment (Aeration)
- Coagulation Addition for Phosphorus Removal
- Final Settling
- Disinfection (UV, May 1 to Nov 1)
- Anaerobic Digestion & Biosolids Disposal

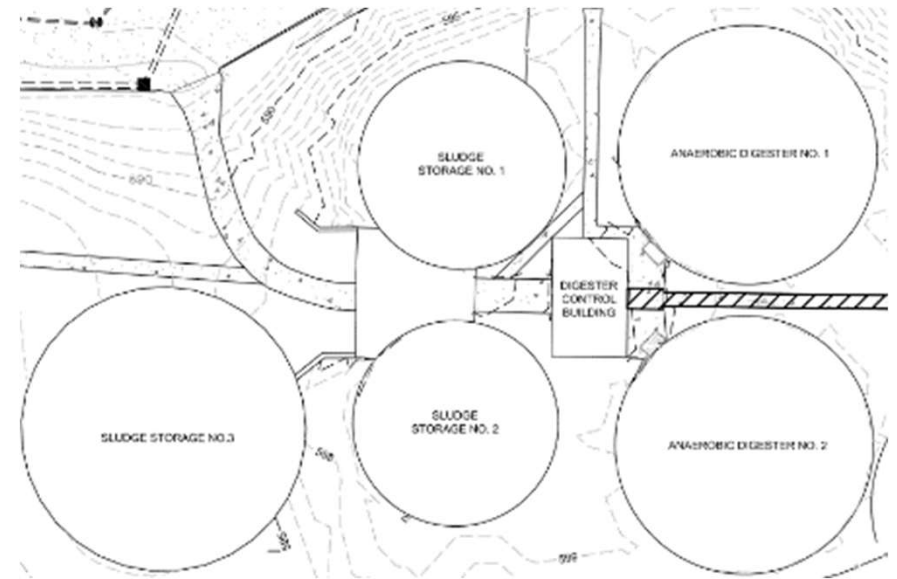


# Lakewood WWTP Process Flow Diagram



# Anaerobic Digester Process Prior to Improvements

- Two (2) 75' Dia. x 22.5' SWD Anaerobic Digesters
- Primary, WAS and Skimmings
- Two (2) 60' Dia. x 22.5 SWD Sludge Storage Tanks
- One (1) 77' Dia. x 21.5 SWD Sludge Storage Tank
- Two (2) Belt Filter Press
- Land Apply Biosolids in Summer Months
- Landfill as Backup
- Sludge Storage to Maximize Land Application





# Digester Improvement Needs Background

1. Safety Improvements
  - NFPA 820 Compliance
  - Flare on Roof of Building
2. General Improvements
  - Old Equipment, Tanks and Covers
3. Maximize Utilization of Methane
  - Storage and Beneficial Use of Gas
4. Two-Phase – Thermophilic-Mesophilic Anaerobic Digestion
  - Class A Sludge



# Lakewood WWTP Digester Improvements

- Primary Digester Cleaning
- Inadequate Digester Mixing (Top Mixers)
- Electrical Equipment Code Compliance
- Primary Digester Concrete and Roof Unknown Condition
- Original Flare and Flame Arrestor Code Compliance
- Boilers and Heat Exchanger Replacement (>35 years old)
- Methane Gas Storage/Utilization
- Allen Bradley PLC5 Controls Upgrade



# NFPA and Electrical Upgrades

- Methane Piping in Building
- Electrical Code Compliance
- Adjacent to Electrical
- Corrosion in Piping
- Limited Access



# Flare Replacement

- New Flare away from Structures
- Code Compliant Equipment
- Located on Digester Building Roof





# Project Phasing

1. Design Phase -  
Preconstruction
  - Digester Cleaning
  - Alternative Evaluation
  - Design / Pricing
2. Build - Construction



# Digester Cleaning

## 1. Clean Digester

- Temp Press
- Sludge Hauled Away
- Tank Cleaned

## 2. Assess Conditions

- Cover Evaluated
- Concrete (walls / slab) Reviewed

## 3. Determine Life Expectancy / Scope



# Alternatives Evaluation

- Number of Primary Digesters Required
- Digester Cover Types
- CHP Engine Generator vs. Microturbines
- Sludge Mixing Systems
- Heat Exchangers
- Recirculation Pumps
- Gas Conditioning
- Future Capacity
- Gas Utilization



