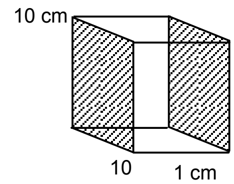
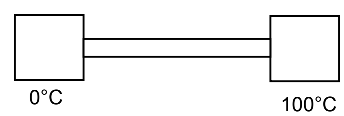
CHAPTER 28
HEAT TRANSFER



1. $t_1 = 90°C$, $t_2 = 10°C$
   $l = 1 \text{ cm} = 1 \times 10^{-3}$ m
   $A = 10 \text{ cm} \times 10 \text{ cm} = 0.1 \times 0.1 \text{ m}^2 = 1 \times 10^{-2} \text{ m}^2$
   K = 0.80 w/m-°C
   $$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{l} = \frac{8 \times 10^{-1} \times 1 \times 10^{-2} \times 80}{1 \times 10^{-2}} = 64 \text{ J/s} = 64 \times 60\ 3840 \text{ J.}$$
2. t = 1 cm = 0.01 m, $A = 0.8 \text{ m}^2$
   $\theta_1 = 300$, $\theta_2 = 80$
   K = 0.025,
   $$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{l} = \frac{0.025 \times 0.8 \times (30030)}{0.01} = 440 \text{ watt.}$$
3. K = 0.04 J/m-5°C, $A = 1.6 \text{ m}^2$
   $t_1 = 97°F = 36.1°C$ $t_2 = 47°F = 8.33°C$
   l = 0.5 cm = 0.005 m
   $$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{l} = \frac{4 \times 10^{-2} \times 1.6 \times 27.78}{5 \times 10^{-3}} = 356 \text{ J/s}$$
4. $A = 25 \text{ cm}^2 = 25 \times 10^{-4} \text{ m}^2$
   $l = 1 \text{ mm} = 10^{-3}$ m
   K = 50 w/m-°C
   $\frac{Q}{t}$ = Rate of conversion of water into steam
   $$= \frac{100 \times 10^{-3} \times 2.26 \times 10^6}{1 \text{ min}} = \frac{10^{-1} \times 2.26 \times 10^6}{60} = 0.376 \times 10^4$$
   $$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{l} \Rightarrow 0.376 \times 10^4 = \frac{50 \times 25 \times 10^{-4} \times (\theta - 100)}{10^{-3}}$$
   $$\Rightarrow \theta = \frac{10^{-3} \times 0.376 \times 10^4}{50 \times 25 \times 10^{-4}} = \frac{10^5 \times 0.376}{50 \times 25} = 30.1 \approx 30$$
5. K = 46 w/m-s°C
   l = 1 m
   $A = 0.04 \text{ cm}^2 = 4 \times 10^{-6} \text{ m}^2$
   $L_{\text{fussion ice}} = 3.36 \times 10^5$ j/Kg



   $$\frac{Q}{t} = \frac{46 \times 4 \times 10^{-6} \times 100}{1} = 5.4 \times 10^{-8} \text{ kg} \approx 5.4 \times 10^{-5} \text{ g.}$$
6. $A = 2400 \text{ cm}^2 = 2400 \times 10^{-4} \text{ m}^2$
   $\ell = 2 \text{ mm} = 2 \times 10^{-3}$ m
   K = 0.06 w/m-°C
   $\theta_1 = 20°C$
   $\theta_2 = 0°C$
   $$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{\ell} = \frac{0.06 \times 2400 \times 10^{-4} \times 20}{2 \times 10^{-3}} = 24 \times 6 \times 10^{-1} \times 10 = 24 \times 6 = 144 \text{ J/sec}$$
   Rate in which ice melts = $\frac{m}{t} = \frac{Q}{t \times L} = \frac{144}{3.4 \times 10^5}$ Kg/h = $\frac{144 \times 3600}{3.4 \times 10^5}$ Kg/s = 1.52 kg/s.
7. $\ell = 1 \text{ mm} = 10^{-3}$ m m = 10 kg
   $A = 200 \text{ cm}^2 = 2 \times 10^{-2} \text{ m}^2$
   $L_{vap} = 2.27 \times 10^6$ J/kg
   K = 0.80 J/m-s-°C

$dQ = 2.27 \times 10^6 \times 10$,

$$\frac{dQ}{dt} = \frac{2.27 \times 10^7}{10^5} = 2.27 \times 10^2 \text{ J/s}$$

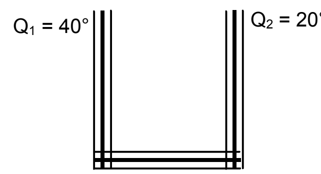
Again we know

$$\frac{dQ}{dt} = \frac{0.80 \times 2 \times 10^{-2} \times (42 - T)}{1 \times 10^{-3}}$$

So, $\dfrac{8 \times 2 \times 10^{-3}(42 - T)}{10^{-3}} = 2.27 \times 10^2$

$\Rightarrow 16 \times 42 - 16T = 227 \Rightarrow T = 27.8 \approx 28°C$

8. K = 45 w/m-°C
$\ell = 60 \text{ cm} = 60 \times 10^{-2}$ m
$A = 0.2 \text{ cm}^2 = 0.2 \times 10^{-4} \text{ m}^2$
Rate of heat flow,



$$= \frac{KA(\theta_1 - \theta_2)}{\ell} = \frac{45 \times 0.2 \times 10^{-4} \times 20}{60 \times 10^{-2}} = 30 \times 10^{-3}\ 0.03 \text{ w}$$

9. $A = 10 \text{ cm}^2$, h = 10 cm

$$\frac{\Delta Q}{\Delta t} = \frac{KA(\theta_1 - \theta_2)}{\ell} = \frac{200 \times 10^{-3} \times 30}{1 \times 10^{-3}} = 6000$$

Since heat goes out from both surfaces. Hence net heat coming out.

$= \dfrac{\Delta Q}{\Delta t} = 6000 \times 2 = 12000$, $\dfrac{\Delta Q}{\Delta t} = MS\dfrac{\Delta \theta}{\Delta t}$

$\Rightarrow 6000 \times 2 = 10^{-3} \times 10^{-1} \times 1000 \times 4200 \times \dfrac{\Delta \theta}{\Delta t}$

$\Rightarrow \dfrac{\Delta \theta}{\Delta t} = \dfrac{72000}{420} = 28.57$

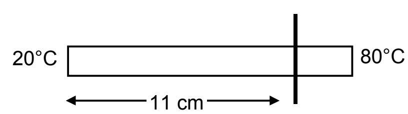
So, in 1 Sec. 28.57°C is dropped

Hence for drop of 1°C $\dfrac{1}{28.57}$ sec. = 0.035 sec. is required

10. $\ell = 20 \text{ cm} = 20 \times 10^{-2}$ m
$A = 0.2 \text{ cm}^2 = 0.2 \times 10^{-4} \text{ m}^2$
$\theta_1 = 80°C$, $\theta_2 = 20°C$, K = 385

(a) $\dfrac{Q}{t} = \dfrac{KA(\theta_1 - \theta_2)}{\ell} = \dfrac{385 \times 0.2 \times 10^{-4}(80 - 20)}{20 \times 10^{-2}} = 385 \times 6 \times 10^{-4} \times 10 = 2310 \times 10^{-3} = 2.31$

