# Optimizing for Biological Phosphorus Removal

### **Operator Training Committee of Ohio April 26, 2023**

**Presented by:** 

Jon van Dommelen

**Ohio EPA – Compliance Assistance Unit** 

### Troubleshooting Noncompliance in Small Communities and Larger Communities

And maybe save some cash as well.....

### Troubleshooting BNR Systems in Small and Large Communities

**Causes of Noncompliance in Small BNR Systems:** 

- 1) System operators are not trained very well to run BNR systems
- 2) Systems typically do not have their own labs to run process control tests
- 3) Systems are designed using textbook characteristics for influent waste streams
- 4) Systems often suffer from inadequate soluble carbon that drives denitrification and orthophosphate release reactions

How BNR is supposed to work:

Most Important – A good <u>soluble</u> influent cBOD<sub>5</sub>

Second Most Important – <u>Low nitrates</u> in Anaerobic Zone

Third Most Important – <u>Low nitrates</u> in Anoxic Zone

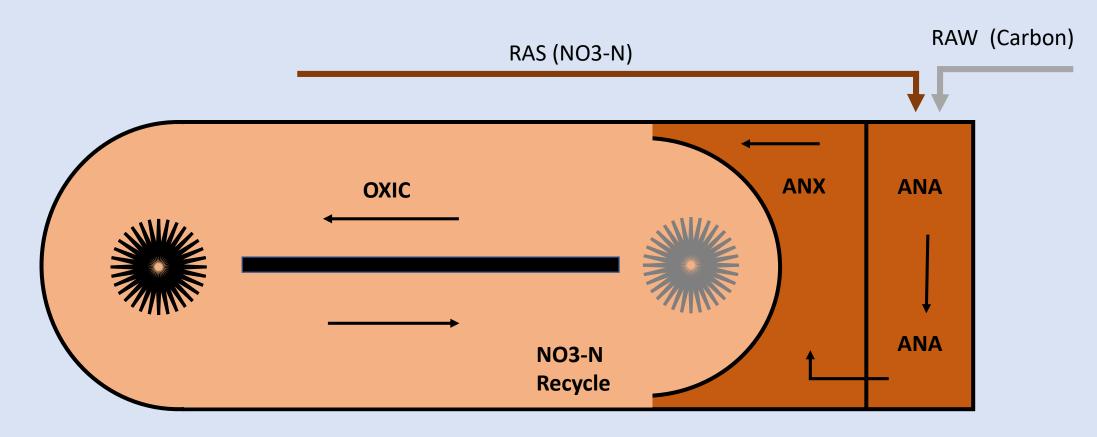
Fourth Most Important – Process Control so you know!

First, we will look at a small community:

- That abandoned one wastewater treatment plant
- Constructed a new BNR wastewater treatment plant
- Suffered from nearly random compliance for 4 years
- Then reached out to the Compliance Assistance Unit to visit their BNR system.



### BNR (Carrousel type)





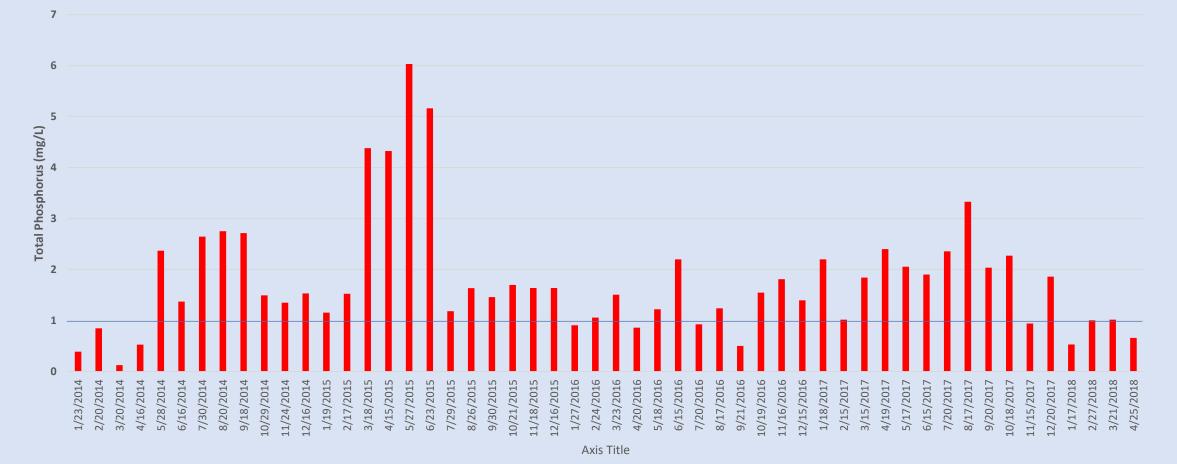








Bradford Wastewater Treatment Plant Effluent Total Phosphorus 1/1/2014 to 4/25/2018



Monthly

Date Range	Monthly Average Reported	Compliant	% Compliant	Noncompliant	% Noncompliant
Jan 2014 to Mar 2018	51	10	19.6	41	80.4

Location	COD	NH3-N	N03-N	P04-P		
Standard (300 mg/L)	299					
Influent	190	19.0		1.27		
Anaerobic Tank	119	4.5	11.9	1.01		
Anoxic Tank	113	0.1	14.6	0.99		
Oxic Tank		0.02	14.7	0.99		
Final Effluent	99	0.09	13.9	0.79		
RAS			14.2			
Note all samples are grab samples (Samples run on 3/15)						

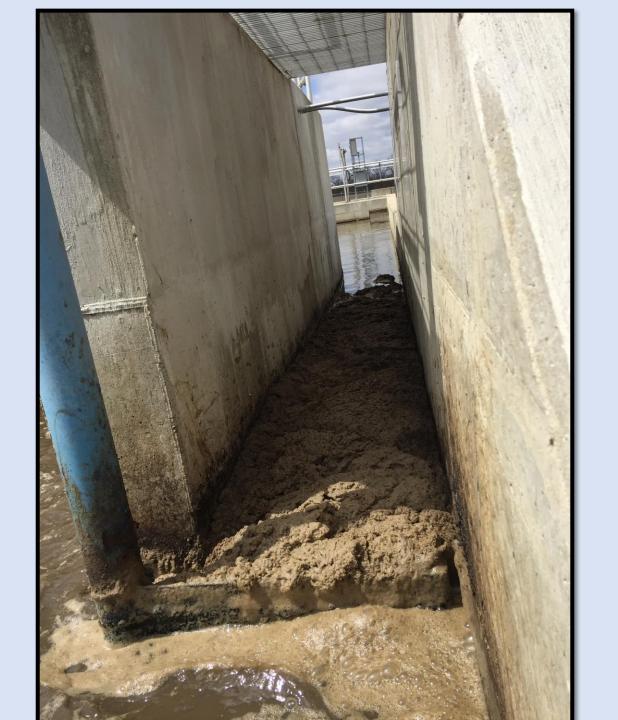
Nitrate Profile (mg/L)			
	RAS	Anaerobic	Anoxic
3/15/2018	14.3	11.9	14.6
→ 3/19/2018	8.7	12.5	11.9
3/20/2018	11.6	7.9	11.8
3/21/2018	11.5	7.5	12.0
3/22/2018	8.6	8.2	11.1

