

### System design

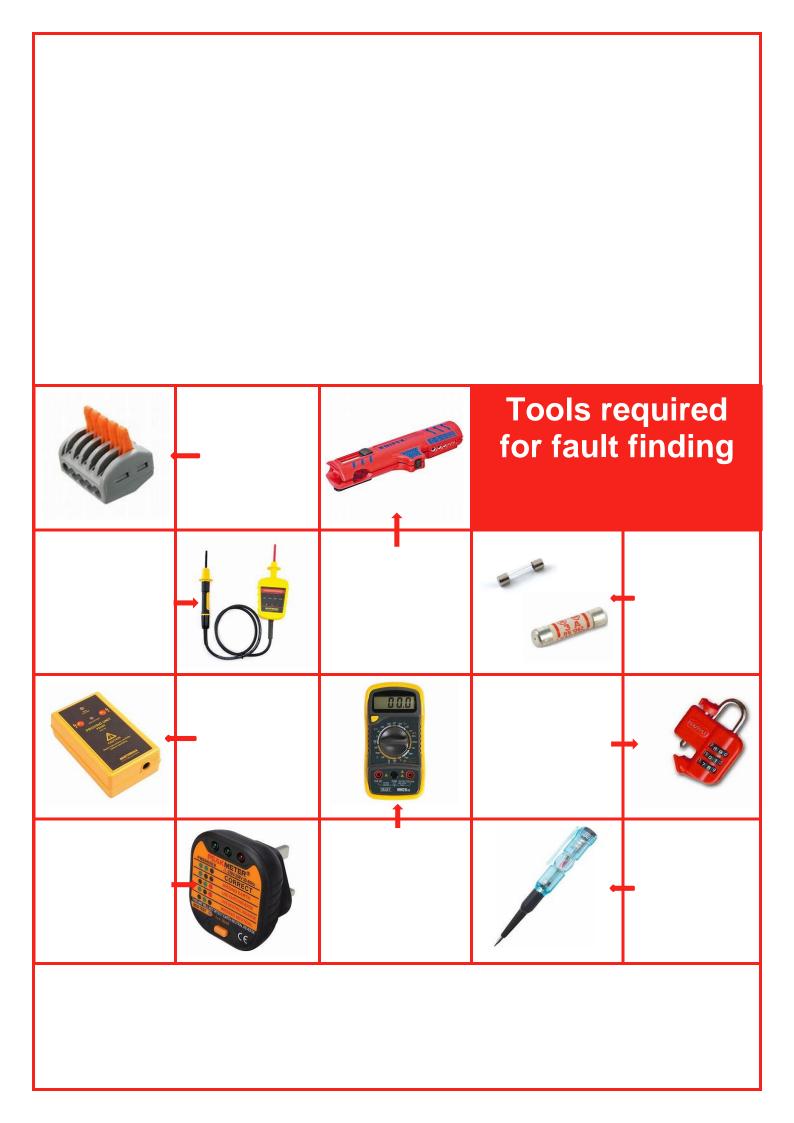
#### **Fault finding**

Jonathon Hallam

#### Disclaimer

The following information is a guide only for training purposes, under no circumstancces will Jonathon Hallam or Warriors of Warmth be laible for any content

Happy to help, here to help





#### **Disclaimer**

It is illegal to work on gas appliances if you are not qualified or registered.

Do not work with electricty if you are not qualified

The following information is a guide for training purposes only. Under no circumstances will Warriors of Warmth or Jonathon Hallam be liabe for any consequence relating to information from this booklet