(b) Let the temp of the 11 cm point be θ



$$\frac{\Delta \theta}{\Delta l} = \frac{Q}{tKA}$$

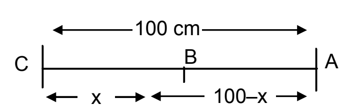
$$\Rightarrow \frac{\Delta \theta}{\Delta l} = \frac{2.31}{385 \times 0.2 \times 10^{-4}}$$

$$\Rightarrow \frac{\theta - 20}{11 \times 10^{-2}} = \frac{2.31}{385 \times 0.2 \times 10^{-4}}$$

$$\Rightarrow \theta - 20 = \frac{2.31 \times 10^4}{385 \times 0.2} \times 11 \times 10^{-2} = 33$$

$\Rightarrow \theta = 33 + 20 = 53$

11. Let the point to be touched be ‘B’
No heat will flow when, the temp at that point is also 25°C
i.e. $Q_{AB} = Q_{BC}$



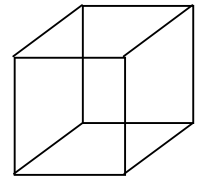
So, $\dfrac{KA(100 - 25)}{100 - x} = \dfrac{KA(25 - 0)}{x}$

$\Rightarrow 75x = 2500 - 25x \Rightarrow 100x = 2500 \Rightarrow x = 25$ cm from the end with 0°C

12. $V = 216\ cm^3$

$a = 6$ cm, Surface area $= 6\ a^2 = 6 \times 36\ m^2$

$t = 0.1$ cm $\frac{Q}{t} = 100$ W,



$$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{\ell}$$

$$\Rightarrow 100 = \frac{K \times 6 \times 36 \times 10^{-4} \times 5}{0.1 \times 10^{-2}}$$

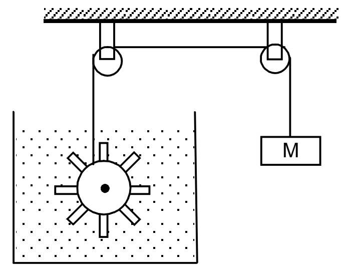
$$\Rightarrow K = \frac{100}{6 \times 36 \times 5 \times 10^{-1}} = 0.9259\ W/m°C \approx 0.92\ W/m°C$$

13. Given $\theta_1 = 1°C$, $\theta_2 = 0°C$

$K = 0.50$ w/m-°C, $d = 2\ mm = 2 \times 10^{-3}$ m

$A = 5 \times 10^{-2}\ m^2$, $v = 10$ cm/s $= 0.1$ m/s

Power = Force × Velocity = Mg × v



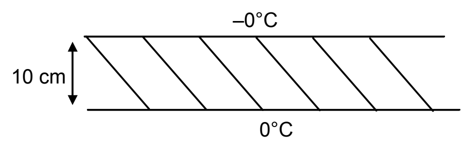
Again Power $= \frac{dQ}{dt} = \frac{KA(\theta_1 - \theta_2)}{d}$

So, Mgv $= \frac{KA(\theta_1 - \theta_2)}{d}$

$$\Rightarrow M = \frac{KA(\theta_1 - \theta_2)}{dvg} = \frac{5 \times 10^{-1} \times 5 \times^{-2} \times 1}{2 \times 10^{-3} \times 10^{-1} \times 10} = 12.5\ kg.$$

14. $K = 1.7$ W/m-°C $f_w = 1000\ Kg/m^3$

$L_{ice} = 3.36 \times 10^5$ J/kg $T = 10\ cm = 10 \times 10^{-2}$ m

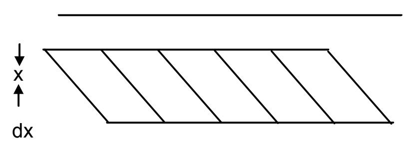


(a) $\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{\ell} \Rightarrow \frac{\ell}{t} = \frac{KA(\theta_1 - \theta_2)}{Q} = \frac{KA(\theta_1 - \theta_2)}{mL}$

$$= \frac{KA(\theta_1 - \theta_2)}{At f_w L} = \frac{1.7 \times [0 - (-10)]}{10 \times 10^{-2} \times 1000 \times 3.36 \times 10^5}$$

$$= \frac{17}{3.36} \times 10^{-7} = 5.059 \times 10^{-7} \approx 5 \times 10^{-7}\ m/sec$$

(b) let us assume that x length of ice has become formed to form a small strip of ice of length dx, dt time is required.



$$\frac{dQ}{dt} = \frac{KA(\Delta\theta)}{x} \Rightarrow \frac{dmL}{dt} = \frac{KA(\Delta\theta)}{x} \Rightarrow \frac{Adx f\omega L}{dt} = \frac{KA(\Delta\theta)}{x}$$

$$\Rightarrow \frac{dx f\omega L}{dt} = \frac{K(\Delta\theta)}{x} \Rightarrow dt = \frac{xdx f\omega L}{K(\Delta\theta)}$$

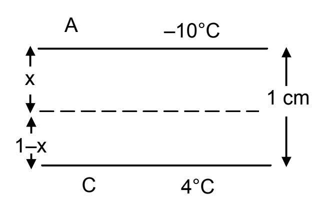
$$\Rightarrow \int_0^t dt = \frac{f\omega L}{K(\Delta\theta)}\int_0^t xdx \qquad \Rightarrow t = \frac{f\omega L}{K(\Delta\theta)}\left[\frac{x^2}{2}\right]_o^l = \frac{f\omega L}{K\Delta\theta}\frac{l^2}{2}$$

Putting values

$$\Rightarrow t = \frac{1000 \times 3.36 \times 10^5 \times (10 \times 10^{-2})^2}{1.7 \times 10 \times 2} = \frac{3.36}{2 \times 17} \times 10^6\ \text{sec.} = \frac{3.36 \times 10^6}{2 \times 17 \times 3600}\ \text{hrs} = 27.45\ \text{hrs} \approx 27.5\ \text{hrs.}$$

15. let 'B' be the maximum level upto which ice is formed. Hence the heat conducted at that point from both the levels is the same.

Let AB = x

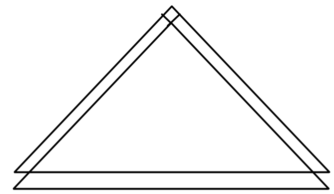


i.e. $\frac{Q}{t}\text{ice} = \frac{Q}{t}\text{water} \qquad \Rightarrow \frac{K_{ice} \times A \times 10}{x} = \frac{K_{water} \times A \times 4}{(1-x)}$

$$\Rightarrow \frac{1.7 \times 10}{x} = \frac{5 \times 10^{-1} \times 4}{1 - x} \Rightarrow \frac{17}{x} = \frac{2}{1 - x}$$

$$\Rightarrow 17 - 17x = 2x \Rightarrow 19x = 17 \Rightarrow x = \frac{17}{19} = 0.894 \approx 89\ cm$$

16. K_{AB} = 50 j/m-s-°c θ_A = 40°C
K_{BC} = 200 j/m-s-°c θ_B = 80°C
K_{AC} = 400 j/m-s-°c θ_C = 80°C
Length = 20 cm = 20 × 10^{-2} m
A = 1 cm^2 = 1 × 10^{-4} m^2

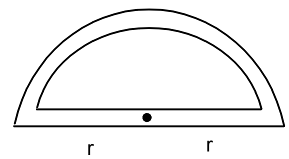


(a) $\frac{Q_{AB}}{t} = \frac{K_{AB} \times A(\theta_B - \theta_A)}{l} = \frac{50 \times 1 \times 10^{-4} \times 40}{20 \times 10^{-2}}$ = 1 W.