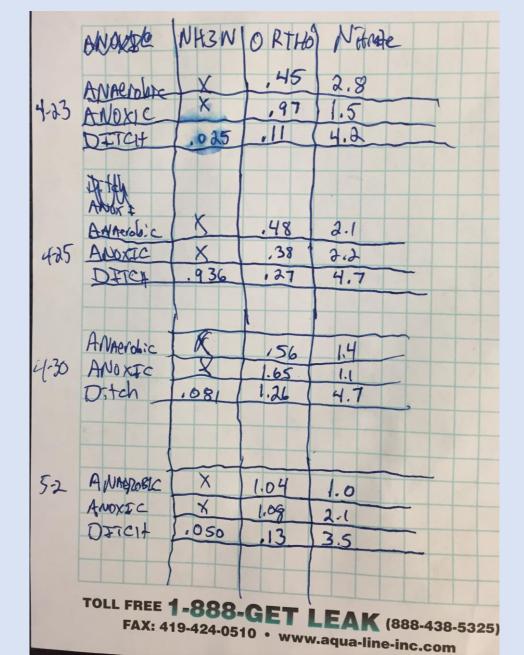
## **Too much Nitrate everywhere**

### Solution: Manage the Nitrates

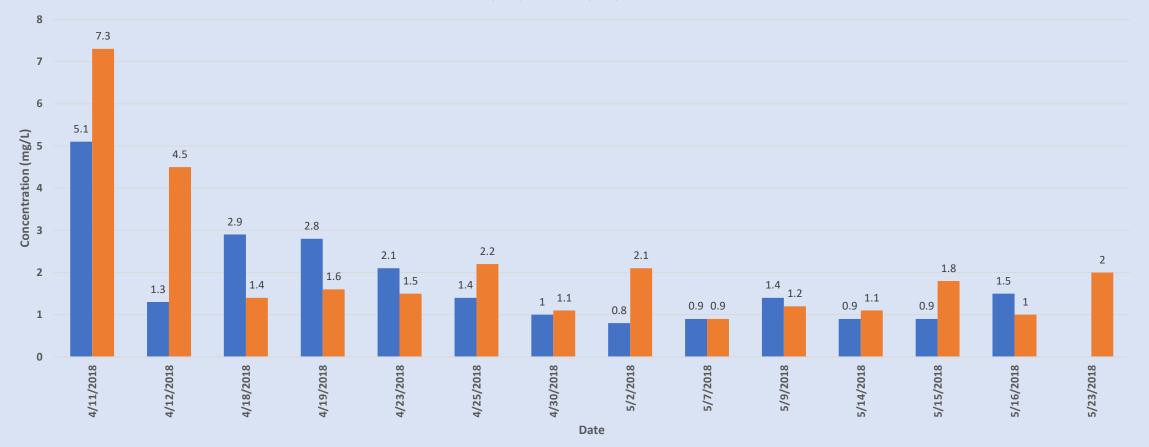
**Solution: Manage the Nitrates** 

- 1) Closed the nitrate recycle gate completely
- 2) Run vertical rotor at 38 Hertz
- 3) Turned 2<sup>nd</sup> Anaerobic Zone Mixer OFF for 3.5 hours, ON for 30 minutes
- 4) Turned Anoxic Zone Mixer OFF for 3.5 hours, ON for 30 minutes
- 5) Profile Ammonia, Nitrate, and Orthophosphate in each zone