# Understanding your Multi meter Permissionable allowance-Com NC NO

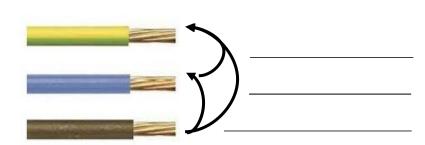
#### Electrical safety



External fuse\_\_\_\_\_

Internal fuse\_\_\_\_\_



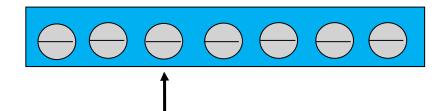




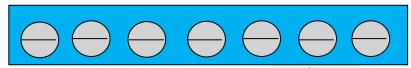
#### Methods of electrical testing



Earth to terminal

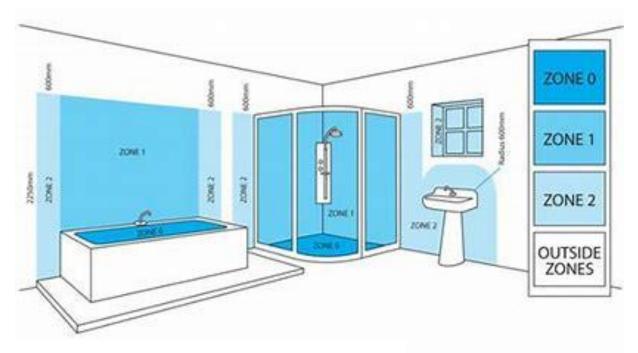


Terminal to terminal





Notes;



**Ingression Protection (IP) Rating Chart** 

**IP67** 

#### **SOLIDS**

Protection against solid object greater than 50mm

Protection against solid object greater than 12.5mm

Protection against solid object greater than 2.5mm

Protection against solid object greater than 1mm

Limited ingress of dust. Will not interfere with equipment

No ingress of dust permitted

Protection level not formally tested

1

2

3

4

5

6

X

**WATER** 

Protection against rertically falling droplets

Protection against vertically falling droplets when titled up at 15°

Protection against spraying water up to an angle of 60°

Protection against splashes of water from all directions

Protection against low pressure jets of water

Protection against high pressure jets of water

Protection against immersion in water between 15cm - 1m deep for 30 minutes

Protection against immersion in water under pressure for long periods

Protection for close-range, powerful, hightemperture water jets

9k

Protection level not formally tested

Above: Guidelines for installing appliances in bathrooms

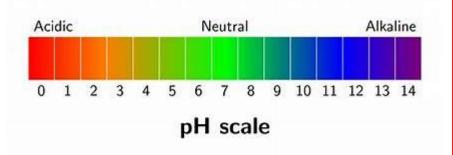
Left: IP codes which are mentioned for Heat pumps

BS7671 Covers electical installations



Testing Ph levels for heating warranty results should be between 8 – 8.5

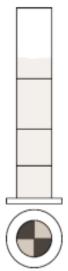
Water Quality

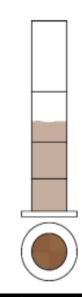


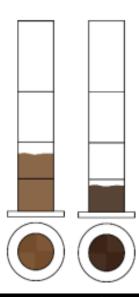
#### **Turbidity**

A turbidity tube is a visual tool to help you judge which water treatment best practice solution is appropriate.

#### Examples

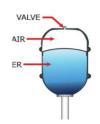






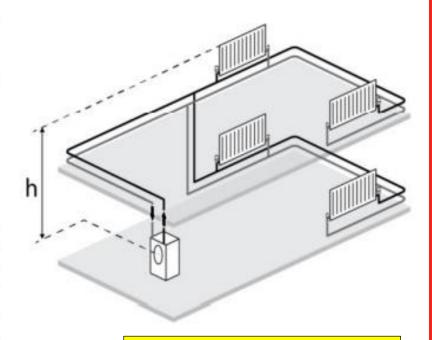
Clean System	Light Fouling	Heavy Fouling
Recommend check	Recommend drain system	Recommend system to be
inhibitor levels.	and re-dose with inhibitor.	cleaned.