(b) $\frac{Q_{AC}}{t} = \frac{K_{AC} \times A(\theta_C - \theta_A)}{l} = \frac{400 \times 1 \times 10^{-4} \times 40}{20 \times 10^{-2}}$ = 800 × 10^{-2} = 8

(c) $\frac{Q_{BC}}{t} = \frac{K_{BC} \times A(\theta_B - \theta_C)}{l} = \frac{200 \times 1 \times 10^{-4} \times 0}{20 \times 10^{-2}}$ = 0

17. We know Q = $\frac{KA(\theta_1 - \theta_2)}{d}$

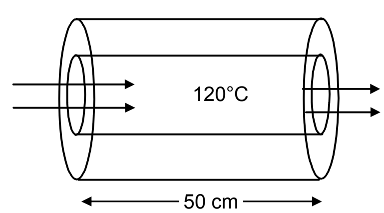


$Q_1 = \frac{KA(\theta_1 - \theta_2)}{d_1}$, $Q_2 = \frac{KA(\theta_1 - \theta_2)}{d_2}$

$\frac{Q_1}{Q_2} = \frac{\frac{KA(\theta_1 - \theta_1)}{\pi r}}{\frac{KA(\theta_1 - \theta_1)}{2r}} = \frac{2r}{\pi r} = \frac{2}{\pi}$ [$d_1 = \pi r$, d_2 = 2r]

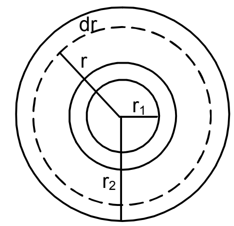
18. The rate of heat flow per sec.
$= \frac{dQ_A}{dt} = KA\frac{d\theta}{dt}$
The rate of heat flow per sec.
$= \frac{dQ_B}{dt} = KA\frac{d\theta_B}{dt}$
This part of heat is absorbed by the red.
$\frac{Q}{t} = \frac{ms\Delta\theta}{dt}$ where $\frac{d\theta}{dt}$ = Rate of net temp. variation
$\Rightarrow \frac{msd\theta}{dt} = KA\frac{d\theta_A}{dt} - KA\frac{d\theta_B}{dt}$ $\Rightarrow ms\frac{d\theta}{dt} = KA\left(\frac{d\theta_A}{dt} - \frac{d\theta_B}{dt}\right)$
$\Rightarrow 0.4 \times \frac{d\theta}{dt}$ = 200 × 1 × 10^{-4} (5 – 2.5) °C/cm
$\Rightarrow 0.4 \times \frac{d\theta}{dt}$ = 200 × 10^{-4} × 2.5
$\Rightarrow \frac{d\theta}{dt} = \frac{200 \times 2.5 \times 10^{-4}}{0.4 \times 10^{-2}}$ °C/m = 1250 × 10^{-2} = 12.5 °C/m

19. Given
K_{rubber} = 0.15 J/m-s-°C $T_2 - T_1$ = 90°C
We know for radial conduction in a Cylinder



$\frac{Q}{t} = \frac{2\pi Kl(T_2 - T_1)}{\ln(R_2/R_1)}$
$= \frac{2 \times 3.14 \times 15 \times 10^{-2} \times 50 \times 10^{-1} \times 90}{\ln(1.2/1)}$ = 232.5 ≈ 233 j/s.

20. $\frac{dQ}{dt}$ = Rate of flow of heat
Let us consider a strip at a distance r from the center of thickness dr.
$\frac{dQ}{dt} = \frac{K \times 2\pi rd \times d\theta}{dr}$ [$d\theta$ = Temperature diff across the thickness dr]



$\Rightarrow C = \dfrac{K \times 2\pi rd \times d\theta}{dr}$ $\left[c = \dfrac{d\theta}{dr}\right]$

$\Rightarrow C\dfrac{dr}{r} = K2\pi d\ d\theta$

Integrating

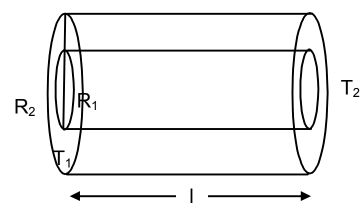
$\Rightarrow C\int_{r_1}^{r_2} \dfrac{dr}{r} = K2\pi d \int_{\theta_1}^{\theta_2} d\theta$ $\Rightarrow C[\log r]_{r_1}^{r_2} = K2\pi d\ (\theta_2 - \theta_1)$

$\Rightarrow C(\log r_2 - \log r_1) = K2\pi d\ (\theta_2 - \theta_1) \Rightarrow C \log\left(\dfrac{r_2}{r_1}\right) = K2\pi d\ (\theta_2 - \theta_1)$

$\Rightarrow C = \dfrac{K2\pi d(\theta_2 - \theta_1)}{\log(r_2 / r_1)}$

21. $T_1 > T_2$

$A = \pi(R_2^2 - R_1^2)$



So, $Q = \dfrac{KA(T_2 - T_1)}{l} = \dfrac{KA(R_2^2 - R_1^2)(T_2 - T_1)}{l}$

Considering a concentric cylindrical shell of radius 'r' and thickness 'dr'. The radial heat flow through the shell

$H = \dfrac{dQ}{dt} = -KA\dfrac{d\theta}{dt}$ [(-)ve because as r – increases θ decreases]

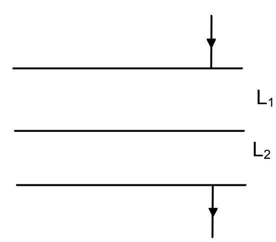
$A = 2\pi rl$ $H = -2\pi rl\ K\ \dfrac{d\theta}{dt}$

or $\int_{R_1}^{R_2} \dfrac{dr}{r} = -\dfrac{2\pi LK}{H}\int_{T_1}^{T_2} d\theta$

Integrating and simplifying we get

$H = \dfrac{dQ}{dt} = \dfrac{2\pi KL(T_2 - T_1)}{Loge(R_2 / R_1)} = \dfrac{2\pi KL(T_2 - T_1)}{\ln(R_2 / R_1)}$

22. Here the thermal conductivities are in series,



$\therefore \dfrac{\dfrac{K_1A(\theta_1 - \theta_2)}{l_1} \times \dfrac{K_2A(\theta_1 - \theta_2)}{l_2}}{\dfrac{K_1A(\theta_1 - \theta_2)}{l_1} + \dfrac{K_2A(\theta_1 - \theta_2)}{l_2}} = \dfrac{KA(\theta_1 - \theta_2)}{l_1 + l_2}$

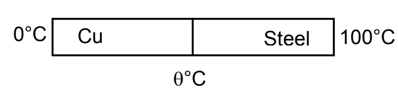
$\Rightarrow \dfrac{\dfrac{K_1}{l_1} \times \dfrac{K_2}{l_2}}{\dfrac{K_1}{l_1} + \dfrac{K_2}{l_2}} = \dfrac{K}{l_1 + l_2}$

$\Rightarrow \dfrac{K_1K_2}{K_1l_2 + K_2l_1} = \dfrac{K}{l_1 + l_2} \Rightarrow K = \dfrac{(K_1K_2)(l_1 + l_2)}{K_1l_2 + K_2l_1}$

23. $K_{Cu} = 390$ w/m-°C $K_{St} = 46$ w/m-°C

Now, Since they are in series connection,

So, the heat passed through the crossections in the same.



