FLUID MECHANICS

A fluid is a substance that can flow when external force is applied on it. The term fluids include both liquids and gases. Though liquids and gases are termed as fluids, there are marked differences between them. For example, gases are compressible whereas liquids are nearly incompressible. We only use those properties of liquids and gases, which are linked with their ability to flow, while discussing the mechanics of fluids.

Pressure = Force / Area

• MKS system N/m²

Pressure due to a líquíd column

Let h be the height of the liquid column in a cylinder of cross-sectional area A. If ho is the density of the liquid, then weight of the liquid column W is given by-

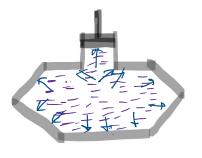


Relative Density

Relative density of a substance is defined as the ratio between the density of the substance to the density of water at <u>4°C</u>. Relative density is also known as specific gravity

Pascal's law

Pascal's law states that if the effect of gravity can be neglected then the pressure in a fluid in equilibrium is the same everywhere.

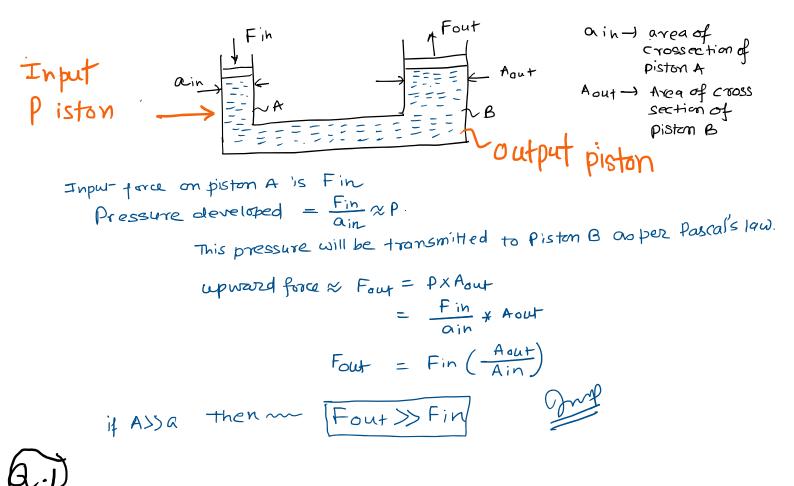


Application - Hydraulic Lift - Hydraulic Press - Hydraulic brakes.

Hydraulic Lift (Application of Pascal's Law)

The most useful feature of fluid power is the ease with which it is able to multiply force. This is accomplished by using an output piston that is larger than the input piston. Such a system is shown in Fig





A hydraulic lift is used to lift cars of up to 3500 kg of mass. The platform of the lift has a mass of 500 kg. The smaller cylinder has a diameter of $d_1 = 25$ cm. If the maximum force that the operator can apply on this cylinder is $F_1 = 100$ N, find the diameter of the larger cylinder.

total mass (Uith) ~ F = 100 M F = 100 M $F = 4000 \times 10 \text{ M}$ We know that We know that $W = F \text{ out} = F \text{ in } \frac{A \text{ out}}{A \text{ in}}$ $A_{\text{out}} = \frac{F_{\text{out}}}{F_{\text{in}}} \times A \text{ in}$ $A_{\text{out}} = \frac{F_{\text{out}}}{I + 0} \times A \text{ in}$ $A_{\text{out}} = \frac{F_{\text{out}}}{I + 0} \times A \text{ in}$ $R^2 = \frac{4000 \text{ M}^2}{I + 0}$ $R^2 = 400 \text{ M}^2$ $R = \sqrt{400} \times 10^2$ $R = \sqrt{400} \times 10^2$ $D = 400 \text{ M}^2$ $= 500 \text{ cm} \text{ AM}^2$

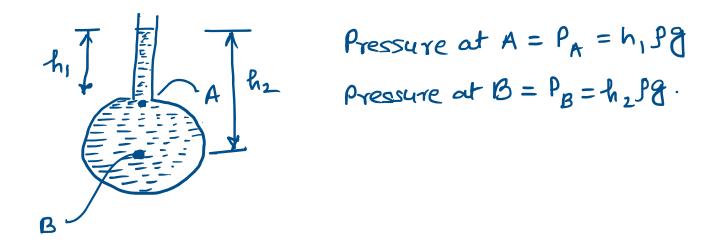
Pressure Measurement by Manometer

The relationship between pressure and head is used to measure pressure with a manometer

The Piezometer Tube Manometer

The simplest manometer is a tube, open at the top, which is attached to the top of a vessel containing liquid at a pressure (higher than atmospheric) to be measured.

