#### and Selection Criteria for Water and Wastewater Activated Carbon Classifications

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#### Agenda

- Activated carbon basics
- Uses for activated carbon treatment
- Activated carbon manufacturing
- Carbon adsorption kinetics
- General properties for activated carbon products
- Why proper carbon selection is important
- Carbon dosing and usage predictions
- Selecting activated carbon products for performance

- Activated carbon has two basic classifications
- Powdered activated carbon (PAC)
- Granular activated carbon (GAC)
- Generally GAC out performs PAC in all cases, but should it always be preferred?
- Carbon selection is complex and site specific
- PAC generally used or seasonal treatment issues, one time use
- GAC typically used when source contaminants persist year round, run carbon to breakthrough
- Cost effective solutions utilize carbon selection according to treatment performance and NOT according to unit cost



- Activated carbon treatment is an adsorption aqueous solutions process that removes organic contaminants from
- Adsorption involves adherence of the adsorbate to the surface structure of the carbon
- Occurs in the micropores of the carbon material deep

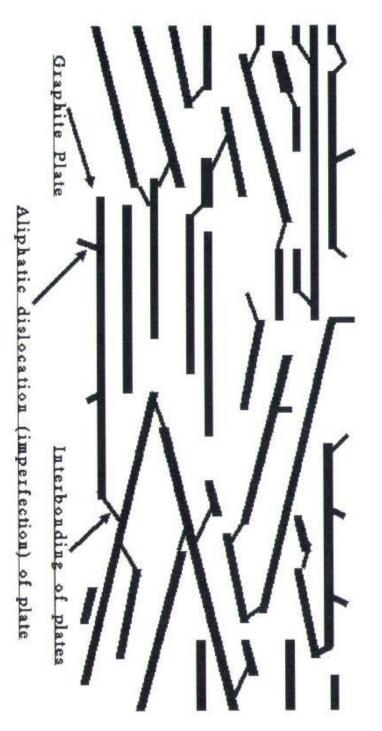
within the carbon particle, not on the particle surface

- Carbon ionic bonding holds contaminants within the
- Organics can be desorbed (pushed off) from carbon
- When more active organic material is introduced into the system
- If inlet concentration decreases significantly
- Organics can be removed from carbon by chemical and thermal means (reactivation processes)

- Activated carbon is a hybrid mixture of a wide variety of graphite platelets interconnected by carbon bonding organized in a random tashion (definition from Calgon Carbon)
- Pathways between the platelets make up the carbon pore structure
- Configuration of the platelets influenced carbon source material
- Generally determines pore structures, internal surface area, and surface chemistry
- Density of the source carbon develops into an extensive platelet structure of the final product
- Dense materials create tighter platelet structures with smaller pores
- Ease of transport needed for contaminants to reach the adsorption sites

#### Molecular Structure of Coal-based Carbon

10,000,000 X magnification
100 Angstroms

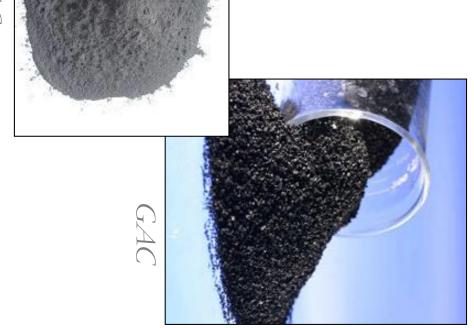


Courtesy of Calgon Carbon Corporation

Unique trimodal pore structure of carbons

>500	>50	Macropores
20 to 500	2 to 50	Mesopores
<20	<2	Micropores
Size in Angströms (Å)	Size in nanometers (nm)	Category
TED CARBONS	TYPICAL PORE SIZES IN ACTIVATE	TYPICAL

- Bituminous-based carbons
- Good development of micropore, mesopore, and macropore mixtures
- Good transport capabilities
- Good adsorptive capacity
- 500 mg/g to 1,100 mg/g IN
- Relatively high surface area
- $600 \text{ m}^2/\text{g}$  to 1,400 m<sup>2</sup>/g



PAC



Lignite coal (brown coal)

### Lignite-based carbons

- Good development of macropores with less development of mesopores and micropores
- Good transport capabilities for smaller molecules (MW 1,650 or less)
- Lower adsorptive capacity
- Up to 600 mg/g IN
- Relatively lower surface area
- Up to  $1,250 \text{ m}^2/\text{g}$

- Wood-based carbons
- Good development of micropore, mesopore, and macropore mixtures
- Good transport capabilities
- Good adsorptive capacity
- 500 mg/g to 1,100 mg/g IN
- Relatively high surface area

   Up to 1,480 m²/g

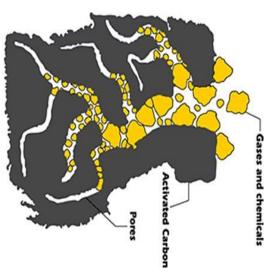




### Coconut-based carbons

- Good development of micropores with less development of mesopores and macropores
- Lower transport capabilities, but good for smaller molecules (MW 700 or less)
- Good adsorptive capacity
- Up to  $1{,}100 \,\mathrm{mg/g~IN}$
- Relatively high surface area
- Up to  $1,480 \text{ m}^2/\text{g}$

- Adsorption occurs in the micropore structures of carbon
- Adsorbates must travel (transport) from the outer surface of the carbon particle to the internal surface area of the carbon
- Macropores and mesopores responsible for transport
- High transport capabilities are needed for molecules to enter the internal spaces