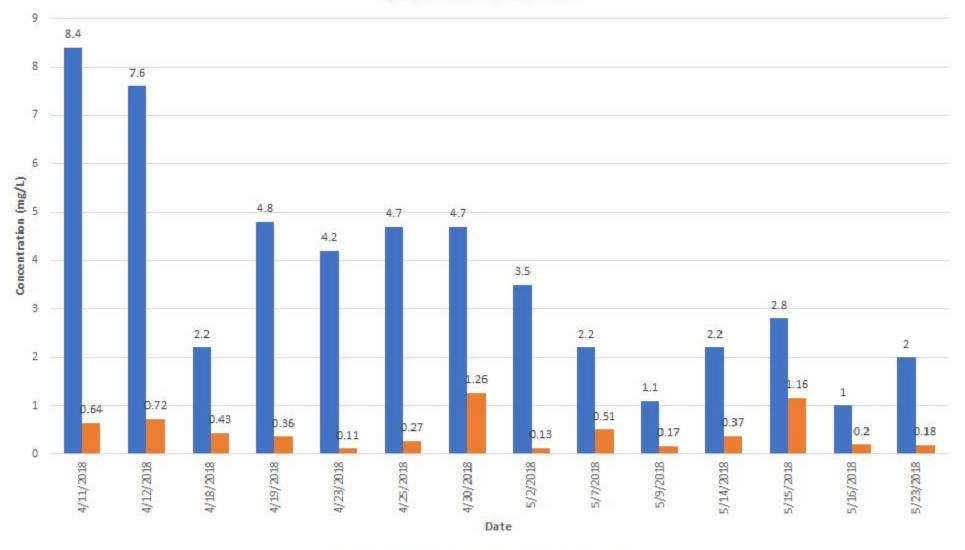


#### Bradford WWTP Nutrient Profile Nitrate Grab Sampling 4/11/2018 - 5/23/2018



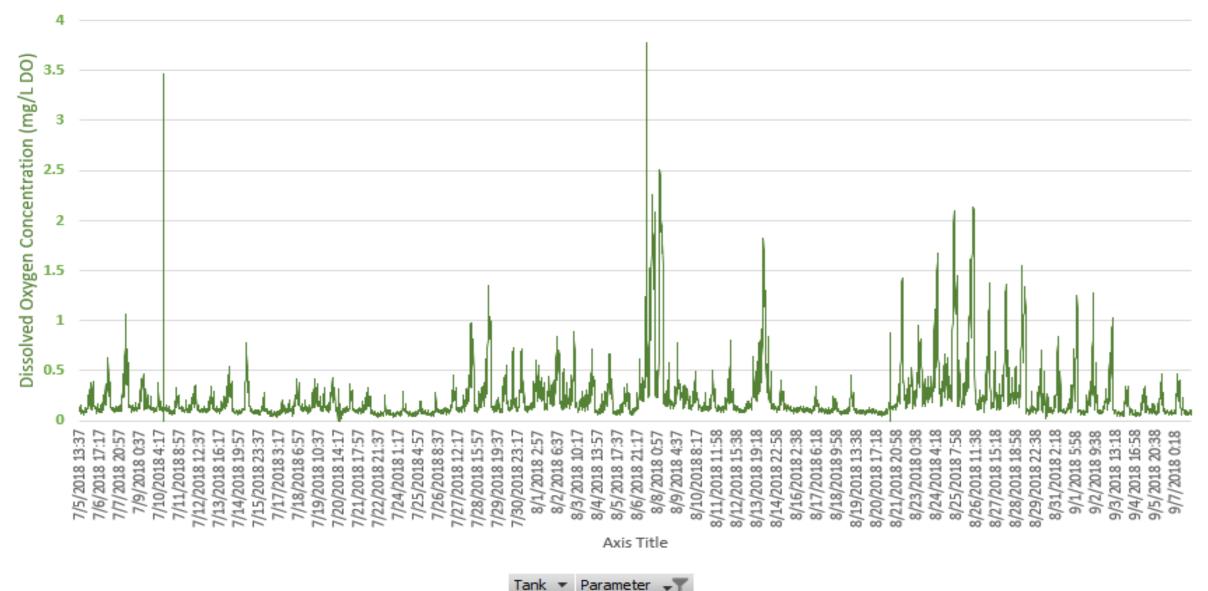
Anaerobic - NO3-N Anoxic - NO3-N

#### Bradford WWTP Nutrient Profile Grab Sampling 4/11/2018 - 5/23/2018

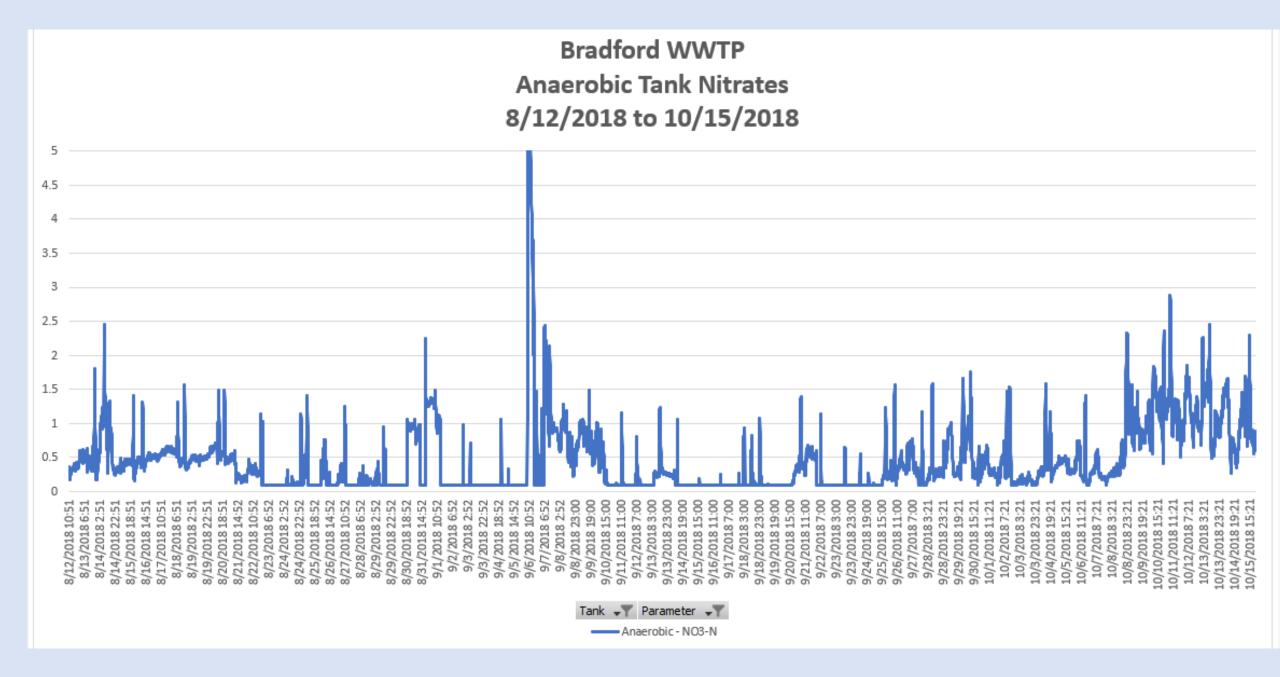


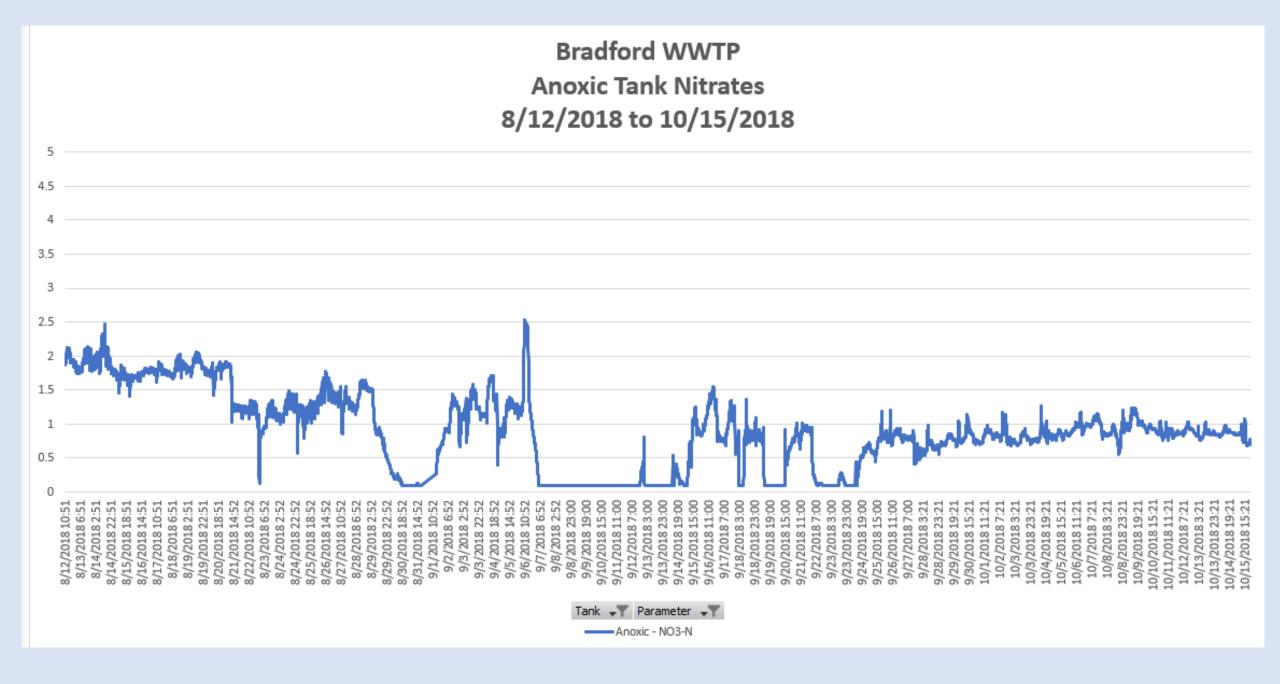
Final Effluent - NO3-N Final Effluent - PO4-P

#### Bradford WWTP Oxic Tank Dissolved Oxygen July -September, 2018



-	CONTROLLER 19 Apr 2018 12:56 2 A						
01	3.0*mg/l	NH4-N	10.8 %	C ANX NH3			
02	1.9 mg/l -	NO3-N	10.8 °	C ANX NO3			
03	188 mg/l	CI	10.8 °				
04	4.6 mg/l	NH4-N	10.7 °C	ANA NH3			
05	2.1*mg/l	NO3-N	10.7 °C	ANA NO3			
06	8.7 mg/l	К	10.7 °C	ANA K			
Next	Next sensor +++, Display/Options 🎬						





First April sample was high (1.25 mg/L), but the rest of the samples brought the monthly down to 0.66 mg/L

Alum feed was shut down 5/2

May 2018 another consecutive month of compliance for TP

In addition, the village was spending \$800 - \$1000/month for alum previously.