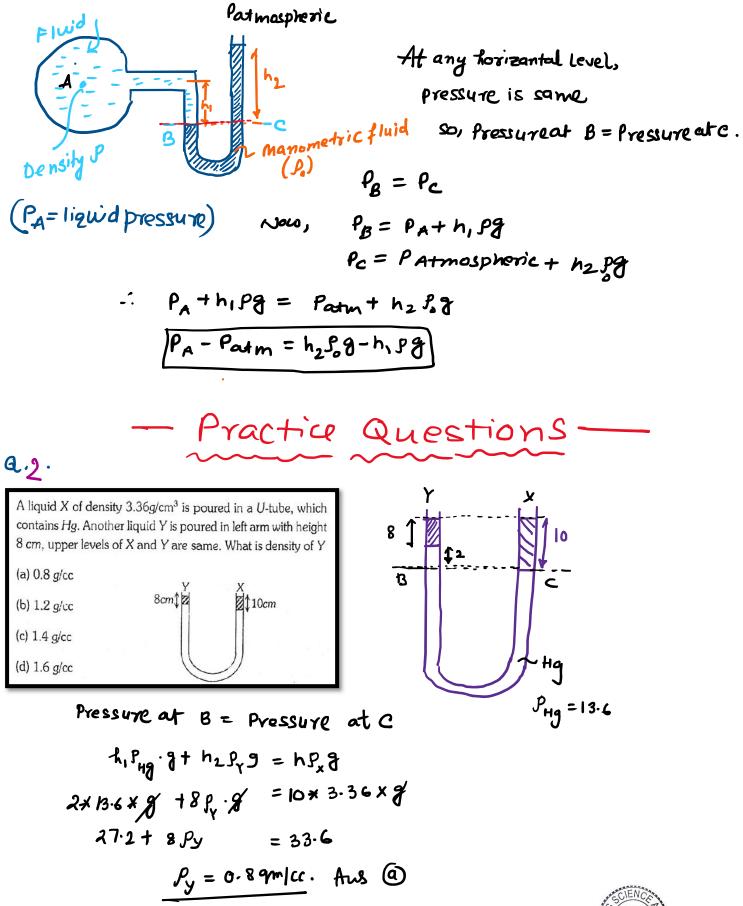
An example can be seen in the figure below. This simple device is known as a Piezometer tube. As the tube is open to the atmosphere the pressure measured is relative to atmospheric so is gauge pressure.



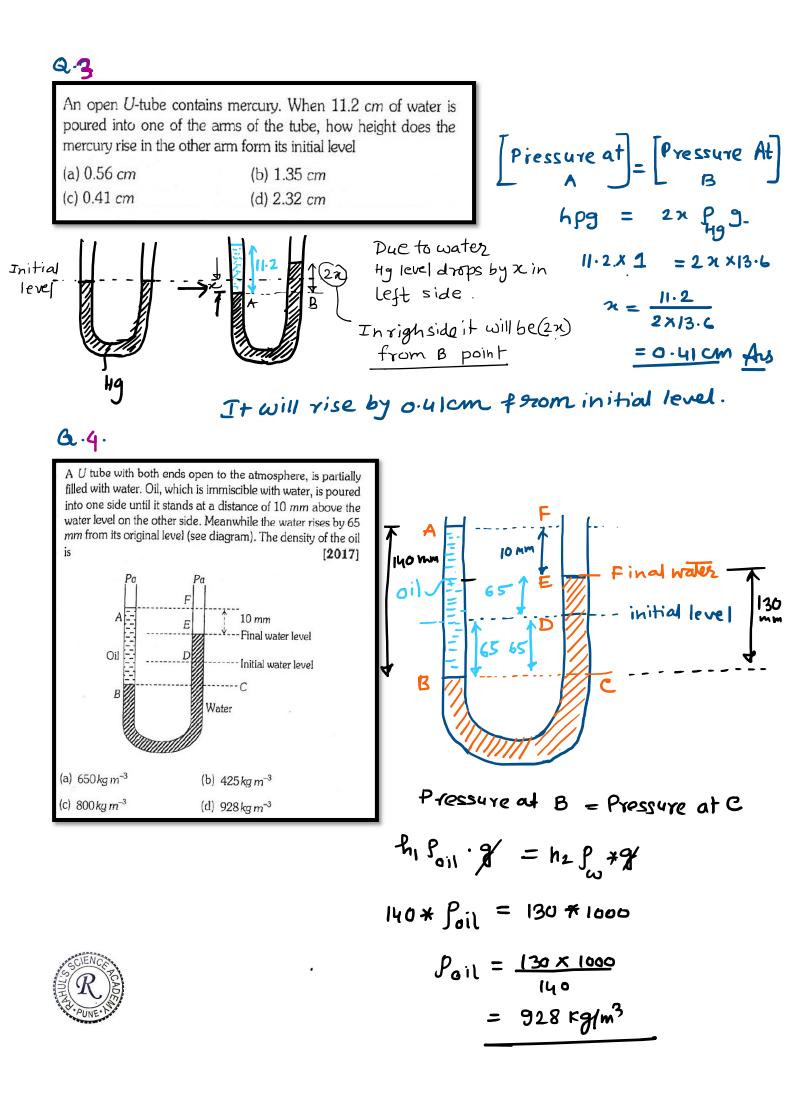
The "U"-Tube Manometer

Using a "".-Tube enables the pressure of both liquids and gases to be measured with the same instrument. The "" is connected as in the figure below and filled with a fluid called the manometric fluid. The fluid whose pressure is being measured should have a mass density less than that of the manometric fluid and the two fluids should not be able to mix readily - that is, they must be immiscible.

