

## Gaskell and 152<sup>nd</sup> Well



**Figure 1. Well at Gaskell and 152<sup>nd</sup>**

This well was originally selected to be the 50kW project demonstration site for APH. The SCE Interconnection application (NST-206659) was submitted in November 2021.

SCE performed well tests on the WSWB wells in October and November of 2021. These tests (Table 1) found some results for the Gaskell/152<sup>nd</sup> (G152) well that were worrisome. Historically this well had produced about 1,200 gpm but that production level had dropped to between 919 and 819 gpm. Especially worrisome was the drawdown of between 111 and 125 feet. This meant that the well was pumping water out faster than the water could enter the well casing.

ANTELOPE VLY WATER STORAGE LLC

Pumping Plant Name	WELL G1608U	KINGBIRD 170 WELL	WELL 160 KINGBIRD	WELL AVE A 163	WELL G152	
Test Date	10/7/21	11/8/21	11/8/21	11/8/21	11/9/21	
Pump Tester Name	Frederick J Koch	Frederick J Koch	Frederick J Koch	Frederick J Koch	Frederick J Koch	
Contract ID	8002087301	8002085989	8001939331	8001323688	8002925997	
Meter Number	345M-001174	259000-072396	345M-007094	259000-071242	259000-062195	
Reference Number	2710	2870	2914	25880	25881	
Rate	TP2D49	TP2E49	TP2E49	TP2E49	TP2D49	
Average \$ Cost/kWh	\$0.14476	\$0.18000	\$0.18000	\$0.18000	\$0.18000	
Pump Type	Turbine Well	Turbine Well	Turbine Well	Turbine Well	Turbine Well	
Motor HP	200	200	150	200	250	
Motor Mfg.	US	US	US	GE	US	
Pump Mfg.	JOHNSTON	PEERLESS		L & B	PEERLESS	
Test Points / Frequency						
Discharge Pressure, PSI	46.1 64.3 88.9	123.0	30.8 30.8	15.6	38.1 89.5	
Suction Pressure, PSI						
Drawdown, Ft.	60.4 55.4 43.4	11.0	43.2 42.0	21.0	124.8 111.4	
Pumping Level, Ft.	336.0 331.0 319.0	252.4	299.2 298.0	249.7	420.4 407.0	
Standing Level, Ft.	275.6 275.6 275.6	241.4	256.0 256.0	228.7	295.6 295.6	
Discharge Head Ft.	106.5 148.5 205.4	204.1	71.1 117.3	36.0	88.0 206.7	
Suction Head Ft.	336.0 331.0 319.0	252.4	299.2 298.0	249.7	420.4 407.0	
Total Head Ft.	442.5 479.5 524.4	456.5	370.3 415.3	285.7	508.4 613.7	
Customer GPM	1,216		851		910	
Capacity GPM	1,131 976 762	880	773 725	1,682	919 819	
GPM/Ft. Drawdown, Ft.	18.7 17.6 17.6	80.0	17.9 17.3	80.1	7.4 7.4	
Acre Ft./24 Hour	4.999 4.314 3.368	3.890	3.417 3.205	7.434	4.062 3.620	
kWh Input	159.1 156.0 148.0	151.4	112.2 112.5	182.9	134.3 138.8	
HP Input	213.4 209.2 198.5	203.0	150.5 150.9	245.3	180.1 186.1	
Pump Speed, RPM	1,783	1,785	1,782	1,779	1,790	
Motor Load %	99.7 97.8 92.8	94.9	93.3 93.5	114.7	69.0 71.3	
kWh/Acre Ft.	764 868 1,035	934	788 843	591	794 920	
Overall Plant Eff., %	59.23 56.50 50.84	58.73	48.05 50.40	49.48	65.51 68.20	
Improved Plant Eff., %	70	69	70	69	75	
Improved kWh/Acre Ft.	646	793	541	434	693	
Potential Savings, \$	\$11,856	\$0	\$1	\$1	\$0	

Note: For more detailed information pertaining to pump test results, please refer to Pump Test Results and Cost Analysis Letters

Table 1. SCE Pump Test Results

A well video log was performed to find out what was the issue was. The well casing was perforated with vertical slots approximately 1/8 inch in width and 1 inch in length, spaced about 2-inch intervals to let water into the well itself. Significant tuberculation (iron oxide blisters formed by aerobic bacteria known as biofouling) was observed. Below about 490 feet deep 80 percent of the casing slots were blocked (Figure 2), increasing to 100 percent of the casing slots blocked below 580 ft (the well is about 800 ft deep) as Figure 3 shows. This biofouling was an issue. Not only did it compromise the ability of the well to produce water but, under an APH scenario where we are putting water back down into the well, this would force the biofouling into the aquifer, contaminating the aquifer.