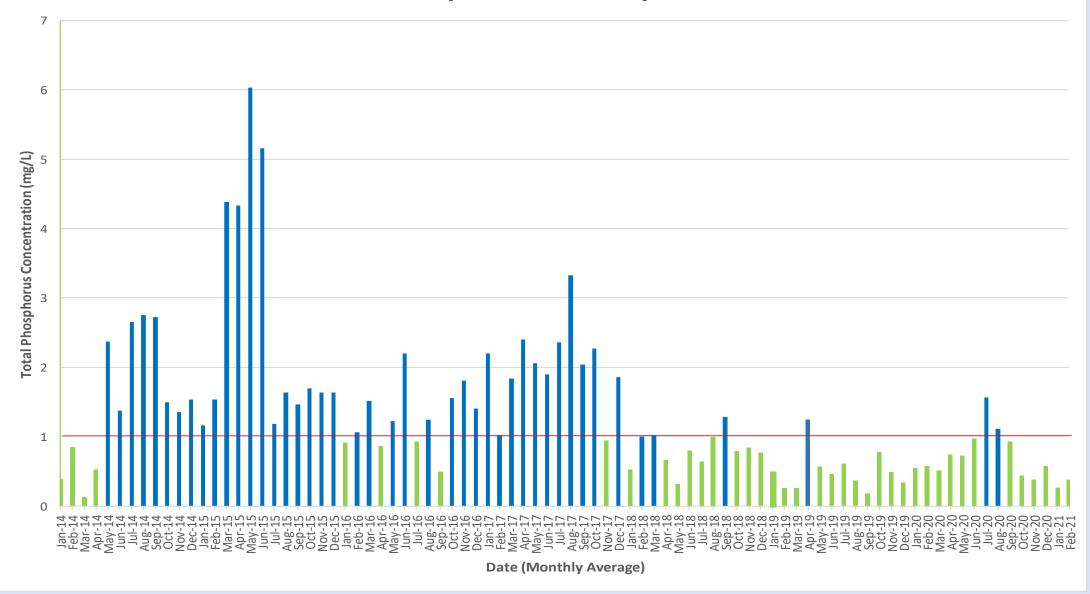
Electricity demand should also be reduced due to mixer turndown



## **Digester Nutrient Profile**

Ammonia Nitrogen	Dilution	Nitrate Nitrogen	Dilution	Orthophosphate	Dilution
Nondetect	(1:4)	504 mg/L	(1:20)	220 mg/L	(1:200)

Bradford Wastewater Treatment Plant Effluent Total Phosphorus Concentration January 2014 - February 2021



Date Range	Monthly Average Reported	Compliant	% Compliant	Noncompliant	% Noncompliant
January 2014 to March 2018	51	10	19.6	41	80.4
April 2018 To February 2021	35	31	88.6	4	11.4

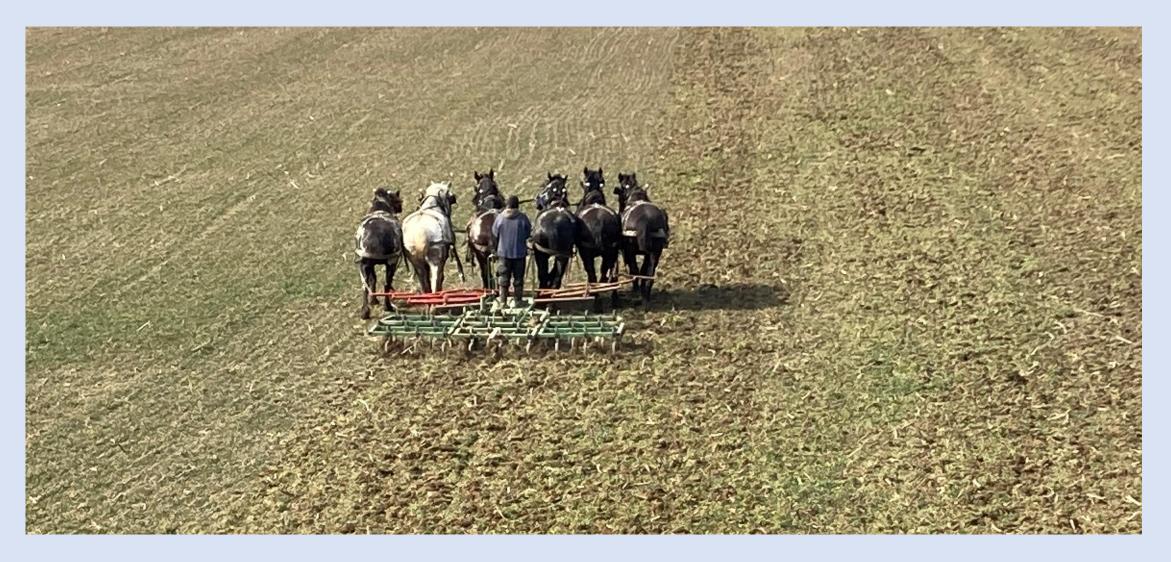
#### **Troubleshooting BNR Systems**

Keys to BNR:

### **Process Control!**

- 1) Monitor the nutrients in the Inputs to each zone
- 2) Monitor the nutrients in Internal Recycles (Digester Supernatant)
- 3) If the Chemistry is correct in the zones, the bacterial response will be compliant.
- 4) Know the chemical environment in each zone of the WWTP.