#### Vessel <u>Pressures</u>

Static Height, h (m)	Pre-Charge Pressure (bar)
0	\$1000000 B
1	
2	0.5
3	0.5
4	
5	
6	0.6
7	0.7
8	0.8
9	0.9
10	1.0



Example 150litres @1bar/PRV3bar = 16.3litre vessel

Or

150 x 0.109 = 16.3

#### Fact

Connections on heating vessels can block with sludge, when charging vessels lubricate Shrader valve

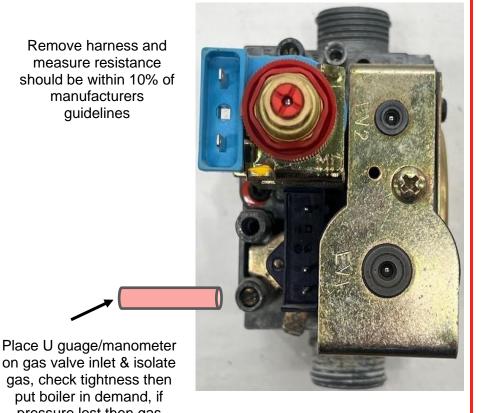
Safety valve setting (bar)		3.0			2.5			2.0		
Vessel charge and initial system pressure (bar)	0.5	1.0	1.5	0.5	1.0	1.5	0.5	1.0		
Total water content of system (litres)	Select an Expansion Vessel with a nominal volume not less than that given below (litres)									
25	2.1	2.7	3.9	2.3	3.3	5.9	2.8	5.0		
50	4.2	5.4	7.8	4.7	6.7	11.8	5.6	10.0		
75	6.3	8.2	11.7	7.0	10.0	17.7	8.4	15.0		
100	8.3	10.9	15.6	9.4	13.4	23.7	11.3	20.0		
125	10.4	13.6	19.5	11.7	16.7	29.6	14.1	25.0		
150	12.5	16.3	23.4	14.1	20.1	35.5	16.9	30.0		
175	14.0	19.1	27.3	16.4	23.4	41.4	19.7	35.0		
200	16.7	21.8	31.2	18.8	26.8	47.4	22.6	40.0		
225	18.7	24.5	35.1	21.1	30.1	53.3	25.4	45.0		
250	20.8	27.2	39.0	23.5	33.5	59.2	28.2	50.0		
275	22.3	30.0	42.9	25.8	36.8	65.1	31.0	55.0		
300	25.0	32.7	46.8	28.2	40.2	71.1	33.9	60.0		
Multiplying factors for other system volumes	0.0833	0.109	0.156	0.094	0.134	0.237	0.113	0.2		



Check filter to gas valve is clear Warm base with hair dryer this may free solenoid jumper

Remove harness and measure resistance should be within 10% of manufacturers guidelines

put boiler in demand, if pressure lost then gas





Isolate power and remove cables before using a multi metre on NTC

Vaillant/Glow Worm NTC



Clean wet pocket



Move clip on NTC to reconnect on pipe surface

Temperature	Resistance				
-15 °C	30.501 Ω				
-10 °C	27.917 Ω				
-5 °C	25.537 Ω				
0 °C	22.913 Ω				
5 ℃	20.387 Ω				
10 °C	17.862 Ω				
15 °C	15.649 Ω				
20 °C	12.486 Ω				
25 °C	10.000 Ω				
30 ℃	8.060 Ω				
35 ℃	6.535 Ω				
40 °C	5.330 Ω				
45 °C	4.372 Ω				
50 °C	3.605 Ω				
55 ℃	2.989 Ω				
60 °C	2.490 Ω				
65 °C	2.084 Ω				
70 ℃	1.753 Ω				
75 ℃	1.481 Ω				
80 °C	1.256 Ω				
85 °C	1.070 Ω				
90 ℃	0.916 Ω				
95 °C	0.786 Ω				
100 ℃	0.678 Ω				
105 ℃	0.586 Ω				
110 °C	0.509 Ω				
115 °C	0.443 Ω				

