

BONDED CHEMICALS Inc.

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Safety First

- Wear your PPE -- Even Clint Eastwood or Chuck Norris aren't tough enough to beat chemicals



- Goggles are the best eye protection.
- If you do have an accident – TELL SOMEONE, and GET HELP

Horse Race – and they're off



Chemicals That Can Be Used For Phosphorous Reduction

- Ferrous Chloride
- Ferric Chloride 38%
- Aluminum Sulfate 48%
- PAC – Poly Aluminum Chlorides
- ACH – Aluminum Chloro Hydrates
- Sodium Aluminate 37-45%

What Info Is Needed?

- Flow (normal & max)
- P Influent Concentration
- P Effluent – Limit
- pH Limits (low – high)

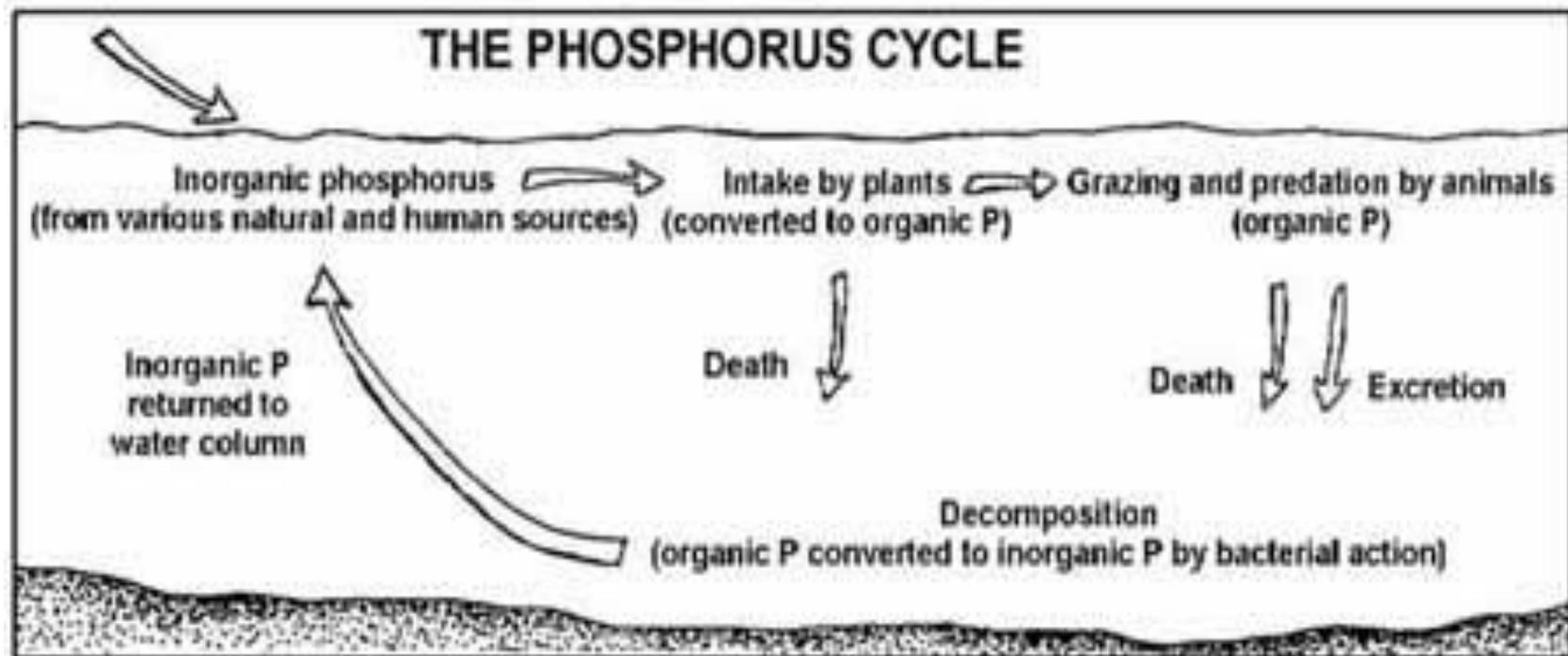
Phosphorus Removal

- EPA-mandated <1 ppm PO_4 in plant effluent
 - Restriction will tighten in future
 - Depends on discharge water (stream vs. lake, etc.)
- PO_4 Removal Techniques
 - **Biological**
 - High capital expense (\$\$\$)-system configuration
 - Limited effectiveness (typically removes <1 ppm PO_4)
 - Better for nitrogen (N) removal
 - Requires volatile fatty acids to work
 - **Chemical** - Aluminum or Iron

