

Nutrient Optimization: Why? How? What?

Operator Training Committee of Ohio
Compliance Workshop
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Grant Weaver, PE & wastewater operator
President
CleanWaterOps.com, an ERG subcontractor

Nutrient Optimization: Why, How & What

Why

Facility Planning solutions can be very expensive

Optimizing existing facilities is often quicker and more sustainable

How

Create optimal habitats for N&P removal

What: Case Studies

Chinook, Montana

Conrad, Montana

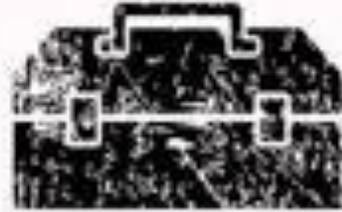
Cookeville, Tennessee

Palmer, Massachusetts

Cost of Nutrient Removal

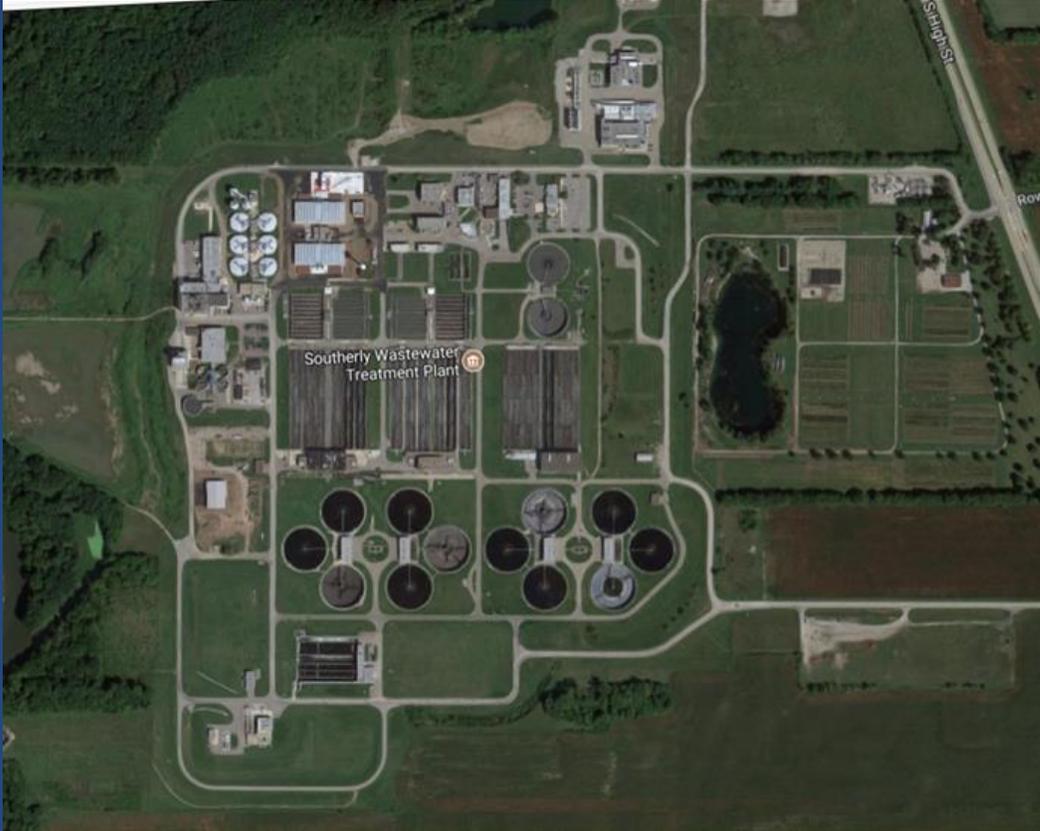
	Effluent Concentration	Capital Cost (\$/MGD)	O&M Cost (\$/yr/MGD)
Nitrogen	3-8 mg/L	0-\$98 million	0-\$1.8 million
Phosphorus	1 mg/L or less	\$30,000-\$22 million	\$40,000-\$2.3 million
	1 mg/L +	\$50,000-\$13 million	0-\$1.5 million

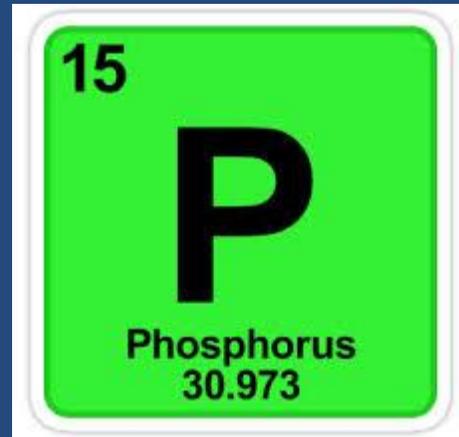
Source: EPA 2015 "A Compilation of Cost Data Associated with the Impacts and Control of Nutrient Pollution"



OPERATIONS CHALLENGE™

Change day-to-day operations to create ideal habitats for bacteria to remove Nitrogen & Phosphorus





Phosphorus Removal: What an Operator needs to know

ONE. Convert soluble phosphorus to TSS ...

Biologically

Chemically

TWO. Remove TSS



Biological Phosphorus Removal

Step 1: prepare “dinner”

VFA (volatile fatty acids) production in anaerobic/fermentive conditions

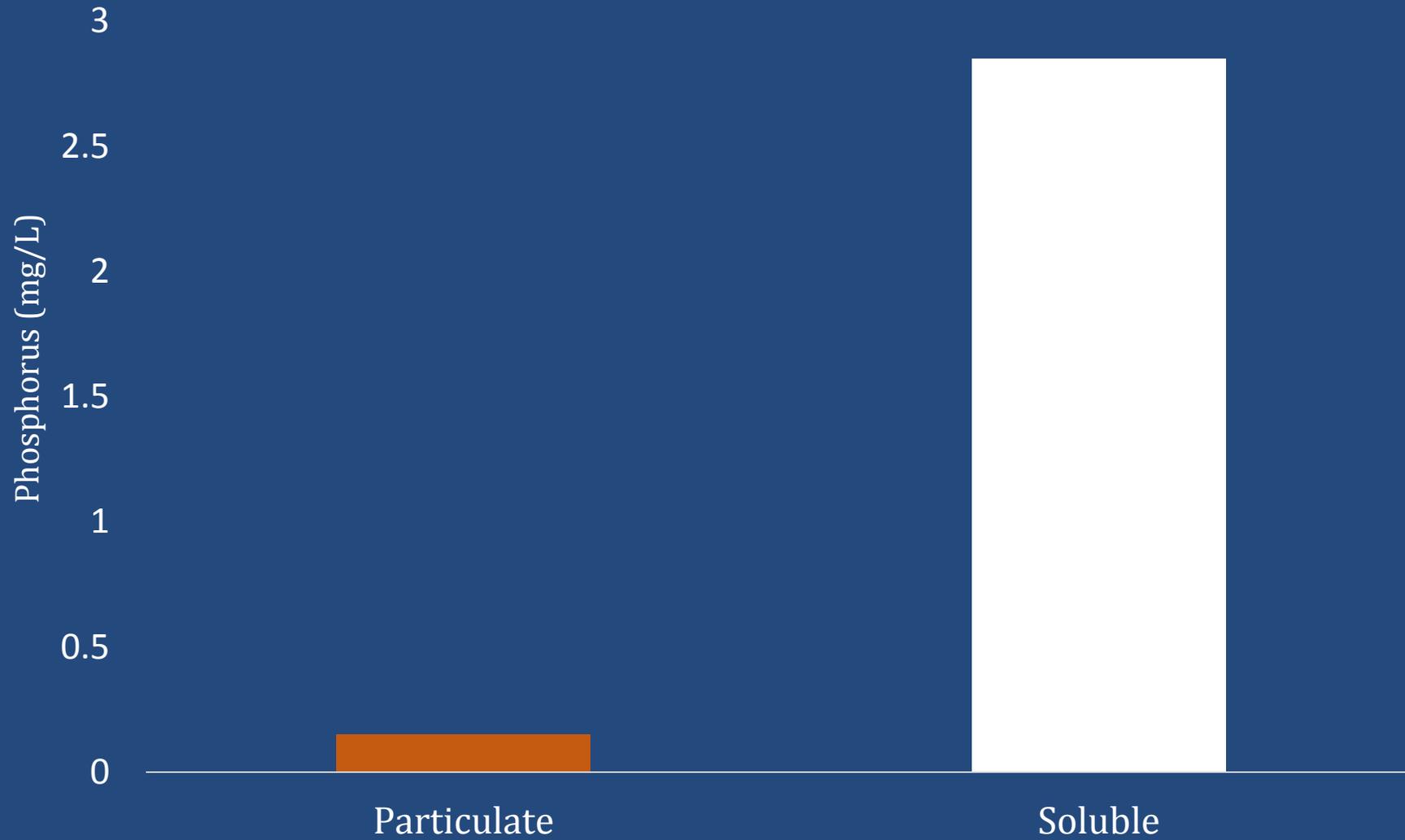
Step 2: “eat”

Bio-P bugs (PAOs) eat VFAs in anaerobic/fermentive conditions ... temporarily releasing more P into the water

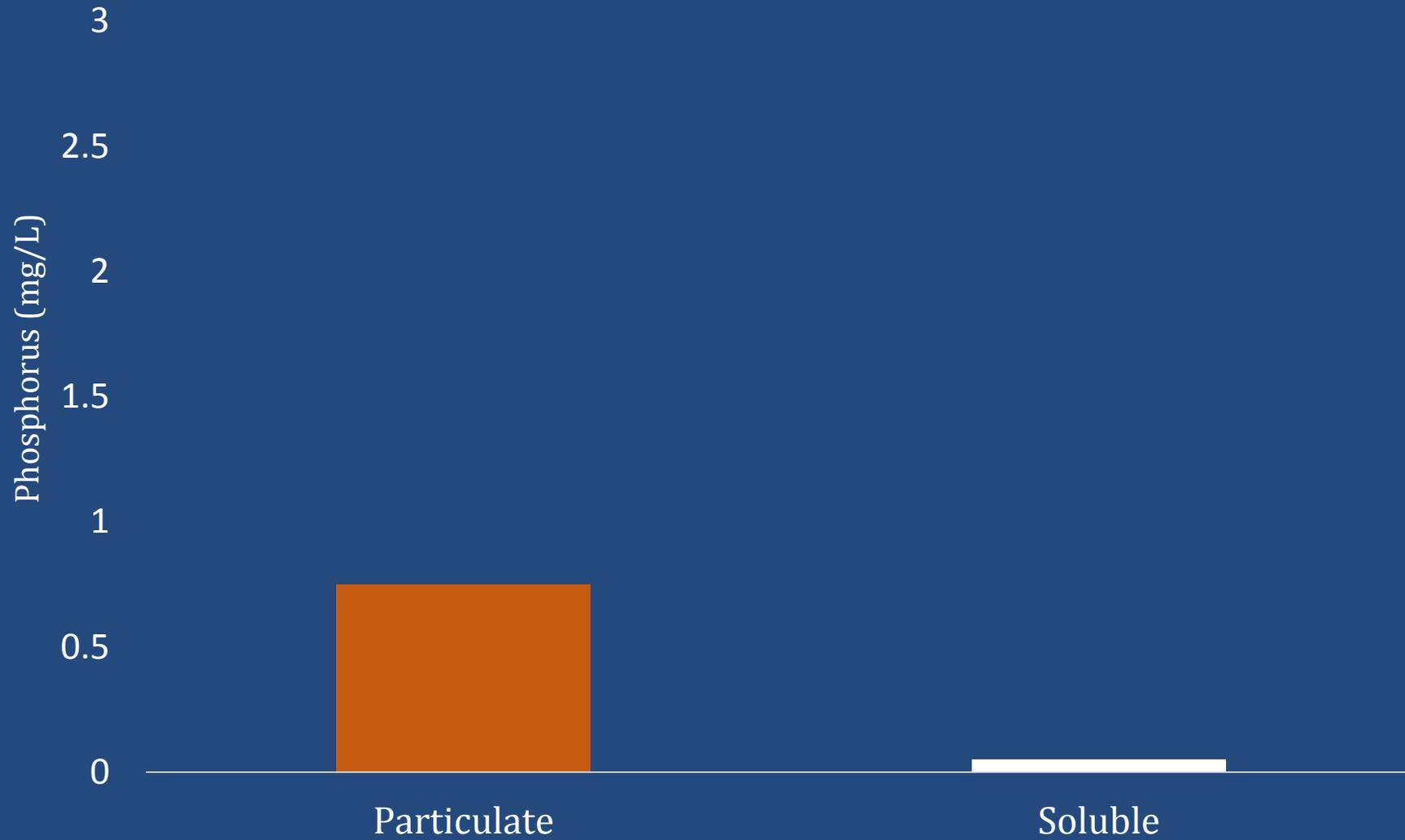
Step 3: breathe and grow

Bio-P bugs (PAOs) take in almost all of the soluble P in aerobic conditions as they grow and reproduce

Example: effluent phosphorus (mg/L)
Before Phosphorus Removal (Biological or Chemical)



Example: effluent phosphorus (mg/L)
After Phosphorus Removal (Biological or Chemical)



TSS Removal Requirements

Since all but 0.05 mg/L of the soluble Phosphorus can be converted to TSS Phosphorus (Biologically and/or Chemically)

And, because approximately 5% of Effluent TSS is Phosphorus

... To meet a total-P limit, the effluent TSS needs to be kept to the max TSS number shown in the table.

P Limit	max TSS
0.1	1
0.2	3
0.3	5
0.4	7
0.5	9
0.6	11
0.7	13
0.8	15
0.9	17
1.0	19
1.1	21
1.2	23
1.3	25
1.4	27
1.5	29

Phosphorus Removal without Facility Upgrades

	<u>t-P Before</u>	<u>t-P After</u>
Conrad, MT	2.1	0.2
Chinook, MT	2.8	0.3
Westfield, MA	1.0	0.5*
Palmer, MA	0.65	0.65*
Cookeville, TN	3	0.8
Montague, MA	3	0.9
Athens, TN	3	1.8*

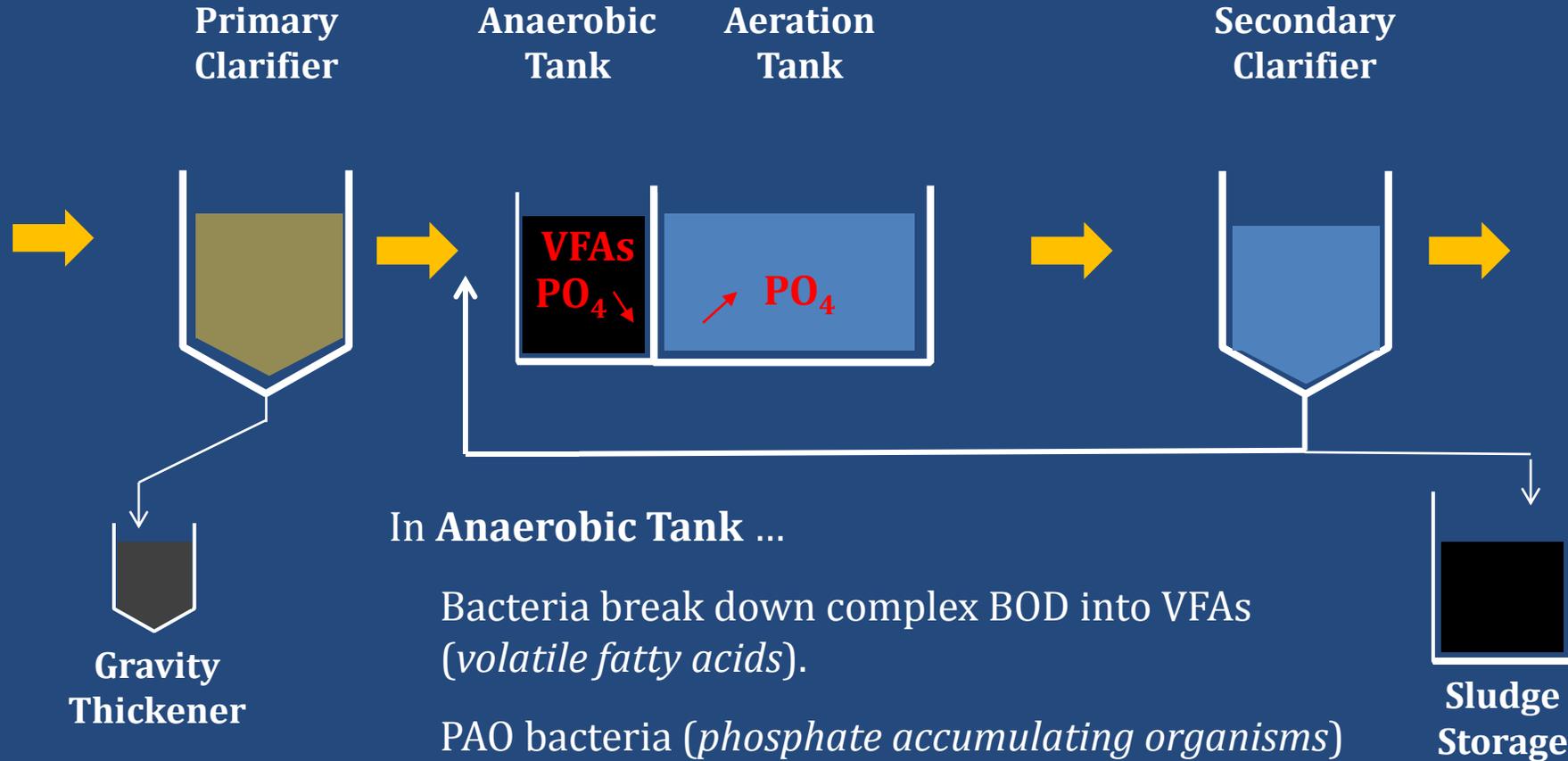
*chemical reduction of 50% or more



*Biological Phosphorus Removal:
Mainstream Flow Fermentation Processes*



Bio-P Removal: Mainstream Fermentation Process



In Anaerobic Tank ...

Bacteria break down complex BOD into VFAs (*volatile fatty acids*).

PAO bacteria (*phosphate accumulating organisms*) take in VFAs as energy source & temporarily release PO₄ (*phosphate*) into solution.