Temp (°C)	Resistance	Temp (°C)	Resistance
± 10%	$(\Omega)$	± 10%	$(\Omega)$
5	28,490	50	4,608
10	22,161	55	3,856
15	18,088	60	3,243
20	14,772	65	2,744
25	11,981	70	2,332
30	9,786	75	1,990
35	8,047	80	1,704
40	6,653	85	1,464
45	5,523	90	1,262



Check internal fuse, usually most Boilers are 1amp slow blow

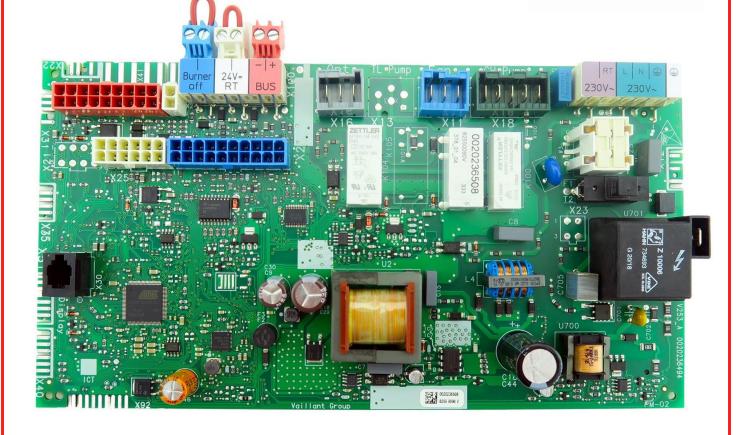




Try warming hair PCBs with hair dryers to reenergise capacitors

Whilst carrying out wet repairs on appliances use cling film to protect PCB



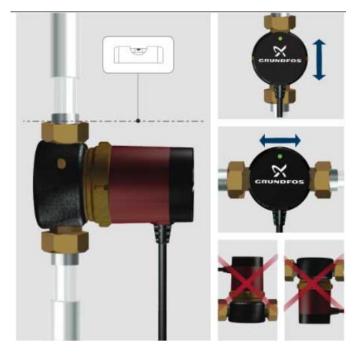


#### Youtube Video

https://youtu.be/mLzEWmsyKwE

# Heating pumps

- Set multi meter to resistance Ω
- Use probes across L & N
- Less than  $100\Omega$  = replace
- No resistance/infinity = replace
- Approx 120 250Ω = Ok
- If loud clean bearings
- Free & bleed shaft using anti seize screw
- If water runs out anti seize screw pump insufficant
- Usually blows fuse



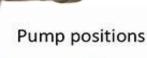
Above are recommended pump positions

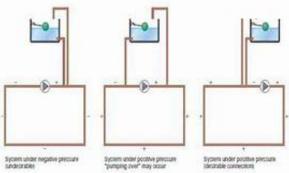


Above is an unprofessional situation the pump screw is above the electical connections so ideally the head needs rotating

Stock pump nuts, incase old connections are cut off







# Pump settings

Flow rate =

10m = 1bar1bar = 9.807Kpa

Kw = Kw of boiler

TD = temperature difference 20

SH = Specific heat 4.2

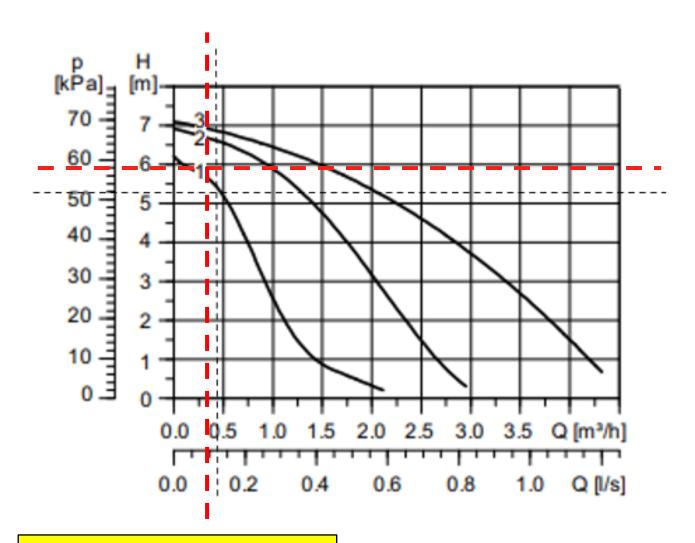
Multiply by 1000 for kg/s

Example;