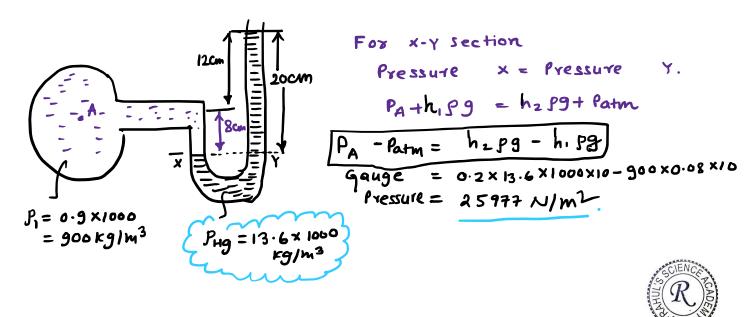






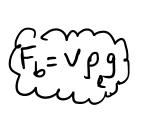


The right limb of a simple 11 tube manometer containing mercury is open to the atmosphere while the left limb is connected to a pipe in which a fluid of sp. Gr. 0.9 is flowing. The center of the pipe is 12 cm below the level of mercury in the right limb. Find the pressure of fluid in the pipe if the difference of mercury in the two limbs is 20 cm.

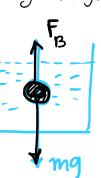


<u>Archímedes' Príncíple</u>

Archimedes' Principle states that when an object is immersed fully or partially in a liquid, it experiences an upward force which is equal to the weight of liquid displaced by the object

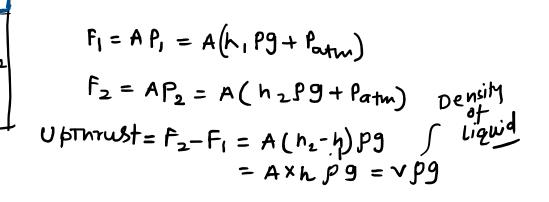


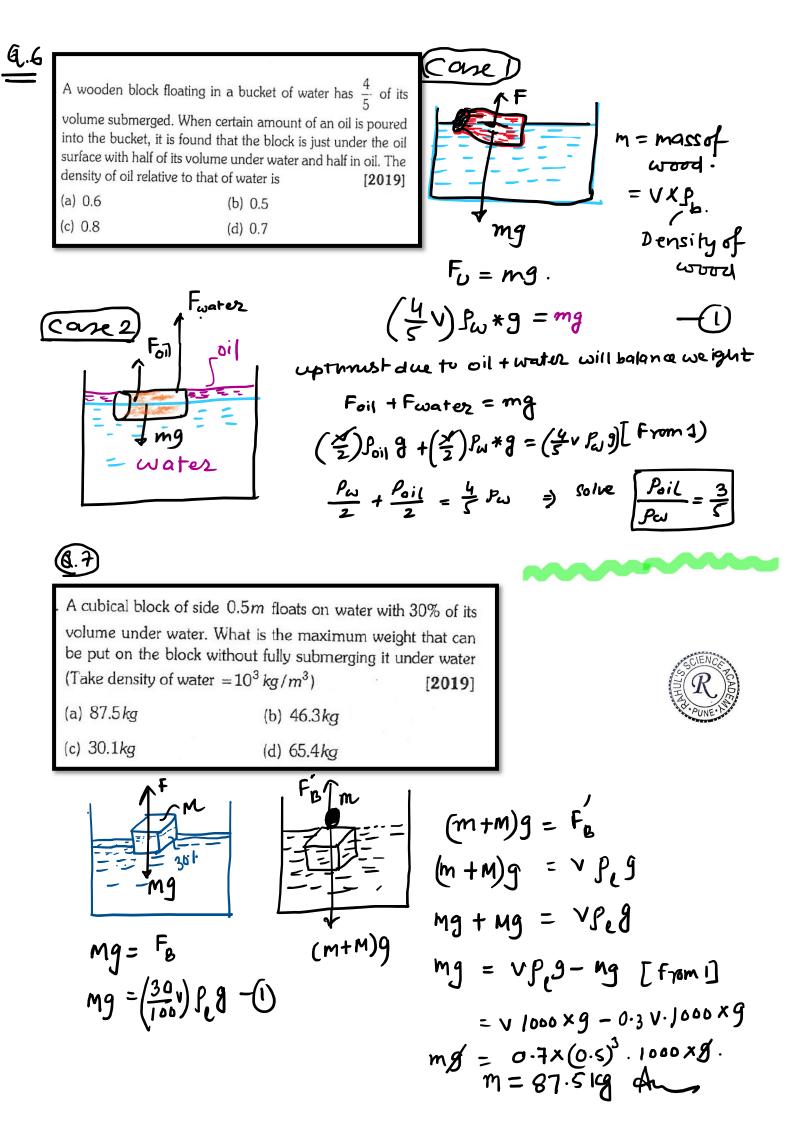
 $(-h = h_2 - h_1)$



Fb = buoyancy = v Peg volume of



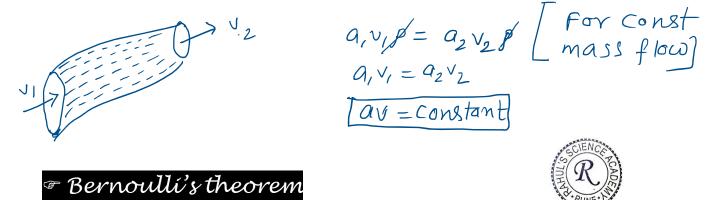




Continuity Equations

Consider a non-viscous liquid in streamline flow through a tube AB of varying cross section as shown in Fig. Let a_1 and a_2 be the area of cross section, v1 and v2 be the velocity of flow of the liquid at A and B respectively.