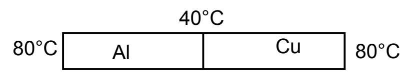
So, $Q_1 = Q_2$

Or $\dfrac{K_{Cu} \times A \times (\theta - 0)}{l} = \dfrac{K_{St} \times A \times (100 - \theta)}{l}$

$\Rightarrow 390(\theta - 0) = 46 \times 100 - 46\ \theta \Rightarrow 436\ \theta = 4600$

$\Rightarrow \theta = \dfrac{4600}{436} = 10.55 \approx 10.6°C$

24. As the Aluminum rod and Copper rod joined are in parallel



$$\frac{Q}{t} = \left(\frac{Q}{t_1}\right)_{Al} + \left(\frac{Q}{t}\right)_{Cu}$$

$$\Rightarrow \frac{KA(\theta_1 - \theta_2)}{l} = \frac{K_1A(\theta_1 - \theta_2)}{l} + \frac{K_2A(\theta_1 - \theta_2)}{l}$$

$\Rightarrow K = K_1 + K_2 = (390 + 200) = 590$

$$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{l} = \frac{590 \times 1 \times 10^{-4} \times (60 - 20)}{1} = 590 \times 10^{-4} \times 40 = 2.36 \text{ Watt}$$

25. $K_{Al} = 200$ w/m-°C $\quad\quad K_{Cu} = 400$ w/m-°C

$A = 0.2 \text{ cm}^2 = 2 \times 10^{-5} \text{ m}^2$

$l = 20 \text{ cm} = 2 \times 10^{-1} \text{ m}$

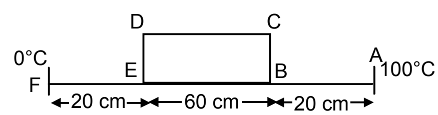
Heat drawn per second

$$= Q_{Al} + Q_{Cu} = \frac{K_{Al} \times A(80 - 40)}{l} + \frac{K_{Cu} \times A(80 - 40)}{l} = \frac{2 \times 10^{-5} \times 40}{2 \times 10^{-1}}[200 + 400] = 2.4 \text{ J}$$

Heat drawn per min = 2.4 × 60 = 144 J

26. $(Q/t)_{AB} = (Q/t)_{BE\ bent} + (Q/t)_{BE}$

$$(Q/t)_{BE\ bent} = \frac{KA(\theta_1 - \theta_2)}{70} \qquad (Q/t)_{BE} = \frac{KA(\theta_1 - \theta_2)}{60}$$



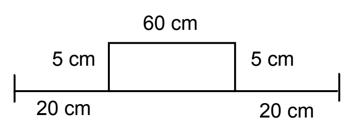
$$\frac{(Q/t)_{BE\ bent}}{(Q/t)_{BE}} = \frac{60}{70} = \frac{6}{7}$$

$(Q/t)_{BE\ bent} + (Q/t)_{BE} = 130$

$\Rightarrow (Q/t)_{BE\ bent} + (Q/t)_{BE}\ 7/6 = 130$

$$\Rightarrow \left(\frac{7}{6} + 1\right)(Q/t)_{BE\ bent} = 130 \qquad \Rightarrow (Q/t)_{BE\ bent} = \frac{130 \times 6}{13} = 60$$

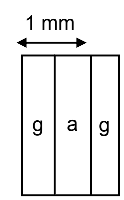
27. $$\frac{Q}{t}\text{bent} = \frac{780 \times A \times 100}{70}$$



$$\frac{Q}{t}\text{str} = \frac{390 \times A \times 100}{60}$$

$$\frac{(Q/t)\text{bent}}{(Q/t)\text{ str}} = \frac{780 \times A \times 100}{70} \times \frac{60}{390 \times A \times 100} = \frac{12}{7}$$

28. (a) $$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{\ell} = \frac{1 \times 2 \times 1(40 - 32)}{2 \times 10^{-3}} = 8000 \text{ J/sec.}$$



(b) Resistance of glass = $\dfrac{\ell}{ak_g} + \dfrac{\ell}{ak_g}$

Resistance of air = $\dfrac{\ell}{ak_a}$

Net resistance = $\dfrac{\ell}{ak_g} + \dfrac{\ell}{ak_g} + \dfrac{\ell}{ak_a}$

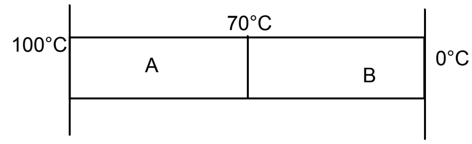
$$= \frac{\ell}{a}\left(\frac{2}{k_g} + \frac{1}{k_a}\right) = \frac{\ell}{a}\left(\frac{2k_a + k_g}{K_g k_a}\right)$$

$$= \frac{1 \times 10^{-3}}{2}\left(\frac{2 \times 0.025 + 1}{0.025}\right)$$

$$= \frac{1 \times 10^{-3} \times 1.05}{0.05}$$

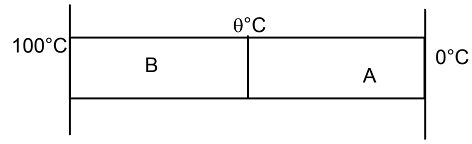
$$\frac{Q}{t} = \frac{\theta_1 - \theta_2}{R} = \frac{8 \times 0.05}{1 \times 10^{-3} \times 1.05} = 380.9 \approx 381 \text{ W}$$

29. Now; Q/t remains same in both cases



In Case I : $\frac{K_A \times A \times (100-70)}{\ell} = \frac{K_B \times A \times (70-0)}{\ell}$

$\Rightarrow 30\ K_A = 70\ K_B$



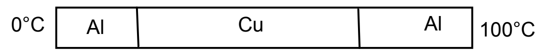
In Case II : $\frac{K_B \times A \times (100-\theta)}{\ell} = \frac{K_A \times A \times (\theta-0)}{\ell}$

$\Rightarrow 100K_B - K_B\ \theta = K_A\ \theta$

$\Rightarrow 100K_B - K_B\ \theta = \frac{70}{30} K_B\ \theta$

$\Rightarrow 100 = \frac{7}{3}\theta + \theta$ $\qquad \Rightarrow \theta = \frac{300}{10} = 30°C$

30. $\theta_1 - \theta_2 = 100$



$\frac{Q}{t} = \frac{\theta_1 - \theta_2}{R}$

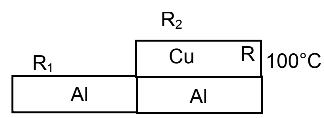
$R = R_1 + R_2 + R_3 = \frac{\ell}{aK_{Al}} + \frac{\ell}{aK_{Cu}} + \frac{\ell}{aK_{Al}} = \frac{\ell}{a}\left(\frac{2}{200} + \frac{1}{400}\right) = \frac{\ell}{a}\left(\frac{4+1}{400}\right) = \frac{\ell}{a}\frac{1}{80}$

$\frac{Q}{t} = \frac{100}{(\ell / a)(1/80)} \Rightarrow 40 = 80 \times 100 \times \frac{a}{\ell}$

$\Rightarrow \frac{a}{\ell} = \frac{1}{200}$

For (b)