**Figure 2. Biofouling with some open casing perforations at 414 ft deep**



**Figure 3. Completely blocked casing perforations at 540 ft deep.**

Rehabilitation of the well would include mechanically cleaning the casing, acidifying the well with phosphoric acid and swabbing it out, and purging the well to try and remove accumulated sediment. The cost of this rehabilitation would be several hundred thousand dollars with no guarantee of success – the biofouling on the well casing usually indicates that gravel pack and

formation on the outside of the casing is also plugged and simply cleaning the well casing will not solve the problem

The Interconnection application (NST-206659) approved by SCE on March 22, 2022. We notified SCE that we were not going to use this well for the APH demonstration project due to biofouling issue and needed to switch to an adjacent well.

### **Gaskell and 160<sup>th</sup>SE Well**



**Figure 4. Well at Gaskell and 160thSE**

The well just around the corner (Gaskell and 160thSE) from the original fouled well was selected for the replacement demonstration project. It is a slightly smaller well (200 hp versus 250hp) but there was no indication of any issues with this well from the pump tests (Table 1). The interconnection application (NST-290291) was submitted in early July 2022.

Pulling the well (removing all the well pipe in the well hole) and installing the APH valve below the pump impellers (Figure 5) and then reinstalling the pipe down the well hole was scheduled August 30-September 2, 2022. We immediately ran into two problems.



**Figure 5. Pump Bowls and Impellers**

### **Patch**

The well pipe hung up pulling it out of the well hole. While the drilling crew was able to pull the pipe out but we had to find out what the pipe caught on, so a well video log was conducted. At about 353 ft down there was a perforation in the well column that had been patched (basically taking a sheet of metal and pressing it up against the sides of the well column<sup>1</sup>) and the patch had deteriorated, resulting in a very rough internal surface to the well column (Figure 6).

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<sup>1</sup> Perforations in the well column allow sand and small gravel bits into the well when it is being pumped, resulting in significantly increased wear and tear on the pumping equipment and eventual clogging the well.



**Figure 6. Patch and Obtrusions at 353 Ft.**

This was a serious problem. The APH valve at the bottom of the well operates using hydraulic tubing running down the side of the well pipes (Figure 7), and the protrusions at 553 ft would chafe and eventually sever the tubing, rendering the APH valve inoperable.



**Figure 7. APH Valve Hydraulic Hoses on Exterior of Well Pipe**

## **Severe Rust on Pipes**

The second issue we ran into was severe rusting on some of the column pipes. The interior of some of the pipes was as bad or worse than the rusting shown in Figure 8. This was another concern. The pulsing of water in the well (pumping it out and then reinjecting it) would dislodge large areas of scale and rust on the pipes and clog the APH valve and can get trapped in the pump impellers and ruin them. The scaling can increase pipe friction and reduce the efficiency of the energy storage.



**Figure 8. Severe Rusting on Well Pipes**

## **The Solution**

There was enough good pipe available that it was decided to install the APH valve (Figure 9) at a depth of above 350 ft, above where the torn patch was in the well<sup>2</sup>, and include a screen (Figure 10) above the valve to catch any debris that would fall through the pipes before it entered the APH valve. The APH valve was installed at the bottom of the well piping (Figure 11).

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<sup>2</sup> This level was still below the standing water level minus the recorded draw down, so APH should continue to work.



**Figure 9. APH Valve**



**Figure 10. Screen above APH Valve**





**Figure 11. APH Valve Installed at Bottom of Pipe Column**

The well at Gaskell and 160thSE installation with the APH valve was completed on September 6<sup>th</sup> and all the components tested out working correctly.