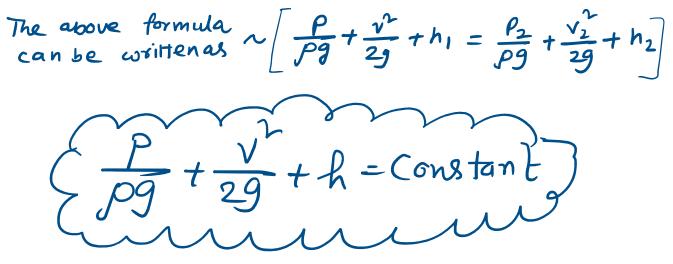
Volume of líquid entering per second at $A = a_1v_1$. If ρ is the density of the líquid, then mass of líquid entering per second at $A = a_1v_1\rho$. Similarly, mass of líquid leaving per second at $B = a_2v_2\rho$.



According to Bernoulli's theorem, for the streamline flow of a non-viscous and incompressible liquid, the sum of the pressure energy, kinetic energy and potential energy per unit mass is a constant.

$$\frac{p}{p} + \frac{\sqrt{2}}{2} + hg = constant$$

This equation is known as Bernoulli's equation.



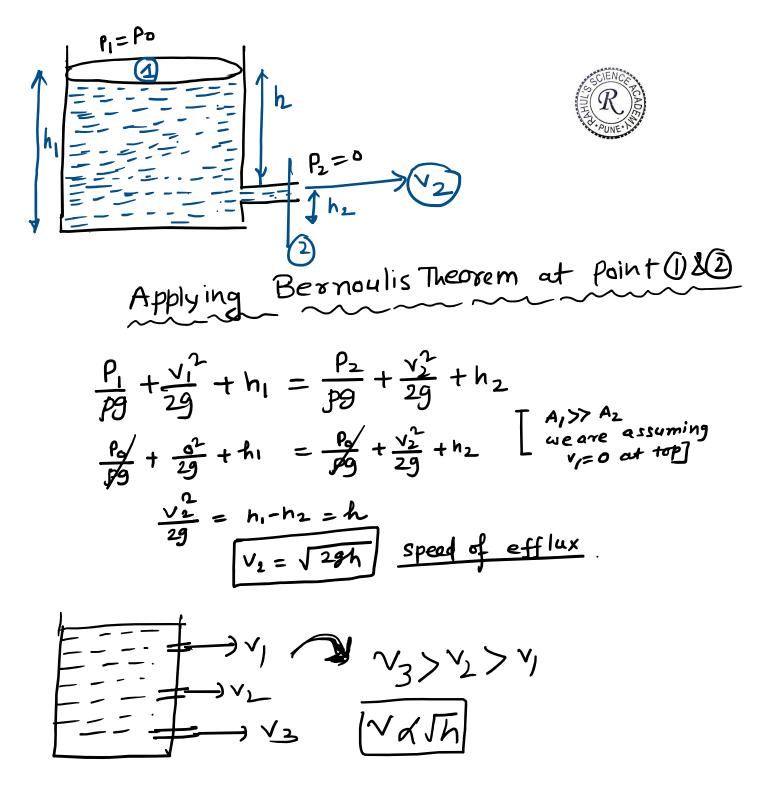
Proof
Proof
Proof
Prove and level.
Styreamline flow.
Form continuity e2ⁿ
alv₁ = a₂v₂ [mass flow
constant]

$$= v = \frac{m}{p}$$

Styreamline flow.
Force acting on liquid at $A = P_1 a_1$
work done per sec on liquid at $A = P_1 a_1 u_1 = P_1 V$
gimikry,
work done per sec on liquid at $B = P_2 a_2 u_2 = P_2 V$
Net work done per second on the liquid by the
pressure energy in moving the liquid from A toB
 $= P_1 V - P_2 V$
Increase in KE/see of the liquid = $\frac{1}{2}mv_2^2 - \frac{1}{2}mv_1^2$
Increase in PE = mgh_2-mgh_1
Now by the law of conservation of
Mee hanical Energy
 $dW = AU + dK$
 $P_1 V + mgh_1 + \frac{1}{2}v_1^2 = \frac{P_1 V}{m} + gh_2 + \frac{1}{2}w_2^2$
 $\frac{P_1 V + gh_1 + \frac{1}{2}v_1^2}{\frac{P_1 + gh_2}{2} + \frac{1}{2}w_2} = \frac{P_1 M_1}{2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}v_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2} = \frac{P_2 M_1}{2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2} = \frac{P_2 M_1}{2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_1 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_2 + \frac{1}{2}w_1^2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$
 $\frac{P_1 + gh_2}{\frac{P_2 + gh_2}{2} + \frac{1}{2}w_2}$

[©] Torrícellí's law

Torricelli's law, also known as Torricelli's theorem, is a theorem in fluid dynamics relating the speed of fluid flowing out of an opening to the height of fluid above the opening



Let's understand this concepts by solving few more numerical.....