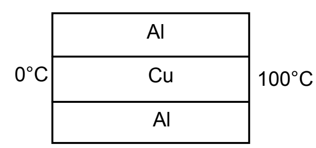
$R = R_1 + R_2 = R_1 + \frac{R_{Cu}R_{Al}}{R_{Cu} + R_{Al}} = R_{Al} + \frac{R_{Cu}R_{Al}}{R_{Cu} + R_{Al}} = \frac{\frac{l}{AK_{Al}} + \frac{l}{AK_{Cu}} + \frac{l}{AK_{Al}}}{\frac{l}{A_{Cu}} + \frac{l}{A_{Al}}}$



$= \frac{l}{AK_{Al}} + \frac{l}{A} + \frac{l}{K_{Al} + K_{Cu}} = \frac{l}{A}\left(\frac{1}{200} + \frac{1}{200+400}\right) = \frac{l}{A} \times \frac{4}{600}$

$\frac{Q}{t} = \frac{\theta_1 - \theta_2}{R} = \frac{100}{(l/A)(4/600)} = \frac{100 \times 600}{4}\frac{A}{l} = \frac{100 \times 600}{4} \times \frac{1}{200} = 75$

For (c)



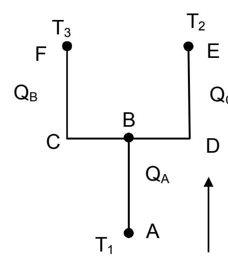
$\frac{1}{R} = \frac{1}{R_1} + \frac{1}{R_2} + \frac{1}{R_3} = \frac{1}{\frac{l}{aK_{Al}}} + \frac{1}{\frac{l}{aK_{Cu}}} + \frac{1}{\frac{l}{aK_{Al}}}$

$= \frac{a}{l}(K_{Al} + K_{Cu} + K_{Al}) = \frac{a}{l}(2 \times 200 + 400) = \frac{a}{l}(800)$

$\Rightarrow R = \frac{l}{a} \times \frac{1}{800}$

$\Rightarrow \frac{Q}{t} = \frac{\theta_1 - \theta_2}{R} = \frac{100 \times 800 \times a}{l}$

$= \frac{100 \times 800}{200} = 400$ W

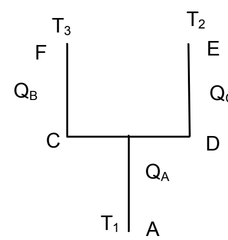


31. Let the temp. at B be T

$\frac{Q_A}{t} = \frac{Q_B}{t} + \frac{Q_C}{t}$ $\qquad \Rightarrow \frac{KA(T_1 - T)}{l} = \frac{KA(T - T_3)}{l + (l/2)} + \frac{KA(T - T_2)}{l + (l/2)}$

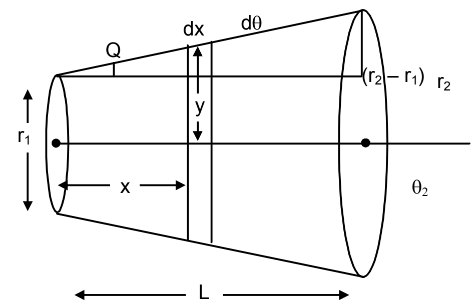
$\Rightarrow \frac{T_1 - T}{l} = \frac{T - T_3}{3l/2} + \frac{T - T_2}{3l/2}$ $\qquad \Rightarrow 3T_1 - 3T = 4T - 2(T_2 + T_3)$

$\Rightarrow -7T = -3T_1 - 2(T_2 + T_3)$ $\qquad \Rightarrow T = \frac{3T_1 + 2(T_2 + T_3)}{7}$



32. The temp at the both ends of bar F is same
Rate of Heat flow to right = Rate of heat flow through left
$\Rightarrow (Q/t)_A + (Q/t)_C = (Q/t)_B + (Q/t)_D$
$\Rightarrow \frac{K_A(T_1 - T)A}{l} + \frac{K_C(T_1 - T)A}{l} = \frac{K_B(T - T_2)A}{l} + \frac{K_D(T - T_2)A}{l}$
$\Rightarrow 2K_0(T_1 - T) = 2 \times 2K_0(T - T_2)$
$\Rightarrow T_1 - T = 2T - 2T_2$
$\Rightarrow T = \frac{T_1 + 2T_2}{3}$

33. Tan $\phi = \frac{r_2 - r_1}{L} = \frac{(y - r_1)}{x}$
$\Rightarrow xr_2 - xr_1 = yL - r_1L$
Differentiating wr to 'x'
$\Rightarrow r_2 - r_1 = \frac{Ldy}{dx} - 0$
$\Rightarrow \frac{dy}{dx} = \frac{r_2 - r_1}{L} \Rightarrow dx = \frac{dyL}{(r_2 - r_1)}$ …(1)



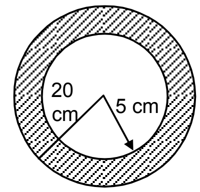
Now $\frac{Q}{T} = \frac{K\pi y^2 d\theta}{dx} \Rightarrow \frac{\theta dx}{T} = k\pi y^2 d\theta$
$\Rightarrow \frac{\theta L dy}{r_2 r_1} = K\pi y^2 d\theta$ from(1)
$\Rightarrow d\theta \ \frac{QLdy}{(r_2 - r_1)K\pi y^2}$
Integrating both side
$\Rightarrow \int_{\theta_1}^{\theta_2} d\theta = \frac{QL}{(r_2 - r_1)k\pi} \int_{r_1}^{r_2} \frac{dy}{y}$
$\Rightarrow (\theta_2 - \theta_1) = \frac{QL}{(r_2 - r_1)K\pi} \times \left[\frac{-1}{y}\right]_{r_1}^{r_2}$
$\Rightarrow (\theta_2 - \theta_1) = \frac{QL}{(r_2 - r_1)K\pi} \times \left[\frac{1}{r_1} - \frac{1}{r_2}\right]$
$\Rightarrow (\theta_2 - \theta_1) = \frac{QL}{(r_2 - r_1)K\pi} \times \left[\frac{r_2 - r_1}{r_1 + r_2}\right]$
$\Rightarrow Q = \frac{K\pi r_1 r_2(\theta_2 - \theta_1)}{L}$

34. $\frac{d\theta}{dt} = \frac{60}{10 \times 60} = 0.1°C/sec$
$\frac{dQ}{dt} = \frac{KA}{d}(\theta_1 - \theta_2)$
$= \frac{KA \times 0.1}{d} + \frac{KA \times 0.2}{d} + ... + \frac{KA \times 60}{d}$
$= \frac{KA}{d}(0.1 + 0.2 + ... + 60) = \frac{KA}{d} \times \frac{600}{2} \times (2 \times 0.1 + 599 \times 0.1)$
[$\therefore$ a + 2a +……….+ na = n/2{2a + (n – 1)a}]
$= \frac{200 \times 1 \times 10^{-4}}{20 \times 10^{-2}} \times 300 \times (0.2 + 59.9) = \frac{200 \times 10^{-2} \times 300 \times 60.1}{20}$
= 3 × 10 × 60.1 = 1803 w ≈ 1800 w

35. $a = r_1 = 5\text{ cm} = 0.05\text{ m}$

$b = r_2 = 20\text{ cm} = 0.2\text{ m}$

$\theta_1 = T_1 = 50°C$ $\qquad\qquad \theta_2 = T_2 = 10°C$



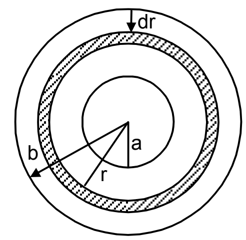
Now, considering a small strip of thickness 'dr' at a distance 'r'.