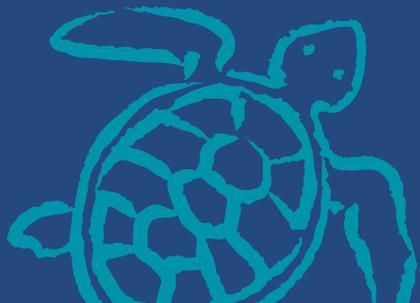
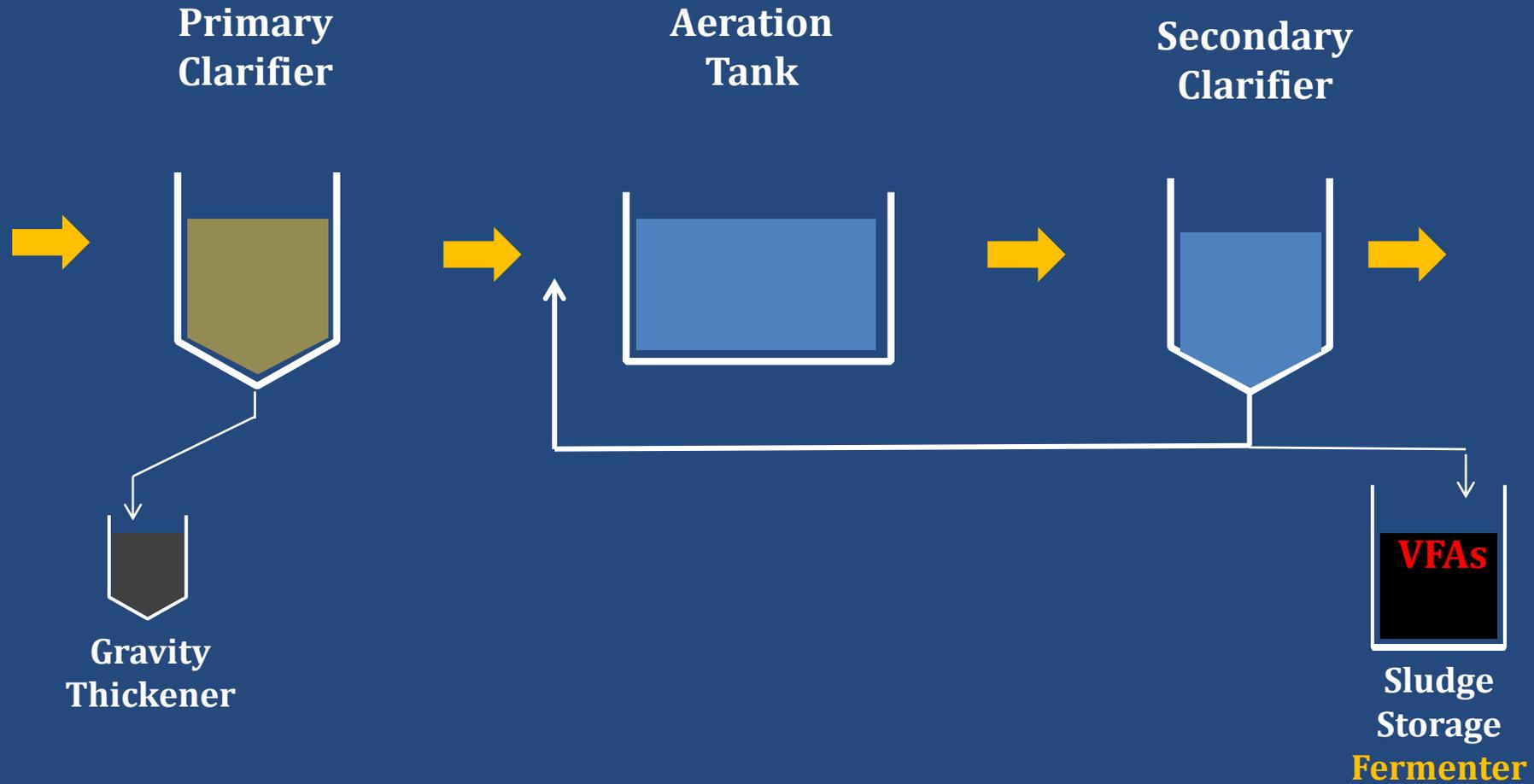
In Aeration Tank ...

Energized PAO bacteria take PO₄ out of solution.

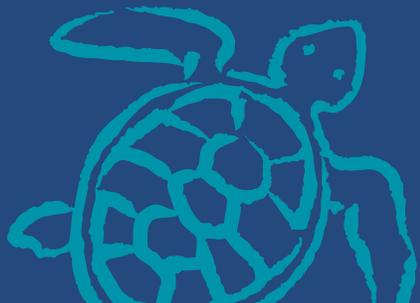
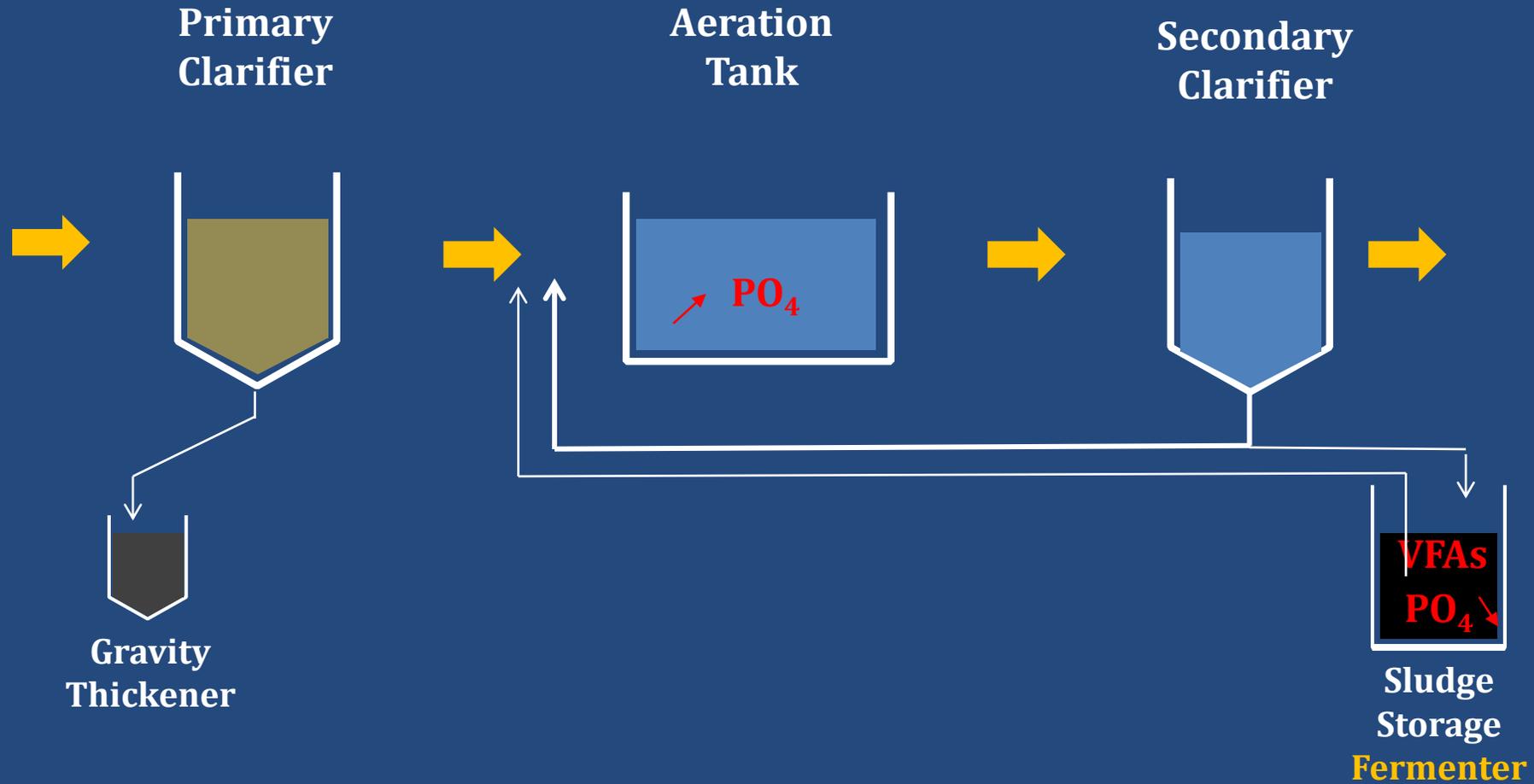
*Biological Phosphorus Removal:
Sidestream Flow Fermentation Processes*



Sidestream Biological-P Removal: Sludge Storage



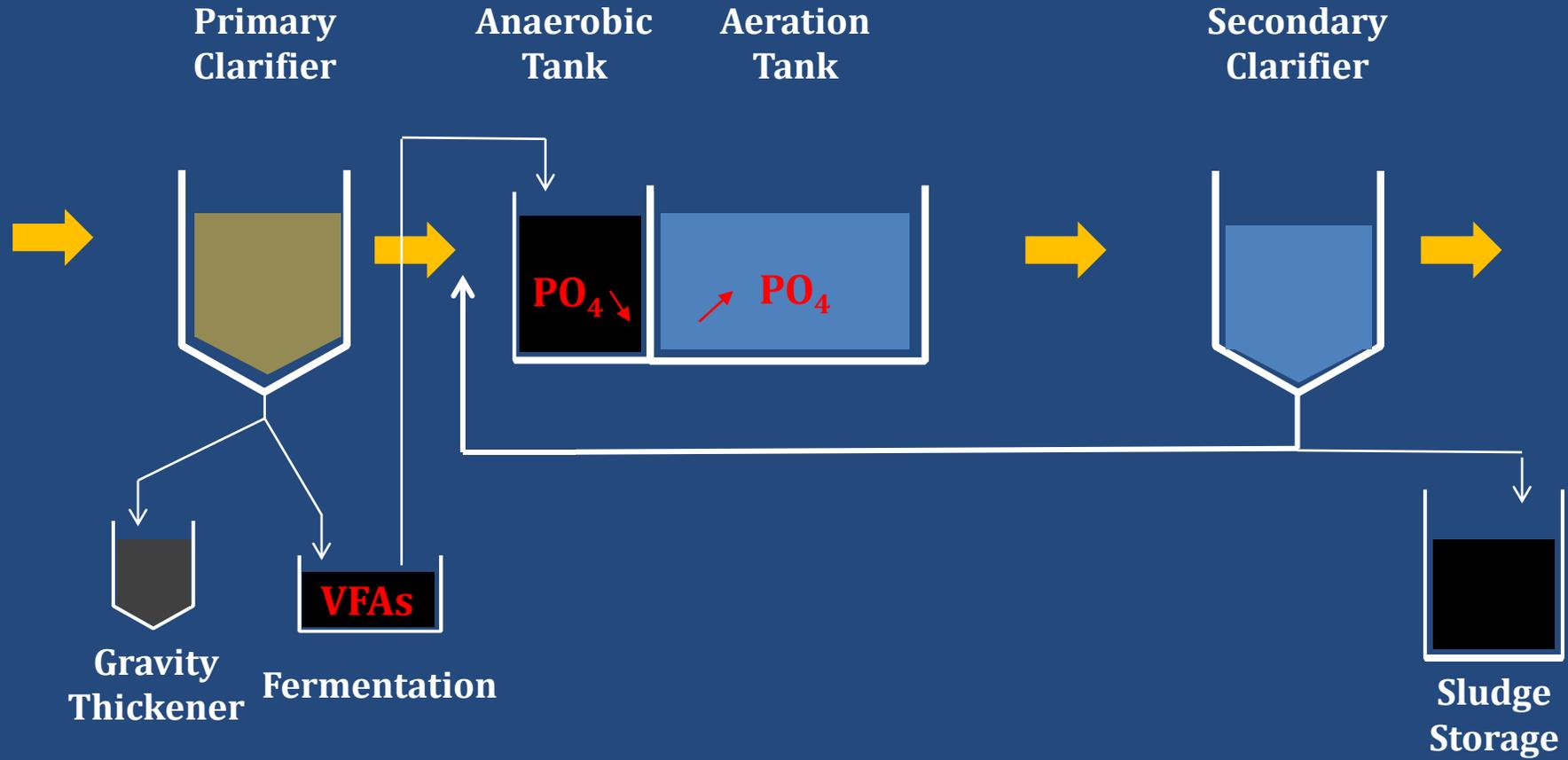
Sidestream Biological-P Removal: Sludge Storage



*Biological Phosphorus Removal: Combined
Sidestream & Mainstream Fermentation*



Bio-P Removal: Sidestream & Mainstream Fermentation



Optimizing Bio-P Removal: Mainstream, Sidestream or Combination Fermentation

Anaerobic Tank

~1 hour HRT*

ORP of -200 mV*

25 times as much BOD as influent ortho-P*

Ortho-P release (3-4 times influent ortho-P)*

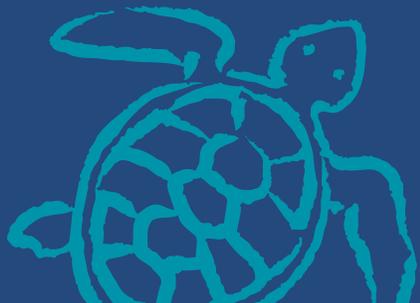
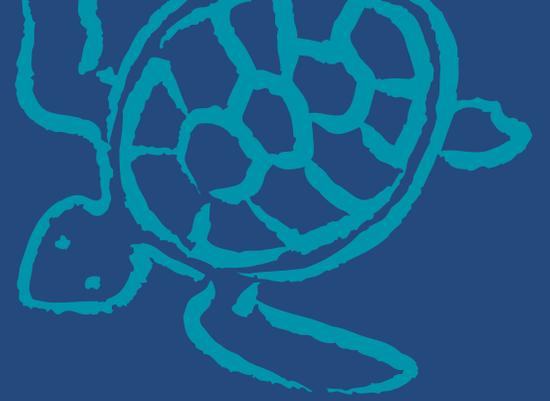
Aeration Tank

High DO / High ORP

pH of 6.8+*

Ortho-P concentration of 0.05 mg/L*

*Approximate: Every Plant is Different



Ammonia Removal

Ammonia (NH₄) is converted to Nitrate (NO₃)

Ammonia
(NH₄)

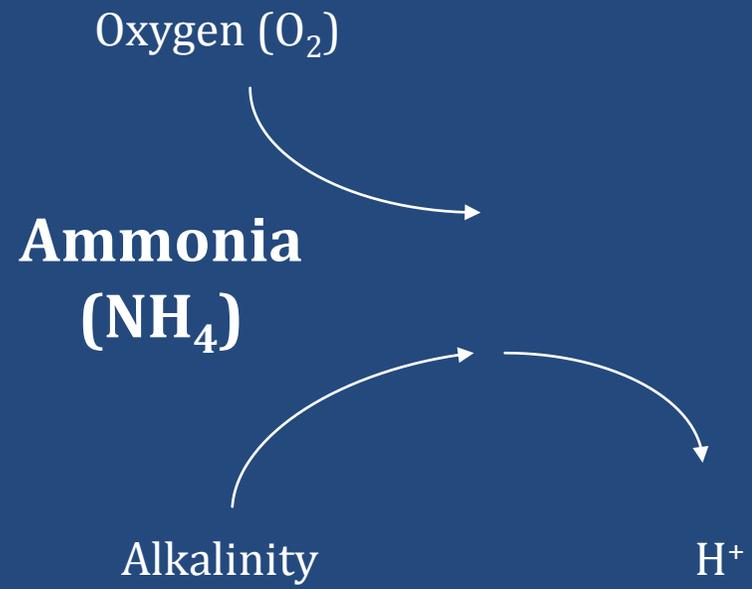
Ammonia Removal

Oxygen (O_2)

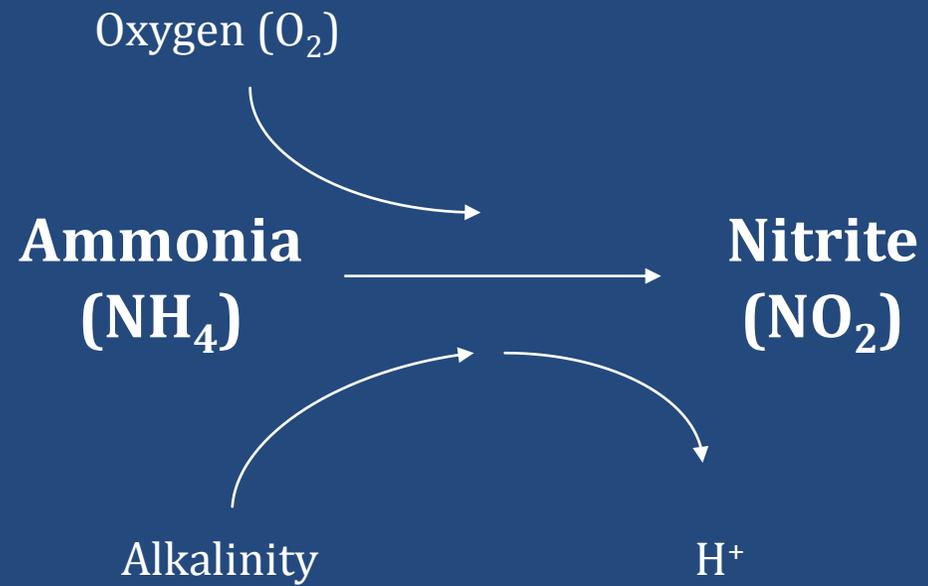


Ammonia
(NH_4)

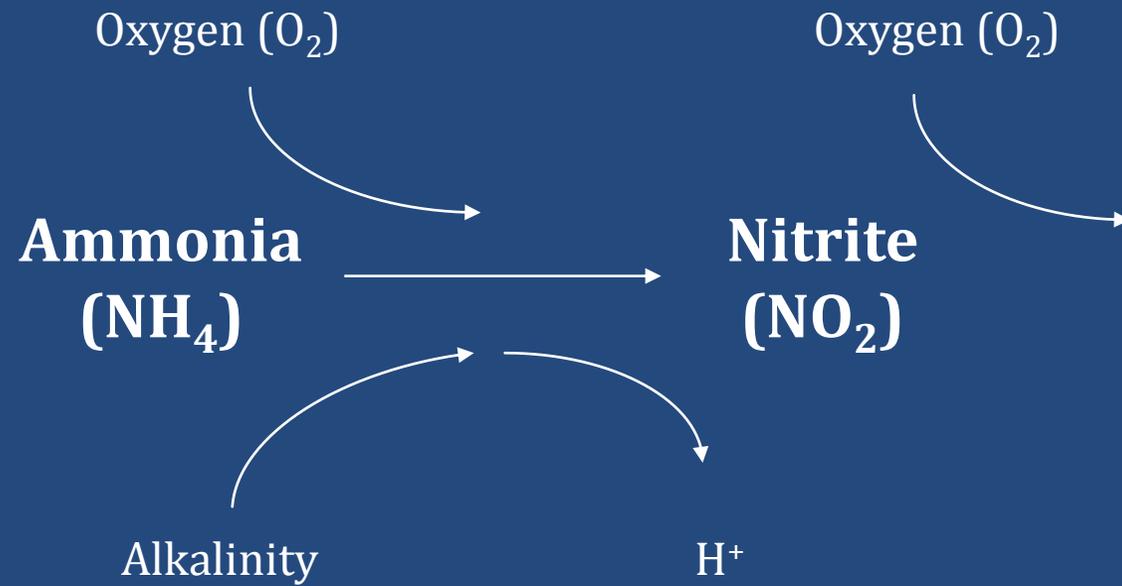
Ammonia Removal



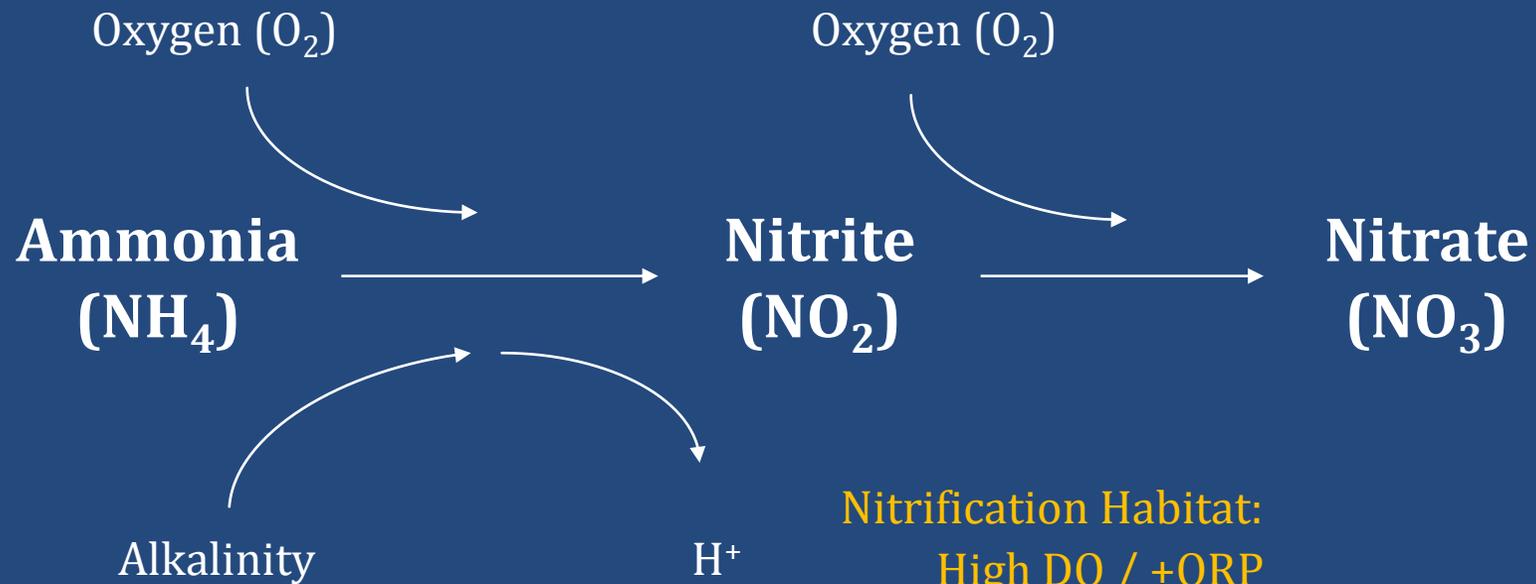
Ammonia Removal



Ammonia Removal



Ammonia Removal



Nitrification Habitat:

- High DO / +ORP
- Low BOD
- High MLSS/MCRT
- High HRT

Consumes oxygen

Consumes alkalinity: lowers pH

Nitrification:

Ammonia (NH₄) is converted to Nitrate (NO₃)

Oxygen Rich Habitat

MLSS* of 2500+ mg/L (High Sludge Age / MCRT / low F:M)

ORP* of +100 to +150 mV (High DO)

Time* (high HRT ... 24 hr, 12 hr, 6 hr)

Low BOD

Consumes Oxygen

Adds acid - Consumes 7 mg/L alkalinity per mg/L of NH₄ → NO₃

*Approximate, each facility is different.