10)	The top of a water tank is open to air and its water level is maintained. It is giving out $0.74m^3$ /min water per minute through a circular opening of 2cm radius in its wall. The depth of the centre of the opening from the level of water in the tank is close to [2019] (a) $2.9m$ (b) $9.6m$ (c) $4.8m$ (d) $6.0m$ $G = A \cdot \sqrt{9}$ $G = A \cdot \sqrt{9}$ $G = \pi \sqrt{2} \cdot \sqrt{9}$	$Q = 0.74 \text{ m}^3/\text{min}$ = $\frac{0.74}{60} \text{ m}^3/\text{sec}$.
I)	velocity - 9.81mlc	$v = \sqrt{2gh}$ $h = \frac{v^2}{2g} = \frac{9.8I^2}{2*9.8I} = 4.8m$
Ζ	$A = I con^{2}$ $= I o^{2} m^{2}$	Volume flow, $Q = area \times Velocity.$ $= A * \sqrt{29h}$ $h = \frac{Q^2}{A^2} = \frac{(10^4)^2}{(10^4)^2} \times 9.81$ = 5.1 cm Aus

12) Water is filled in a cylindrical container to a height of 3m. The ratio of the cross-sectional area of the orifice and the beaker is 0.1. The square of the speed of the liquid coming out from the orifice is $(g = 10 m/s^2)$ [2005] $\frac{Given}{A} = 0.1$ (a) 50 m^2/s^2 (b) 50.5 m²/s² 3m (c) $51 m^2/s^2$ (d) 52 m^2/s^2 $Av_1 = Av_2$ [continuity] $v_1 = \frac{A}{A} \cdot v_2$ eqn. Applying Bernoulis theorem for (120) $\frac{P}{Pg} + \frac{V_1^2}{2g} + h_1 = \frac{P_2}{Pg} + \frac{V_2^2}{2g} + h_2 \begin{bmatrix} P_1 = P_2 = atmospheric \text{ pressure} \\ Both are open \end{bmatrix}$ $\left(\frac{A}{A}\right)^{2}\frac{v_{1}^{2}}{24} + h_{1} = \frac{v_{2}^{2}}{2g} + h_{2}$ $h_1 - h_2 = \frac{V_2^{2}}{2g} - \left(\frac{a}{A}\right)^{2} \cdot \frac{V_2^{2}}{2g}$ $h = \frac{\sqrt{2}}{2g} \left\{ 1 - \left(\frac{a}{A}\right)^{2} \right\}.$ $V_{2}^{2} = \frac{2gh}{1 - \left(\frac{a}{A}\right)^{2}} = \frac{2 \times 10 \times (3 - 0.525)}{1 - (0.1)^{2}}$ $V_{2}^{2} = 50 (m/s)^{2} Avs$ Note} if a<<A Then v= J2gn (use) if a ~ some const $v = \sqrt{\frac{2gh}{1 - \frac{a}{2}}} \in use This$

(3) A large open tank has two holes in the wall. One is a square hole of side L at a depth y from the top. When the tax is completely filled with water the quantities of water flowing out per second from both the holes are the same. Then R is equal to [2000]
(a)
$$2\pi L$$
 (b) $\frac{L}{2\pi}$
(c) L (d) $\frac{L}{2\pi}$
(c) L

15)

19

A submarine experiences a pressure of $5.05 \times 10^6 Pa$ at a depth of d_1 in a sea. When it goes further to a depth of d_2 , d, ρ= 5.05×16 Pa it experiences a pressure of $8.08 \times 10^6 \, Pa$. Then $d_2 - d_1$ is d2 (density of water = $10^3 kg/m^3$ and approximately acceleration due to gravity $= 10 m s^{-2}$) [2019] P2=8.08×166Pa (a) 400m (b) 500m (c) 600m (d) 300m $P_2 - P_2 = h_2 P_3 - h_1 P_3$ -h,= 303m h2 $=(h_2-h_1)pg$ Water flows in a horizontal tube (see figure). The pressure of water changes by 700 Nm⁻² between A and B where the area of cross section are 40 cm² and 20 cm², respectively. Find the rate of flow of water through the tube. (density of water = 1000 kgm⁻³) [2020] A В 20cm 40 cm $A_1 \vee_1 = A_2 \vee_2$ $40 \times \vee_1 = 20^{\vee} \Sigma$ (a) 2720 cm³/s (b) 2420 cm³/s (c) 3020 cm³/s (d) 1810 cm³/s Applying. Bernoulis ezh beth (18)

$$\frac{P_{1}}{Pg} + \frac{v_{1}^{2}}{2g} + \frac{v_{1}}{2g} + \frac{v_{2}}{2g} + \frac{v_{1}^{2}}{2g} + \frac{v_{1}}{2g} + \frac{v_{1}}{2g} + \frac{v_{1}^{2}}{10pp\times 10} = \frac{v_{1}^{2}}{2xy0} \left(1 - \frac{1}{4}\right)$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{2}^{2}}{2g} - \frac{v_{1}^{2}}{2g} + \frac{v_{1}}{2g}$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{2}^{2}}{2g} - \frac{v_{1}^{2}}{2g} + \frac{v_{1}}{2g}$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{2}^{2}}{2g} - \frac{v_{1}^{2}}{2g} + \frac{v_{1}}{2g}$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{2}^{2}}{2g} + \frac{v_{1}^{2}}{2g} + \frac{v_{1}^{2}}{2g} + \frac{v_{1}^{2}}{2g} + \frac{v_{1}^{2}}{15} = \frac{v_{2}^{2}}{2} + \frac{v_{1}}{4}$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{2}^{2}}{2g} + \frac{v_{1}^{2}}{2g} + \frac{v_{1}^{2}}{2g} + \frac{v_{1}^{2}}{2g} + \frac{v_{1}^{2}}{15} = \frac{v_{2}^{2}}{2}$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{1}^{2}}{2g} + \frac{v_{1}^{2}}{4 + 2g}$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{1}^{2}}{2} + \frac{v_{1}^{2}}{4} + \frac{v_{1}^{2}}{2}$$