Nutrient Removal

- Nitrogen / phosphorus are essential nutrients for aquatic plant growth
- When available in excess, water body can become “eutrophic” – literally “well-fed”
 - Excess algae growth results in loss of oxygen for fish, unsightly growth and odor problems
 - Potential for toxins (microcystin) that can jeopardize public health (water supply, contact)
- Algae growth is limited by nutrient that is least available
 - In fresh water, this is usually phosphorus
- In water bodies where eutrophication is a problem, nutrient load from wastewater (point source discharge) must be controlled
 - Phosphorus in WWTP effluent, therefore, can cause eutrophication of lakes and rivers

THE PHOSPHORUS CYCLE



Municipal Wastewater Treatment Plants

- Typical P Concentrations
 - Raw domestic wastewater: 4-8 ppm
 - Will be higher with certain types of industry dischargers (food, metal processing)
- Focus should be on allowing treatment process to remove as much particulate and soluble P as possible. Chemical treatment applied to remove soluble P. A polishing agent if you will.
- What portion of your effluent total P is soluble vs. insoluble ? Depending on the result you may also have a settling issue which will dictate the type of chemical needed.

Qualifying Opportunities

- Do a people and technical survey prior to running any tests.
- Type of system- conventional, oxidation ditch, trickling filter
- Flow, Influent P, Effluent P (are they getting any BNR?)
- Current status of treatment /removal?
- Using caustic or any other pH adjustment chemicals.
- Do they have UV for disinfection
- Do they need just a P removal agent or also a solids settling aid. (coagulant)
- Industrial applications- BOD,COD, FOG removal ?

Testing Protocol

- Sample collection point is critical. If currently using a chemical we want to collect a testing sample PRIOR to addition. (Consider any recycle)
- Test the sample for filtered and unfiltered PO₄. The filtered PO₄ is your baseline. The amount you want to remove is the filtered PO₄ minus the plant's effluent target. This is the value you put into the dosage calculator.
- Dose the jars according to plan. Mix ~20 minutes. Settle ~10 min.
- Using the syringe collect water and filter to test each jar for soluble phosphorus remaining.
- Comparing your baseline filtered PO₄ to the jar PO₄ provides a evaluation of soluble phosphorus reduction efficacy of the chemical at the specific dosage and Al:P ratio

Aluminum vs. Iron

- Iron negatively affects UV disinfection
 - Iron salts can precipitate onto the UV system's quartz tubes forming an adsorbing film.
 - Dissolved iron molecules adsorb UV radiation in the critical wavelength, aluminum doesn't
 - Iron can be adsorbed into suspended solids and bacterial floc, where it can prevent UV light from reaching embedded target microorganisms
 - UV disinfection unit more efficient with aluminum based chemicals
- Same dosage of aluminum will combine with twice as much phosphorus vs. iron
 - Al molecule weighs less than half Fe molecule, therefore twice as many molecules in pound of LSA as pound of FeCl_3
 - Takes 0.87 lbs. aluminum / 1.8 lbs. iron to remove 1 lb. of phosphorus
- Unlike iron phosphate, aluminum phosphate does not re-dissolve under anoxic conditions
 - Increased flexibility / efficiency
- Not as corrosive / messy as FeCl_3
 - Can use metal storage tanks / piping / valves
- Fewer contaminants = reduced sludge generation

Key Considerations for Successful Chemical Removal of Phosphorus

- Thoroughly understand raw water P sources, type, and fluctuations (seasonal/otherwise). Look for sidestream contributors (filter press)
- Conduct extensive testing of a few Al+ based coagulants to find the best performing and cost effective product for your water/treatment process. Are your needs solely for P removal or do you also need a settling aid?
- Evaluate/ test each product based on the metal to phosphorus ratio. (1:1,2:1,3:1 etc.). Best performer at the lowest ratio. Keep in mind that below 0.3 ppm PO₄ the molar ratio increases significantly, as does the dosage requirement
- Feed point and mixing are key. Feeding at the headworks will “work” but other constituents (BOD,COD) are competing with P for aluminum. Good mixing required for efficient HMO formation. Both of the above impact chemical dosage/usage
- Examine intended or unintended consequences:
 - impact of chemical on effluent PH and system alkalinity (ammonia removal)
 - sludge dewatering and generation
 - efficiency of UV system impact
- Thoroughly review current delivery systems for compatibility and or design around best coagulant.
- Review /Discuss Final Clarification-limiting factor in P removal
- Monitoring and Control Protocol