Biological Nitrogen Removal:

Next,

*The Nitrate (NO_3) created during Nitrification ...
is converted to Nitrogen Gas (N_2)*



Nitrate Removal

**Nitrate
(NO₃)**

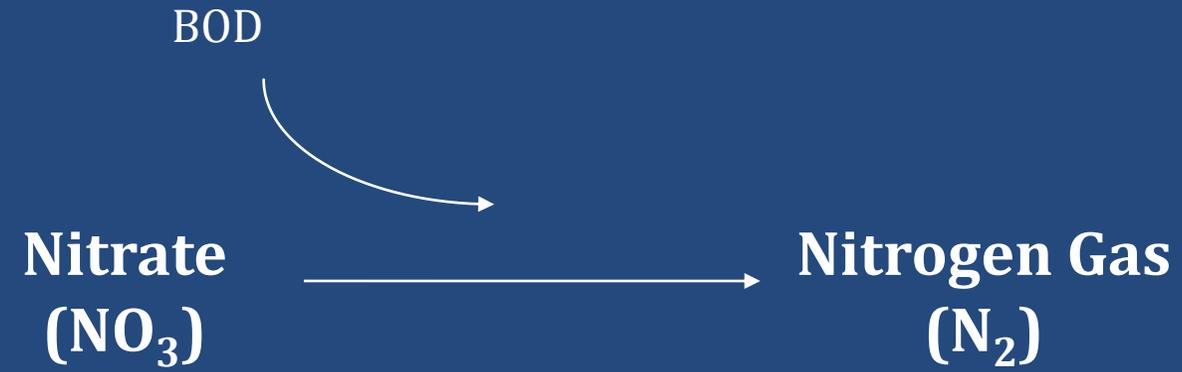
Nitrate Removal

BOD

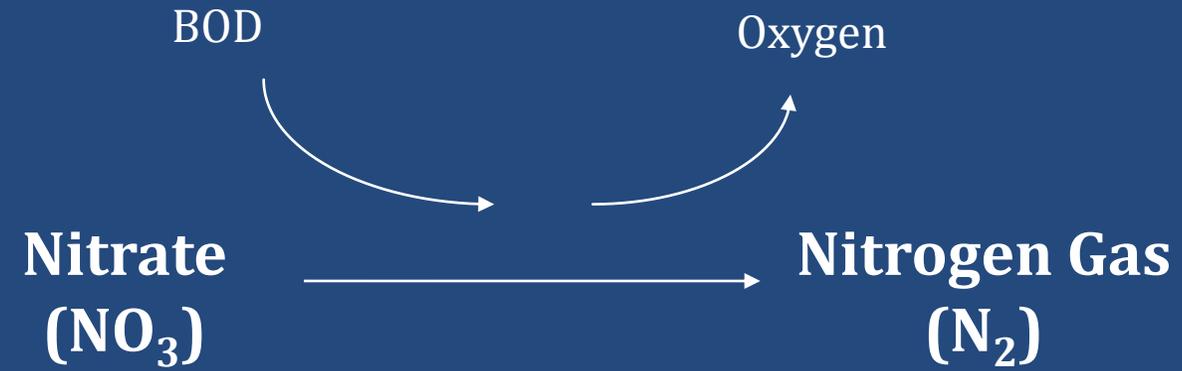


Nitrate
(NO₃)

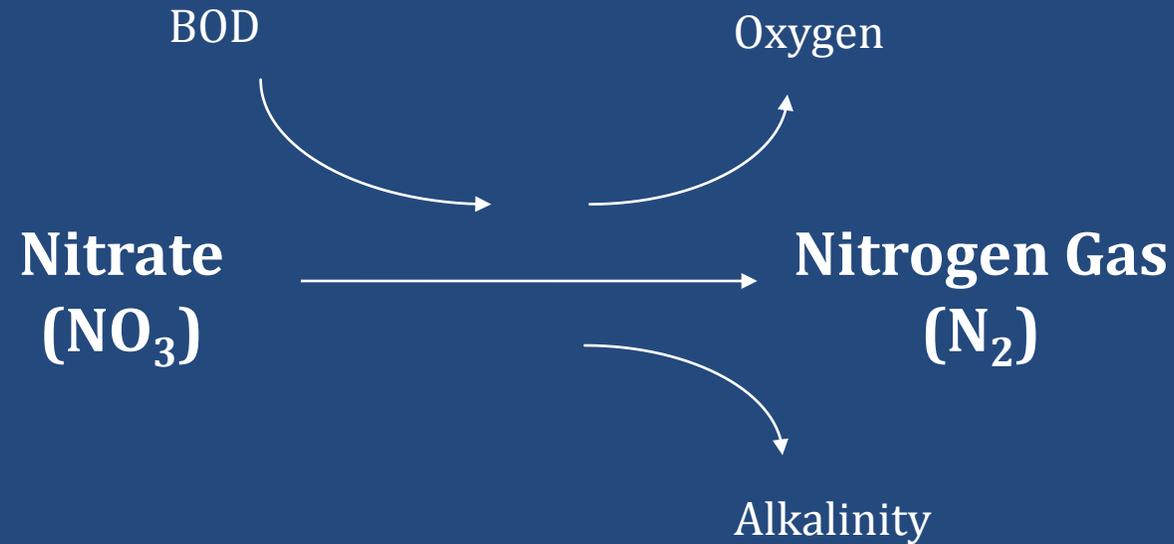
Nitrate Removal



Nitrate Removal



Nitrate Removal



Denitrification Habitat:

Low DO / -ORP
High BOD

Adds DO

Gives back ½ the alkalinity: beneficially raises pH

Denitrification:

Nitrate (NO_3) is converted to Nitrogen Gas (N_2)

Oxygen Poor Habitat

ORP* of -100 mV or less (DO < 0.3 mg/L)

Surplus BOD* (100-250 mg/L: 5-10 times as much as NO_3)

Retention Time* of 45-90 minutes

Gives back Oxygen

Gives back Alkalinity (3.5 mg/L per mg/L of $\text{NO}_3 \rightarrow \text{N}_2$)

*Approximate, each facility is different.



Nitrogen Removal

	1. Nitrification Ammonia Removal $\text{NH}_4 \rightarrow \text{NO}_3$	2. Denitrification Nitrate Removal $\text{NO}_3 \rightarrow \text{N}_2$
DO: Dissolved Oxygen	>1 mg/L	<0.3 mg/L
ORP: Oxygen Reduction Potential	>+100 mV	<-100 mV
MLSS	>2500 mg/L	>2500 mg/L
HRT (Hydraulic Retention Time)	>6 hr	~1 hr
BOD: Biochemical Oxygen Demand	<20 mg/L	>100 mg/L
Alkalinity	>60 mg/L	NA
	Alkalinity is lost	Alkalinity is gained

Notes:

> means "greater than"

< means "less than"

~ means "approximately"

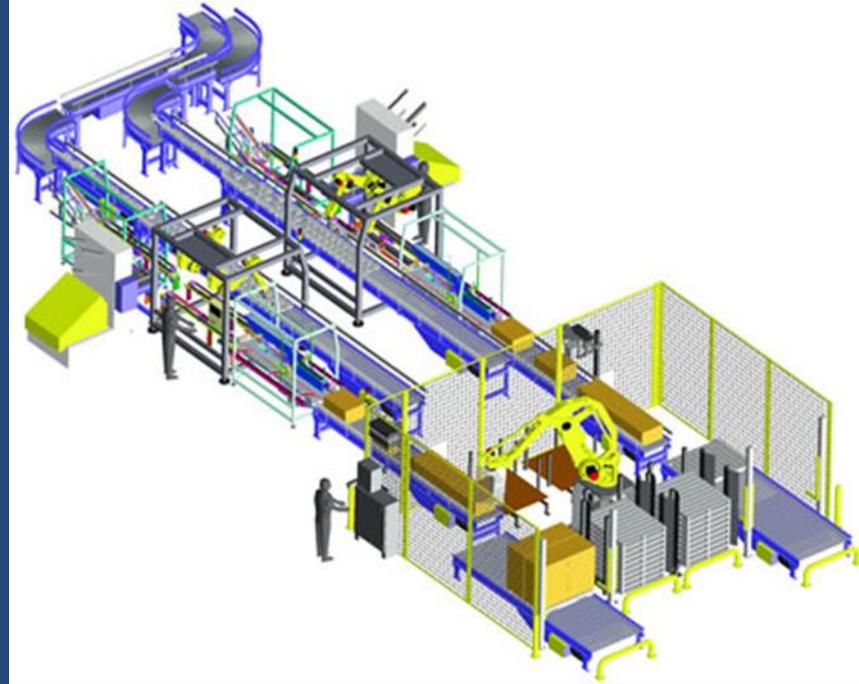
All numbers are "rules of thumb"

Nitrogen Removal without Facility Upgrades



	<u>t-N Before</u>	<u>t-N After</u>
Suffield, CT	7	2
Chinook, MT	26	3
Hardin, MT	18	4
Conrad, MT	35	5
Montague, MA	30	5
Cookeville, TN	25	5
Upton, MA	22	6
Plainfield, CT	25	10
Colchester-East Hampton, CT	24	12
Big Sky, MT	25	14
Libby, MT	32	21

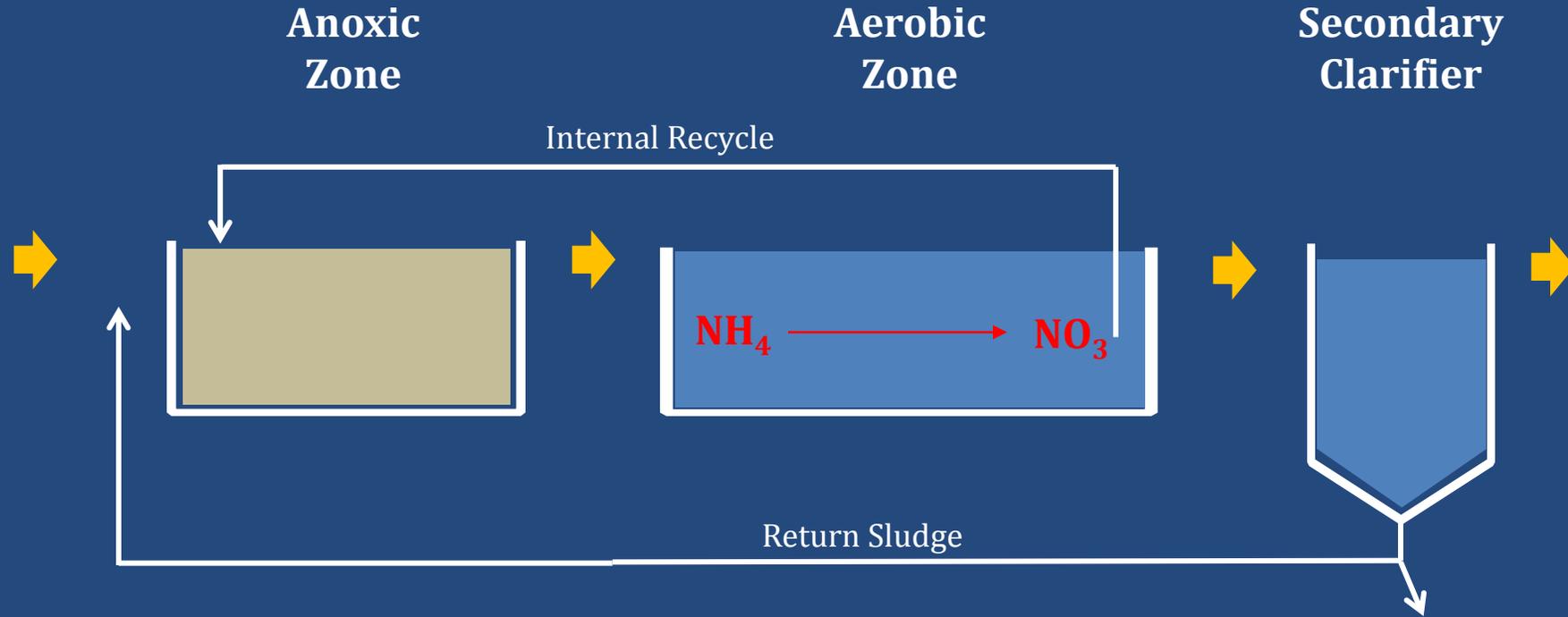
Technology!



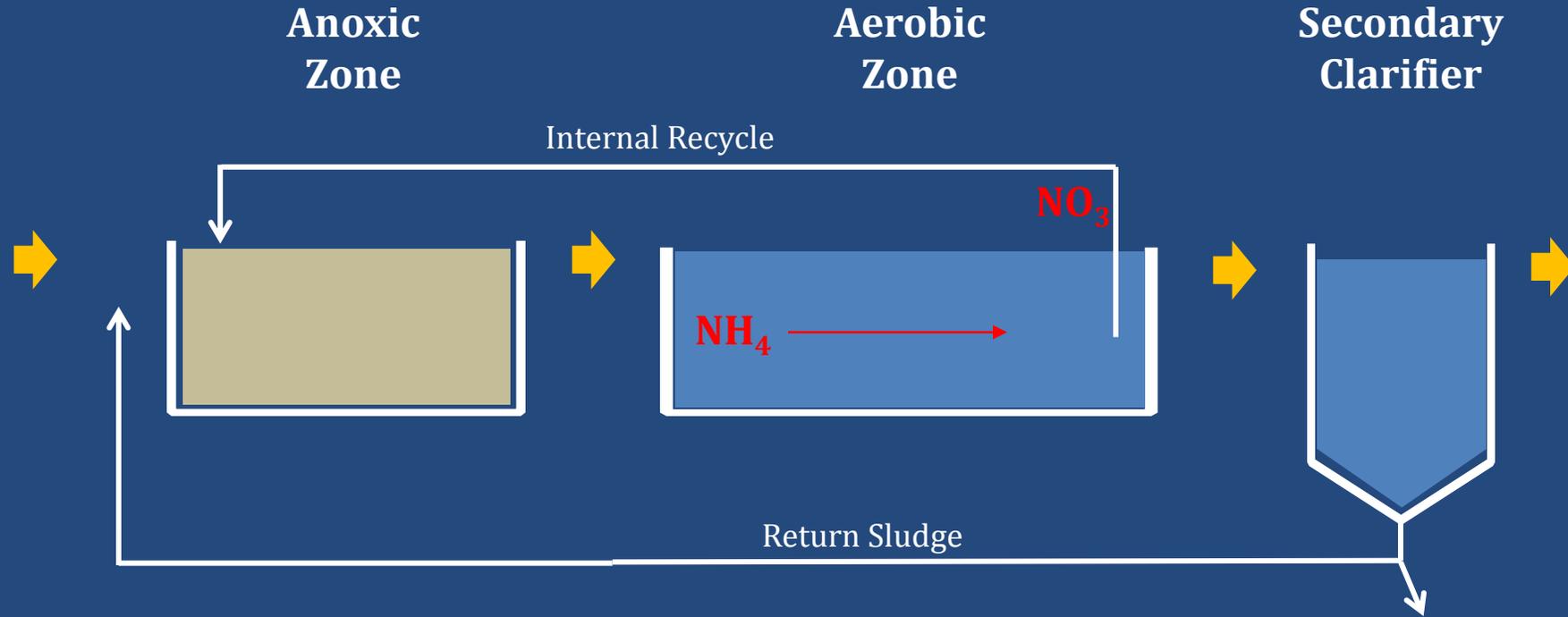
MLE (Modified Ludzack-Ettinger) Process



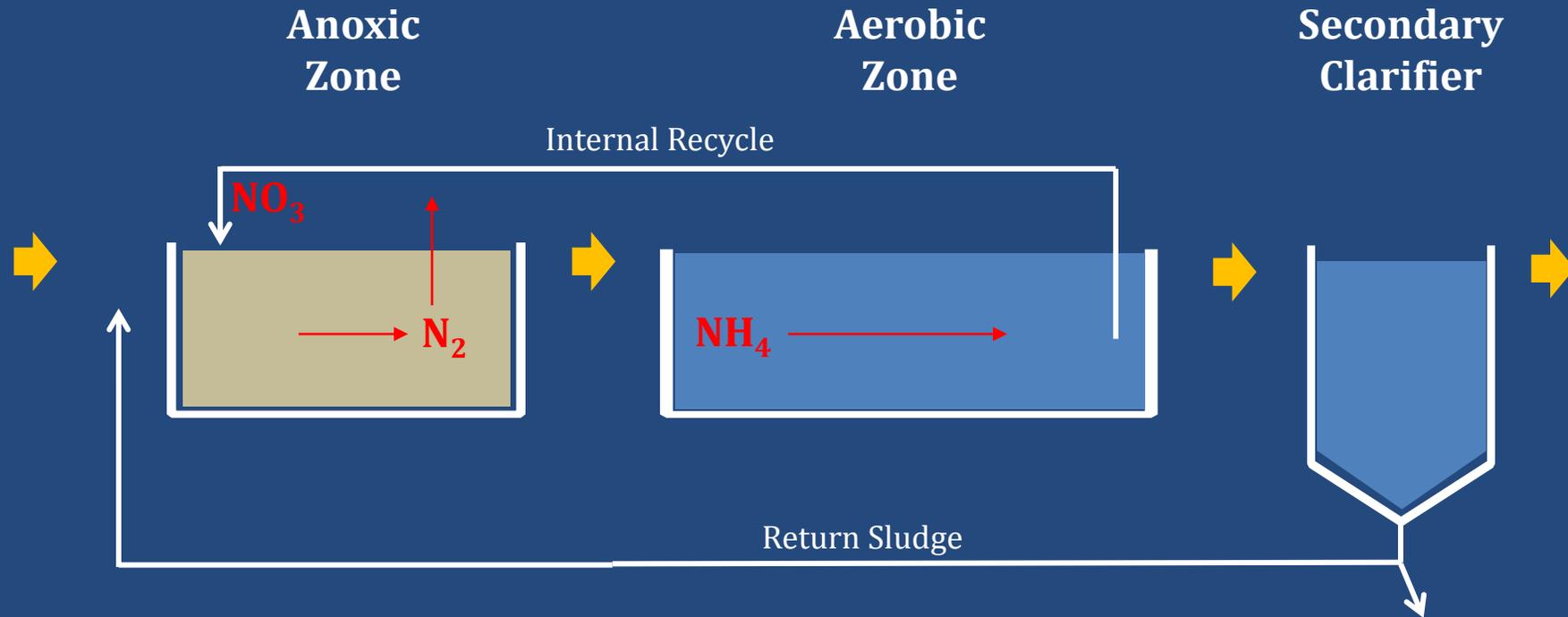
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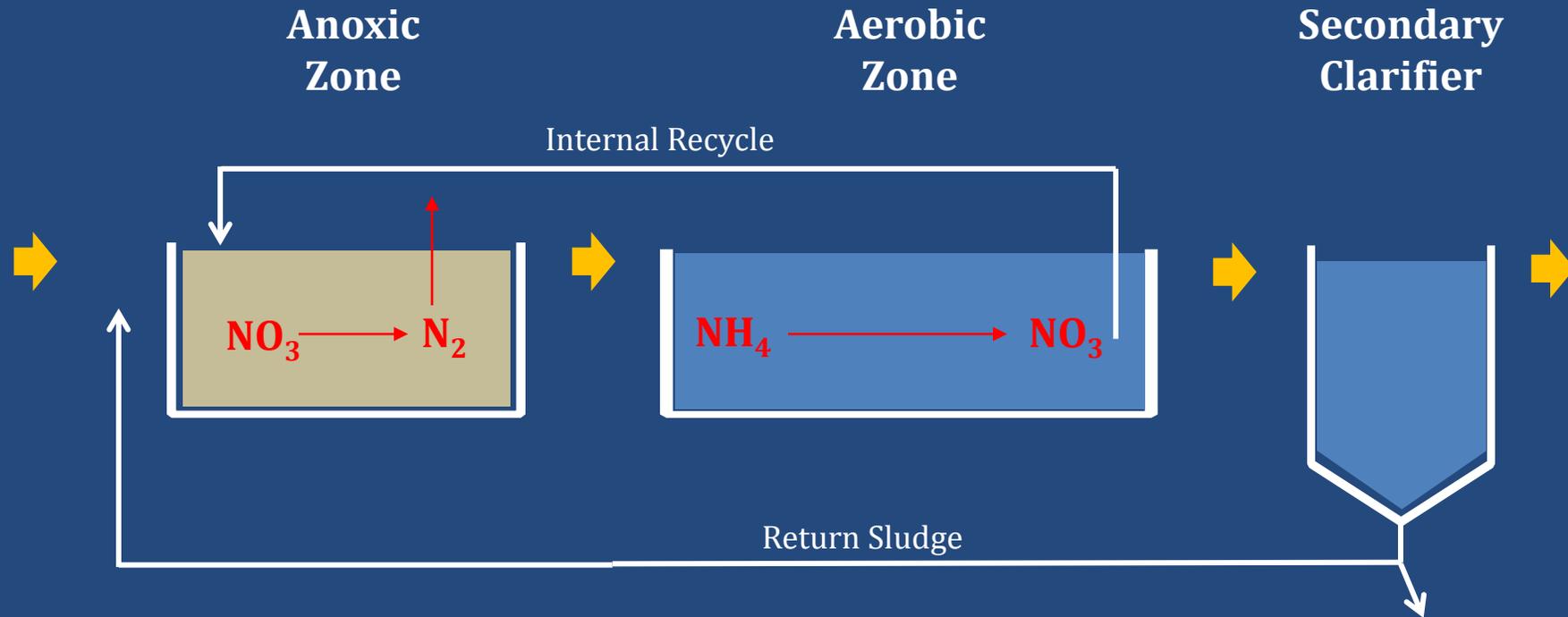
Ammonia (NH_4) Removal