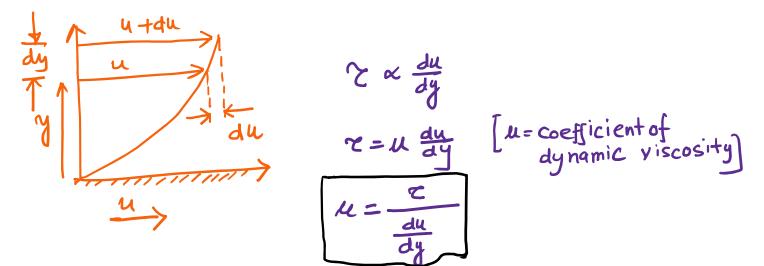
$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{1}^{2}}{2} + \frac{v_{1}^{2}}{4} + \frac{v_{1}^{2}}{2}$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{1}^{2}}{2} + \frac{v_{1}^{2}}{4} + \frac{v_{1}^{2}}{2}$$

$$\frac{P_{1} - P_{2}}{Pg} = \frac{v_{1}^{2}}{2} + \frac{v_{1}^{2}}{4} + \frac{v_{1}^{2$$



Viscosity is defined as the property of fluid which offers resistance to the movement of one layer of fluid over another adjacent layer of fluid. When two layers of fluid, a distance 'dy' apart, move one over other a different velocity, say u and u+du as shown in figure, the viscosity together with relative velocity causes a shear stress acting between two fluids.



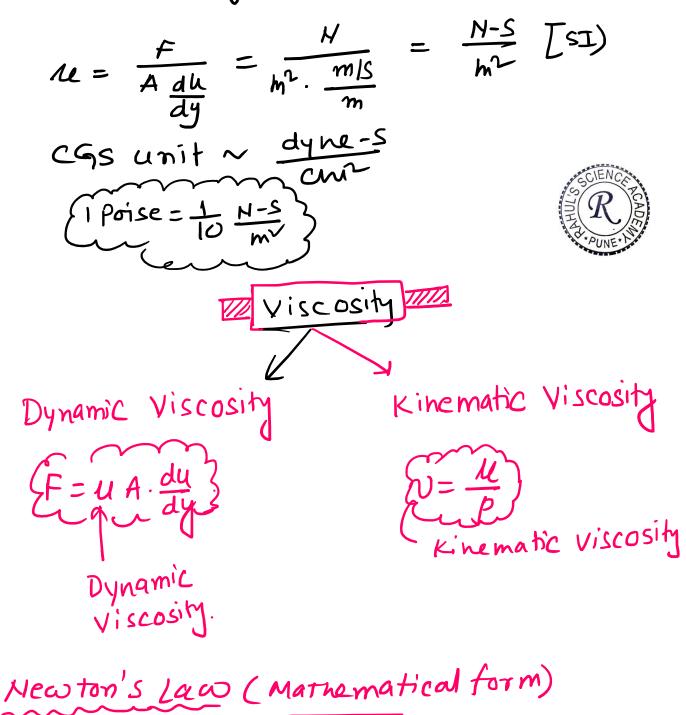
Víscosíty ís also defined as the shear stress required to produce unit rate of shear straín

$$\begin{aligned} \mathcal{Z} &= \mathcal{U} \cdot \frac{du}{dy} \\ \frac{f}{A} &= \mathcal{M} \cdot \frac{du}{dy} \\ F &= \mathcal{U} A \cdot \frac{du}{dy} \cdot if \quad A &= 1 \text{ m}^2 \\ \frac{dy}{dy} &= 1 \text{ s}^1 \\ \text{Then } F &= \mathcal{U} \end{aligned}$$

The coefficient of viscosity of a liquid is numerically equal to the viscous force acting tangentially between two layers of liquid having unit area of contact and unit velocity gradient normal to the direction of flow of liquid.



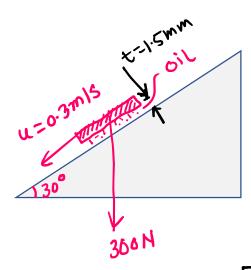
Units of Viscosity



$$F = \mathcal{U}A \frac{du}{dy}$$

Ð

Calculate the dynamic viscosity of an oil, which is used for lubrication between a square plate of size 0.8m x0.8m and an inclined plane with angle of inclination 30 degree. The weight of the square plate is 300 N and it slides down the inclined plane with uniform velocity of 0.3 m/s. the thickness of oil film is 1.5 mm $\Delta = 0.8 \times 0.8 = 0.64 \text{m}^{2}$



Force which is causing shear is my sind 30° sint 300050 : F = 300 sin 0 300K) = 300 Sin30 - 150 H

 $F = \mathcal{U}A \cdot \frac{du}{dy} = \frac{150 = \mathcal{U}*(0.64)*}{1.5\times10^{3}} + \frac{0.3}{1.5\times10^{3}}$ $\mathcal{U} = \frac{150\times1.5\times10^{3}}{0.64\times0.3}$ = 1.17 N-s/m2 11.7 poise And

81

A square plate of 0.1 m side moves parallel to a second plate with a velocity of 0.1 m/s, both plates being immersed in water. If the viscous force is 0.002 N and the coefficient of viscosity is 0.01 *poise*, distance between the plates in m is