- EMT (external mass transfer) delivers adsorbates to the outer surface of carbon (film diffusion)
- IMT (internal mass transfer) conveys adsorbates to micropore adsorption sites (carbon bonding)
- EMT and IMT are driven by the concentration gradient of the solution
- Adsorption typically involves chemical bonding to the carbon
- Poor transport develops into carbon fouling (blocking of pore

- Very general demonstration of available pore size
- Micropores should be 1.3 to 1.8 times larger than the molecular size of the adsorbates to be removed
- Mesopores should be about 5 times larger than the molecular size of the adsorbates to be removed
- Think of adsorbates as spheres rather than elongated shapes

$$\begin{array}{c} CH_3 \\ H \\ CCH_3 \\ CCH_3 \\ CCH_3 \\ CCH_4 \\ CCH_5 \\ CCH_6 \\ CCH_7 \\ CCH_$$

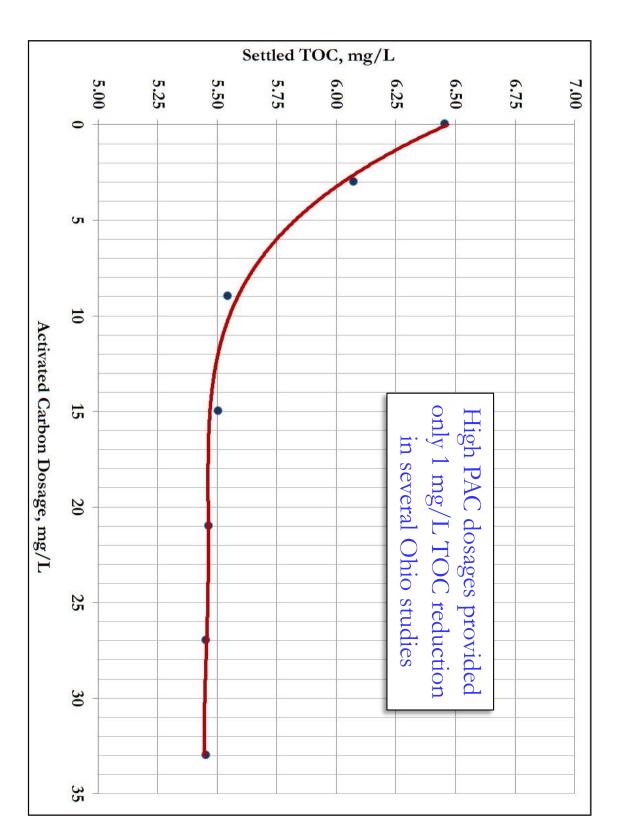
- General sizing of adsorbates according to molecular weight
- Spherical shape has a volume
- Volume has associated diameter and radius
- The diameter of the sphere must fit between the pores to reach adsorption sites

$$V = \frac{(0.73 \frac{cm^3}{g})(\frac{10^{21}nm^3}{cm^3})}{6.023 * 10^{23}MW/g} * MW = 1.212 * \frac{10^{-3}nm^3}{MW} * MW$$

$$R_{min} = \left(\frac{3V}{4\pi}\right)^{1/3} * MW = 0.066 * MW^{1/3}$$

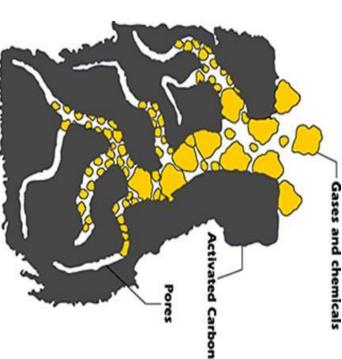
$$D_{min} = 2 * R_{min} * MW$$

Contaminant	Formula	Molecular weight	Approx. diameter, nm	Transport pore size, nm	Adsorption pore size, nm
2-Methylisoborneol	$\mathrm{C_{11}H_{20}O}$	168.3	0.73	3.7	1.31
Geosmin	$\mathrm{C_{12}H_{22}O}$	182.3	0.75	3.8	1.35
Atrazine	$\mathrm{C_8H_{14}CIN_5}$	215.7	0.79	4.0	1.42
Alachlor	$\mathrm{C_{14}H_{20}CINO_2}$	269.8	0.85	4.3	1.53
MTBE	$\mathrm{C_5H_{12}O}$	88.2	0.59	3.0	1.06
Mucidone	$\mathrm{C_{11}H_{16}O_2}$	180.2	0.75	3.8	1.35
Isobutyl mercaptan	$\mathrm{C_4H_{10}S}$	90.2	0.59	3.0	1.06
Dimethyl sulfide	$C_2H_6S$	62.1	0.52	2.6	0.94
Methyl mercaptan	$\mathrm{CH_{3}SH}$	48.1	0.48	2.4	0.86
Fulvic acids	-	>3,500	2.01	10.1	3.6
Humic acids	-	>100,000	6.14	30.7	11.1
Benzene	$\mathrm{C_6H_6}$	78.1	0.57	2.9	1.03
Toluene	$\mathrm{C_7H_8}$	92.1	0.60	3.0	1.08
Xylene	$\mathrm{C_8H_{10}}$	106.2	0.63	3.2	1.13
Ethylbenzene	$\mathrm{C_8H_{10}}$	106.2	0.63	3.2	1.13
Microcystin	$C_{49}H_{74}N_{10}O_{12}$	1,040	0.67	3.4	1.21
Cylindrospermopsin	$\mathrm{C_{15}H_{21}N_{5}O_{7}S}$	415.4	0.49	2.5	0.88
Anatoxin-a	$\mathrm{C_{10}H_{15}NO}$	165.2	0.36	1.8	0.65
Saxitoxin	$\mathrm{C_{10}H_{17}N_{7}O_{4}}$	299.3	0.88	4.4	1.58
Trihalomethanes (THMs)	varies	119 - 253	0.65 - 0.84	3.3 - 4.2	1.2 - 1.5