Impact of Secondary Clarifiers on P and TSS in Effluent

- Effective Solids Capture is critical- understand final clarifier operation/history
- Function: Clarification, Thickening(sludge wasting and return), and Storage (catch solids in high flow)
- Downward velocity of solids vs. upward velocity of water
- Failure
 - > If overflow velocity (flow/surface area of clarifier) is higher =
carryover of solids
 - > Thickening- putting more solids in than taking out

P Removal Info

Average Total Flowrate, MGD	2.250
P Influent Concentration, mg/l	3.50
Daily Flowrate, gpm	10.410
P Effluent concentration, mg/l (target)	0.7
Ferric Solution Concentration, %	38
Weight Ratio, g Fe/g P	1.8
Feed Safety Margin	1.5
Solution density, lb/gal	10.91
lb FeCl ₃ per gal of solution	4.1458
lb Fe III per gal of solution	1.427

Using Ferric Chloride 38%

Ferric Chloride 38% Solution			
Average P Loading per Day, lbs	65.67750		
Average P Loading per hour, lbs	2.73656		
Total Peak Influent Loading, lbs/hr	2.73656		
Total Peak FeCl ₃ Solution Required, gal/hr	3.45081		
Total Peak FeCl ₃ Solution Required, gpm	0.05751		
Concentration P to Precipitate, mg/L	2.80		
Amount P to Precipitate per day, lbs	52.542		
FeCl ₃ Solution Required, gal/day	99.4	412	Dry pounds Ferric Chloride/day
FeCl ₃ Solution Required, gal/week	695.7	2,884	Dry pounds Ferric Chloride/week
FeCl ₃ Solution Required, gal/month	2956.7	12,258	Dry pounds Ferric Chloride/month

Using Alum

Aluminum Sulfate Solution			
Concentration P to Precipitate, mg/L	2.80	11.1 Pounds per gallon	
Amount P to Precipitate per day, lbs	52.5420		
Aluminum Sulfate required, gal/day	132.0	706	Dry pounds Aluminum sulfate/day
Aluminum Sulfate required, gal/week	924.1	4,944	Dry pounds Aluminum sulfate/week
Aluminum Sulfate required, gal/month	3927.6	21,013	Dry pounds Aluminum sulfate/month

Using Sodium Aluminate 38%

Sodium Aluminate 38%	
Million Gallon per Day MGD	2.250
Desired ppm P removal	2.80 ppm
Weight of Water	8.34 lb/gal
Weight of P per day:	52.542 P in pounds per day
Al Atomic Wt.:	27 g/mole
P Atomic Wt.:	31 g/mole
Al ₂ O ₃ Atomic Wt.:	102 g/mole
%Al ₂ O ₃ in USALCO 38	20% 20 percent
USALCO 38% density	12.3 Lb/gal
Desired Al:P Ratio	2
Required Al/day	91.5 Pounds
% Al in USALCO 38	0.106
Sodium aluminate 38%/day	70.2 gallons per day
Sodium aluminate 38%/week	491.4 gallons per week
Sodium aluminate 38%/month	2063.8 gallons per month

Cost Comparison

Costs	price/pound	Day	Week	Month
Ferric Chloride	\$ 0.21	\$227.70	\$1,593.88	\$6,773.98
Aluminum Sulfate	\$ 0.21	\$307.74	\$2,154.16	\$9,155.19
Sodium Aluminate	\$ 0.48	\$414.45	\$2,901.16	\$12,184.88