$A = 4\,\pi r^2$

$H = -4\,\pi r^2 K \dfrac{d\theta}{dr}$ $\quad$ [(–)ve because with increase of r, θ decreases]

$= \int_a^b \dfrac{dr}{r^2} = \dfrac{-4\pi K}{H}\int_{\theta_1}^{\theta_2} d\theta$ $\qquad$ On integration,

$H = \dfrac{dQ}{dt} = K\dfrac{4\pi ab(\theta_1 - \theta_2)}{(b-a)}$



Putting the values we get

$$\frac{K \times 4 \times 3.14 \times 5 \times 20 \times 40 \times 10^{-3}}{15 \times 10^{-2}} = 100$$

$$\Rightarrow K = \frac{15}{4 \times 3.14 \times 4 \times 10^{-1}} = 2.985 \approx 3\text{ w/m-°C}$$

36. $\dfrac{Q}{t} = \dfrac{KA(T_1 - T_2)}{L}$ $\qquad$ Rise in Temp. in $T_2 \Rightarrow \dfrac{KA(T_1 - T_2)}{Lms}$

Fall in Temp in $T_1 = \dfrac{KA(T_1 - T_2)}{Lms}$ $\qquad$ Final Temp. $T_1 \Rightarrow T_1 - \dfrac{KA(T_1 - T_2)}{Lms}$

Final Temp. $T_2 = T_2 + \dfrac{KA(T_1 - T_2)}{Lms}$

Final $\dfrac{\Delta T}{dt} = T_1 - \dfrac{KA(T_1 - T_2)}{Lms} - T_2 - \dfrac{KA(T_1 - T_2)}{Lms}$

$$= (T_1 - T_2) - \frac{2KA(T_1 - T_2)}{Lms} = \frac{dT}{dt} = -\frac{2KA(T_1 - T_2)}{Lms} \Rightarrow \int_{(T_1-T_2)}^{(T_1-T_2)} \frac{dt}{(T_1 - T_2)} = \frac{-2KA}{Lms}dt$$

$$\Rightarrow Ln\frac{(T_1 - T_2)/2}{(T_1 - T_2)} = \frac{-2KAt}{Lms} \qquad \Rightarrow \ln(1/2) = \frac{-2KAt}{Lms} \qquad \Rightarrow \ln_2 = \frac{2KAt}{Lms} \qquad \Rightarrow t = \ln_2\frac{Lms}{2KA}$$

37. $\dfrac{Q}{t} = \dfrac{KA(T_1 - T_2)}{L}$ $\qquad$ Rise in Temp. in $T_2 \Rightarrow \dfrac{KA(T_1 - T_2)}{Lm_1s_1}$

Fall in Temp in $T_1 \Rightarrow \dfrac{KA(T_1 - T_2)}{Lm_2s_2}$ $\qquad$ Final Temp. $T_1 = T_1 - \dfrac{KA(T_1 - T_2)}{Lm_1s_1}$

Final Temp. $T_2 = T_2 + \dfrac{KA(T_1 - T_2)}{Lm_1s_1}$

$$\frac{\Delta T}{dt} = T_1 - \frac{KA(T_1 - T_2)}{Lm_1s_1} - T_2 - \frac{KA(T_1 - T_2)}{Lm_2s_2} = (T_1 - T_2) - \left[\frac{KA(T_1 - T_2)}{Lm_1s_1} + \frac{KA(T_1 - T_2)}{Lm_2s_2}\right]$$

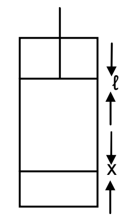
$$\Rightarrow \frac{dT}{dt} = -\frac{KA(T_1 - T_2)}{L}\left(\frac{1}{m_1s_1} + \frac{1}{m_2s_2}\right) \qquad \Rightarrow \frac{dT}{(T_1 - T_2)} = -\frac{KA}{L}\left(\frac{m_2s_2 + m_1s_1}{m_1s_1m_2s_2}\right)dt$$

$$\Rightarrow \ln\Delta t = -\frac{KA}{L}\left(\frac{m_2s_2 + m_1s_1}{m_1s_1m_2s_2}\right)t + C$$

At time $t = 0$, $T = T_0$, $\qquad \Delta T = \Delta T_0$ $\qquad \Rightarrow C = \ln\Delta T_0$

$$\Rightarrow \ln\frac{\Delta T}{\Delta T_0} = -\frac{KA}{L}\left(\frac{m_2s_2 + m_1s_1}{m_1s_1m_2s_2}\right)t \;\Rightarrow\; \frac{\Delta T}{\Delta T_0} = e^{-\frac{KA}{L}\left(\frac{m_1s_1 + m_2s_2}{m_1s_1m_2s_2}\right)t}$$

$$\Rightarrow \Delta T = \Delta T_0\, e^{-\frac{KA}{L}\left(\frac{m_1s_1 + m_2s_2}{m_1s_1m_2s_2}\right)t} = (T_2 - T_1)\, e^{-\frac{KA}{L}\left(\frac{m_1s_1 + m_2s_2}{m_1s_1m_2s_2}\right)t}$$



38. $\frac{Q}{t} = \frac{KA(T_s - T_0)}{x} \Rightarrow \frac{nC_P dT}{dt} = \frac{KA(T_s - T_0)}{x}$

$\Rightarrow \frac{n(5/2)RdT}{dt} = \frac{KA(T_s - T_0)}{x} \Rightarrow \frac{dT}{dt} = \frac{-2LA}{5nRx}(T_S - T_0)$

$\Rightarrow \frac{dT}{(T_S - T_0)} = -\frac{2KAdt}{5nRx} \Rightarrow \ln(T_S - T_0)_{T_0}^{T} = -\frac{2KAdt}{5nRx}$

$\Rightarrow \ln\frac{T_S - T}{T_S - T_0} = -\frac{2KAdt}{5nRx} \Rightarrow T_S - T = (T_S - T_0)e^{-\frac{2KAt}{5nRx}}$

$\Rightarrow T = T_S - (T_S - T_0)e^{-\frac{2KAt}{5nRx}} = T_S + (T_S + T_0)e^{+\frac{2KAt}{5nRx}}$

$\Rightarrow \Delta T = T - T_0 = (T_S - T_0) + (T_S - T_0)e^{+\frac{2KAt}{5nRx}} = (T_S - T_0) + \left(1 + e^{+\frac{2KAt}{5nRx}}\right)$

$\Rightarrow \frac{P_a AL}{nR} = (T_S - T_0) + \left(1 + e^{+\frac{2KAt}{5nRx}}\right)$ [$p_a dv = nRdt$ $P_a Al = nRdt$ $dT = \frac{P_a AL}{nR}$]

$\Rightarrow L = \frac{nR}{P_a A}(T_S - T_0) + \left(1 - e^{-\frac{2KAt}{5nRx}}\right)$

39. $A = 1.6\ m^2$, $T = 37°C = 310\ K$, $\sigma = 6.0 \times 10^{-8}\ w/m^2\text{-}K^4$
Energy radiated per second
$= A\sigma T^4 = 1.6 \times 6 \times 10^{-8} \times (310)^4 = 8865801 \times 10^{-4} = 886.58 \approx 887\ J$