Target: $\text{NH}_4 < 0.5 \text{ mg/L}$

Nitrate (NO_3) Removal

Target NO_3 in Anoxic Tank: 0.5-2 mg/L

MLE (Modified Ludzack-Ettinger) Process



MLE Process Control:

Proper Internal Recycle Rate; not too much / not too little.

ORP of +100 mV in Aerobic Zone for Ammonia (NH_4) Removal.

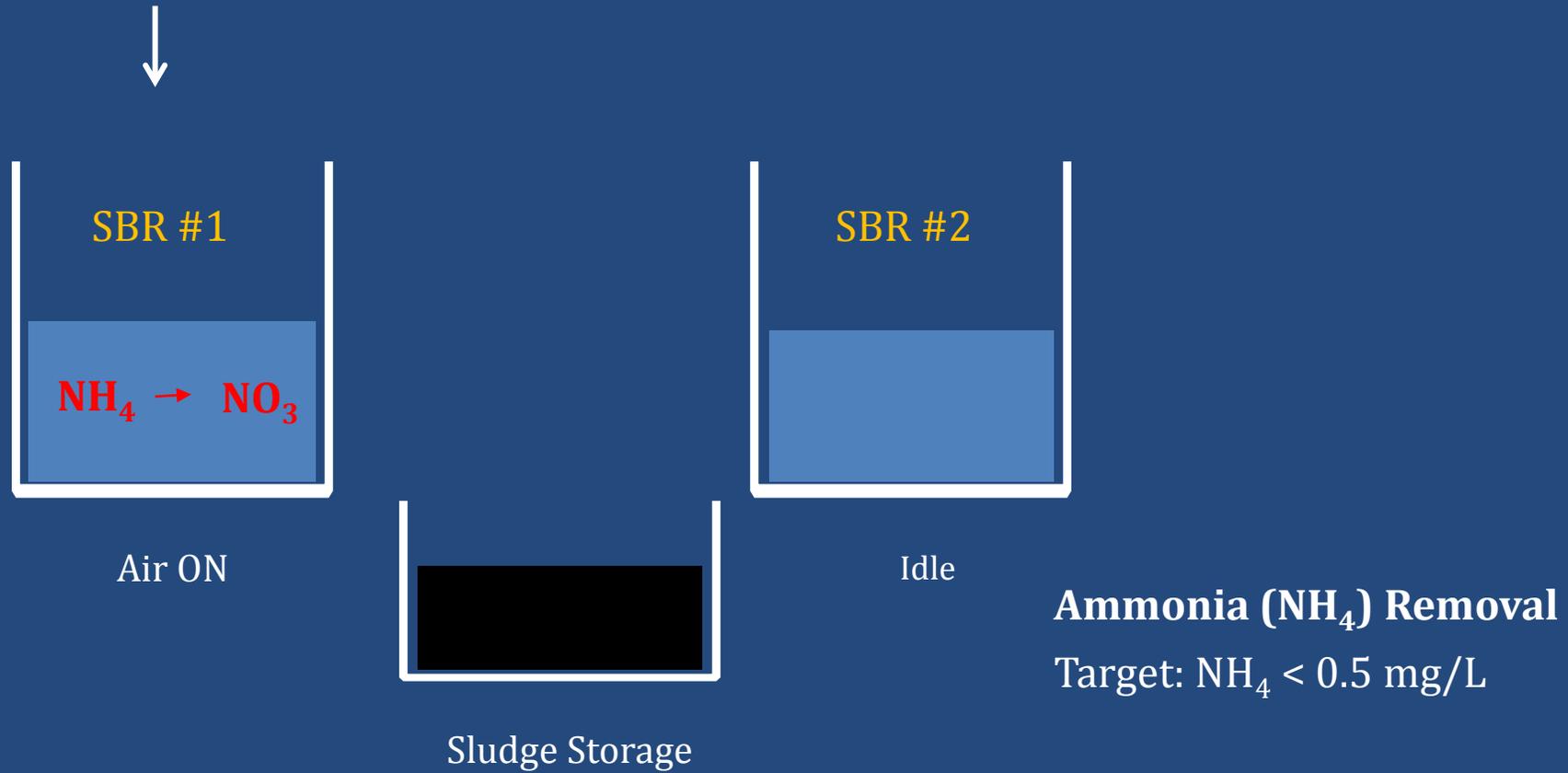
ORP of -75 to -150 mV in Anoxic Zone for Nitrate (NO_3) Removal.

Enough BOD to support Nitrate (NO_3) Removal.

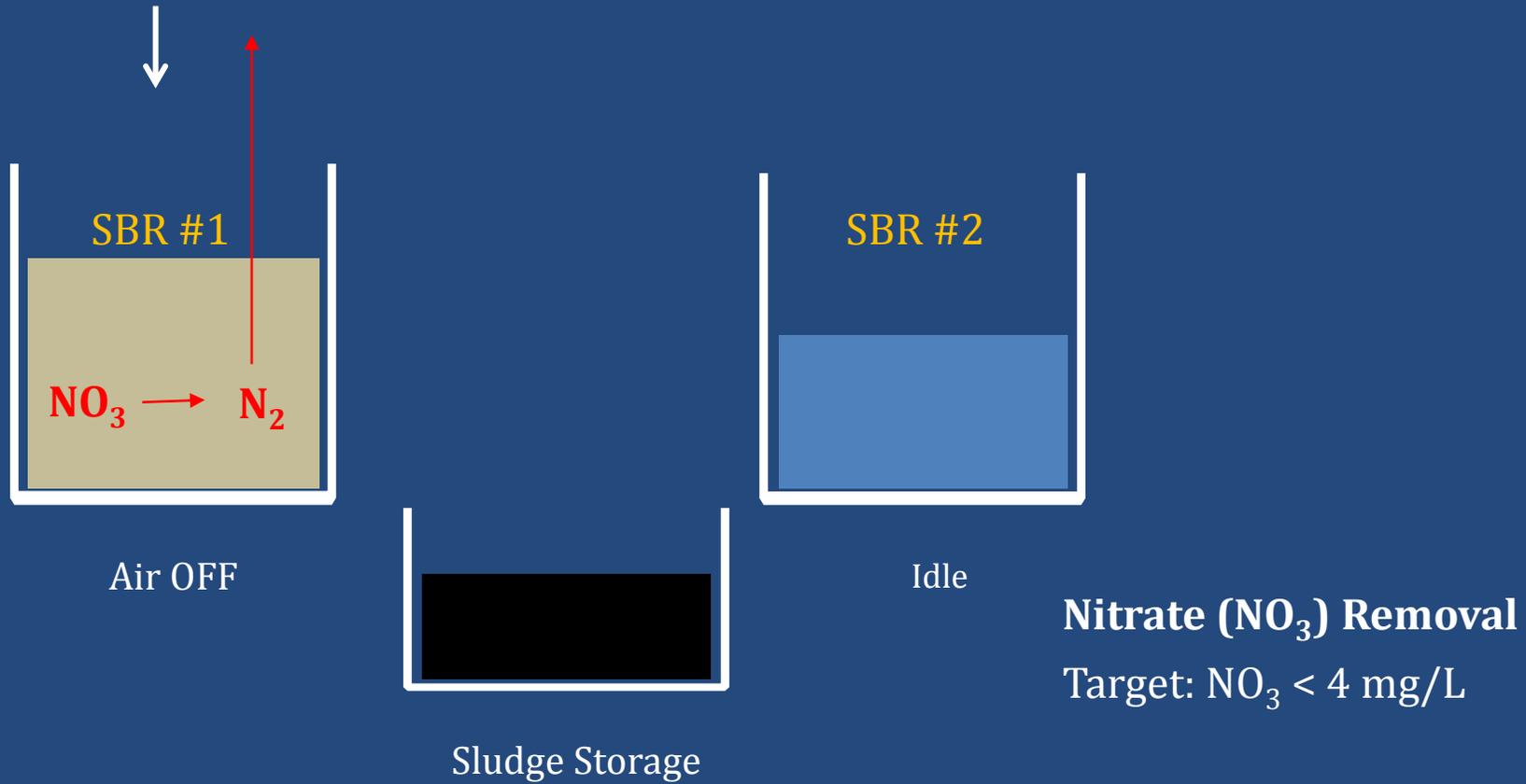
Sequencing Batch Reactor
- *SBR*



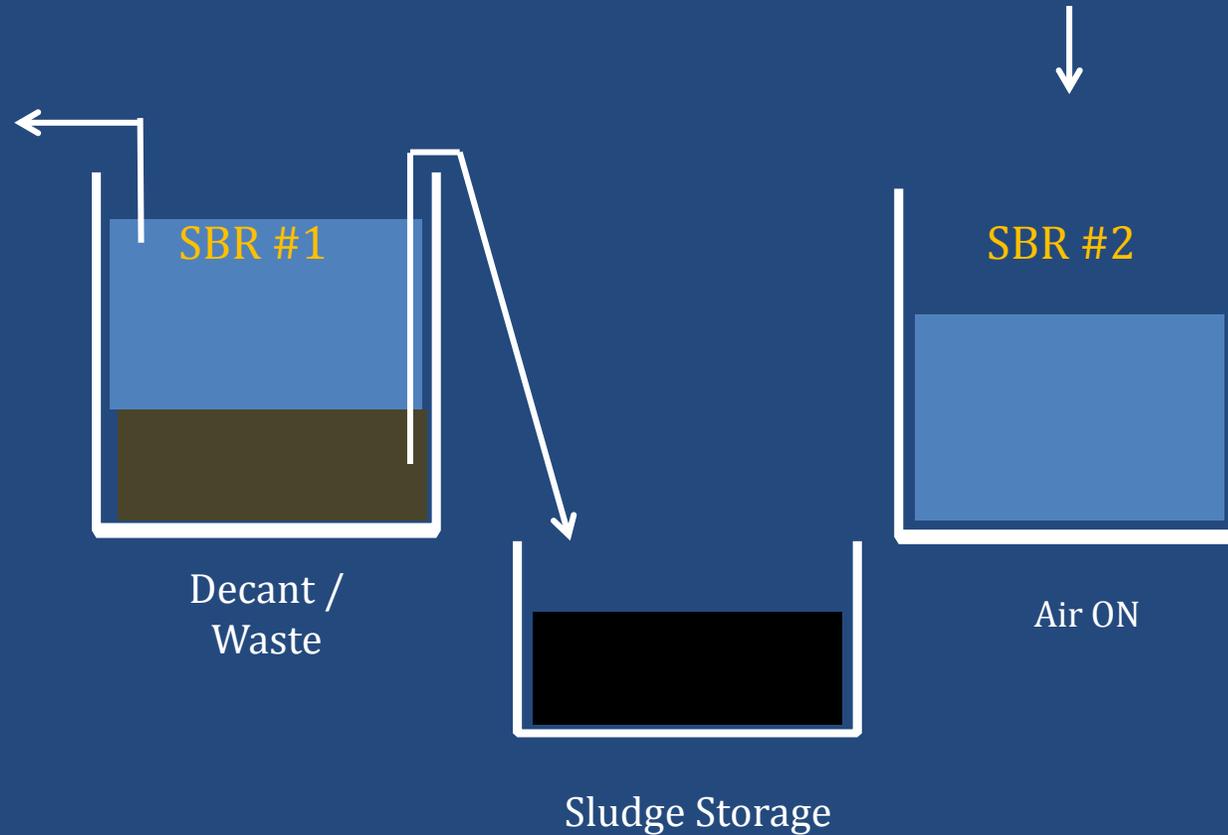
Sequencing Batch Reactor (SBR) Ammonia (NH_4) Removal: Nitrification



Sequencing Batch Reactor (SBR) Nitrate (NO_3) Removal: Denitrification



Sequencing Batch Reactor (SBR) Settle, Decant & Waste Sludge



SBR Process Control:

Establish cycle times that are long enough to provide optimal habitats.

And, short enough to allow all of the flow to be nitrified and denitrified.

Optimizing SBR cycle time

Too short

Will not reach +100 mV for Ammonia (NH_4) Removal.

Will not reach -100 mV for Nitrate (NO_3) Removal.

Note: Temperature and BOD affect Air OFF cycle.

Too long

Wastewater will pass through tank before all Ammonia (NH_4) converted to Nitrate (NO_3).

And, before all Nitrate (NO_3) is converted to Nitrogen Gas (N_2).

Just right

Good habitats ...

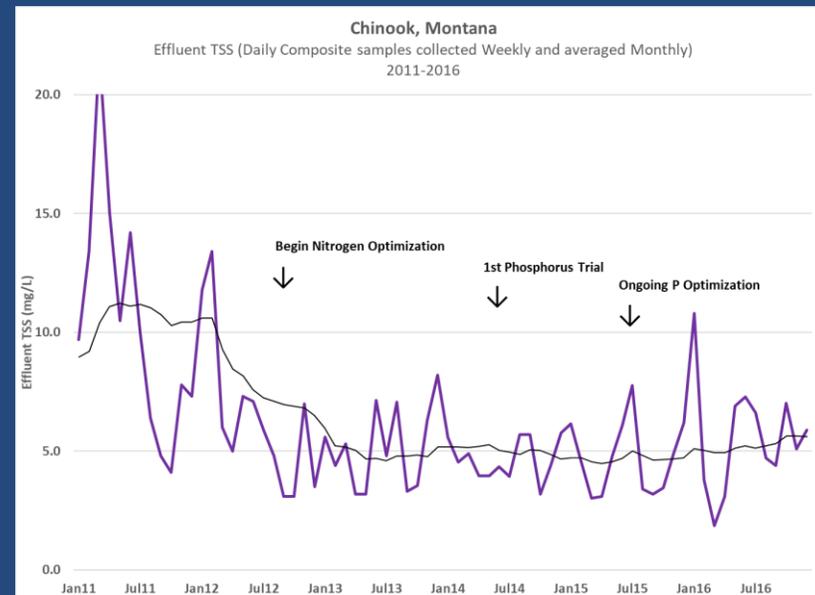
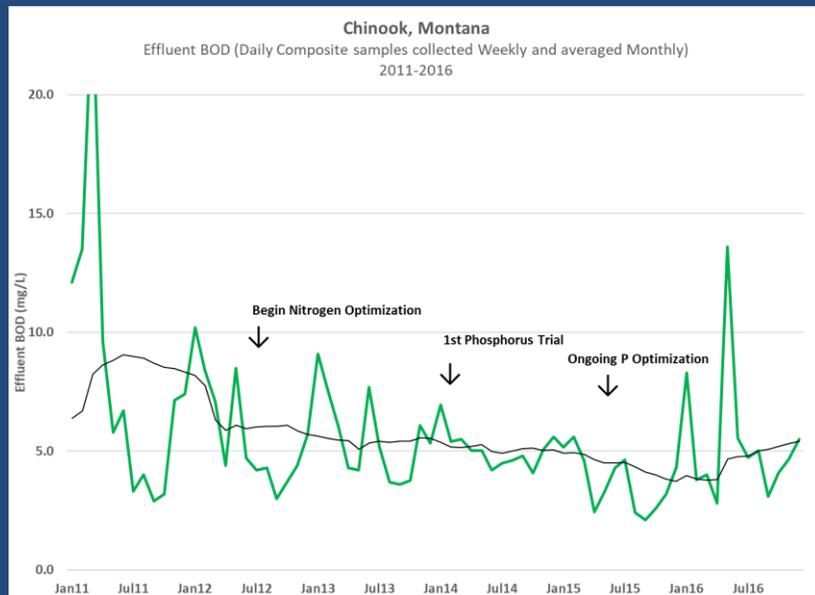
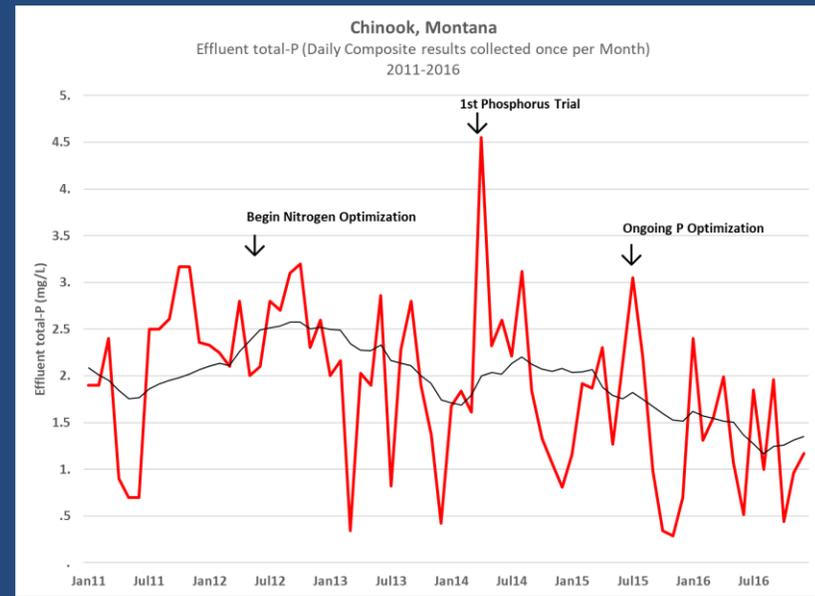
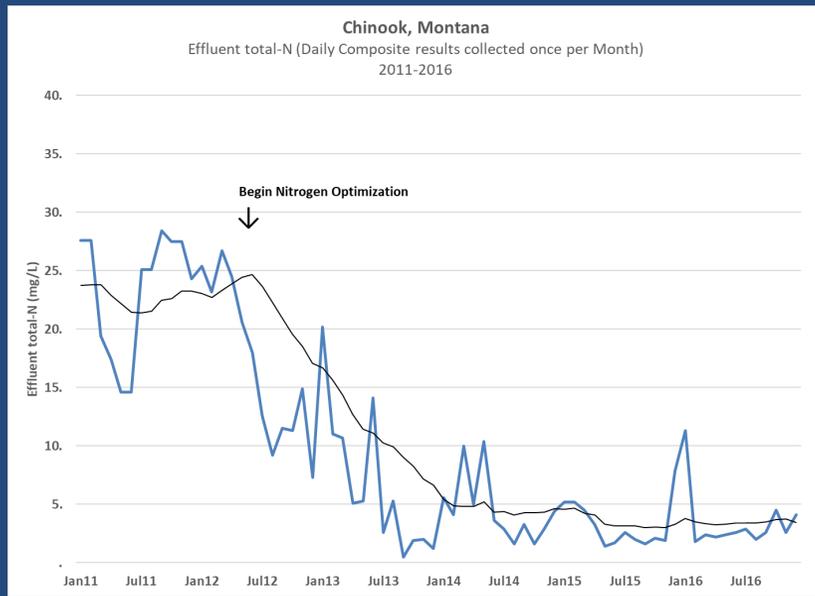
ORP of +100 mV for 60 minutes

And, ORP of -100 mV for 30 minutes.