Molecules that are too large must either be fractionated or elongated to fit through the pore, otherwise they will block the carbon pore structure preventing adsorption





## Uses for Carbon Treatment - Water

- Taste and odor control
- Reductions in VOC's, SOC's, pesticides
- DBP's and precursor removal
- Reduction of PFAS (per-fluoroalkyl & poly-fluoroalkyl substances)
- Removal of BTEX (benzene, toluene, ethylbenzene, xylene) and other hydrocarbons
- Removal of cyanotoxins and other algal byproducts
- Removal of EDC's (endocrine disrupting compounds)
- Organics control (water and air)
- Removal of some PPCP's (pharmacueticals & personal care products)

## Uses for Carbon Treatment - WW

- Reduction of COD, BOD, TOC
- Reductions in AOX (assimilable organic halides)
- Treatment for water reuse
- Flue gas treatment
- Removal of heavy metals (Ni, Cd, Cr, Pb, Zn, Hg)
- Removal of cyanides (CN)
- Treatment for bioassay and toxicity requirements
- Treatment for landfill leachate
- Removal of trace organics and micropollutants

## Activated Carbon Manufacturing

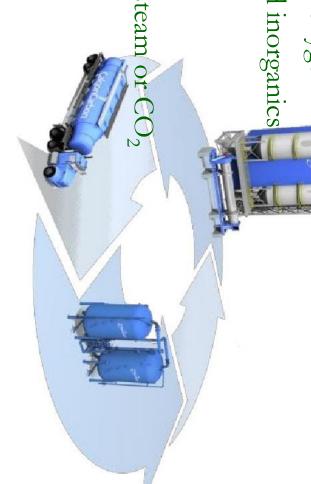
- Common starting materials
- Bituminous coal
- Sub-bituminous coal
- Lignite coal
- Wood products
- Coconut shells (and other nut shells)
- Raw material type
- Affects internal pore structures
- Impacts relative surface area and adsorption capability
- Develops specific carbon surface chemistry



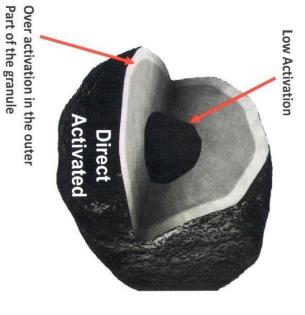
Courtesy of Calgon Carbon Corporation

## Activated Carbon Manufacturing

- Two step process
- Step 1 Carbonization
- Heating to 500°C to 800°C without oxygen
- Drives off undesirable organics and inorganics
- Aligns crystalline structures
- Step 2 Activation
- Heating to 850°C to 1,000°C with steam or CO<sub>2</sub>
- Increases pore sizes
- Creates trimodal pore structures
- Increases internal surface area



# Activated Carbon Manufacturing (GAC)



- Cheaper alternative
- Incomplete activation
- Can increase carbon usage
- Generally shorter life cycle
- May increase treatment costs

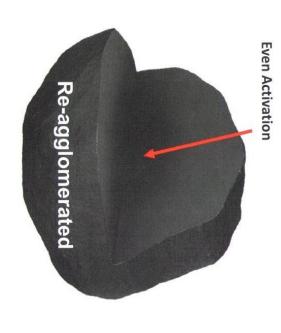
Graphics courtesy of Calgon Carbon Corporation

#### **Direct Activation**



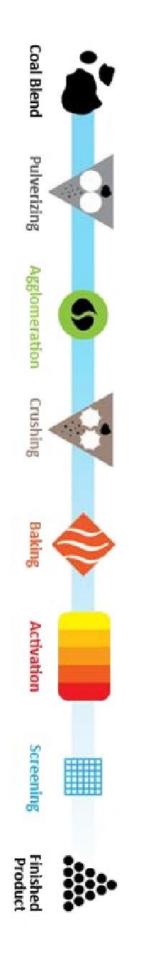
# Activated Carbon Manufacturing (GAC)

- More costly alternative
- About 20% higher unit cost
- More even activation
- Can decrease carbon usage
- Generally longer life cycle
- Up to double useful life observed
- May reduce treatment costs



Graphics courtesy of Calgon Carbon Corporation

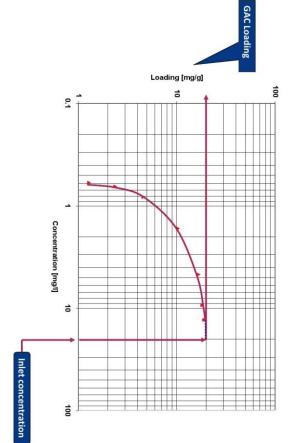
#### Reagglomeration



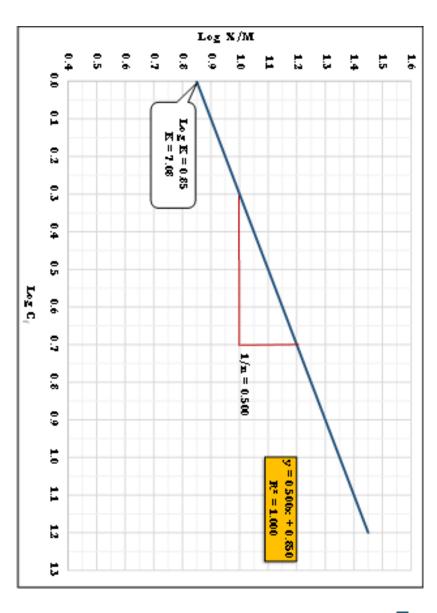
- Different adsorbates removed at different rates
- Adsorption approaches equilibrium levels in solution
- Desorption can occur if multiple adsorbates are in solution
- Highest K tends to win the activation site
- Water pH and temperature play an important role (equilibrium conditions)
- pH levels greater than 8 and temperature < 8°C
- Hinder adsorption
- Increase contact time and dosing
- Particularly important for powdered carbon treatment