(a) 0.1	(b) 0.05	
(c) 0.005	(d) 0.0005	

Soln

 $\mathcal{C} = \mathcal{U} \cdot \frac{dy}{dy}$ $\frac{dy}{dy} = \frac{\mathcal{U}}{\mathcal{L}} \frac{du}{\mathcal{L}}$



12=0.01 poise = 0.001 HS/m

$$= \frac{4 \times A}{F} \cdot du$$

$$= \frac{0 \cdot 001 \times (0 \cdot 1 \times 0 \cdot 1) \cdot 0 \cdot 1}{0 \cdot 002}$$

$$= 0 \cdot 0005 \text{ m}$$

<mark>Stokes Law</mark>

When a body falls through a highly viscous liquid, it drags the layer of the liquid immediately in contact with it. This results in a relative motion between the different layers of the liquid.

As a result of this, the falling body experiences a viscous force F. Stoke performed many experiments on the motion of small spherical bodies in different fluids and concluded that the viscous force F acting on the spherical body depends on

(i) Coefficient of viscosity μ of the liquid

(*íí*) Radíus a of the sphere and

(ííí) Velocíty v of the spherícal body. Dímensíonally ít can be proved that

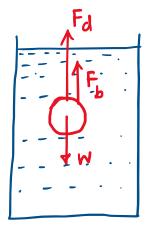
 $F_d = 6\pi \mu a v$ by:

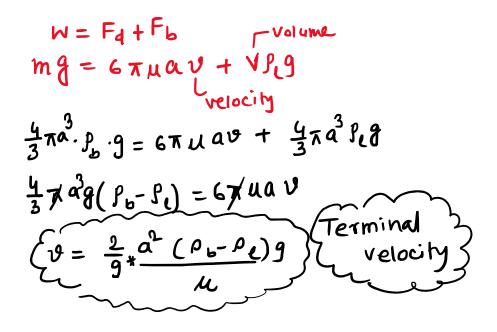
Terminal Velocity

Fa = 6 TH av Stoke's Drag Formula

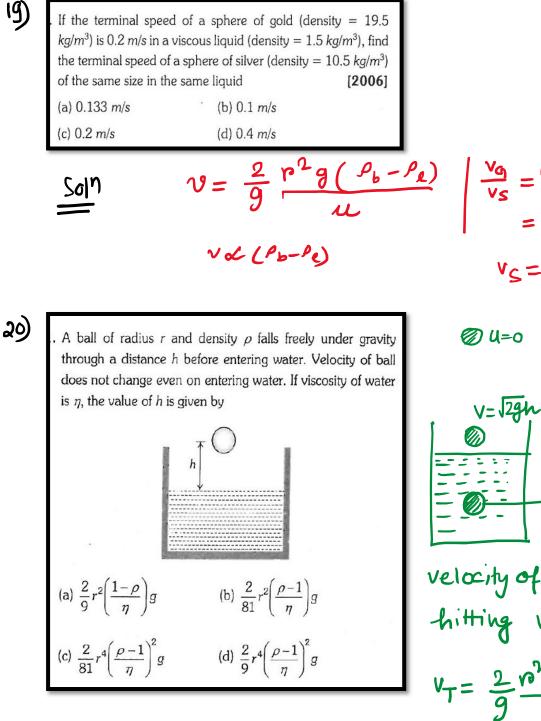


Consider a metallic sphere of radius 'a' and density ρ_l to fall under gravity in a liquid of density ρ_b . The viscous force F acting on the metallic sphere increases as its velocity increases. A stage is reached when the weight W of the sphere becomes equal to the sum of the upward viscous force F_d and the upward thrust F_b due to buoyancy. Now, there is no net force acting on the sphere and it moves down with a constant velocity v called terminal velocity









$$\frac{V_{G}}{V_{S}} = \frac{19 \cdot 5 - 1 \cdot 5}{10 \cdot 5 - 1 \cdot 5}$$
$$= \frac{18}{9} = 2$$
$$V_{S} = \frac{V_{G}}{2} = 0.1 \text{ m/s}$$

 $\sqrt{\tau}$

velocity of ball before hitting V= J2gh.