40. $A = 12\ cm^2 = 12 \times 10^{-4}\ m^2$ $T = 20°C = 293\ K$
$e = 0.8$ $\sigma = 6 \times 10^{-8}\ w/m^2\text{-}k^4$

$\frac{Q}{t} = Ae\ \sigma T^4 = 12 \times 10^{-4}\ 0.8 \times 6 \times 10^{-8}\ (293)^4 = 4.245 \times 10^{12} \times 10^{-13} = 0.4245 \approx 0.42$

41. $E \rightarrow$ Energy radiated per unit area per unit time
Rate of heat flow $\rightarrow$ Energy radiated
(a) Per time = E × A

So, $E_{Al} = \frac{e\sigma T^4 \times A}{e\sigma T^4 \times A} = \frac{4\pi r^2}{4\pi(2r)^2} = \frac{1}{4}$ $\therefore 1 : 4$

(b) Emissivity of both are same

$= \frac{m_1 S_1 dT_1}{m_2 S_2 dT_2} = 1$

$\Rightarrow \frac{dT_1}{dT_2} = \frac{m_2 S_2}{m_1 S_1} = \frac{s_1 4\pi r_1^3 \times S_2}{s_2 4\pi r_2^3 \times S_1} = \frac{1 \times \pi \times 900}{3.4 \times 8\pi \times 390} = 1 : 2 : 9$

42. $\frac{Q}{t} = Ae\ \sigma T^4$

$\Rightarrow T^4 = \frac{\theta}{teA\sigma} \Rightarrow T^4 = \frac{100}{0.8 \times 2 \times 3.14 \times 4 \times 10^{-5} \times 1 \times 6 \times 10^{-8}}$

$\Rightarrow T = 1697.0 \approx 1700\ K$

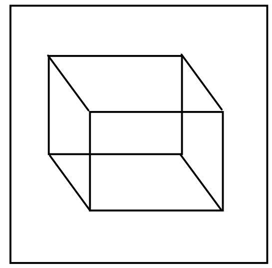
43. (a) $A = 20\ cm^2 = 20 \times 10^{-4}\ m^2$, $T = 57°C = 330\ K$
$E = A\ \sigma T^4 = 20 \times 10^{-4} \times 6 \times 10^{-8} \times (330)^4 \times 10^4 = 1.42\ J$

(b) $\frac{E}{t} = A\sigma e(T_1^4 - T_2^4)$, $A = 20\ cm^2 = 20 \times 10^{-4}\ m^2$

$\sigma = 6 \times 10^{-8}$ $T_1 = 473\ K$, $T_2 = 330\ K$
$= 20 \times 10^{-4} \times 6 \times 10^{-8} \times 1[(473)^4 - (330)^4]$
$= 20 \times 6 \times [5.005 \times 10^{10} - 1.185 \times 10^{10}]$
$= 20 \times 6 \times 3.82 \times 10^{-2} = 4.58\ w$ from the ball.

44. $r = 1\text{ cm} = 1 \times 10^{-3}\text{ m}$
$A = 4\pi(10^{-2})^2 = 4\pi \times 10^{-4}\text{ m}^2$
$E = 0.3,\qquad \sigma = 6 \times 10^{-8}$
$\frac{E}{t} = A\sigma e(T_1^4 - T_2^4)$
$= 0.3 \times 6 \times 10^{-8} \times 4\pi \times 10^{-4} \times [(100)^4 - (300)^4]$
$= 0.3 \times 6 \times 4\pi \times 10^{-12} \times [1 - 0.0081] \times 10^{12}$
$= 0.3 \times 6 \times 4 \times 3.14 \times 9919 \times 10^{-4}$
$= 4 \times 18 \times 3.14 \times 9919 \times 10^{-5} = 22.4 \approx 22\text{ W}$

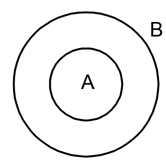
45. Since the Cube can be assumed as black body
$e = \ell$
$\sigma = 6 \times 10^{-8}\text{ w/m}^2\text{-k}^4$
$A = 6 \times 25 \times 10^{-4}\text{ m}^2$
$m = 1\text{ kg}$
$s = 400\text{ J/kg-°K}$
$T_1 = 227°C = 500\text{ K}$
$T_2 = 27°C = 300\text{ K}$



$\Rightarrow ms\frac{d\theta}{dt} = e\sigma A(T_1^4 - T_2^4)$
$\Rightarrow \frac{d\theta}{dt} = \frac{e\sigma A\left(T_1^4 - T_2^4\right)}{ms}$
$= \frac{1 \times 6 \times 10^{-8} \times 6 \times 25 \times 10^{-4} \times [(500)^4 - (300)^4]}{1 \times 400}$
$= \frac{36 \times 25 \times 544}{400} \times 10^{-4} = 1224 \times 10^{-4} = 0.1224°C/s \approx 0.12°C/s.$

46. $Q = e\sigma A(T_2^4 - T_1^4)$
For any body, $210 = eA\sigma[(500)^4 - (300)^4]$
For black body, $700 = 1 \times A\sigma[(500)^4 - (300)^4]$
Dividing $\frac{210}{700} = \frac{e}{1} \Rightarrow e = 0.3$

47. $A_A = 20\text{ cm}^2,\qquad A_B = 80\text{ cm}^2$
$(mS)_A = 42\text{ J/°C},\qquad (mS)_B = 82\text{ J/°C},$
$T_A = 100°C,\qquad T_B = 20°C$
K_B is low thus it is a poor conducter and K_A is high.
Thus A will absorb no heat and conduct all

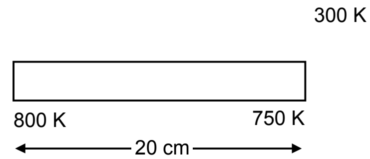


$\left(\frac{E}{t}\right)_A = \sigma A_A [(373)^4 - (293)^4] \qquad \Rightarrow (mS)_A\left(\frac{d\theta}{dt}\right)_A = \sigma A_A [(373)^4 - (293)^4]$
$\Rightarrow \left(\frac{d\theta}{dt}\right)_A = \frac{\sigma A_a\left[(373)^4 - (293)^4\right]}{(mS)_A} = \frac{6 \times 10^{-8}\left[(373)^4 - (293)^4\right]}{42} = 0.03\text{ °C/S}$
Similarly $\left(\frac{d\theta}{dt}\right)_B = 0.043\text{ °C/S}$

48. $\frac{Q}{t} = eAe(T_2^4 - T_1^4)$
$\Rightarrow \frac{Q}{At} = 1 \times 6 \times 10^{-8} [(300)^4 - (290)^4] \qquad = 6 \times 10^{-8} (81 \times 10^8 - 70.7 \times 10^8) = 6 \times 10.3$
$\frac{Q}{t} = \frac{KA(\theta_1 - \theta_2)}{l}$
$\Rightarrow \frac{Q}{tA} = \frac{K(\theta_1 - \theta_2)}{l} = \frac{K \times 17}{0.5} = 6 \times 10.3 = \frac{K \times 17}{0.5} \Rightarrow K = \frac{6 \times 10.3 \times 0.5}{17} = 1.8$

49. $\sigma = 6 \times 10^{-8}$ w/m^2-k^4

L = 20 cm = 0.2 m, K = ?