3 bed house, 2 storey 6m head & 12Kw boiler

$$0.6 \times 9.807 = 5.88$$
kpa

$$20 \times 4.2 = 84 \quad 20 \div 84 = 0.24$$



#### Fact

If you remove anti seize cap and water runs out when pump is on, this can indicate pump is running too slow

### Motorised valves

- Check for demand
- Confirm arm / ball has moved
- Check power is present

#### Y Plan system

- Set multi meter to Ω
- From white to Neutral 2000 2500Ω



#### Cables

White = Htg on Grey = Htg off

Orange = Boiler pump live

#### S Plan system

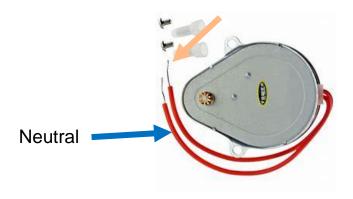
- Brown to Neitral 2000 - 2500Ω

#### Cables

Grey = Permanent live Brown = Htg / DHW

Orange = Boiler pump live

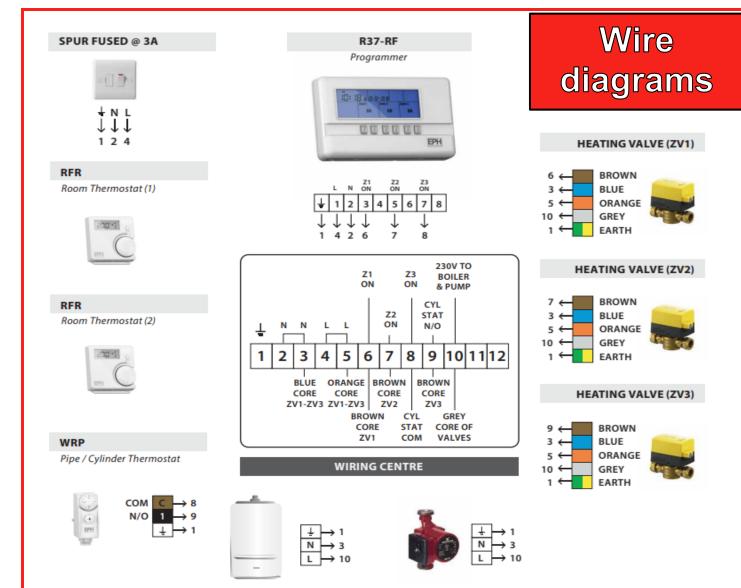
Live (brown)
From room/cylinderstat
Opens zone



Permanent live(Grey)

Switch live (Orange) Sends power to pump & boiler





PUMP

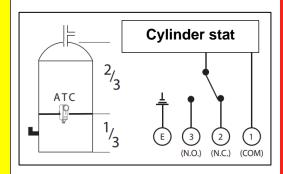
#### **Warning**

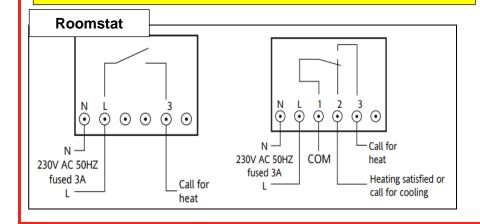
**BOILER** 

Using Ebus connections saves using NC or NO as Ebus sends information including temperatures, faults & helps modulation.

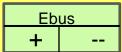
Ebus connections are 5 or 24vdc which can supply controls to function, however in some cases Live & Ebus is required especially recievers are used.