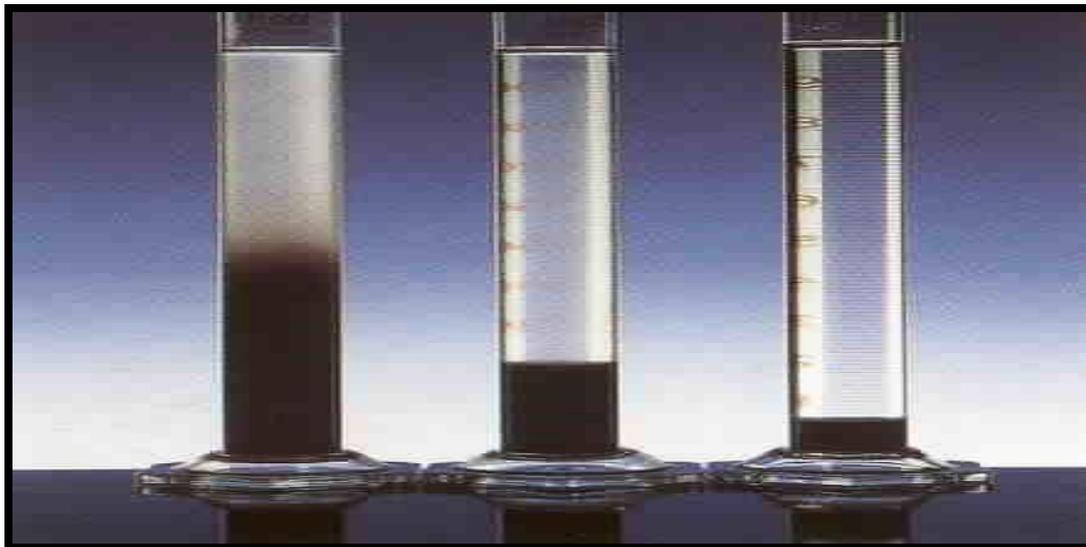


Product Name: Ferric Chloride

Synonyms-Iron (III) Chloride Solution

Chemical Formula- FeCl_3

CAS Number-7705-08-0



Ferric Chloride-Advantages

- Odor Control
- Increased Dewatering
- Quick P Reduction



Phosphorus Removal

Phosphorus

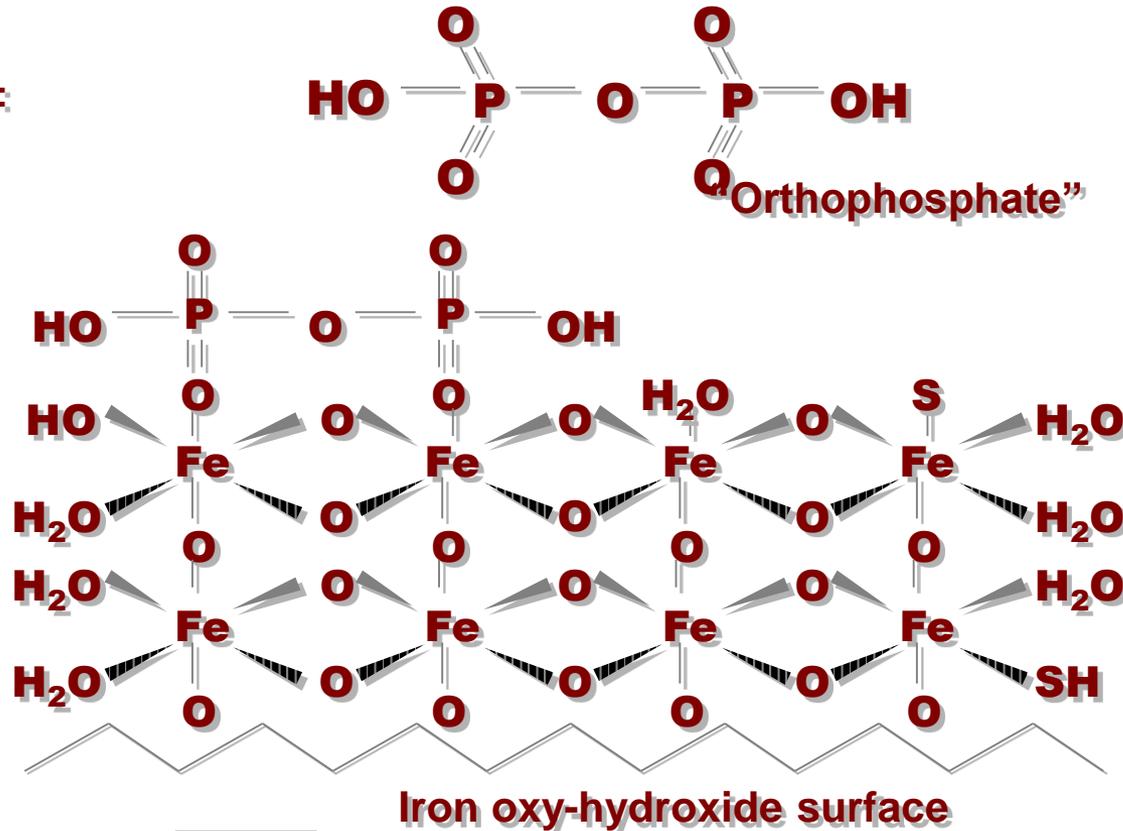
- **Nutrient which can accelerate eutrophication**
- **Many states require its removal**
- **Chesapeake Basin plants meeting .18 mg/l discharge limits using Ferric Chloride**
- **Precursor to “struvite” formation in centrifuge centrate lines**