$\Rightarrow E = \dfrac{KA(\theta_1 - \theta_2)}{d} = A\sigma(T_1^4 - T_2^4)$

$\Rightarrow K = \dfrac{s(T_1 - T_2) \times d}{\theta_1 - \theta_2} = \dfrac{6 \times 10^{-8} \times (750^4 - 300^4) \times 2 \times 10^{-1}}{50}$

$\Rightarrow K = 73.993 \approx 74.$

50. v = 100 cc

$\Delta\theta = 5°C$

t = 5 min

For water

$\dfrac{mS\Delta\theta}{dt} = \dfrac{KA}{l}\Delta\theta$

$\Rightarrow \dfrac{100 \times 10^{-3} \times 1000 \times 4200}{5} = \dfrac{KA}{l}$

For Kerosene

$\dfrac{ms}{at} = \dfrac{KA}{l}$

$\Rightarrow \dfrac{100 \times 10^{-3} \times 800 \times 2100}{t} = \dfrac{KA}{l}$

$\Rightarrow \dfrac{100 \times 10^{-3} \times 800 \times 2100}{t} = \dfrac{100 \times 10^{-3} \times 1000 \times 4200}{5}$

$\Rightarrow T = \dfrac{5 \times 800 \times 2100}{1000 \times 4200} = 2$ min

51. 50°C 45°C 40°C

Let the surrounding temperature be 'T'°C

Avg. t = $\dfrac{50 + 45}{2} = 47.5$

Avg. temp. diff. from surrounding

T = 47.5 – T

Rate of fall of temp = $\dfrac{50 - 45}{5} = 1$ °C/mm

From Newton's Law

1°C/mm = bA × t

$\Rightarrow bA = \dfrac{1}{t} = \dfrac{1}{47.5 - T}$ …(1)

In second case,

Avg, temp = $\dfrac{40 + 45}{2} = 42.5$

Avg. temp. diff. from surrounding

t′ = 42.5 – t

Rate of fall of temp = $\dfrac{45 - 40}{8} = \dfrac{5}{8}$ °C/mm

From Newton's Law

$\dfrac{5}{B} = bAt'$

$\Rightarrow \dfrac{5}{8} = \dfrac{1}{(47.5 - T)} \times (42.5 - T)$

By C & D [Componendo & Dividendo method]

We find, T = 34.1°C

52. Let the water eq. of calorimeter = m

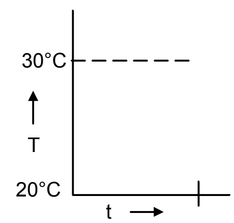
$$\frac{(m + 50 \times 10^{-3}) \times 4200 \times 5}{10} = \text{Rate of heat flow}$$

$$\frac{(m + 100 \times 10^{-3}) \times 4200 \times 5}{18} = \text{Rate of flow}$$

$$\Rightarrow \frac{(m + 50 \times 10^{-3}) \times 4200 \times 5}{10} = \frac{(m + 100 \times 10^{-3}) \times 4200 \times 5}{18}$$

$\Rightarrow (m + 50 \times 10^{-3})18 = 10m + 1000 \times 10^{-3}$
$\Rightarrow 18m + 18 \times 50 \times 10^{-3} = 10m + 1000 \times 10^{-3}$
$\Rightarrow 8m = 100 \times 10^{-3}$ kg
$\Rightarrow m = 12.5 \times 10^{-3}$ kg = 12.5 g

53. In steady state condition as no heat is absorbed, the rate of loss of heat by conduction is equal to that of the supplied.



i.e. H = P
m = 1Kg, Power of Heater = 20 W, Room Temp. = 20°C

(a) $H = \frac{d\theta}{dt} = P = 20$ watt

(b) by Newton's law of cooling

$$\frac{-d\theta}{dt} = K(\theta - \theta_0)$$

$-20 = K(50 - 20) \Rightarrow K = 2/3$

Again, $\frac{-d\theta}{dt} = K(\theta - \theta_0) = \frac{2}{3} \times (30 - 20) = \frac{20}{3}$ w

(c) $\left(\frac{dQ}{dt}\right)_{20} = 0$, $\left(\frac{dQ}{dt}\right)_{30} = \frac{20}{3}$ $\left(\frac{dQ}{dt}\right)_{avg} = \frac{10}{3}$

T = 5 min = 300 ′

Heat liberated = $\frac{10}{3} \times 300 = 1000$ J

Net Heat absorbed = Heat supplied – Heat Radiated = 6000 – 1000 = 5000 J
Now, $m\Delta\theta' = 5000$

$$\Rightarrow S = \frac{5000}{m\Delta\theta} = \frac{5000}{1 \times 10} = 500 \text{ J Kg}^{-1}{}^\circ\text{C}^{-1}$$

54. Given:
Heat capacity = m × s = 80 J/°C

$$\left(\frac{d\theta}{dt}\right)_{increase} = 2 \text{ °C/s}$$

$$\left(\frac{d\theta}{dt}\right)_{decrease} = 0.2 \text{ °C/s}$$

(a) Power of heater = $mS\left(\frac{d\theta}{dt}\right)_{increasing} = 80 \times 2 = 160$ W

(b) Power radiated = $mS\left(\frac{d\theta}{dt}\right)_{decreasing} = 80 \times 0.2 = 16$ W

(c) Now $mS\left(\frac{d\theta}{dt}\right)_{decreasing} = K(T - T_0)$

$\Rightarrow 16 = K(30 - 20)$ $\Rightarrow K = \frac{16}{10} = 1.6$

Now, $\frac{d\theta}{dt} = K(T - T_0) = 1.6 \times (30 - 25) = 1.6 \times 5 = 8$ W

(d) $P.t = H \Rightarrow 8 \times t$

55. $\frac{d\theta}{dt}$ = – K(T – T_0)

Temp. at t = 0 is θ_1

(a) Max. Heat that the body can loose = $\Delta Q_m = ms(\theta_1 - \theta_0)$

($\therefore$ as, $\Delta t = \theta_1 - \theta_0$)

(b) if the body loses 90% of the max heat the decrease in its temp. will be

$$\frac{\Delta Q_m \times 9}{10ms} = \frac{(\theta_1 - \theta_0)\times 9}{10}$$

If it takes time t_1, for this process, the temp. at t_1

$$= \theta_1 - (\theta_1 - \theta_0)\frac{9}{10} = \frac{10\theta_1 - 9\theta_1 - 9\theta_0}{10} = \frac{\theta_1 - 9\theta_0}{10} \times 1$$

Now, $\frac{d\theta}{dt} = -K(\theta - \theta_1)$

Let $\theta = \theta_1$ at t = 0; & θ be temp. at time t

$$\int_{\theta}^{\theta} \frac{d\theta}{\theta - \theta_o} = -K\int_0^t dt$$

or, $\ln\frac{\theta - \theta_0}{\theta_1 - \theta_0} = -Kt$

or, $\theta - \theta_0 = (\theta_1 - \theta_0)\, e^{-kt}$ …(2)

Putting value in the Eq (1) and Eq (2)

$$\frac{\theta_1 - 9\theta_0}{10} - \theta_0 = (\theta_1 - \theta_0)\, e^{-kt}$$

$\Rightarrow t_1 = \frac{\ln 10}{k}$

♣ ♣ ♣ ♣ ♣