Bonus: Changing conditions will serve as a selector.

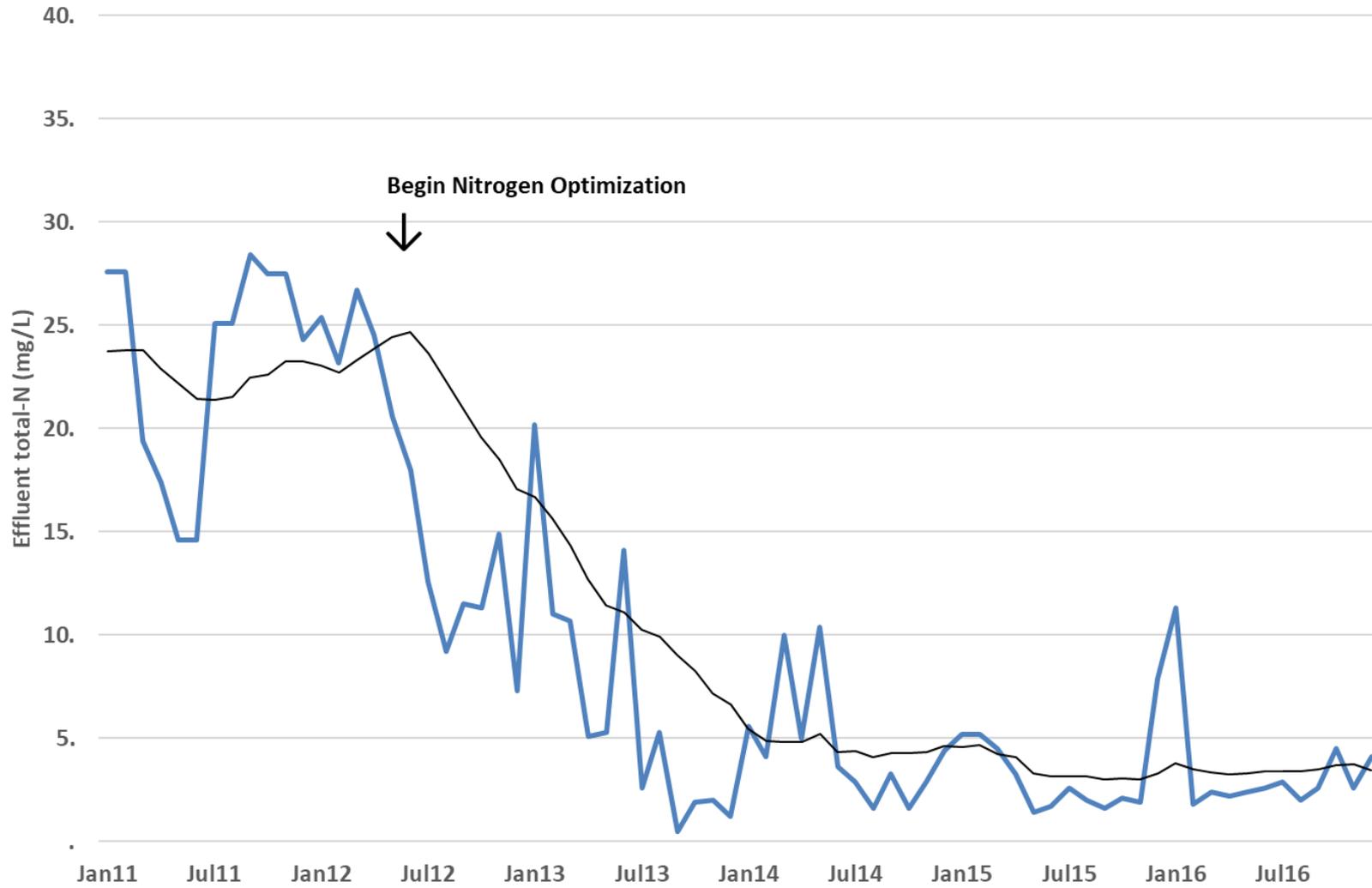
Chinook, Montana



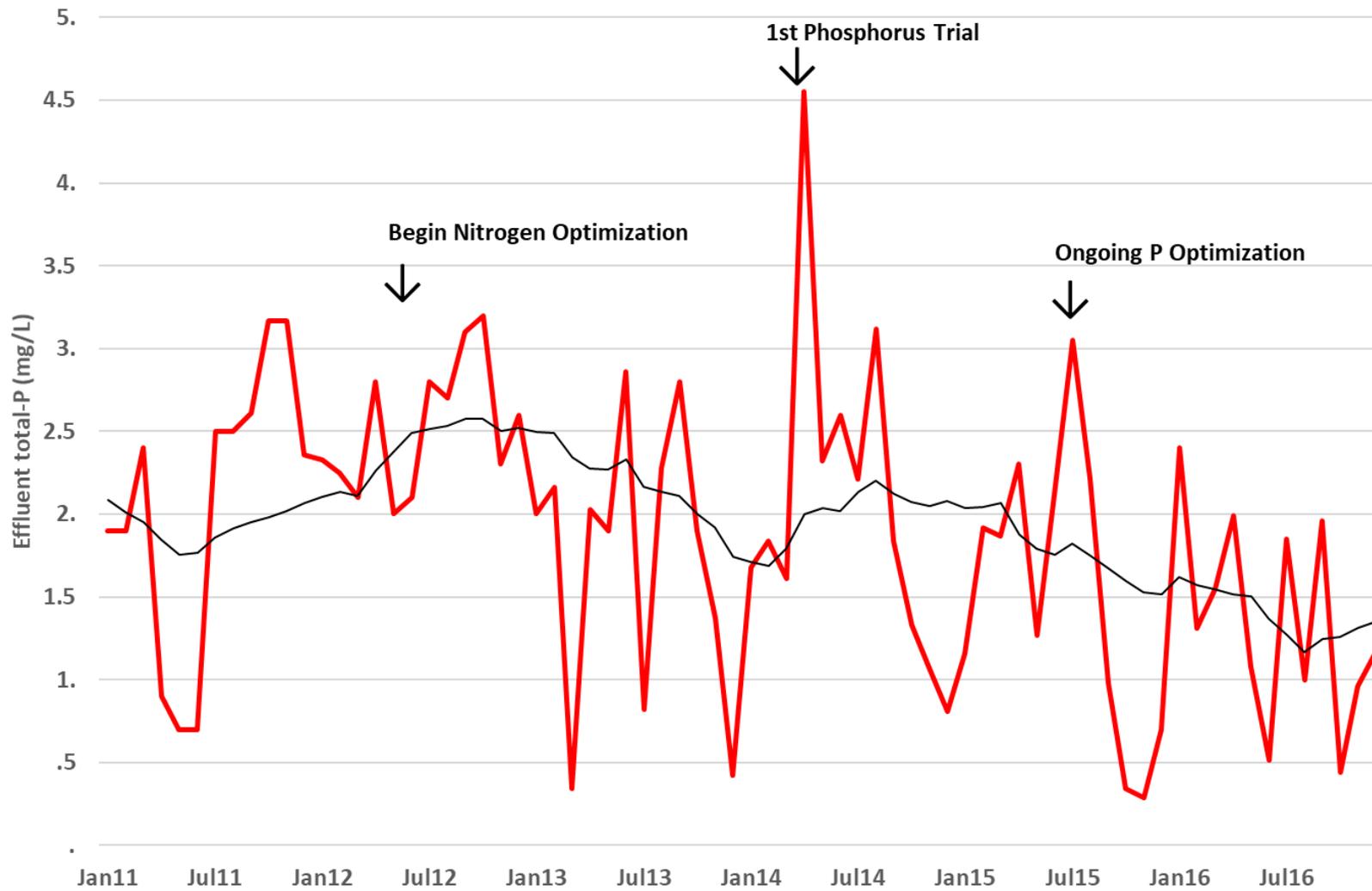


Chinook, Montana

Effluent total-N (Daily Composite results collected once per Month)
2011-2016

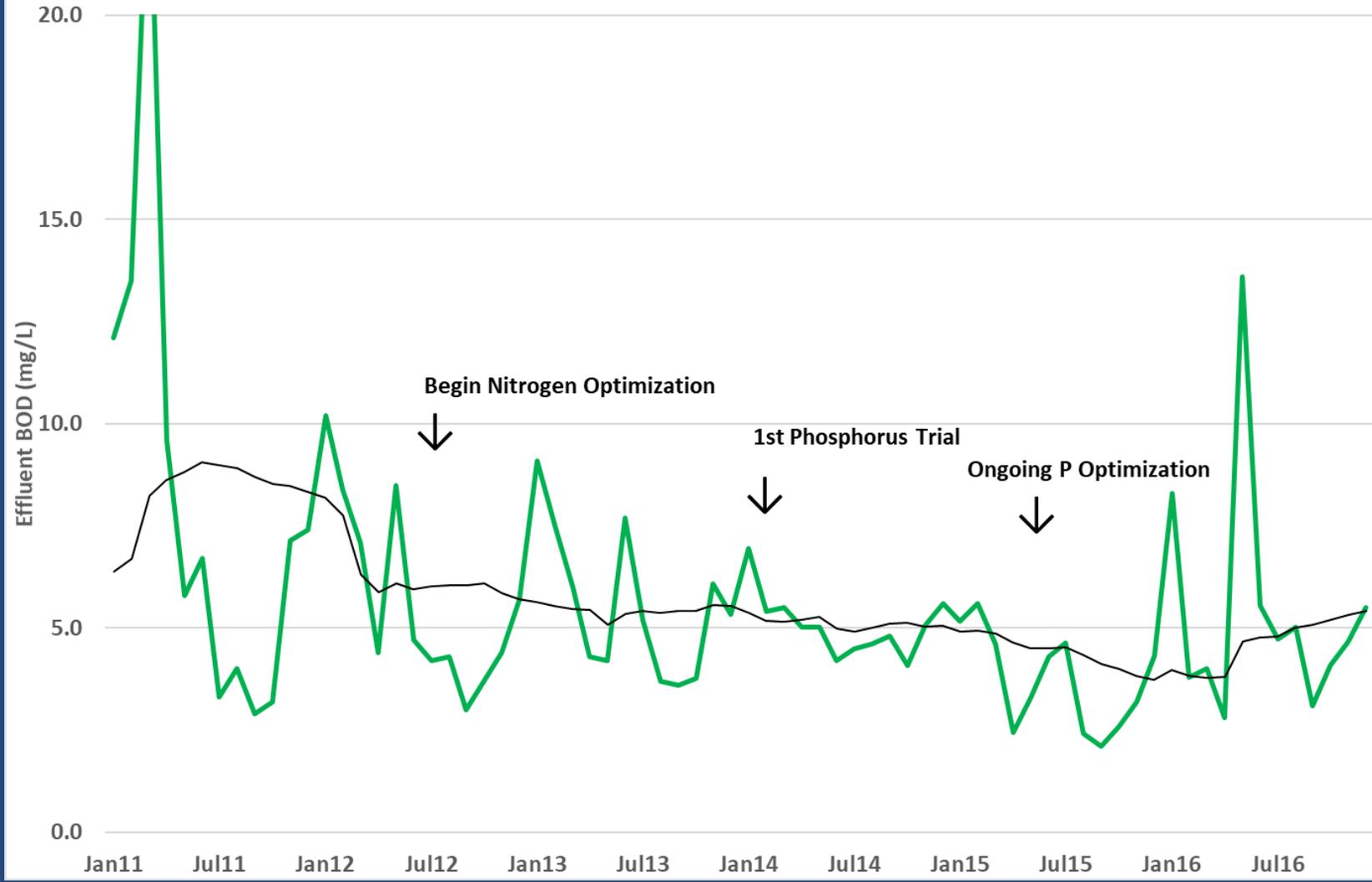


Chinook, Montana
Effluent total-P (Daily Composite results collected once per Month)
2011-2016