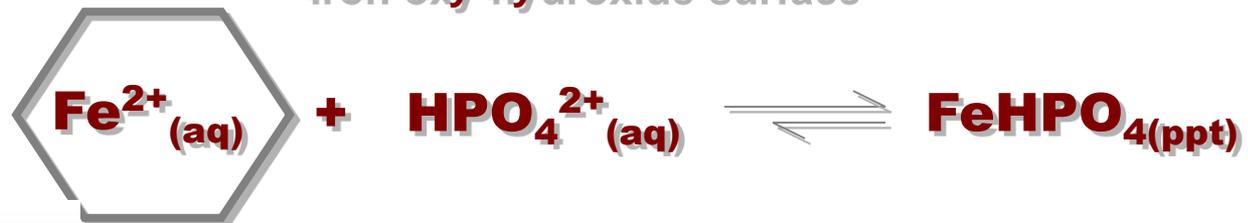
Phosphorus Removal

- Ferric Chloride will adsorb orthophosphates onto the “iron oxyhydroxide surface”

Method 1:

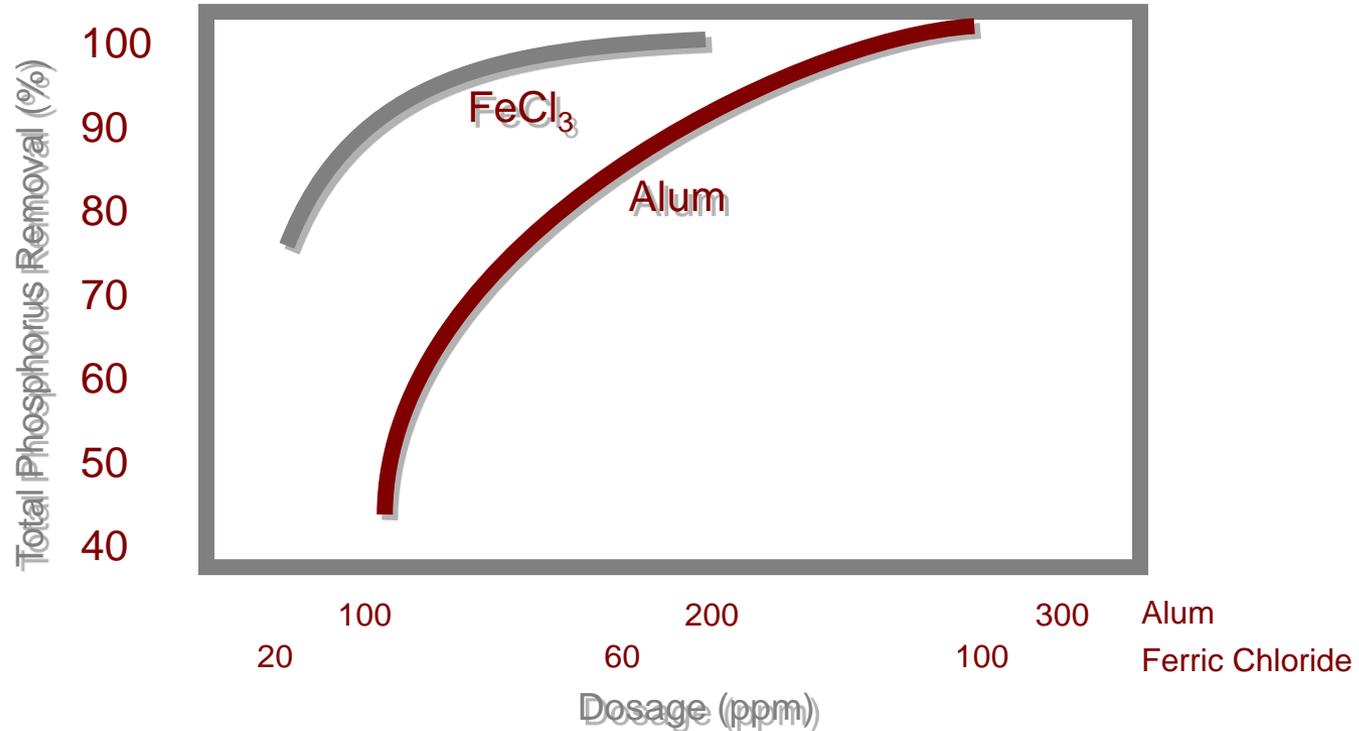


Method 2:





Phosphorus Removal



- **Proven more effective than alum**
- **Each pound of phosphorus removed requires:**
 - 5.6 pounds of Ferric Chloride or 9.6 pounds of alum



Odor Control





Odor Control

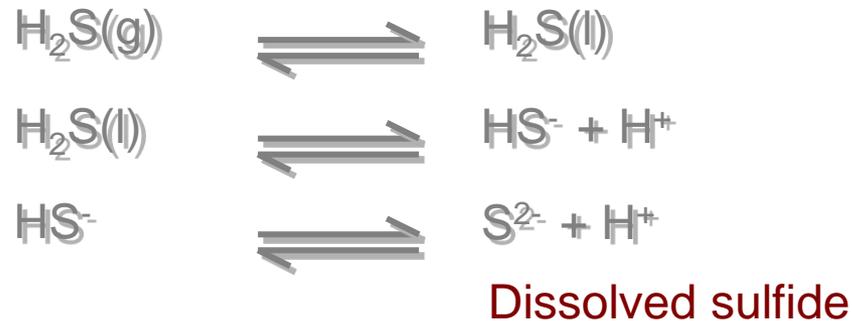
Sulfur Based Odors:

- **Inorganic H₂S most prevalent**
- **Caused by dissolved sulfides**
- **Present in many waste streams**
- **Increased community pressure**
- **Industrial hygiene concerns**



Odor Control

H₂S Chemistry



- **Equilibrium**
- **Dissolved sulfide can come from anaerobic sulfate reduction**
- **Aided by low oxidation/reduction potential (ORP) of waste water**



Odor Control

How Ferric Chloride Helps

Step 1: Fe^{3+} + Waste Water \longrightarrow Fe^{2+}

- Oxidizes waste water
- Raises ORP
- Not possible with Ferrous Chloride



Odor Control

How Ferric Chloride Helps

Step 2: Fe^{2+} + Sulfides \rightarrow Iron Sulfide Precipitate

- Effectively binds up sulfides
- Shifts equilibrium to reduce gaseous H_2S



Odor Control

Advantages:

- Coagulant action
 - **Not possible with ferrous salts**
 - **Not possible with Sodium Hydrochlorite**
 - **Not possible with Potassium Permanganate**
- Does not add sulfates to the process



Why Use Ferric Chloride *Instead of:* **ALUM**

- **Ferric Chloride flocculates over broader pH and temperature range**
- Ferric Chloride typically forms heavier, denser floc allowing better performance in settlers and thickeners
- **Typically lower doses of Ferric Chloride are needed to achieve similar removals producing less chemical sludge.**
- Ferric Chloride is more efficient in control of trihalomethanes (drinking water).
- **Ferric Chloride reacts with dissolved sulfides providing odor control benefits.**



Why Use Ferric Chloride *Instead of:* **FERRIC SULFATE**

- Ferric Chloride molecule has higher percentage of iron than Ferric Sulfate.

ADDS LESS CHEMICALS TO THE PROCESS

- Ferric Chloride does not add sulfates to your process. ***SULFATES MAY BE REDUCED TO SULFIDES EVENTUALLY FORMING ODOROUS HYDROGEN SULFIDE***



Why Use Ferric Chloride *Instead of:* **FERROUS CHLORIDE**

- Pickling Liquor™ sources may vary in concentration causing difficulty in dosing.
- Ferric Chloride floc typically settles faster, allowing for less carryover of flocculated material.
- Ferric Chloride is a mild oxidizer.

***CAN HELP RAISE WASTEWATER ORP
ADDED BENEFIT OF HELPING CONTROL ODORS***

- Ferric Chloride can reduce polymer consumption when used for dewatering system odor control. Ferrous Chloride does not.