# **BNR in an SBR?**







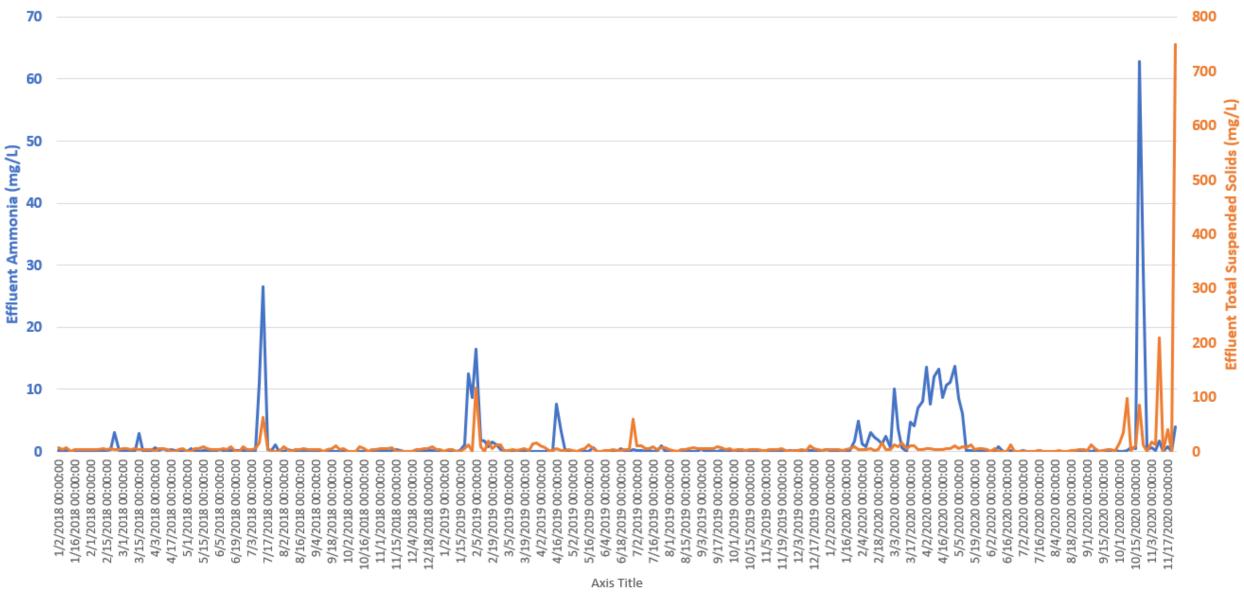
## **BNR** in an SBR

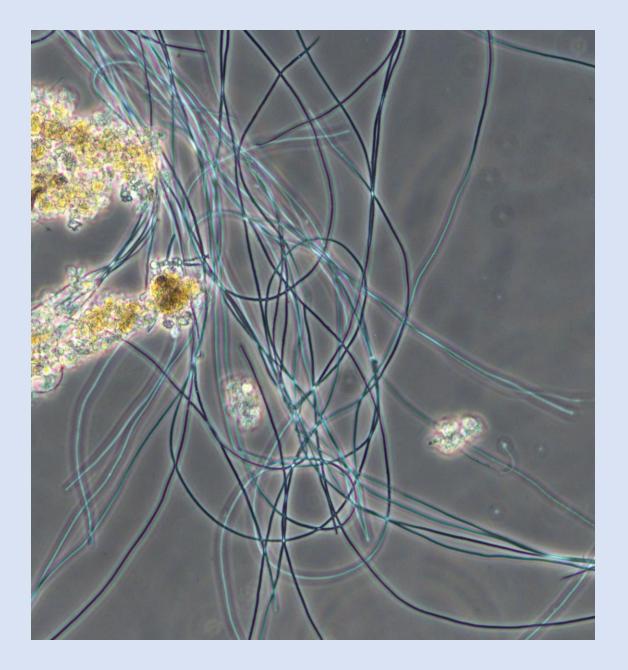
Originally, I was called to diagnose a filament issue.

The SBR had Type O21N, EVERYWHERE.

And it was causing severe noncompliance (11/22/2020)

#### Effluent Ammonia and Total Suspended Solids 1/1/2018 - 11/24/2020







There was more filament than floc, and solids were being decanted

Type O21N is a septicity filament

So, the solution was to track down the septicity source:

Long, low flow force mains and solids handling are first to check.





#### First Visit to Walnut Creek (12/9/2020):

I realized that the WWTP was feeding **sodium aluminate** in the influent to the SBR

This was how they were meeting their permit concentrations for Total Phosphorus

But I suspected that they were inadvertently creating a nutrient imbalance for phosphorus

The orthophosphate concentration was less than 0.3 mg/L in the mix/fill cycle

And the influent CBOD was typically around 400 mg/L!

The community did have a low flow force main that has septic wastewater discharge to the WWTP

What was the cause of the Type O21N filament?

Was it septicity? Was it nutrient deficiency?

The Plan:

SBRs are complete mix tanks, which is good for a septic influent.

SBRs can have the cycles adjusted to almost anything as long as the mix/fill and the react/fill cycles match the react, settle and decant cycles.

This SBR was so over designed that they only ran one tank

They could do this because the system was designed to treat 400,000 gpd

But the WWTP only sees around 180,000 gpd.

When we looked at the SBR cycles, we realized that the initial mix-fill cycle was only 5 minutes long

We expanded the mix-fill cycle to 40 minutes to try to stress the phosphorus accumulating bacteria to release OrthoP

We cycled the digester air ON for 3 hours and OFF for 1 hour to try to reduce the Nitrates and OrthoP in dewatering And on 12/14,

#### We shut the Sodium Aluminate **OFF**

They could run one tank because they had an influent EQ tank that would store the wastewater during react, settle and decant (actually it could almost store an entire day's flow )

Because the online SBR had so much filament, we switched to the unused tank on 12/15 (with no sodium aluminate added!)

The orthophosphate concentration never missed a beat staying typically below the permit limit of **1.0 mg/L** 

But the ammonia crept up slowly settling in at around 10-12 mg/L.

We kept bumping the aeration cycles to ty to oxidize the ammonia

But the ammonia didn't budge and remained around 10 mg/L

What is going on here?

Parameter	Dilution (Sample: DI water)	Meter Read	Multiplier	Concentration
EQ Basin	0.2:9.8	0.66	50	33 mg/L
NH3-N (react-fill)	0.2 : 9.8	0.58	50	29 mg/L
NH3-N (post EQ)	0.5:9.5	0.61	50	30.5 mg/L
NO3-N (react)	1:0	0.7	1	0.7 mg/L
PO4-P (react)	2.5 : 2.5	0.49	2	0.98 mg/L

Grab samples from 12/16/2020

- Interestingly, the nitrate was almost always less than 1 mg/L as well
- But they didn't have a nitrate limit or at total inorganic nitrogen limit
- To take care of the new ammonia violation, we increased the react/fill and the react cycles.
- But the ammonia didn't come down

- Prior to turning off the sodium aluminate, ammonia was near nondetect
- But that was in the tank with the filaments. We switched tanks to the unused tank to stop losing solids to the creek.
- The other factor was that the tanks were above ground and out of direct sight.
- We didn't have good visual cues, only random cues when we collected samples

What we eventually discovered:

The original tank aeration was on a timed cycle

When we switched tanks, the second tank was programed to run aeration with a DO probe

We didn't notice when the air was shut down when it reached a high set point

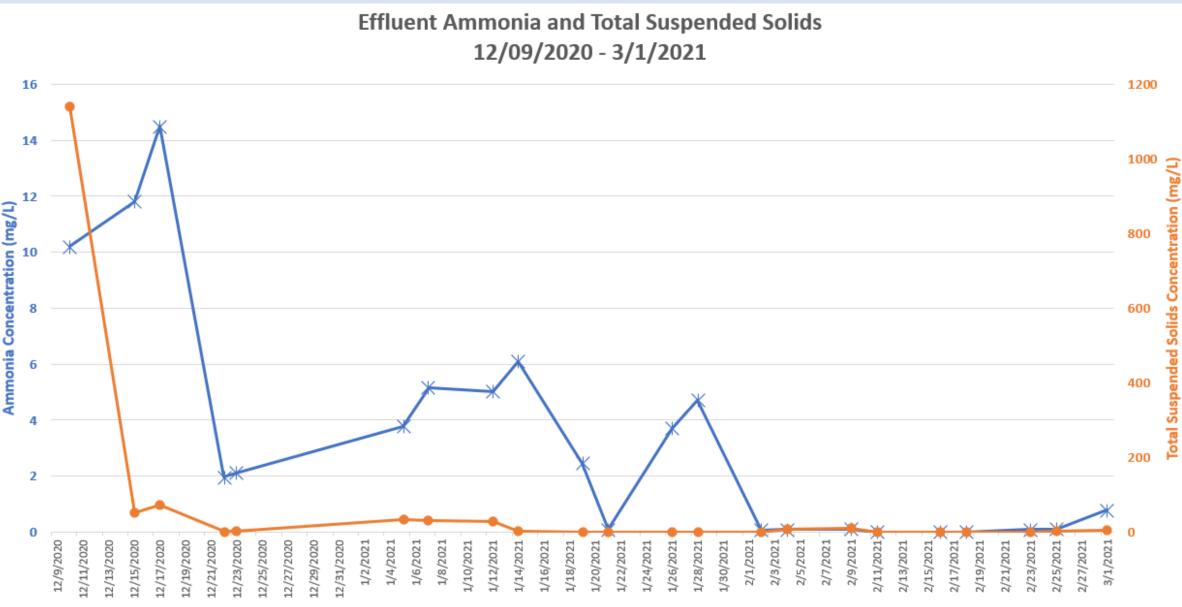
And the influent pump would pump whenever the EQ floats called for pump cycle