- Adsorption isotherms predict carbon use rate
- Define adsorptive capacity and intensity coefficients
- Based on equilibrium conditions between carbon surface, adsorbate concentration, and adsorbate equilibrium concentration
- Developed from experimental data
- Specific activated carbon products
- Specific adsorbates
- Log-log plot of experimental data
- Caution using isotherms
- Multiple adsorbates
- NOM impacts



Courtesy of Calgon Carbon Corporation



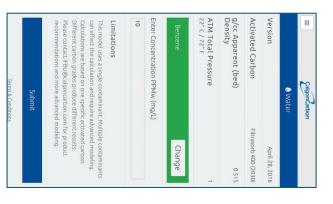
- K and 1/n generated by isotherm log-log plot
- K adsorption capacity onto carbon
- 1/n adsorption intensity (rate)

$$q=K C_f^{1/n}$$

q = adsorption coefficient,  $\mu g/g$  K = adsorptive capacity,  $(\mu g/g)(L/\mu g)^{1/n}$   $C_f$  = final adsorbate level,  $\mu g/L$  1/n = adsorption intensity

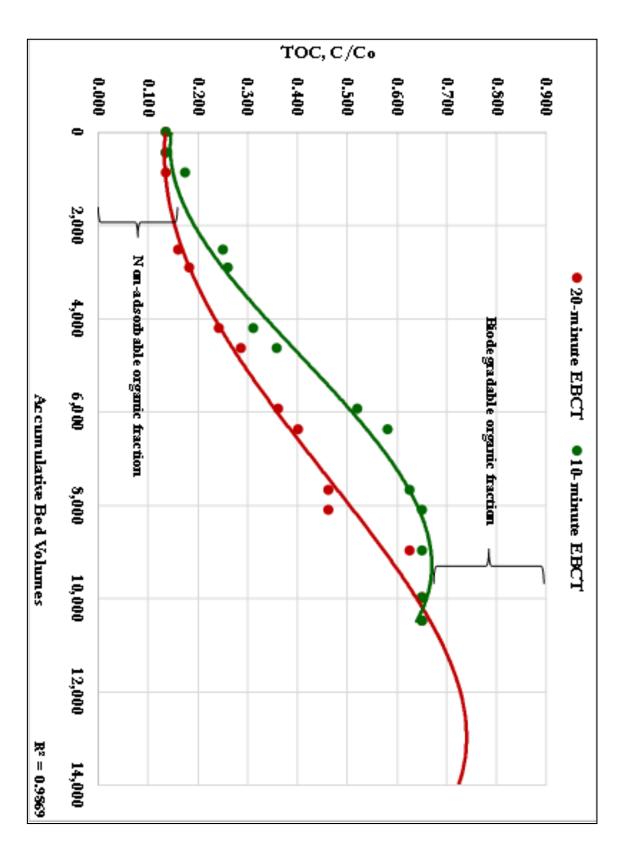
 $C_i$  -  $C_f$  / q = carbon dosage

- Published K and 1/n values
- 70 common adsorbates in Water Quality and Treatment, 6th Edition, Chapter 14
- Specific adsorbates might be obtained from carbon manufacturer
- Some success experienced, but don't expect your contaminant to be tested by manufacturers
- Activated carbon usage rate estimator (iPhone/iPad app)
- Calgon Carbon Corporation free download in app store (CCURE)
- Terms and conditions apply
- Predicts usage rate in pounds per 1,000 gallons for many substances



- Published isotherms
- USEPA "Carbon Adsorption Isotherms for Toxic Organics" 1980
- Contains 130 organic substances with adsorption activity rates and isotherms developed from experimental data





- Adsorption continues in operation
- Breakthrough reached on GAC bed
- Desorption occurs
- EBCT important
- Based on reaction rates and carbon type
- T&O, TOC, DBP precursors 10 minutes
- Cyanotoxins 15 minutes
- DBP's, PFC's 20 minutes



GAC reactors Greater Ouachita, Louisiana

GENERAL ACTIVATED CARBON PROPERTIES ACCORDING TO RAW MATERIAL	
CARBON PROPERTIES ACCORDING TO RAW MATERIAL	GENERAL ACTIVATED
ACCORDING TO RAW MATERIAL	CARBON PROPERTIES
	ACCORDING TO RAW MATERIAL

Property	Coconut-based	Bituminous coal- based	Lignite coal-based	Wood-based
Micropore volume	${ m High}$	${ m High}$	Medium	Low to medium
Mesopore volume	Medium	Medium to High	Low to Medium	Medium to High
Macropore volume	m MOT	m MoT	High	High
<b>GAC Hardness</b>	$\operatorname{High}$	$\operatorname{High}$	Low	Medium
Ash content	Up to 5%	3% to 8%	Up to 20%	3% to 8%
Apparent density	$0.35 \text{ to } 0.50 \text{ g/cm}^3$	$0.32 \text{ to } 0.60 \text{ g/cm}^3$	$0.2 \text{ to } 0.36 \text{ g/cm}^3$	$0.24 \text{ to } 0.39 \text{ g/cm}^3$
Iodine number	Up to $1,100 \text{ mg/g}$	Up to $1,000 \text{ mg/g}$	Up to 600 mg/g	Up to $1,100  \text{mg/g}$
Relative surface area	Up to 1,480 $\mathrm{m}^2/\mathrm{g}$	Up to 1,400 $\mathrm{m}^2/\mathrm{g}$	Up to $1,250 \mathrm{m^2/g}$	Up to 1,480 $\mathrm{m}^2/\mathrm{g}$
GAC Regeneration capability	Good	Good	Poor	Fair