Why Use Ferric Chloride *Instead of:*

POLYALUMINUM CHLORIDE (PAC)

- Ferric Chloride can provide similar or better performance in many cases.
 - Ferric Chloride is significantly less expensive than PAC.
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CHEMICAL REPLACEMENT

REFERENCE CHART

USE	<u>ALUMINUM SULFATE</u>	<u>FERRIC SULFATE</u>	<u>FERROUS CHLORIDE</u>	<u>PAC</u>
Odor Control	-	+	+	-
Coagulation	+	=	-	=
Phosphorus Removal	+	=	=	=
Sludge Conditioning	+	=/+	-	=
Heavy Metal Removal	+	=	-	=
Struvite Control	+	=/+	+	=
Trihalomethane Control	+	+	-	+

+ Ferric Chloride is an IMPROVED replacement

= Ferric Chloride is an drop-in replacement (similar performance)

- Categorical Chemical will NOT do this, Ferric Chloride WILL

Product Information

Product	%Me	%Bas	Specific Gravity
Alum (as liquid)	4.38	0	1.33
Alum (as dry)	9.01	0	1.33
FeCl ₃ (40% avg)	13.20	0	1.41
DeIPAC 2020	5.57	70	1.23
DeIPAC 801	5.29	70	1.20

What is PAC ?

- Polyaluminum Chloride (PACL) are inorganic polymers or polyaluminum complexes that carry a high positive (cationic) charge. Ideal for neutralizing negative charged particles in raw water sources. PAC is a broad family or category of chemicals that differ in basicity, molecular weight, Al_2O_3 content, and thus functionality. Products from low basicity “PAC” to ACH. (aluminum chlorohydrate)
- Unlike inorganic coagulants, namely alum and ferric chloride, PAC requires virtually no alkalinity to develop cationic charge and precipitate as floc.
- Given PAC’s very different mechanism of reaction compared to alum/ferric it performs much better in cold water. Cold water slows the reaction of alum/ferric with water’s alkalinity thus taking longer to develop the required charge for effective turbidity removal. PAC’s come pre charged.

Let's Talk About Sodium Aluminate- “It's a Bit Different”

- Highest Al⁺ content (outside of ACH)
- Only P removal agent that does not consume alkalinity
- Great for phosphorus removal, not so good as a coagulant for solids settling
- Superstar in conventional RAS plants, especially when alkalinity and effluent pH are an issue.
- Struggles in trickling filter plants
- Application and storage considerations

Dosage Rate Calculation

- Example: A 1.5 MGD plant has an influent total phosphorus concentration of 8 ppm, and a discharge limit of 1 ppm.
 - Desired P reduction of 7 ppm
 - Start with a Al:P ratio of 2:1
 - Al atomic weight: 27 g/mole
 - P atomic weight: 31 g/mole
- Weight of P/day to be removed
 - = Flow in MGD x Desired P Removal in ppm x Density of Water
 - = 1.5 MGD (7 ppm x 8.34 lbs./gallon)
 - = 88 lbs./day