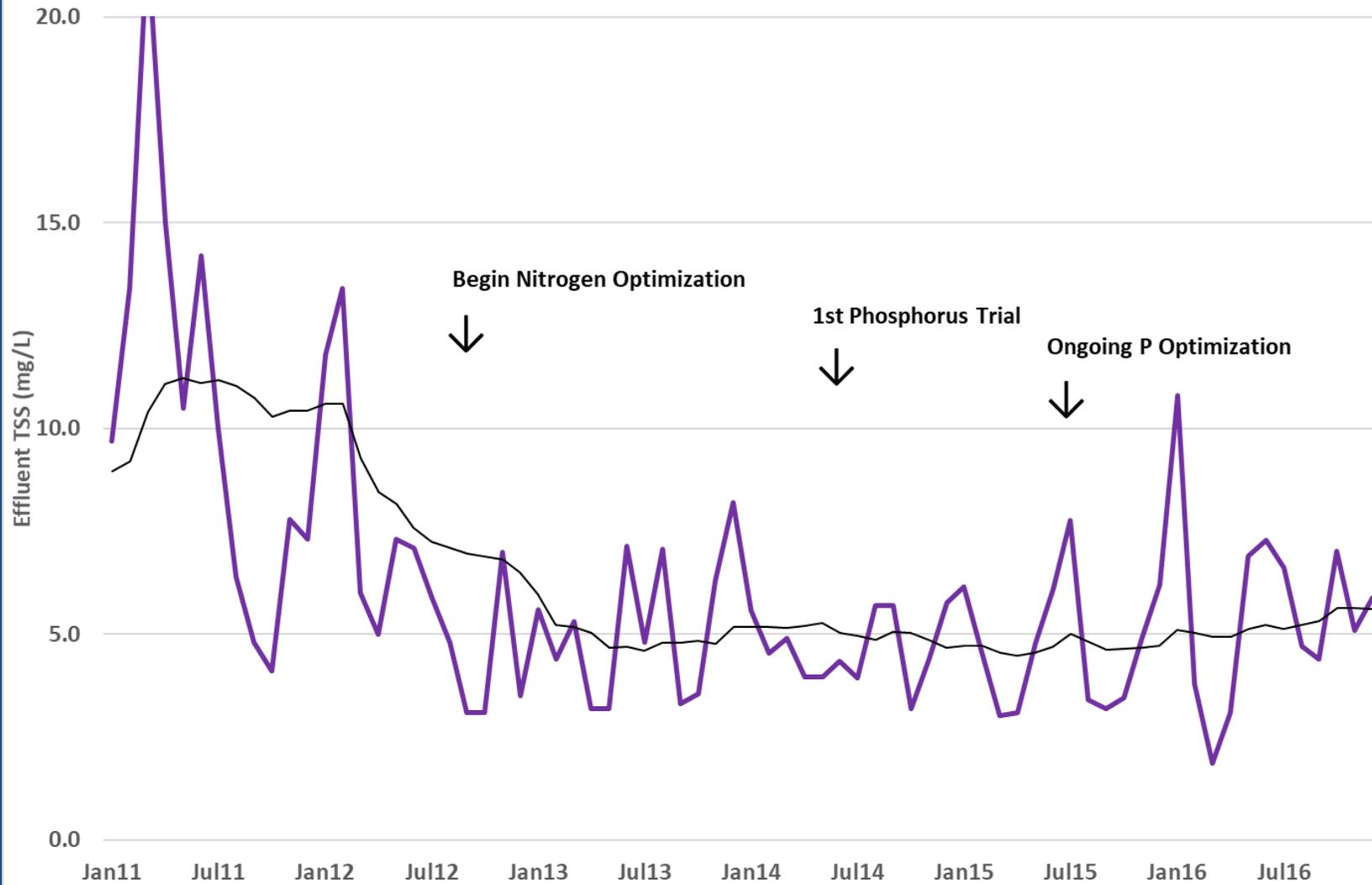
Chinook, Montana

Effluent BOD (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016



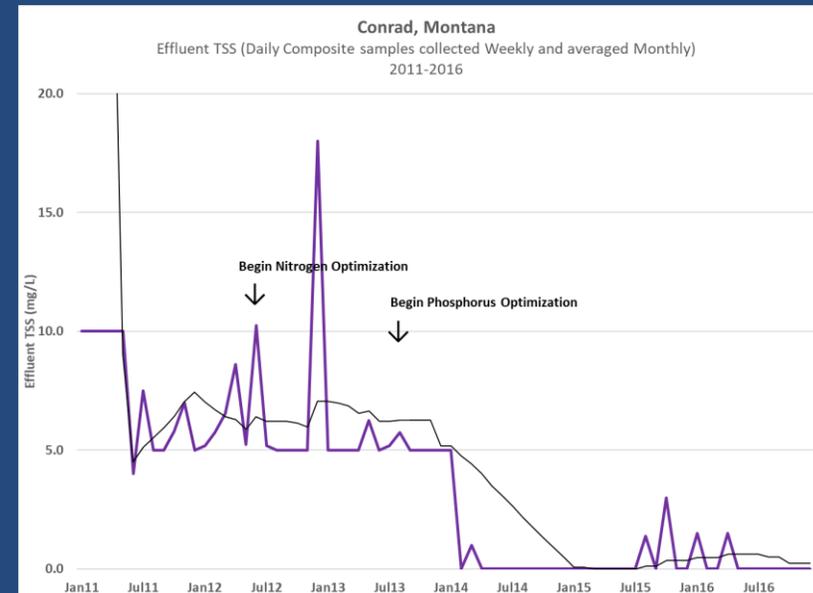
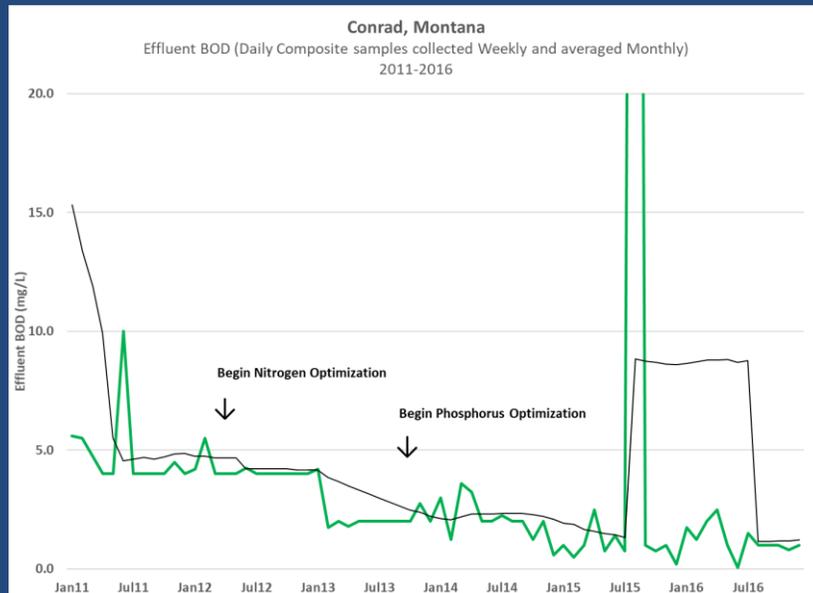
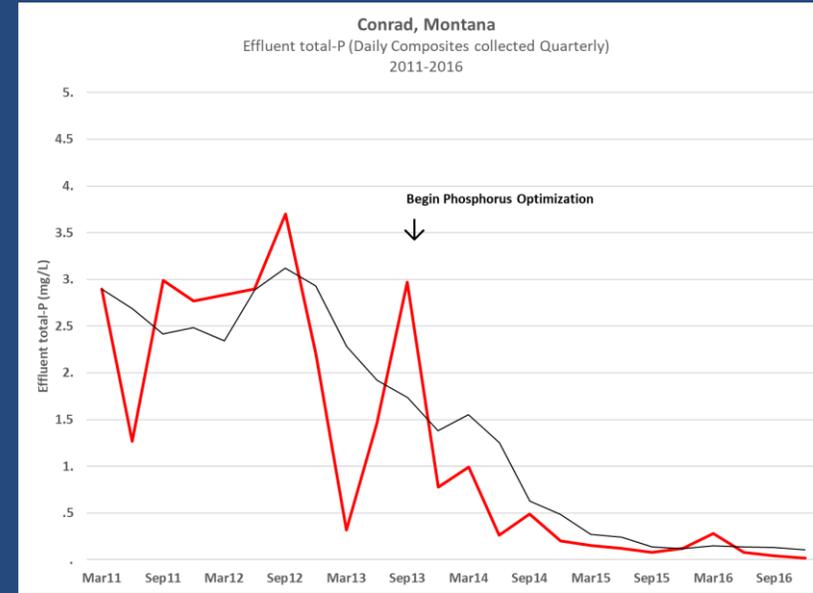
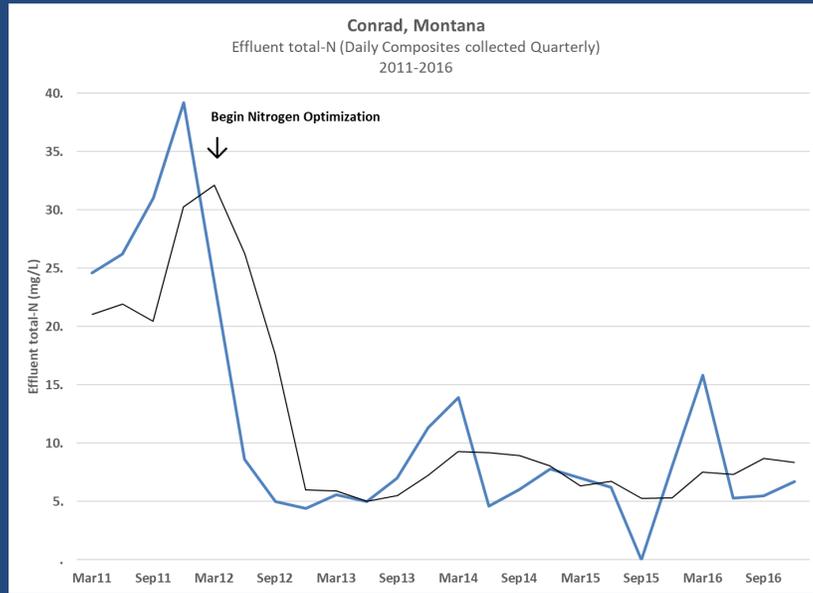
Chinook, Montana