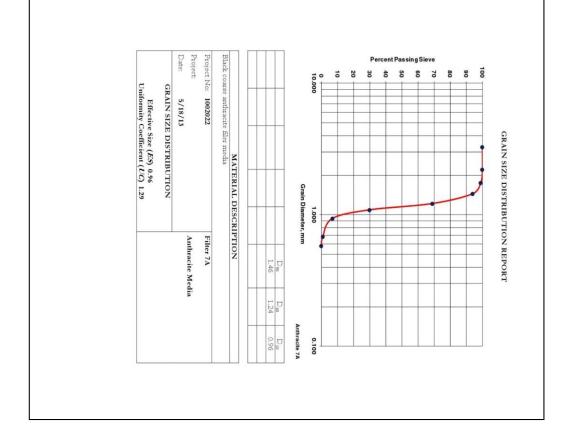
- Ash content (PAC/GAC)
- Reduces adsorption activity
- Reduces reactivation efficiency
- Should be less than 10%



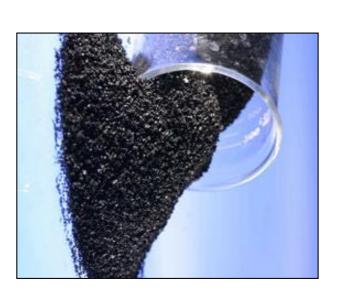
- Abrasion number (GAC only)
- Ro-Tap abrasion test common
- Structural strength of GAC to withstand shear
- Backwash impacts
- Should be greater than 75



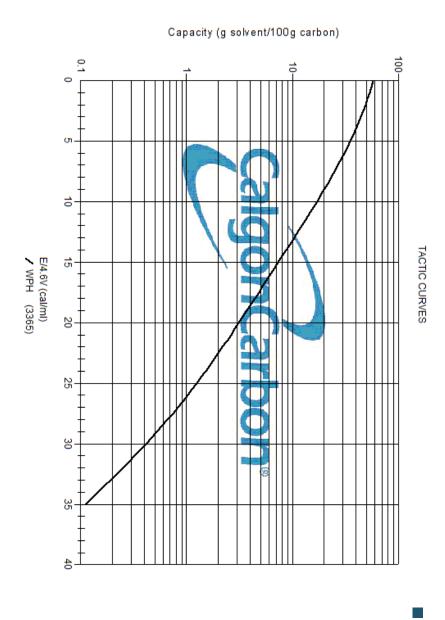
- Effective size(GAC only)
- Grain size distribution in mm similar to filter media
- Differs depending on process use
- Filter GAC caps should be matched to sand for bed expansion (1.0 mm to 2.0 mm ES)
- GAC contactors usually 0.5 mm to 0.8 mm ES
- Uniformity coefficient (GAC only)
- Typical 1.8 to 2.1 for GAC products
- Assists in controlling backwash rates
- Obtain fluidization curve from your GAC manufacturer



- Trace capacity number TCN (PAC/GAC)
- Measures high energy sites needed for adsorption (micropores)
- Greater than 9 grams/cm<sup>3</sup>



- Iodine number IN (PAC and GAC)
- Indicates relative surface area and activity level
- Up to 1,200 mg per gram
- 800 mg/g to 1,000 mg/g common for good quality carbons
- Higher numbers suggest better quality carbon
- 1 gram has surface area up to about 0.36 acres (nearly 16,000 ft<sup>2</sup>)



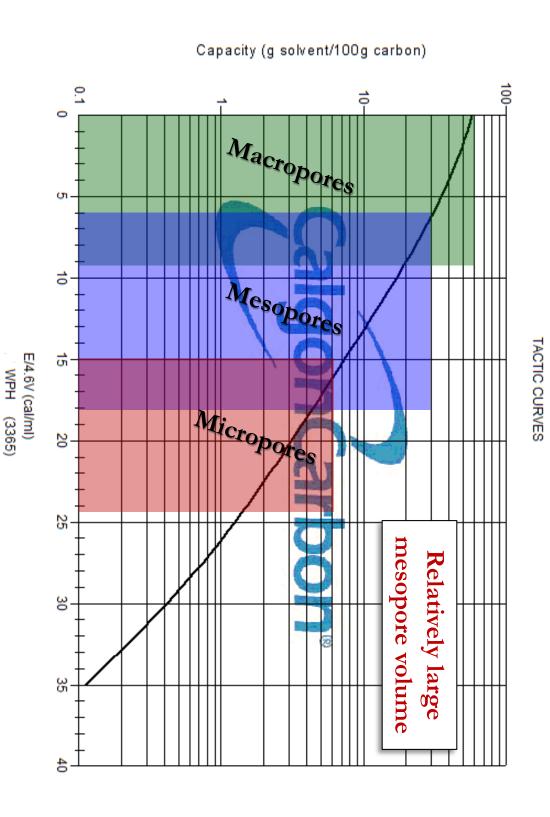
#### TACTIC (PAC/GAC)