$$V_{T} = \frac{2}{9} \frac{n^{2}g(P_{L}-1)}{n}$$

: Velocity does not change

$$\sqrt{2gh} = \frac{2n^2q(f_b-1)}{9} \frac{1}{n}$$

$$h = \frac{2}{81} r^4 \left(\frac{f_b-1}{n}\right)^2 q \cdot f_{m} q$$

A solid sphere of radius R acquires a terminal velocity v_1 $\int_{0}^{0} M = \int_{0}^{1} \frac{4}{3} \pi R^{3}.$ when falling (due to gravity) through a viscous fluid having a coefficient of viscosity η . The sphere is broken into 27 identical solid spheres. If each of these spheres acquires a $O = \frac{4}{3}\pi R^3 = 27(\frac{4}{3}\pi r^3)$ terminal velocity v_2 when falling through the same fluid, the ratio (v_1 / v_2) equals [2019] Radius of $\sim \left[r = \frac{R}{3} \right]$ (a) 27 (b) 1/27 (c) 1/9 (d) 9 $v_{\tau} \propto (Radius)^2$ $\frac{V_T}{V_{\text{NeW}}} = \frac{R^2}{(R_{3})^2} = 9.$ JEE-2019 Thew = y thus Time Required to empty a tank @ volume coming out per second, $\frac{dv}{dt} = A_0 \gamma$ $\frac{dv}{dL} = A_0 \sqrt{2g\gamma}$ Ao $= \sqrt{2gy}$ NOW dv = Ady $A \cdot \frac{dy}{dt} = A_0 \sqrt{2gy}$ $dt = \frac{4}{A_0} \frac{1}{\sqrt{2g}} \frac$ $\int dt = \frac{A}{A_0} \int_{\frac{1}{2q}} \int \frac{-1}{2} \frac{1}{4y} \frac{1}{4y}$ time taken to fall height Hito H' $t = \frac{A}{A_0} \frac{1}{\sqrt{2g}} \cdot \int_{1}^{H_f} \frac{1}{\sqrt{2g}} dt = \frac{A}{A_0} \sqrt{\frac{2}{9}} \left(\sqrt{H} - \sqrt{H_f} \right)$

If the hole is is at the bottom of the tank, then time required to empty the tank is given by



Units.

$$\begin{bmatrix} 1Pa = 1N/m^{2} \\ 1Psi = 7.015 \times 10^{3} Pa \\ 1atm = 760 mmof Hg = 1.013 \times 10^{5} Pa \\ 1Bat = 10^{5} Pa \\ 1Torr = 1mm of Hg \end{bmatrix}$$

Lamínar Flow

The flow is said to be steady, stream line or laminar if every particle of the liquid follows exactly the path of its preceding particle and has the same velocity of its preceding particle at every point



Crítical velocity: velocity up to which it is streamlined

Turbulent

When the velocity of a liquid exceeds the critical velocity. The path and velocities of the liquid become disorderly. At this stage the flow loses all its orderliness and is called turbulent.



Reynold's Number (Re)

It is a dimensionless number comprised of the physical characteristics of the flow. An increasing Reynolds number indicates an increasing turbulence of flow.

It is defined as:

TO_density



Lamínar flow: For practical purposes, if the Reynolds number is less than 2000, the flow is laminar. The accepted transition Reynolds number for flow in a circular pipe is **Re = 2300.**

<mark>Transítíonal flow:</mark> At Reynolds numbers between about 2000 and 4000 the flow ís unstable as a result of the onset of turbulence. These flows are sometímes referred to as transítíonal flows.

Turbulent flow: If the Reynolds number is greater than 3500, the flow is turbulent. Most fluid systems in nuclear facilities operate with turbulent flow.

23)

Water from a pipe is coming at a rate of 100 liters per minute. If the radius of the pipe is 5 cm, the Reynolds number for the flow is the order of (density of water = 1000 kg/m^3 , coefficient of viscosity of water = 1mPas) [2019] (a) 10^6 (b) 10^4 (c) 10^3 (d) 10^2 So M Rate of volume $flow = \pi \pi^3 = 100 \text{ l/min}$

$$Re = \frac{PVD}{u}$$
$$= \frac{1000 \times \frac{2}{3\pi} \cdot \frac{10 \times 10^{2}}{10^{3}}}{10^{3} \times 2}$$
$$= \frac{10^{4} \times 2}{10^{4} \times 2}$$

 $= \frac{2}{3\pi} \text{ m/s}$

 $V = \frac{100 \times 10^3}{60} \frac{1}{21100}$



24)

The water flows from a tap of diameter 1.25 cm with a rate of $5 \times 10^{-5} m^3 s^{-1}$. The density and coefficient of viscosity of water are $10^3 kg m^{-3}$ and 10^{-3} Pas, respectively. The flow of water is

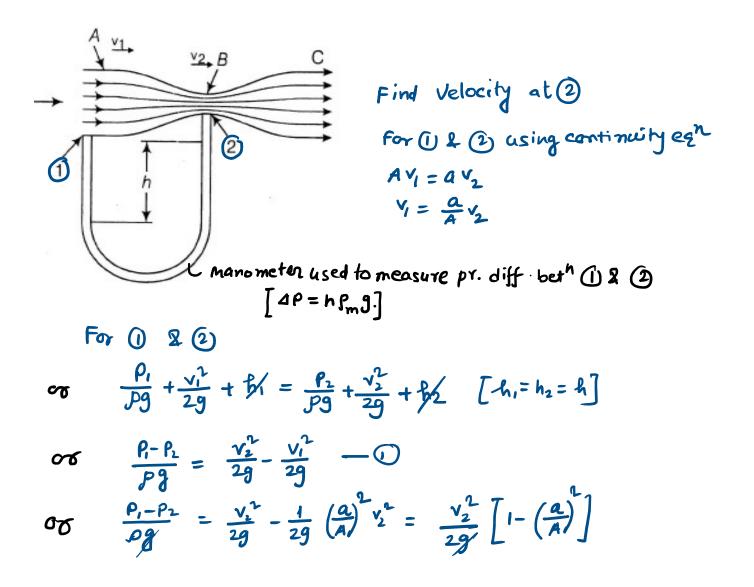
(a) Steady with Reynolds number 5100

- (6) Turbulent with Reynolds number 5100
- (c) Steady with Reynolds number 3900
- (d) Turbulent with Reynolds number 3900





It is used to measure flow of liquid in tube





$$P - density of flowing flow
P - density of flowing flowing flow
P - density of flowing fl$$

•