# Design Build Approach to Improvements

Why go Design-Build? ***COLLABORATION IS THE KEY!!!***

## 1. **COLLABORATION** on Scope / Design

- Team approach to the project
  - Correctly sizing the equipment
  - Equipment selection

## 2. **COLLABORATION** on Pricing

- Historical Cost Application
- Up to date budgeting and vendor input with design progress





# Design Build Approach to Improvements

- ***Original Approach***

- Class A Sludge Process was the original intent

- ***Collaborated Approach***

- Future Proofing / Foundation
- DB Team pitched correcting some of the safety issues in order to future proof the plan
- The Team addressed the NFPA safety issues and took all the gas equipment outside or in a new dedicated facility



# Design Build Solutions to Improvements

## Digester Mixing System – Gas Production Improvement





# Design Build Solutions to Improvements

## Gas Holder Digester Cover – Gas Storage Improvement





# Design Build Solutions to Improvements

NFPA Improvements Solution – Exterior Gas Lines and Equipment



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# Design Build Solutions to Improvements

NFPA Improvements Solution – New Energy Recovery Building (ERB)



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# Design Build Solutions to Improvements

## Biogas Equipment – Gas Conditioning





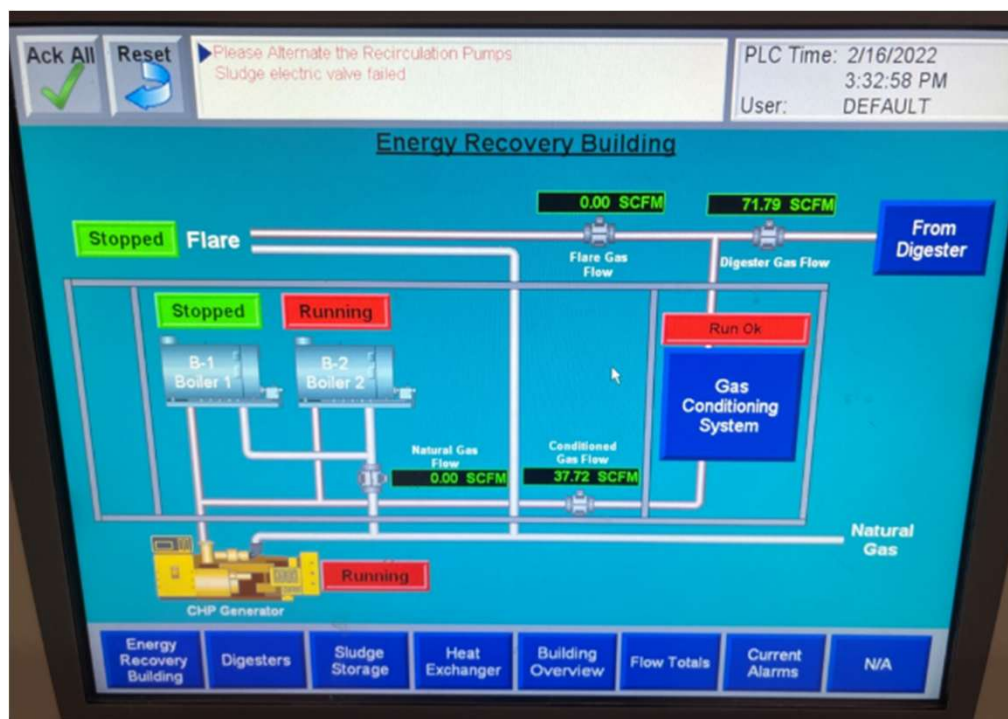
# Design Build Solutions to Improvements

## Biogas Equipment – Gas Utilization



# Design Build Solutions to Improvements

## System Controls and Gas Monitoring



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# Digester Operational Information

- Initial Startup Phase for all Equipment
- Utilizing Boilers and CHP
- Running on One Anaerobic Digester