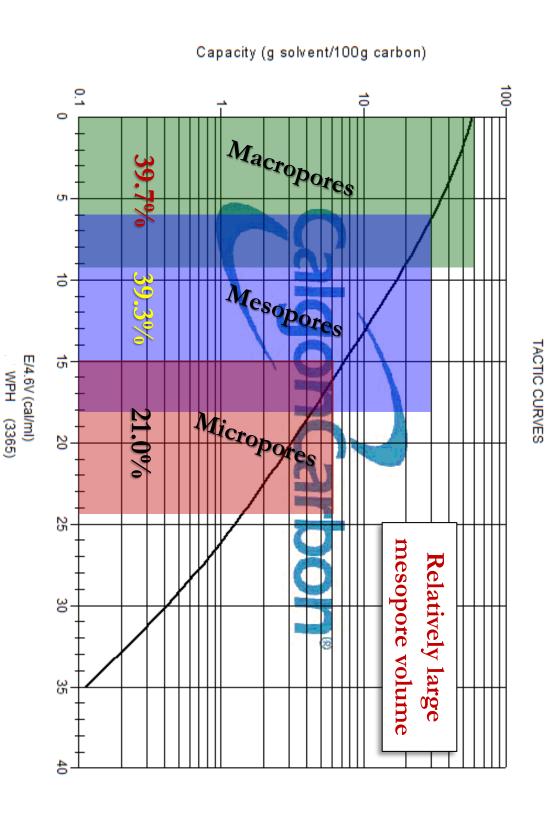
Total Adsorbent
 Characterization via

<u> T</u>emperature <u>I</u>nfluenced

- Correction (Calgon Carbon)

  Fingerprint of carbon surface energy
- Macropores 0 cal/mL to 9 cal/mL
- Mesopores 6 cal/mL to 18 cal/mL
- Micropores 15 cal/mL to 24 cal/mL

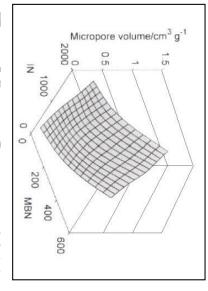




- Methylene blue number MBN (PAC/GAC)
- Measures adsorption of methylene blue dye
- Suggests micropore volume
- Ranges from 150 g/g to 450 g/g
- Values can be used to calculate volumes using IN-MBN ratios

- Molasses number (PAC/GAC)
- Measures adsorption of molasses
- Suggests mesopore and macropore volume
- Ranges from 95 to 600
- Relative to carbon surface area based on IN-MBN ratios

Computer modeling pore volumes

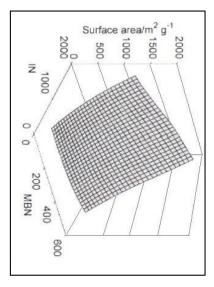


From Nunes-Guerreiro 2011

$$Vm, cm^3/g$$
  
= 5.6 \* 10<sup>-2</sup> - 1.01 \* 10<sup>-3</sup>MBN  
+ 1.55 \* 10<sup>-4</sup>IN + 7 \* 10<sup>-6</sup> MBN<sup>2</sup> + 1  
\* 10<sup>-7</sup>IN<sup>2</sup> - 1.18 \* 10<sup>-7</sup>MBN \* IN

$$Vt, cm^3/g$$
  
= 1.37 \* 10<sup>-1</sup> - 1.9  
\* 10<sup>-3</sup>MBN + 1 \* 10<sup>-4</sup>IN

Computer modeling surface areas



From Nunes-Guerreiro 2011

$$SA, m^2/g$$
  
= 2.28 \* 10<sup>2</sup> - 1.01 \* 10<sup>-1</sup>MBN + 3  
\* 10<sup>-1</sup>IN + 1.05 \* 10<sup>-4</sup>MBN<sup>2</sup> + 2  
\* 10<sup>-4</sup>IN<sup>2</sup> + 9.38 \* 10<sup>-4</sup>MBN \* IN

- Estimate of pore volumes and surface area
- Iodine number 900 mg/g
- Methylene blue number 150
- Total pore volume  $0.26660 \text{ cm}^3/\text{g}$
- Micropore volume  $0.1114 \text{ cm}^3/\text{g}$  (41.8%)
- Meso/Macropore volume  $0.15527 \text{ cm}^3/\text{g}$  (58.2%)
- Surface area  $852 \text{ m}^2/\text{g} (0.21 \text{ acres})$



#### Why Proper Selection is Important

- Activated carbon should be properly match carbon performance to its targeted adsorbates
- Adsorbate molecular size must fit within the pore structures to reach adsorption sites
- Large molecules may not reach adsorption sites and can block pore structures
- Poor treatment performance results in higher organics complaints and/or non-compliance issues concentrations in drinking water and may lead to customer
- Improper carbon type increases chemical treatment dosages and treatment costs
- Take care to avoid oxidant/carbon interactions
- Oxidation byproducts block pore structures

- PAC dosages can be predicted using empirical equations from research literature
- Caution many tests carried out in lab pure water with one organic substance
- Source water dosing can be double the predicted values
- Best practices suggest safety factor of 2 if TOC >5 mg/L
- efficiencies Multiple adsorbates create different kinetics and adsorption
- Interferences often observed when multiple adsorbates are in solution
- Desorption can occur if higher K substance enters carbon particle

- Freundlich equation
- Predicts single adsorbate removal dosing for carbon treatment

$$q = K C_f^{1/n}$$
  
 $q = adsorption coefficient, \mu g/g$   
 $K = adsorptive capacity, (\mu g/g)(L/\mu g)^{1/n}$   
 $C_f = final adsorbate level, \mu g/L$   
 $1/n = adsorption intensity$ 

 $C_i$  -  $C_f$  / q = carbon dosage

#### Estimated PAC for Microcystin

Removal to 0.3 µg/L

132	50	1.0	1,259
41	50	0.9	3,630
16	50	0.56	6,309
Dose, mg/L	Ci	1/n Ci	K

Carbon usage rate (CUR) published WRF 1998

$$CUR, \frac{lbs}{1,000} gallons = \frac{EBCT * \rho GAC * 10^3}{T * 7.48 * 1,440}$$