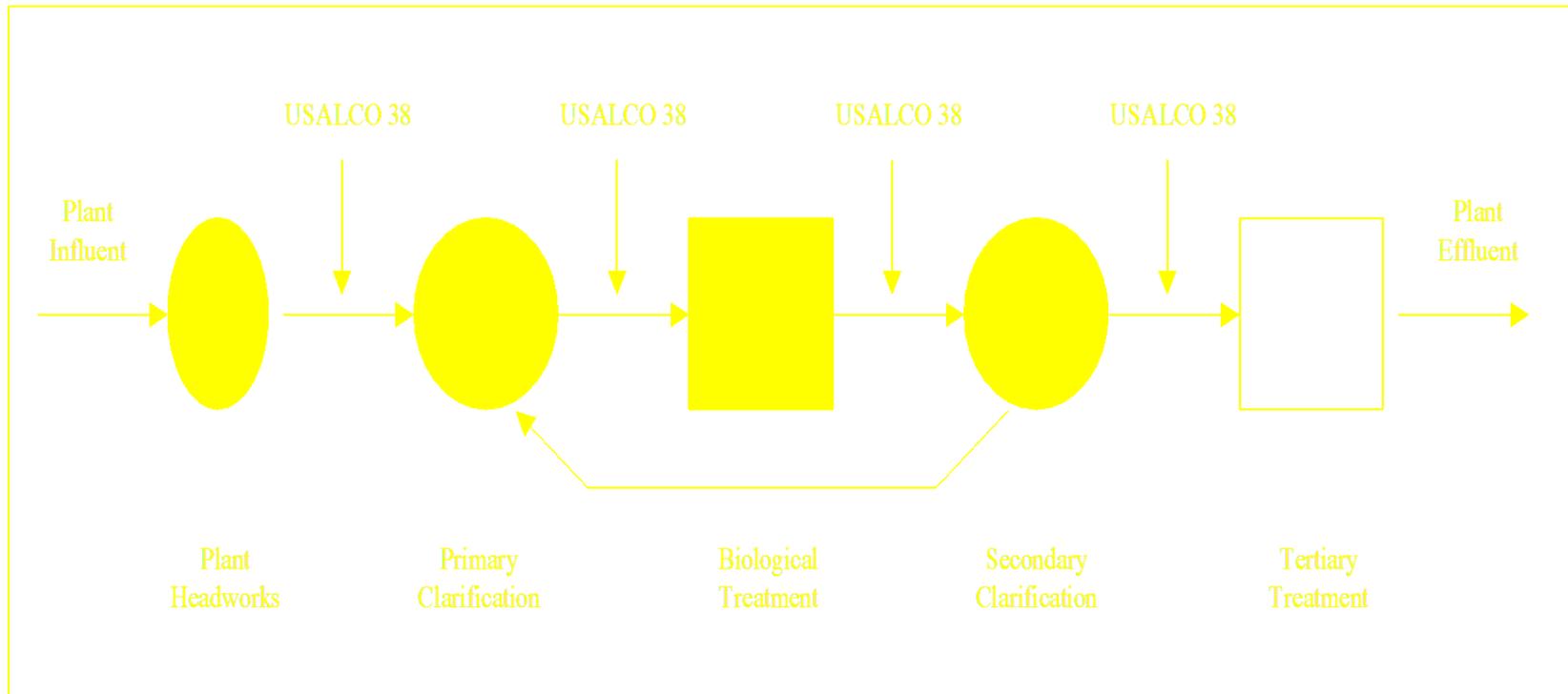
Dosage Rate Calculation

- Required weight Al/day for desired P removal
 - = (Atomic weight ratio of Al to P) x (Al:P feed ratio) x (Pounds of P/day to be removed)
 - = $27/31 \times 2 \times 88$
 - = 153 pounds of Al per day required to remove 88 pounds of P per day.
- Dosage of 38% LSA to provide 153 pounds of Al per day
 - = (Wt. of Al/day) / (Weight of 38% LSA/gal x % Al in 38% LSA)
 - = (153 pounds of Al/day) / (12.3 pounds/gal x 0.106)
 - = 117 gallons/day 38% LSA

Application

- Common feed points:
 - Primary clarifier
 - Aeration basin
 - Return activated sludge
 - Aeration effluent into final clarifier
- Best fed neat if possible.
- Address recycle streams (filter presses)
- Mixing is **CRITICAL** for efficient HMO formation !!

Where's The Best Place to Feed?



Sodium Aluminate Handling and Storage

- Tanks
- Piping
- Valves
- Pumps

Storage & Handling

- Sodium Aluminate solutions are viscous solutions which should be stored at the following temperatures:
 - 38% LSA should be kept above 45° F

Sodium Aluminate Tanks

- Stainless Steel
- Carbon Steel
- Polyethylene
- Rubber-lined (check compatibility)
- Glass-lined
- Fiberglass (check type of resin)

Tanks cont.

- Extend fill pipe to about 6"-12" off the bottom of the tank to minimize air contact.
- Bottom fill.
- Bend vent pipe to prevent precipitation from entering the tank.

Sodium Aluminate Piping

- Carbon Steel (Schedule 40)
- Stainless Steel
- Fiberglass
- CPVC (Schedule 80)
- Teflon-lined
- Use 304 or 316 stainless steel fittings for all hose fittings

Sodium Aluminate - Valves

- Lug body butterfly valves recommended
 - 316 stainless steel disc
 - EPDM seat
- Do not use ball valves!

Sodium Aluminate Pumps

- Recommended: Centrifugal pump (stainless steel, cast iron, or ductile)
- Diaphragm
- Piston

Preventive Maintenance

- Inspect tanks/lines every 3 months.
- Do not flush lines with hot water or steam unless they can be fully dried or flushed with caustic.

Others Are Depending On You!