The other thing we discovered much later:

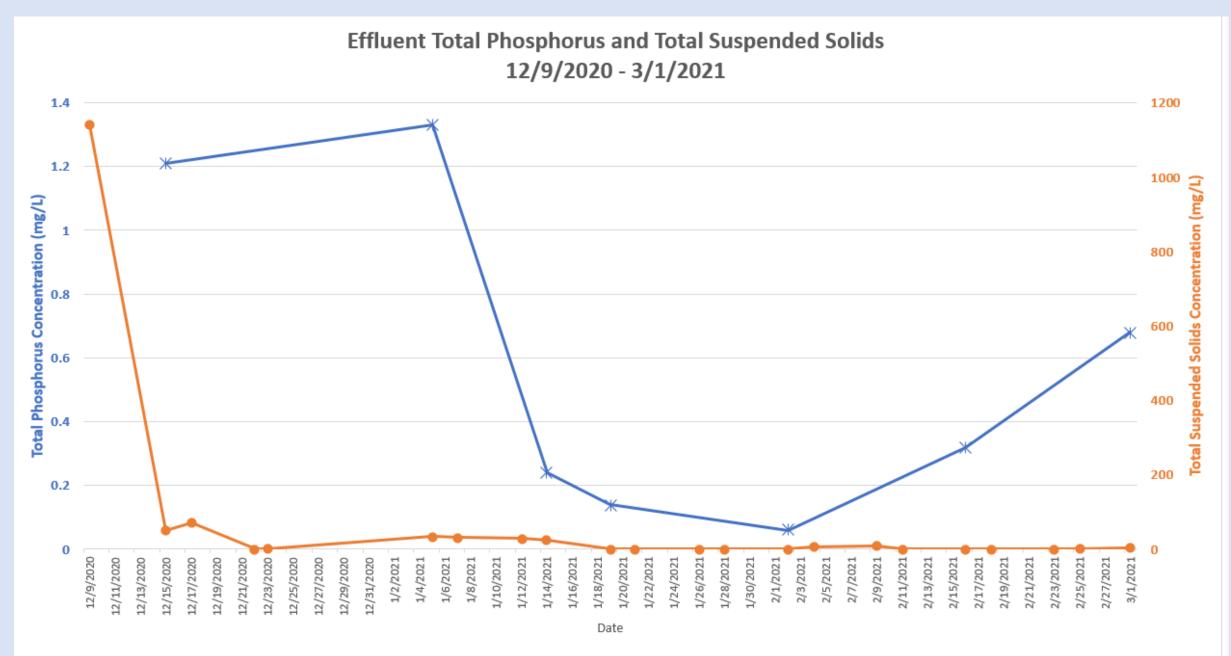
The DO probe was faulty, showing a higher (1-2 mg/L) in the second tank than what my handheld DO probe measured (around 0.5 mg/L)

The tank turned out to be DO limited

And a DO limited MLSS will let the ammonia slip into violation



Date



In summary,

Once we solved the low DO issue, the WWTP ran great

And by increasing the Mix/Fill cycle, we eliminated the chemicals...

...which will result in a huge cost savings

Better effluent water at a cheaper cost.

# Conventional Activated Sludge Biological Phosphorus Removal

#### Niles, Ohio Population: 18,500 6.2 MGD design flow



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In 2017, the City upgrades their WWTP from a typical extended aeration system to modern Biological Nutrient Removal system.

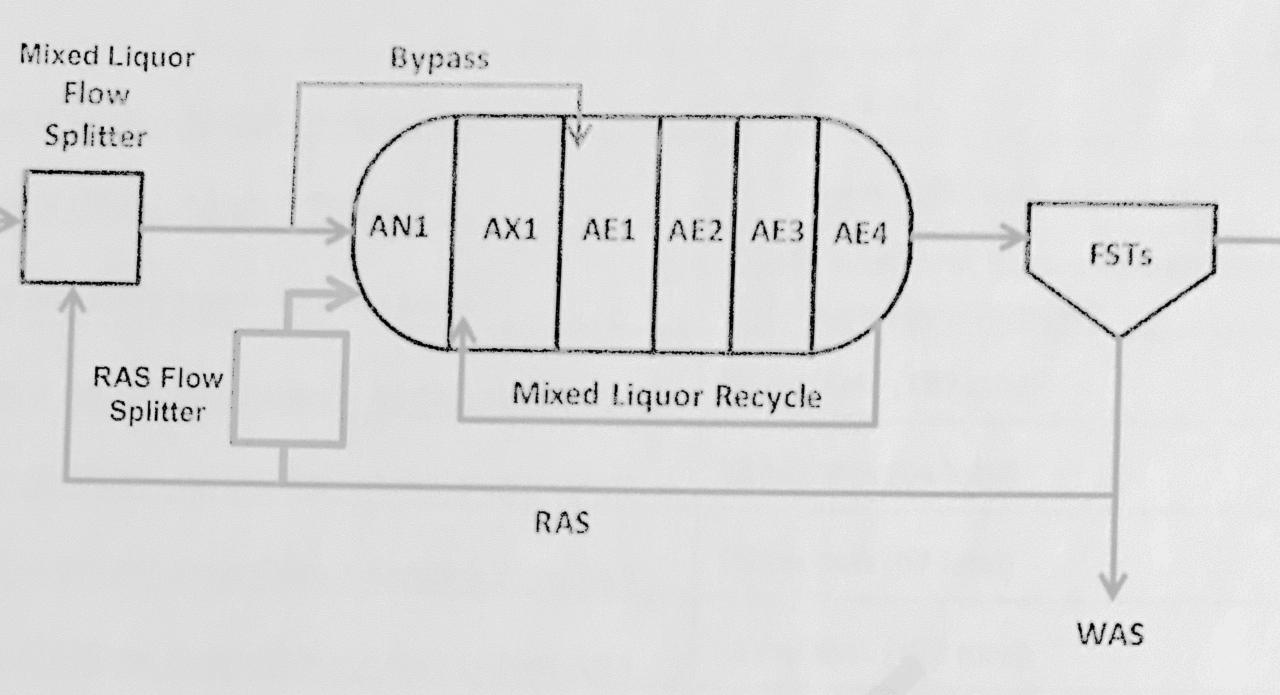
It was a needed rebuild of the heart of the WWTP:

Converted the diffused aeration ditches into 3 – 3 zone BNR tanks Constructed 3 big, new clarifiers

Converted anaerobic digestion to aerobic digestion

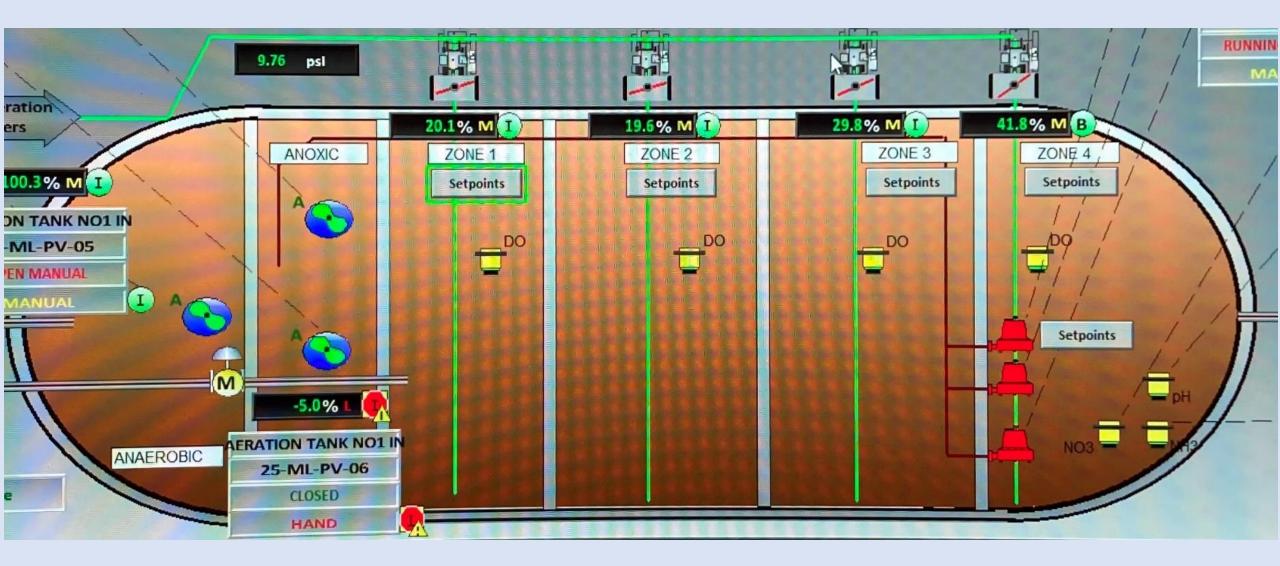
Constructed a new head works

#### It was very expensive













But the design engineers missed one thing:

The WWTP averaged less than 100 mg/L cBOD5 in their influent

There was not enough loading to drive the bacterial reactions that result in effective biological phosphorus removal

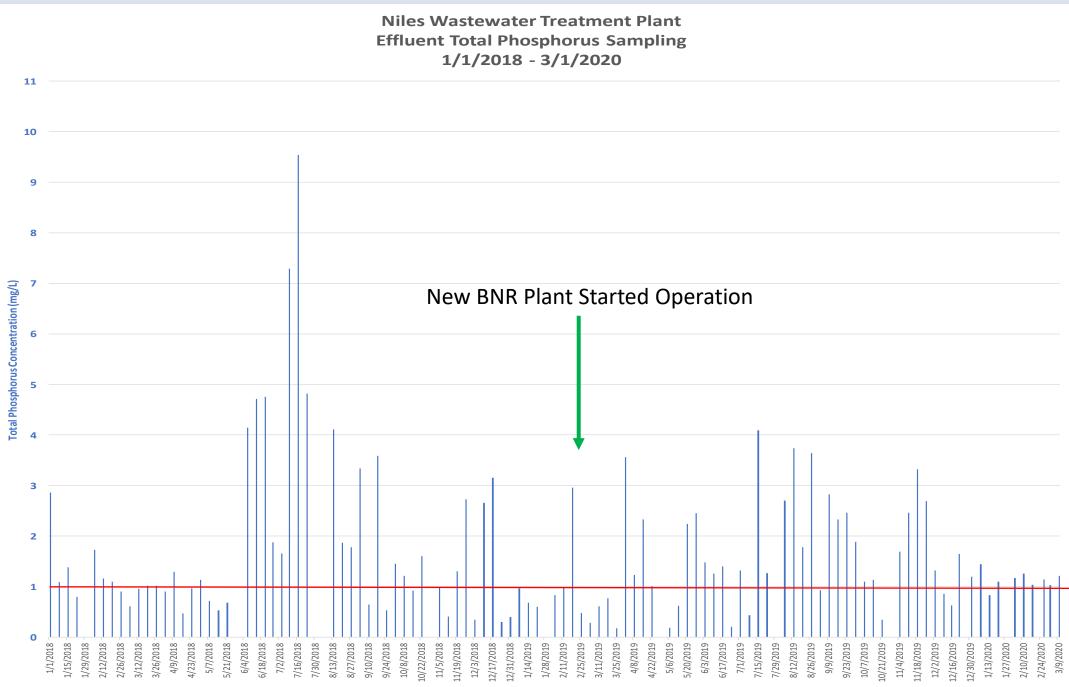
#### **Niles WWTP** Influent cBOD<sub>5</sub> 1/1/2018 - 3/1/2020 27 Month Average of 317 samples = 71.5 mg/L cBOD<sub>5</sub>

The Construction finished up in 2019.

The one-year SRF Certification Period began.

The only problem was that the new WWTP didn't reliably remove phosphorus

It met it's 1 mg/L monthly limit pretty randomly



Since the new WWTP started up, the treatment plant had only:

#### 13 of 49 samples under 1.0 mg/L PO<sub>4</sub>-P

The superintendent called me in late February 2020

I drove up, got a tour of the wwtp and then started to tell him about the success we had in Bradford