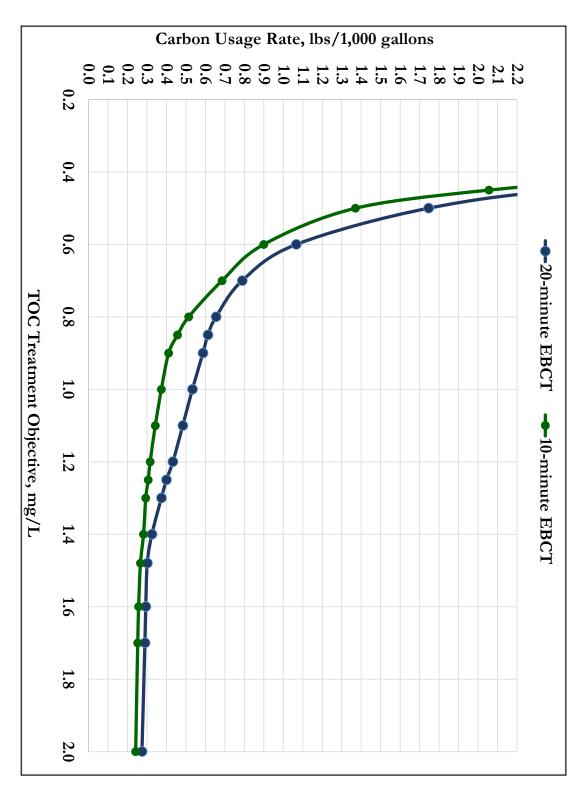
Where  $CUR = Carbon\ Usage\ Rate$ , pounds per 1,000 gallons  $\rho$ GAC = carbon density, pounds/cubic foot EBCT= empty bed contact time, minutes 7.48 = 7.48 gallons per cubic foot T = breakthrough time in days1,440 = 1,440 minutes per day

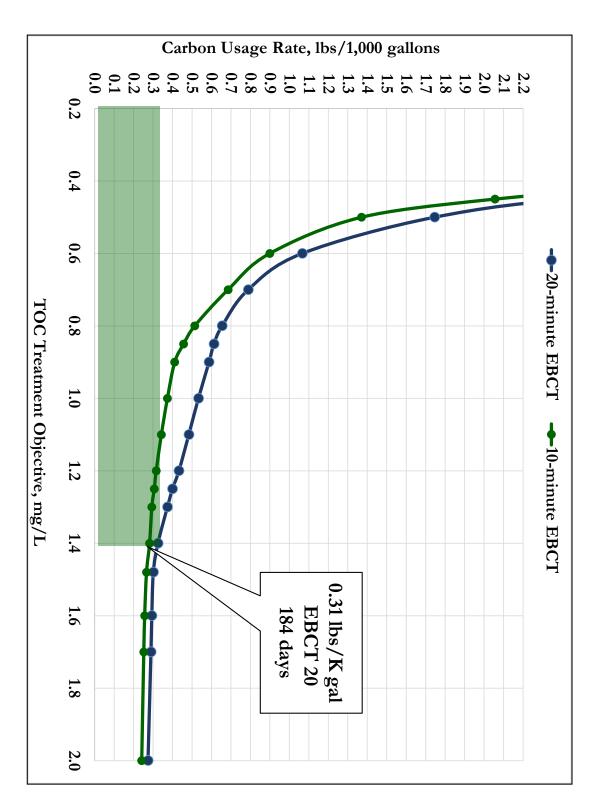
Carbon usage rate (CUR) example

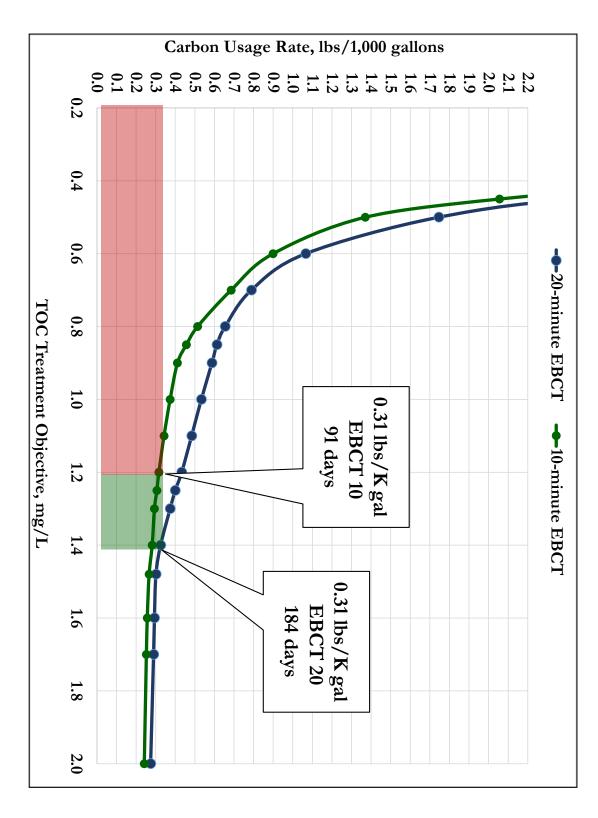
$$CUR, \frac{lbs}{1,000} gallons = \frac{EBCT * \rho GAC * 10^3}{T * 7.48 * 1,440}$$