Effluent TSS (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016



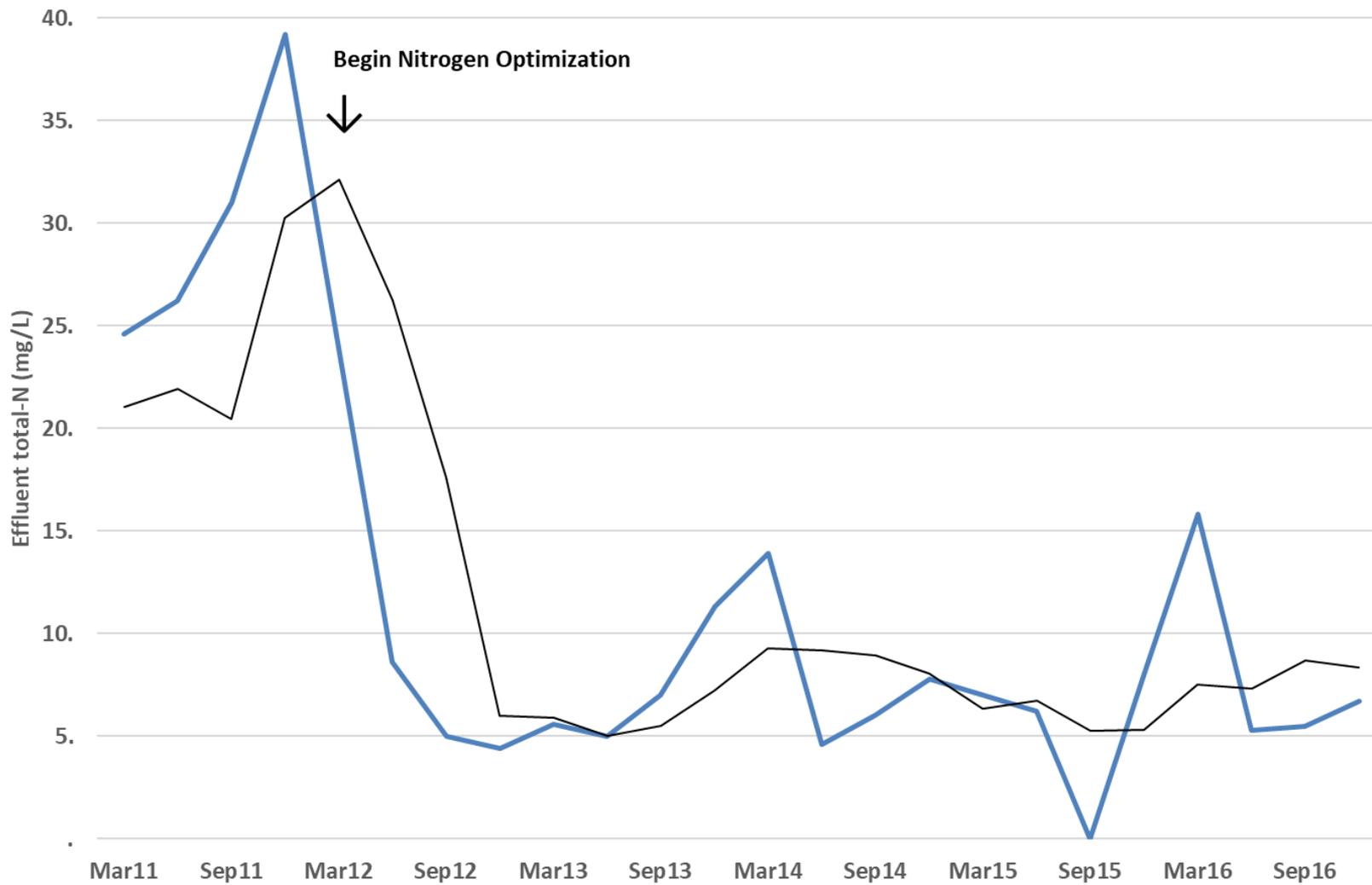
Conrad, Montana





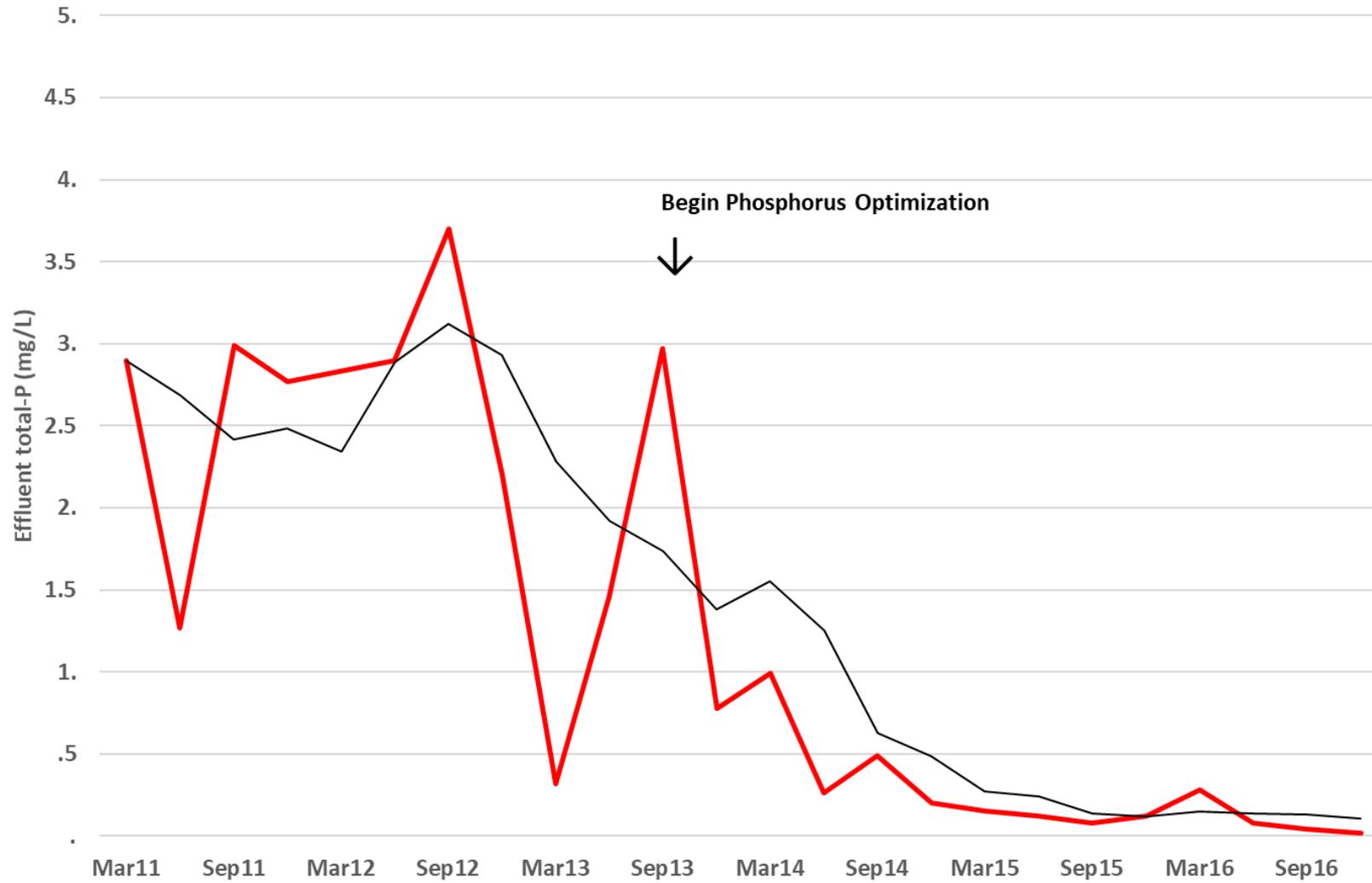
Conrad, Montana

Effluent total-N (Daily Composites collected Quarterly)
2011-2016



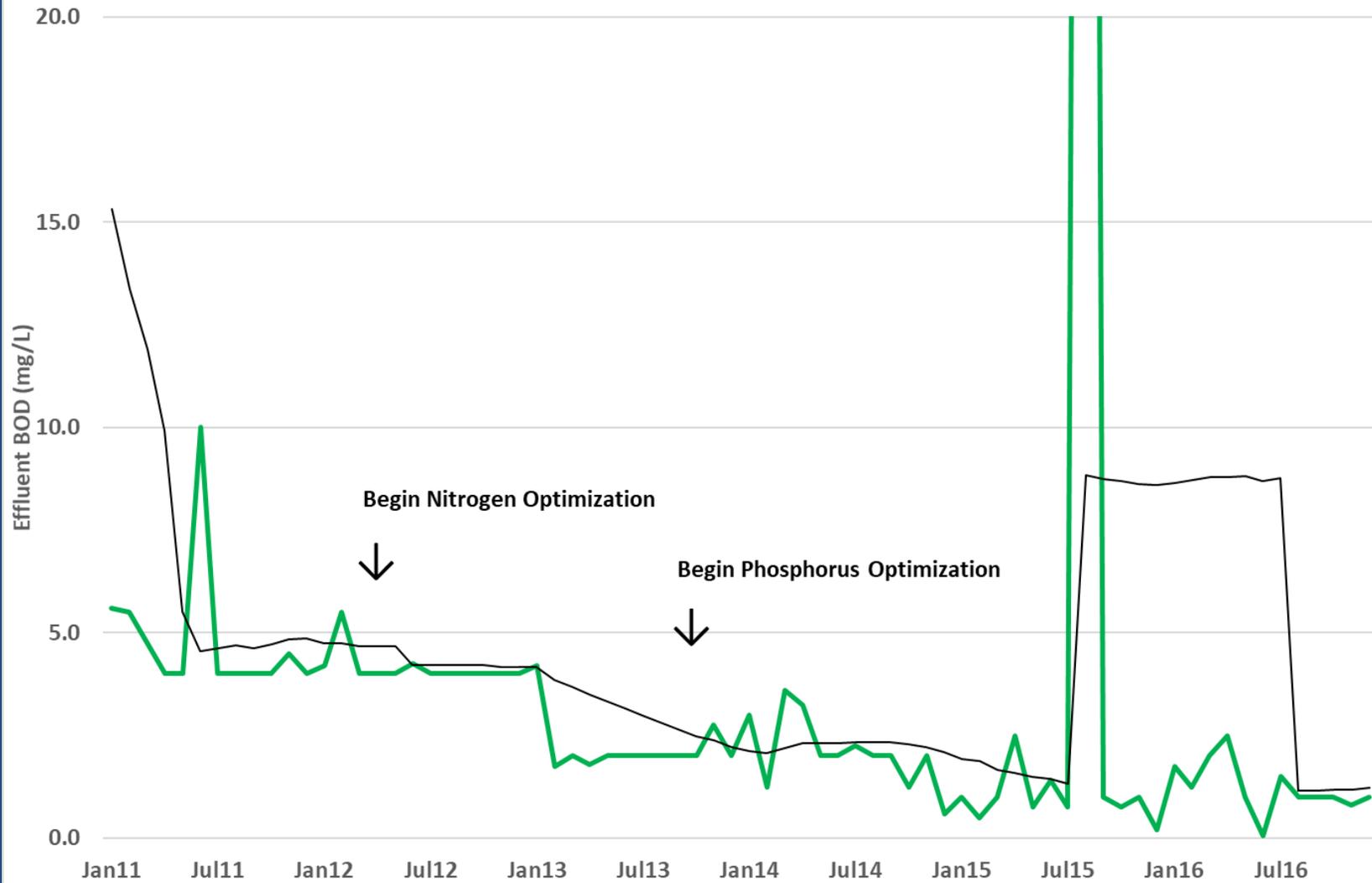
Conrad, Montana

Effluent total-P (Daily Composites collected Quarterly)
2011-2016



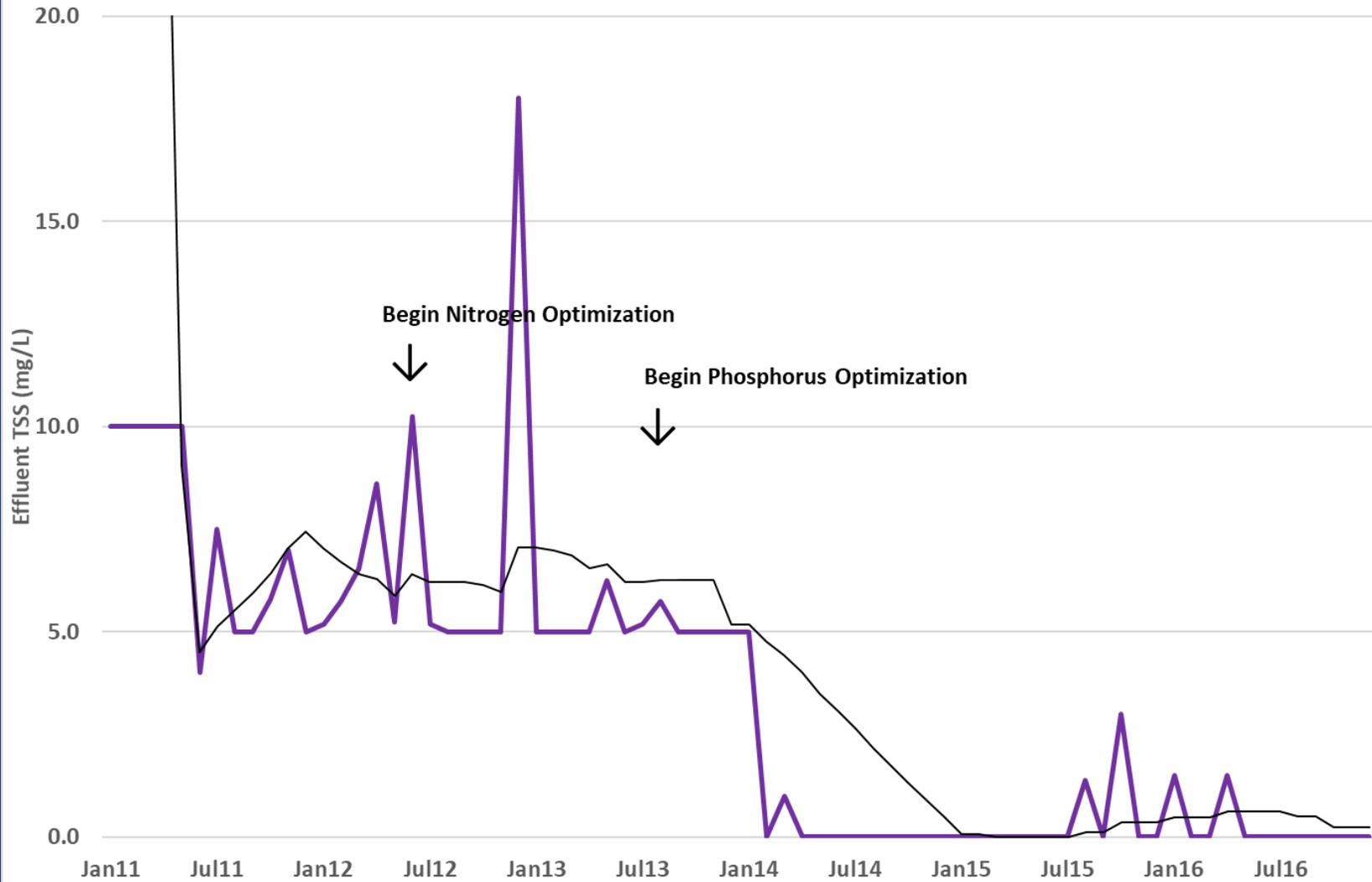
Conrad, Montana

Effluent BOD (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016



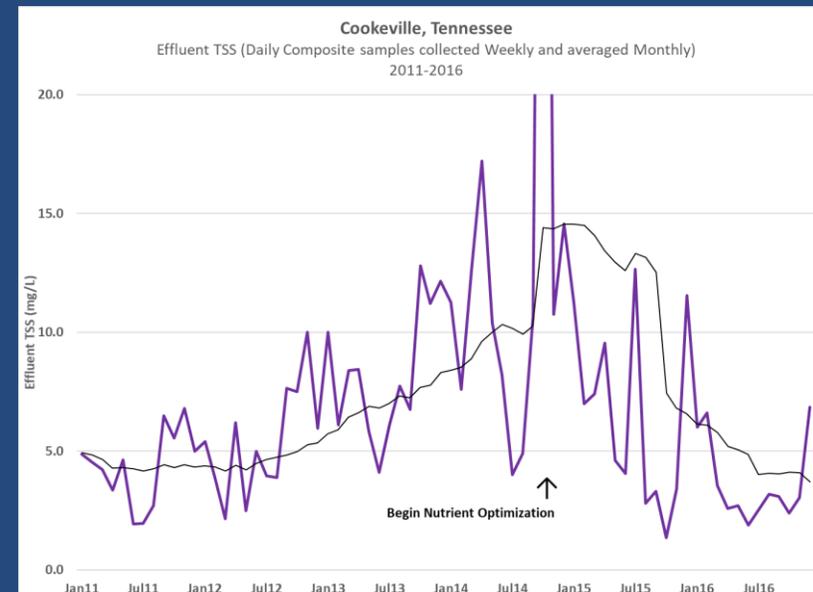
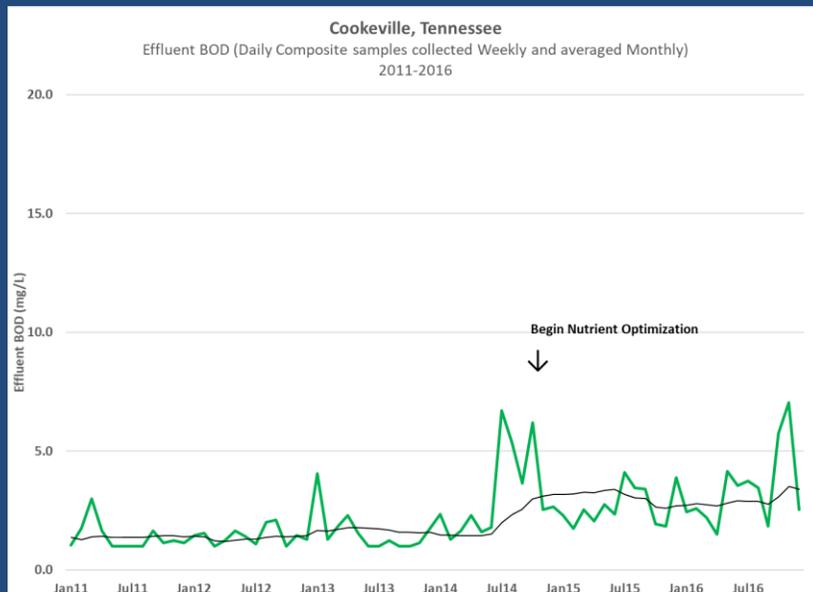
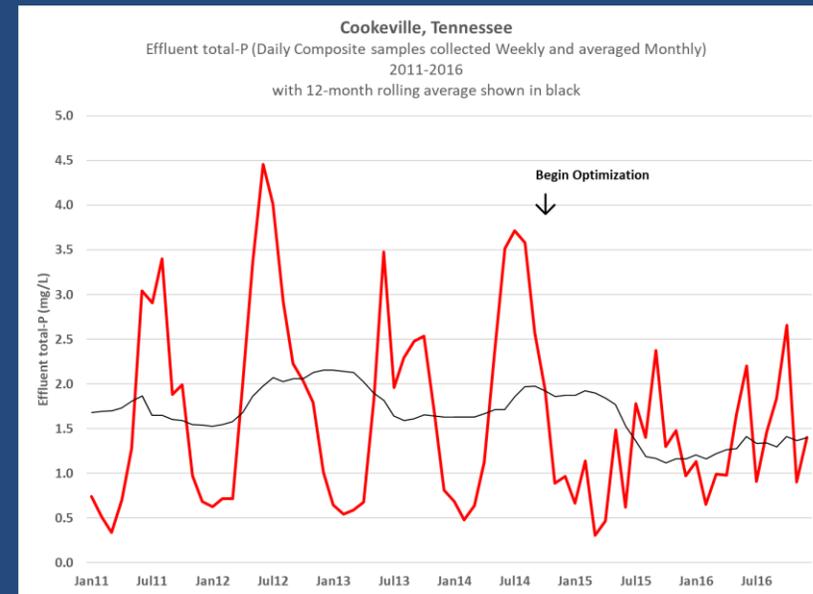
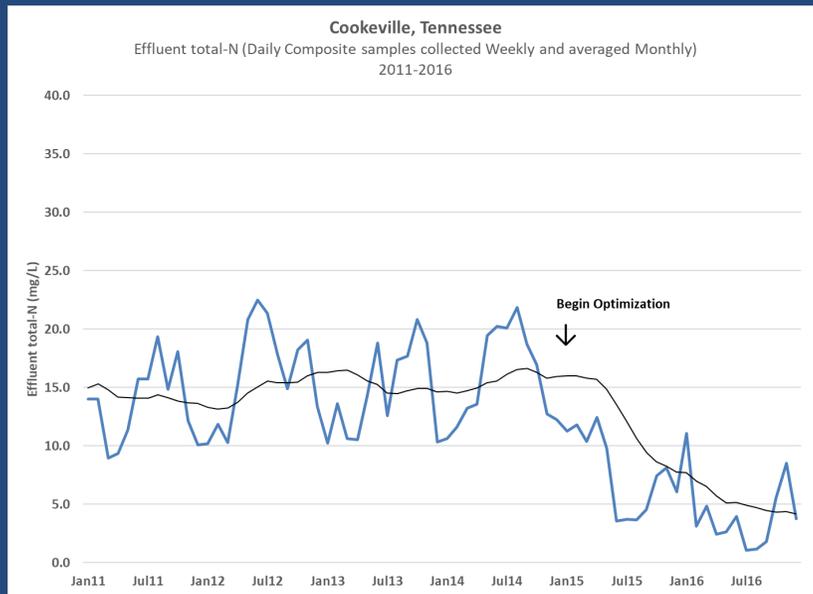
Conrad, Montana

Effluent TSS (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016



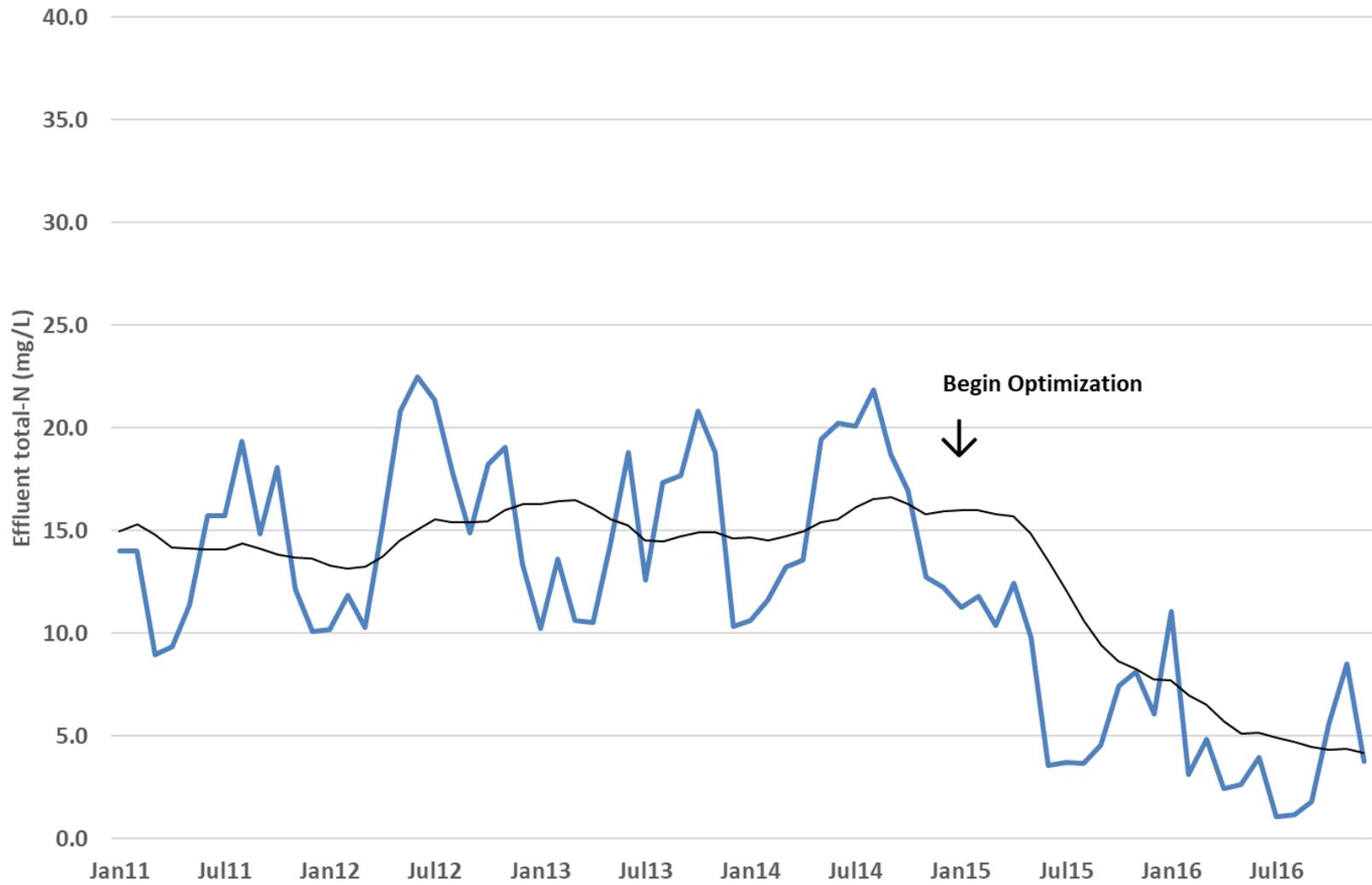
Cookeville, Tennessee





Cookeville, Tennessee

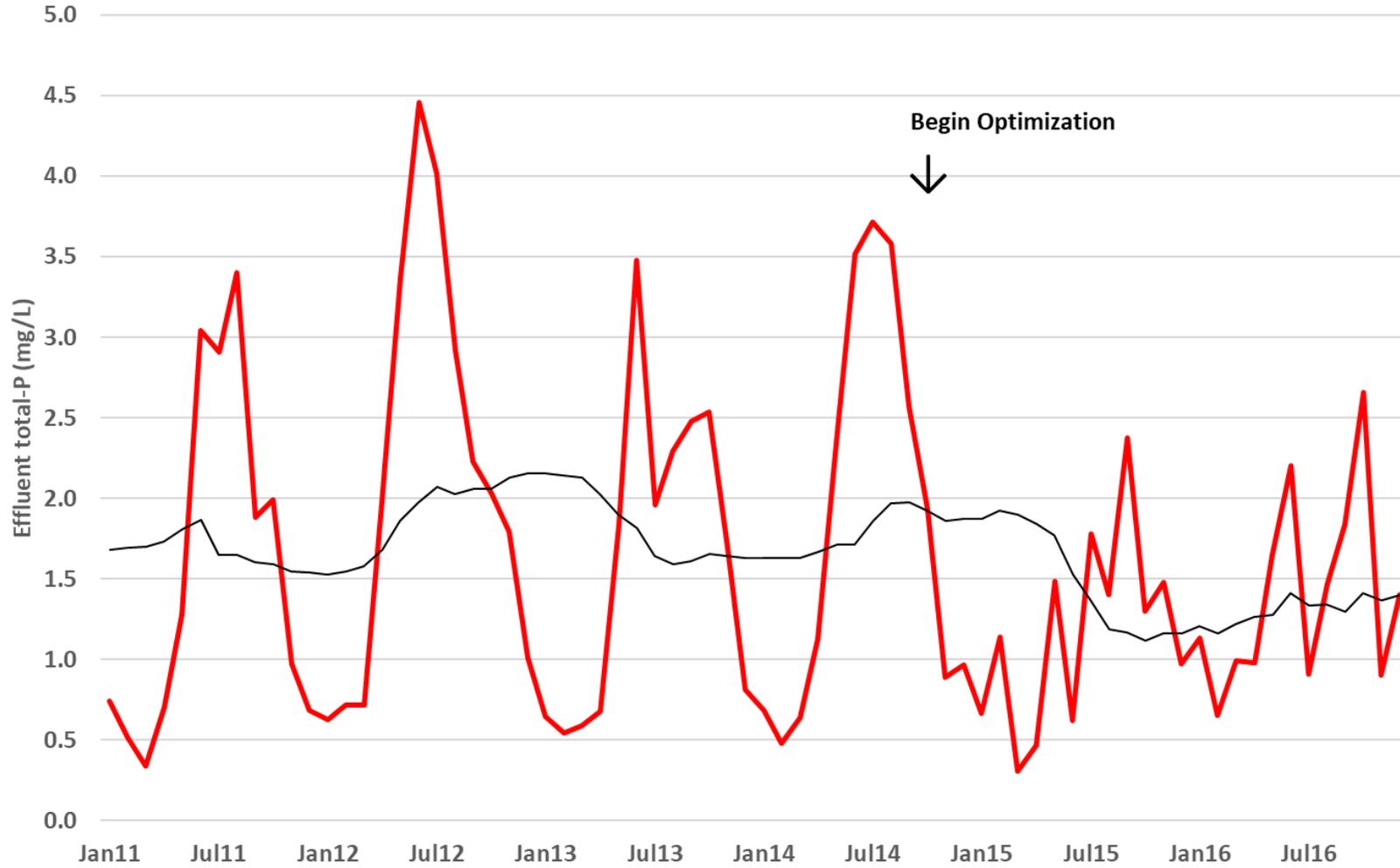
Effluent total-N (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016



Cookeville, Tennessee

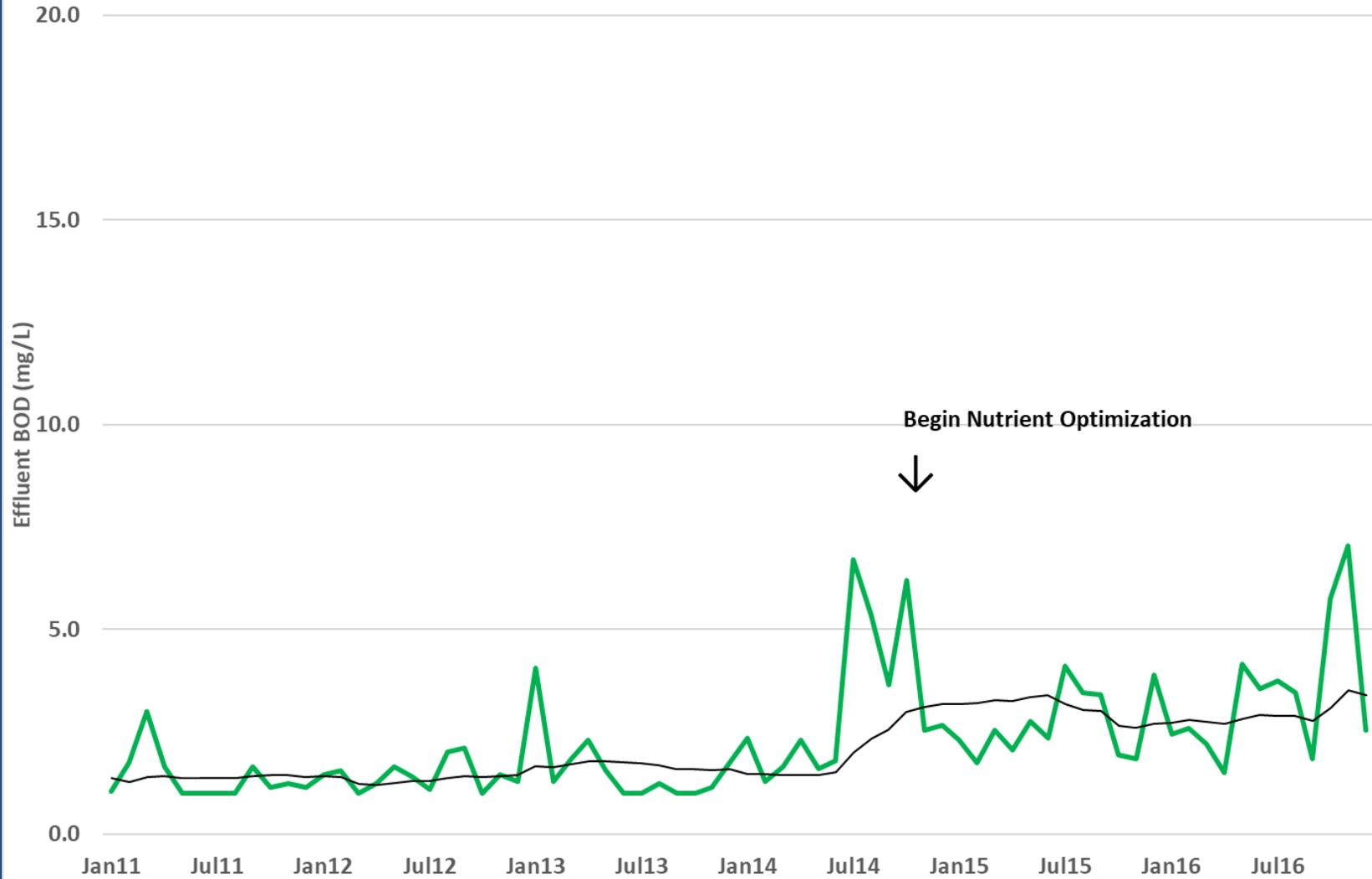
Effluent total-P (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016