And what would be involved to implement it in Niles

Then **COVID-19** arrived on the scene

# And Ohio EPA field staff was grounded (including ME) on 3/18/2020

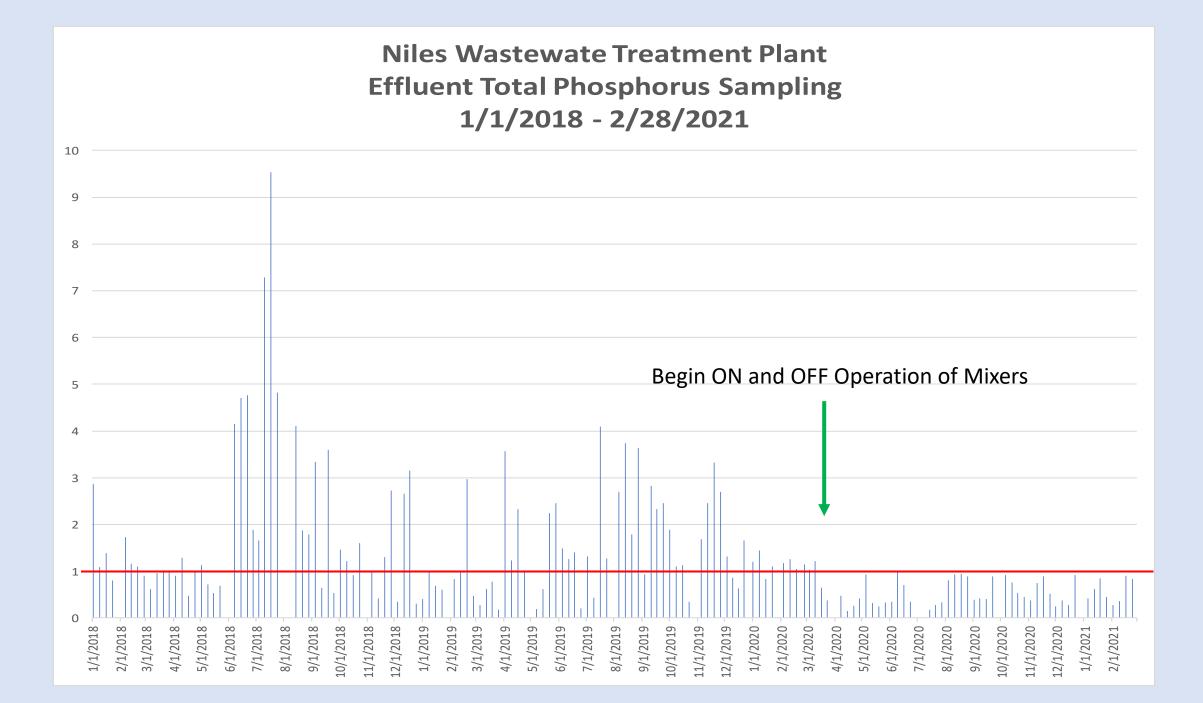
So, we started to troubleshoot noncompliance from a distance,

by Phone by Text by Email The Niles upgrade didn't have VFDs or timers on the mixers

But it was staffed 24/7

So the superintendent assigned treatment plant staff to Turn Mixers **OFF** for 3 hours Turn them back **ON** for 30 minutes

Just like Bradford



In that last year, the WWTP has been under 1.0 mg/L for <u>every</u> Total Phosphorus Sample that has been collected.

Total Phosphorus compliance is no longer a random event

It works, even with an influent  $cBOD_5$  of 73 mg/L

No chemicals are fed for phosphorus removal, either

(and they did install timers on the mixers...)

# **Process Control for Phosphorus Removal**

### Why do Process Control?

Process control procedures will tell you how well the WWTP is performing

Process control methods do not need to be difficult or complex

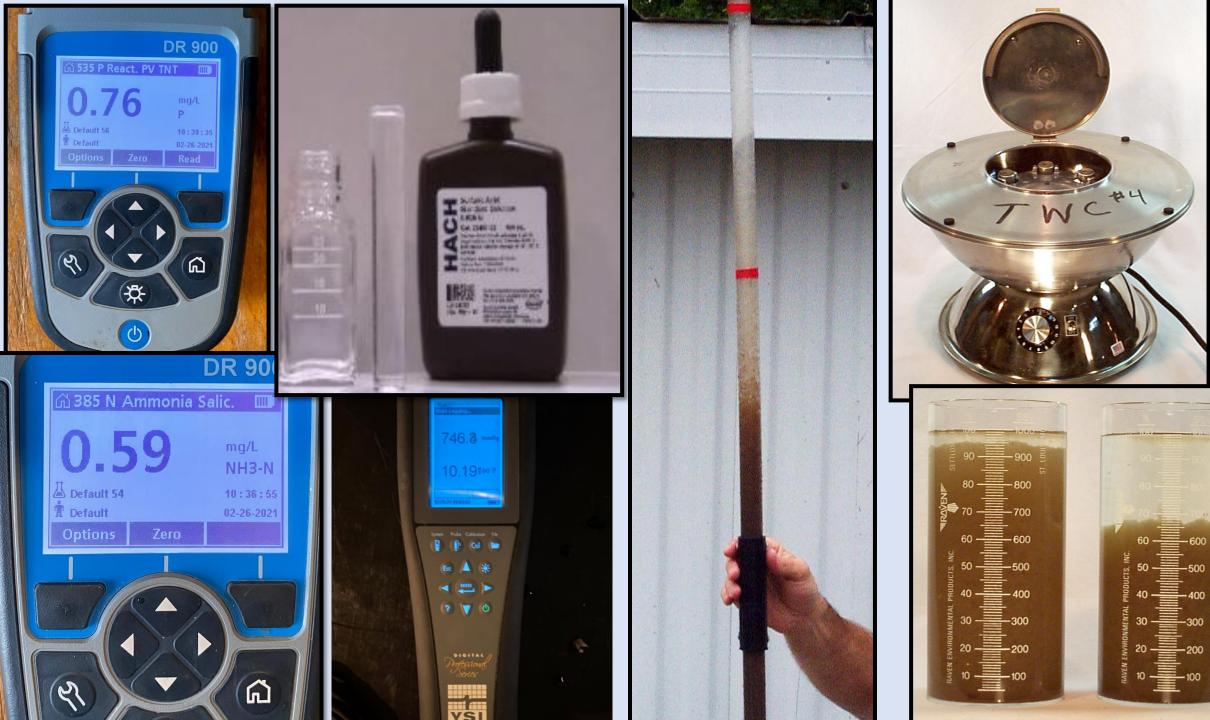
Process control methods should not take all day to get results

Process control should be performed at the WWTP, not sent to a outside lab.

## The CAU Process Control Tools

These tools are cheap, easy, and effective

- 1) Multiparameter colorimeter
- 2) Dissolved Oxygen Meter
- 3) Alkalinity Test Kit
- 4) Wastewater Centrifuge
- 5) Settleometer
- 6) Core sampler



#### The CAU Process Control Tools

These tools are cheap, easy, and effective

Cheap, because most communities do not have a lot cash

Easy, because if it is difficult, then no one will do it

Effective, because if it is not effective, then why bother?

## Why do Process Control?

Effective process control will alert you to when your WWTP begins to move toward noncompliance.

It will give you the data that you need to make the process control decisions that will move the WWTP back toward the middle of the Operational Window and stay in compliance.

Process Control is especially important for effective Biological Phosphorus Removal

### **Process Control for Effective BioP Removal**

Most failures of BioP Removal that I find are:

Too much nitrate in anaerobic environments

Not enough cBOD to drive the orthophosphate release

Not enough DO to drive the orthophosphate uptake

### **Process Control for Effective BioP Removal**

For effective BNR Process Control:

1) Measure nitrate and orthophosphate in the anaerobic environment

- 2) Measure nitrate and orthophosphate in the anoxic environment
- 3) Measure ammonia, nitrate, orthophosphate and DO in the oxic environment

# **Questions?**

Jon van Dommelen Ohio EPA – DEFA –CAU (614) 580-5069 jon.vandommelen@epa.ohio.gov