EBCT - 20 minutes, 184 days breakthrough

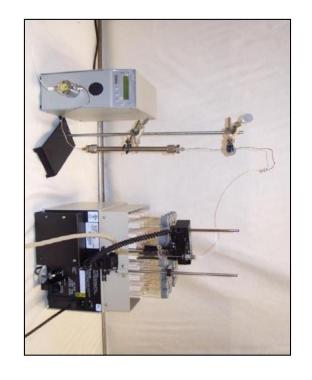
$$CUR = \frac{20 * 31 * 10^3}{184 * 7.48 * 1,440} = 0.31 \frac{lbs}{1,000} gal$$





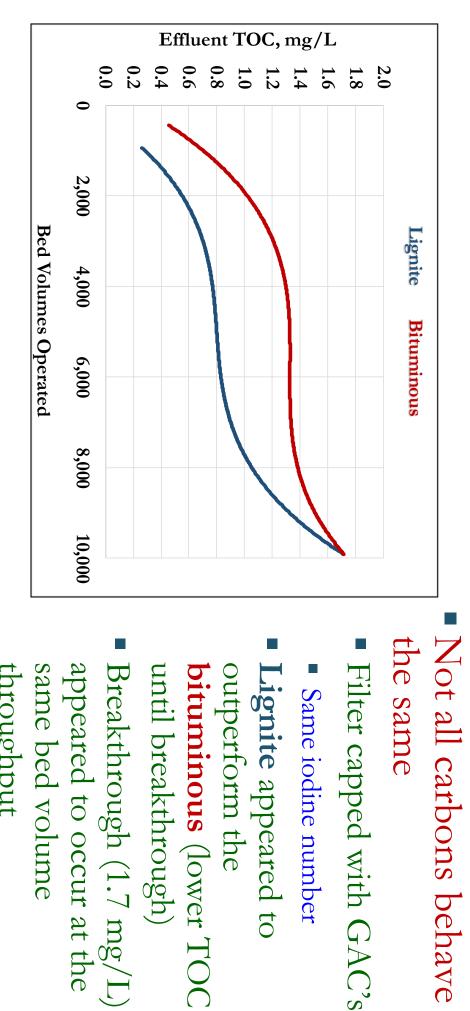


- Experimental testing is best means to determine carbon dosing
- RSSCT, ACT, or pilot scale for GAC
- Jar testing for PAC
- Multiple adsorbates create removal difficulties
- Competing adsorption reactions
- NOM tends to block adsorption sites and transport pathways
- Desorption can occur
- Oxidants create byproducts tending to block adsorption sites



- Contact time and mixing important
- PAC up to 4 hours possible
- GAC EBCT determined from demonstration study
- pH and temperature also play a role in treatment efficiencies
- Dosing difficult to calculated present (predicted) values if multiple adsorbates
- Freundlich equations
- Dosing estimators
- Dosage needed could be double





Lignite appeared to

Same iodine number

outperform the

Breakthrough (1.7 mg/L)

until breakthrough)

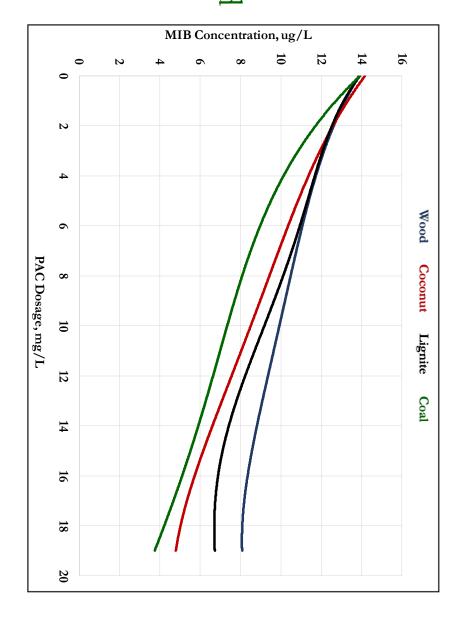
bituminous (lower TOC

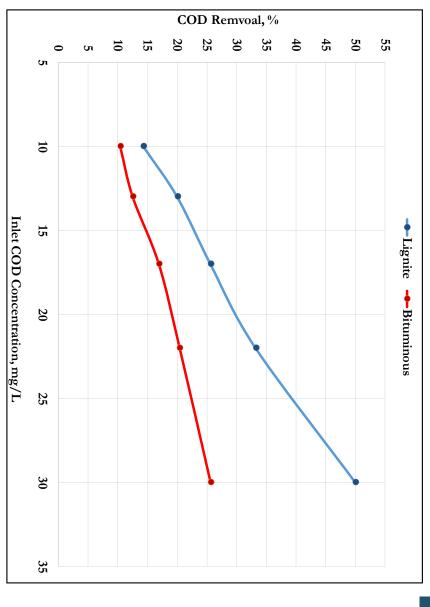
appeared to occur at the

same bed volume

throughput

- Not all carbons behave the same
- PAC's for MIB reductions
- Same iodine numbers
- Bituminous coal appeared to outperform the other carbon products
- Likely have better removals at lower dosages based on this study





- Not all carbons behave the same
- PAC treatment of COD in wastewater
- Lignite appeared to outperform the bituminous (greater COD removals)
- Iodine numbers and PAC dosages not given in literature
- General PAC dosing for wastewater is 10 mg/L or greater

- Determine target adsorbate(s) and concentrations
- Define seasonal or prolonged occurrence in treatment
- Select a PAC or GAC product accordingly
- Consider kinetics of process
- Adsorption isotherms give a best guess
- Published isotherm data can predict dosing
- Choose carbon matched to the adsorbate molecular size
- May need larger mesopore volume for treatment efficiency (40% or higher)
- Use other carbon criteria to properly remove target contaminant
- Conduct testing and life cycle costs for final product selection
- Buy carbon based on performance, not purchase price

#### Questions

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