with 12-month rolling average shown in black



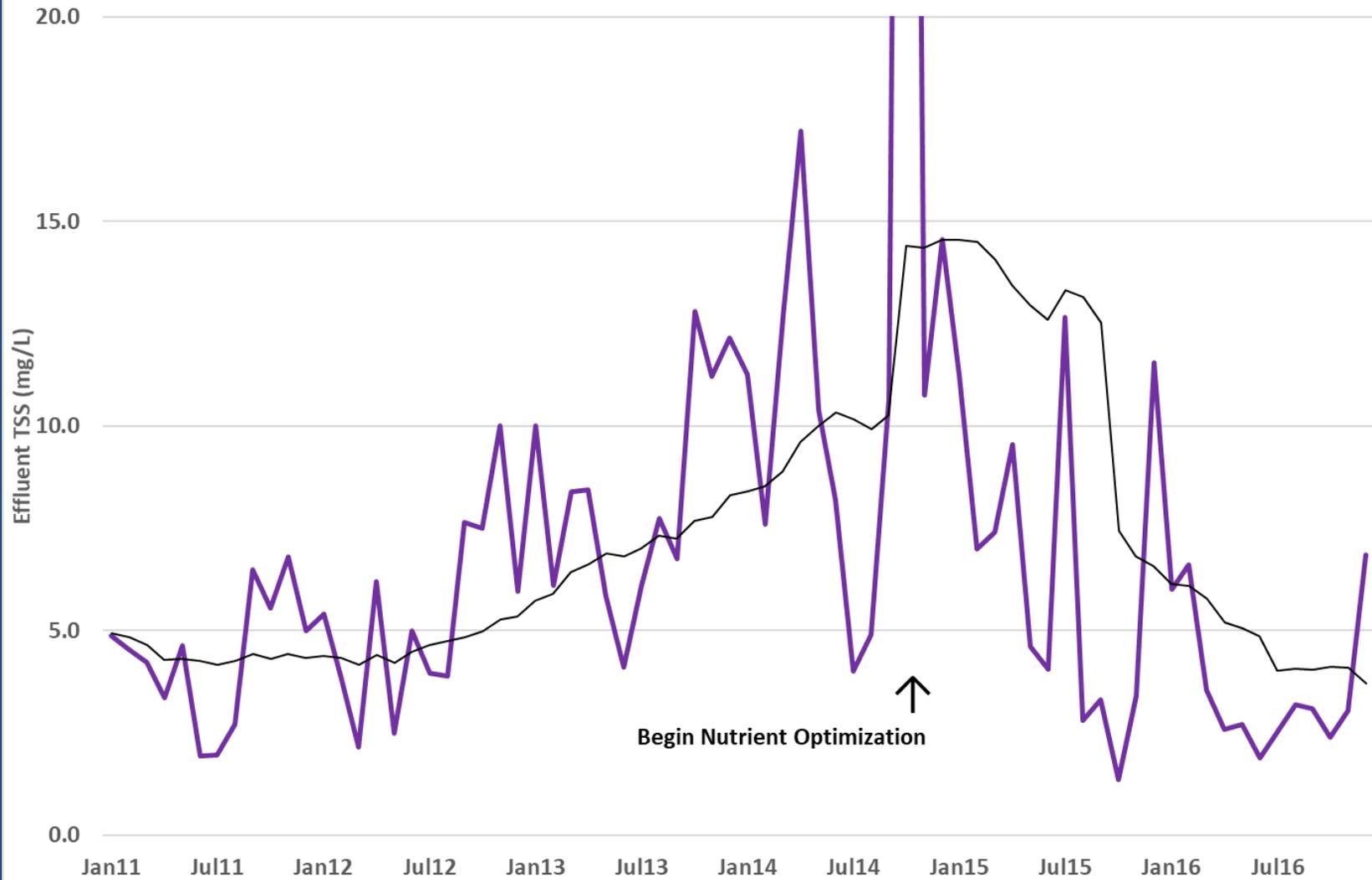
Cookeville, Tennessee

Effluent BOD (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016

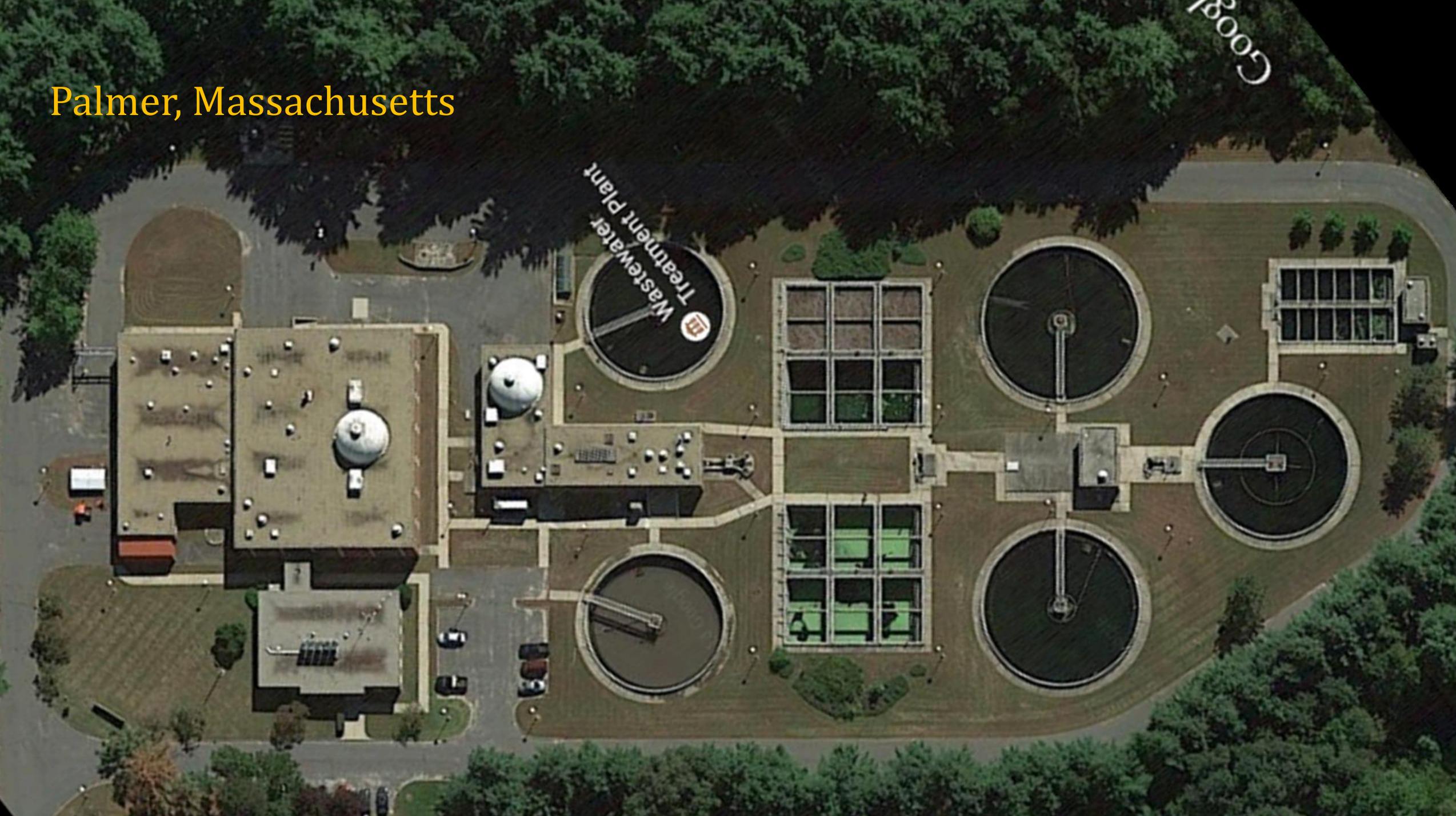


Cookeville, Tennessee

Effluent TSS (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016

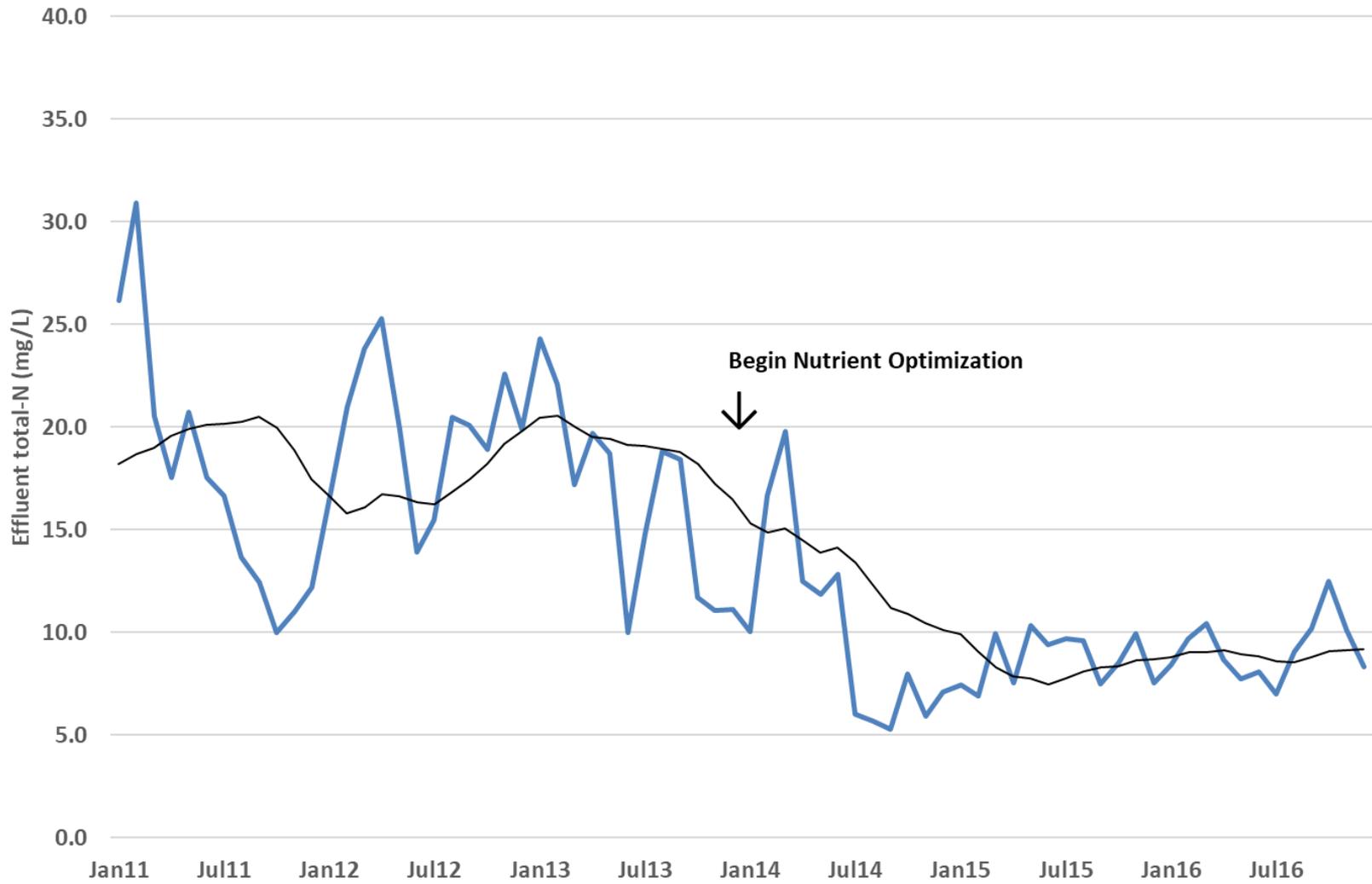


Palmer, Massachusetts



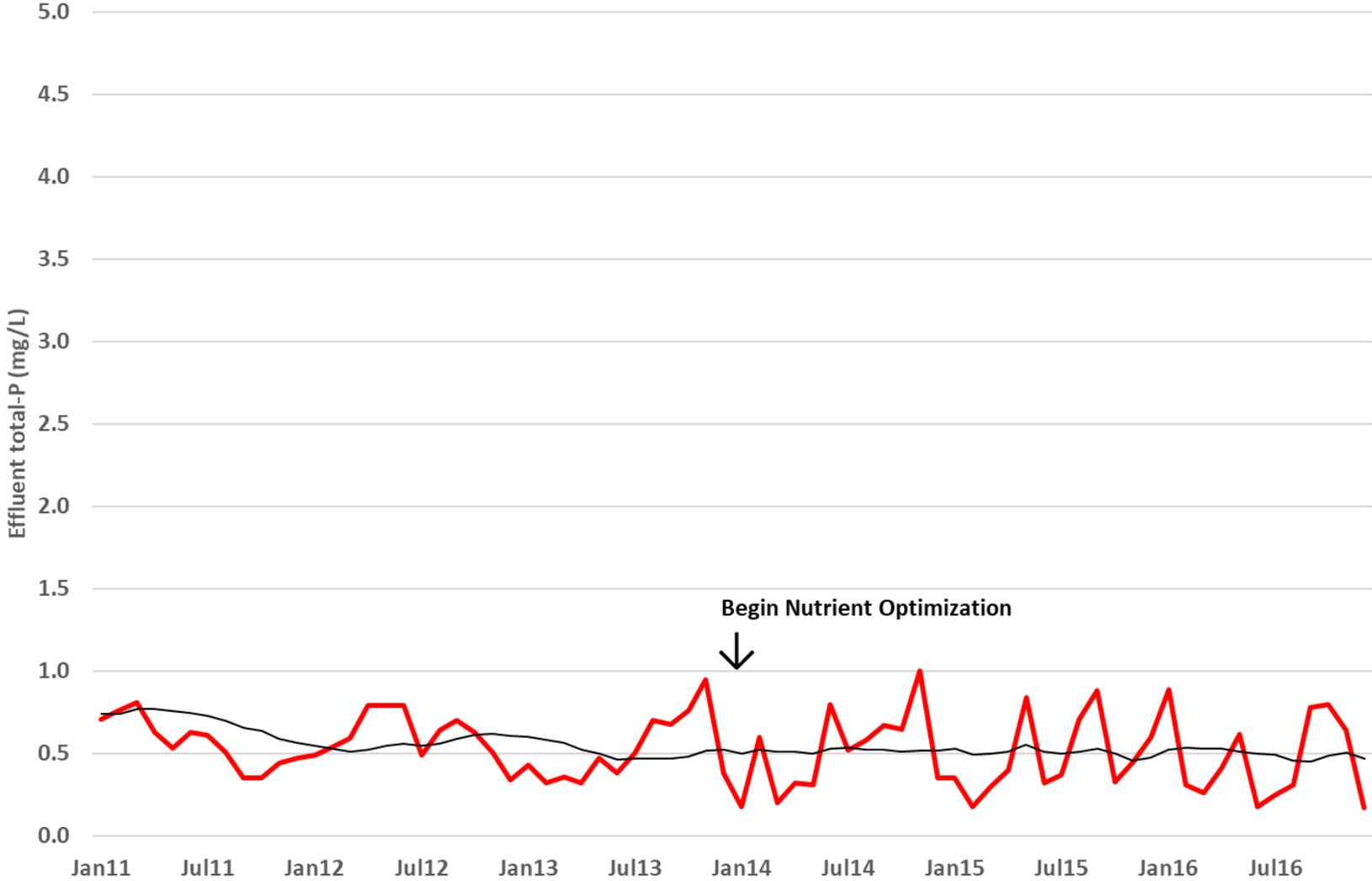
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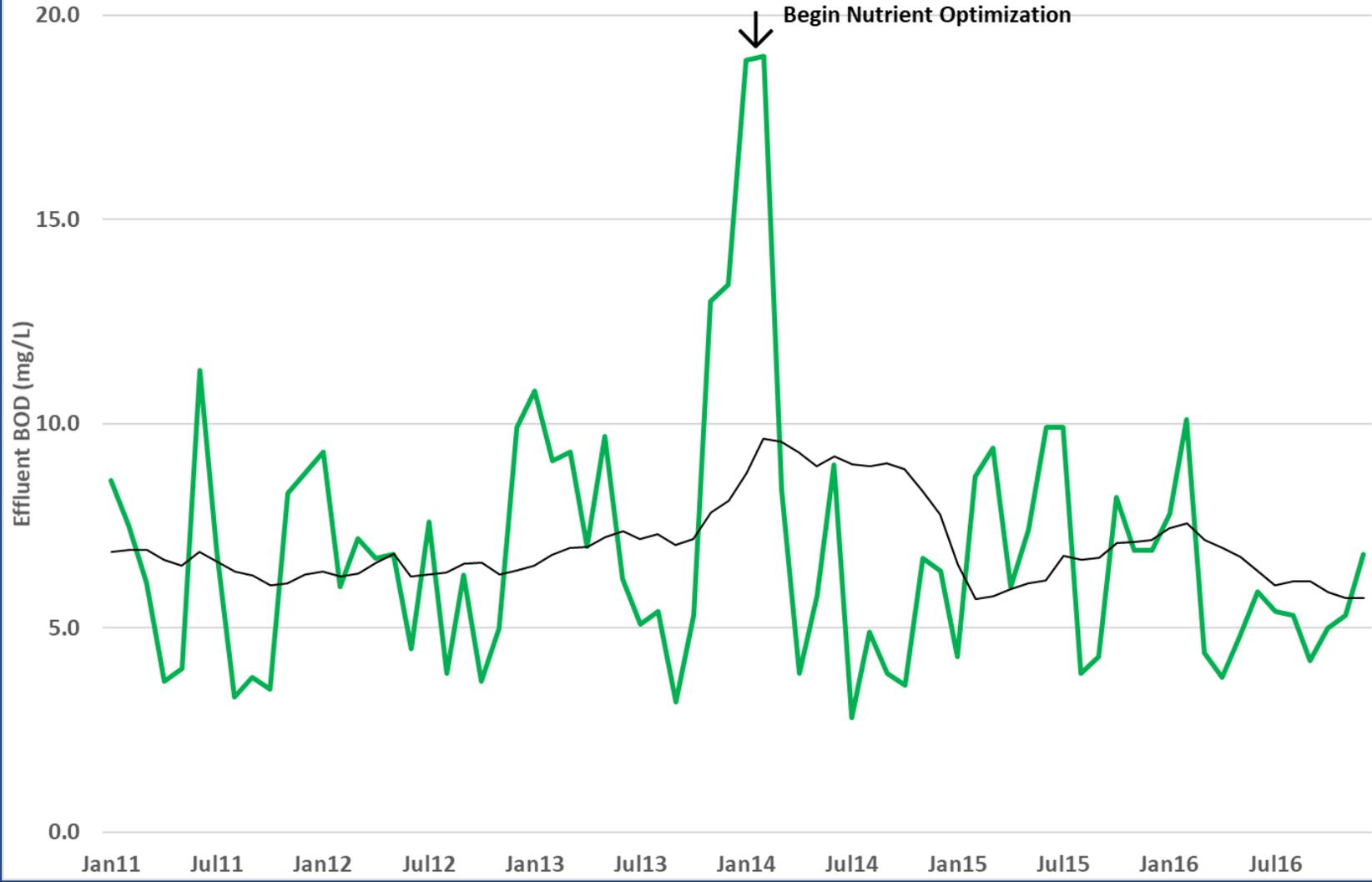
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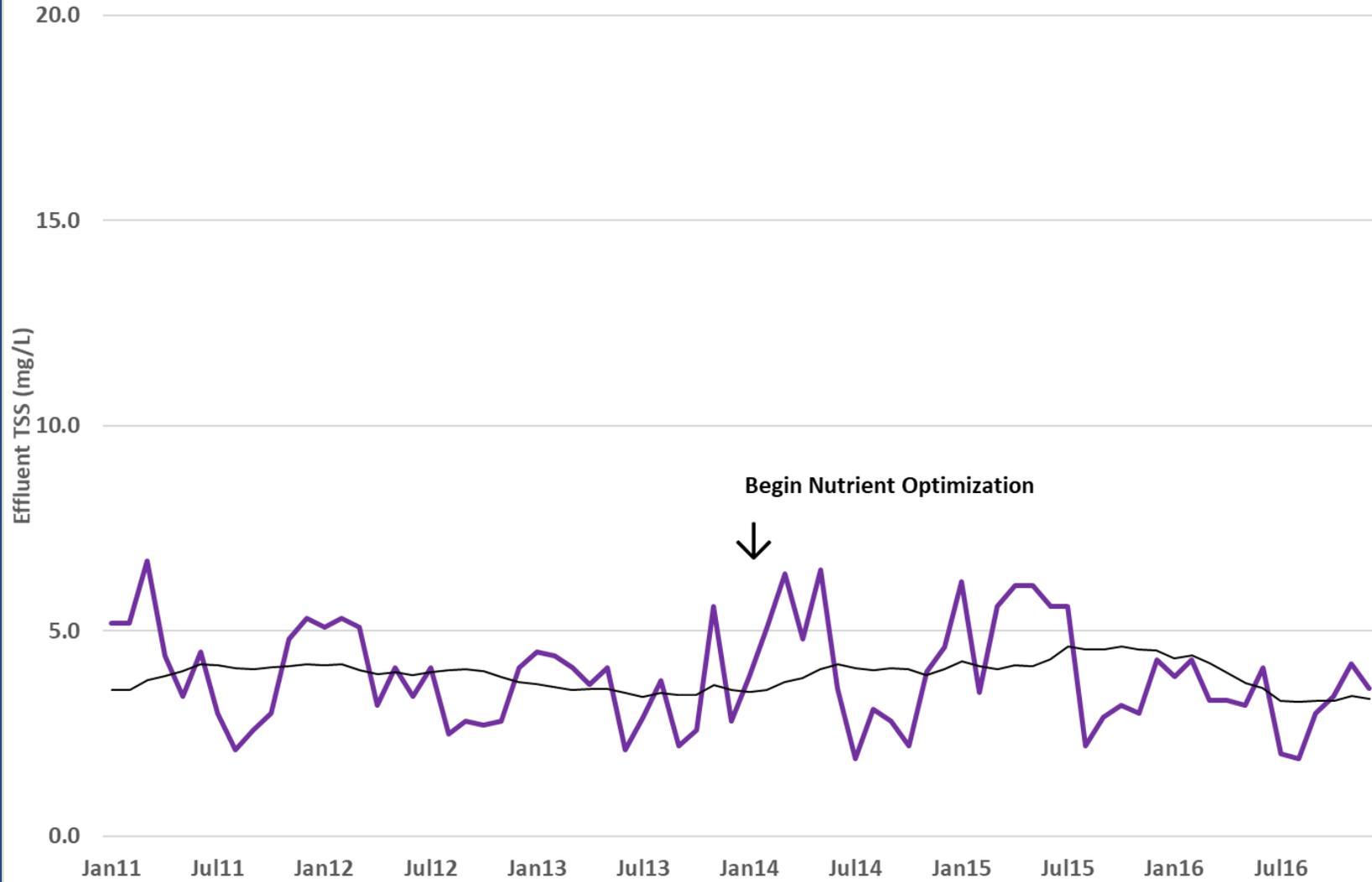
Palmer, Massachusetts

Effluent BOD (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016



Palmer, Massachusetts

Effluent TSS (Daily Composite samples collected Weekly and averaged Monthly)
2011-2016



Comments & Questions