# Digester Methane Production/Usage – 2024 Data

|                | Gas Production | Boiler Usage | Flare Usage | CHP Usage | Boiler NG Use |
|----------------|----------------|--------------|-------------|-----------|---------------|
| <b>Average</b> | 710            | 317          | 92          | 301       | 4             |
| <b>Total</b>   | 260,030        | 116,141      | 33,580      | 110,309   | 1,384         |
| <b>Minimum</b> | 437            | 74           | 2           | 14        | -             |
| <b>Maximum</b> | 1,179          | 641          | 561         | 827       | 114           |

Values in 100 ft<sup>3</sup>/day



# Digester Methane Production Comparison

|         | May 2016 | July 2016 | Oct 2016 | Dec 2017 | Jan 2017 | 2024 Avg. |
|---------|----------|-----------|----------|----------|----------|-----------|
| Average | 597      | 587       | 493      | 486      | 448      | 710       |
| Maximum | 709      | 816       | 583      | 595      | 508      | 1,179     |

Values in 100 ft<sup>3</sup>/day

2016-17 Average: 522

2024 Average: 710

**36% INCREASE IN METHANE**





# Digester Operational Summary Information

- Old system (two digester) gas production – 522 cCF / day
- New system (one digester) gas production – 710 cCF / day
- Increased Methane Production – Approx. 36%
- Methane Utilized in CHP
- Produces Approx. 30% of Plant Electricity
- 13,852 Run Hours
- Total KW/H: 1,162,109



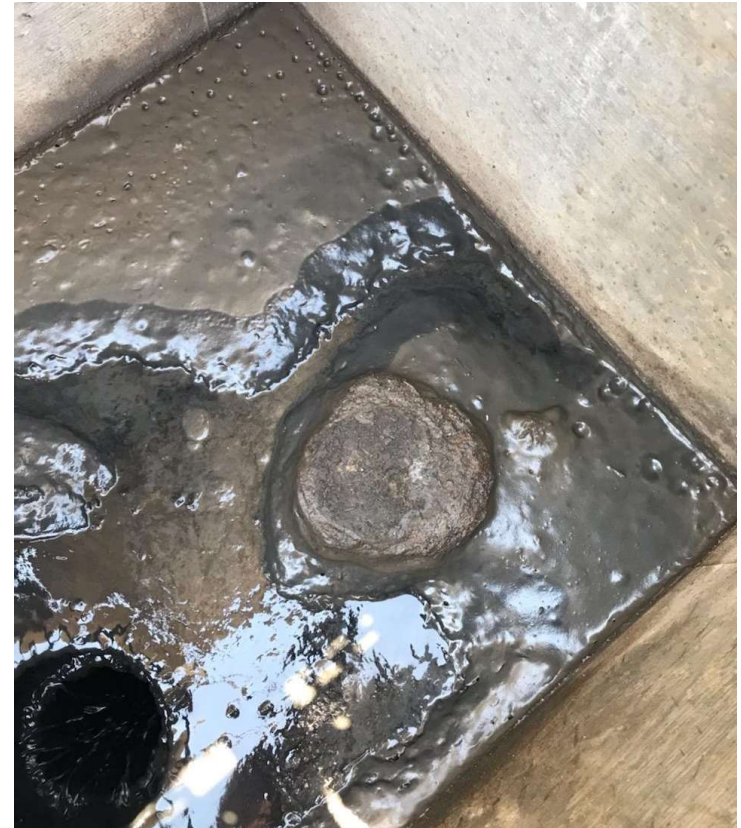
# CHP Maintenance

- Oil Changed – Approx. 8 times
- Spark plugs changed – around 8 times
- Engine heads replaced – once (at 10,000 hours)
- CHP runs between 80% - 90% of power
- Main water recirculating pump replaced – 1 time
- Radiator cooling fan motor replaced – 1 time
- Iron sponge and Siloxane media replaced – 1 time
- Methane gas H<sub>2</sub>S concentration must be below 100 mg/L



# Project Challenges

- High Hydrogen Sulfide Content in Gas
- Foaming During Digester Startup
- Dialing in Methane Gas Parameters
- More Gas to Optimize Boiler and CHP Run Times
- Gas Metering





# General Discussion / Questions?

THANK YOU!!



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# Digester Cover and Mixing Pump



# New Sludge Heat Exchangers and Recirc. Pumps





# New Energy Recovery Building



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# New Flare and Boilers



# New Combined Heat & Power Unit