Ebus cables must be installed 25mm away from other cables





Bus connections are low voltage pulse signals like morse code, which sends information not switch live



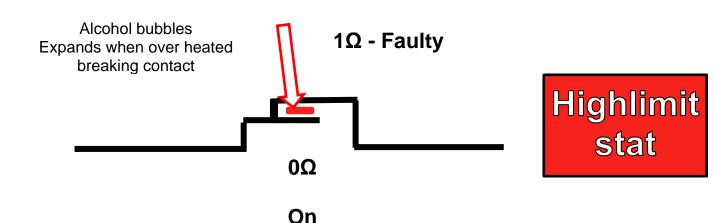
NO = Normal open / on NC = Normally closed / off Com = Live supply

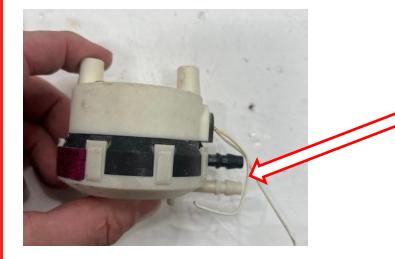


NO = Normally open NC = Normally closed Com = Live

#### **Microswitches**

Com - live NO - On



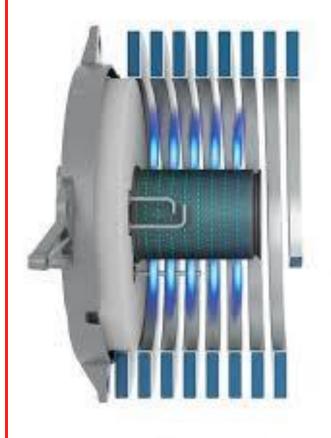


Air tubes connecting air pressure switch must be assessed for bloclages, water or blocked

Air pressure switch

Air pressure can give various faults when the micro switch seizes either leaving the appliance permanently off or on













White vinegar diluted mix or condensate from trap can be sprayed into Hex for cleaning.
Aluminium hot water only



A V	Co/Co2 Ratio				
Appliance type	No Air Gas ratio	With air gas ratio			
Central heating boiler	0.008	0.004			
BBu Fire	0.008 0.020	0.004 N/A			
Fires (Flueless)	0.001	N/A			
Flues (LFE)	0.020	N/A			

Example: 5.1% Oxygen (closest to) 5.0 6.99 CO2 (closest to) 6.8 89ppm meaning the test results come back at 0.0006 in shaded area above this means that it is safe and doesn't require a service Before using 525 ar

#### Using a Flue Analzser

Flue intake tegrity check 20.9%

Shut boiler down as either AR or ID (Unsafe to use)

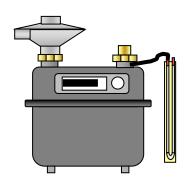
2013 by Martin Switt Date

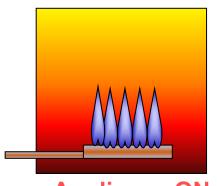
%	%		- 4	GO ppm													
Стурен	co,	10	90	100	150	300	250	200	366	400	460	500	550	600	850	700	790
3.0	10.2	0.0001	0.0005	0.0010	0.0015	0.0020	0.0025	0.0029	0.0034	0.0039	0.0044	8.0049	0.0054	0.0059	0.0064	0.0069	0.0074
40	9.6	0.0001	0.0005	0.0010	0.0016	0.0021	0.0026	0.0031	0.0036	0.0042	0.0047	0.0062	0.0007	0.0063	0.0068	0.0073	0.0078
4.5	9.3	0.0001	0.0005	0.0011	0.0016	0.0022	0.0027	0.0032	0.0038	0.0043	0.0048	0.0054	0.0059	0.0065	8.0070	0.0075	-
10,1	9.1	0.0001	0.0005	0.0011	0.0016	0.0022	0.0027	0.0033	0.0038	0.0044	0.0049	0.0055	0.0000	0.0066	0.0071	0.0077	
	8.8	0.0001	0.0006	0.0011	0.0017	0.0023	0.0028	6.0034	0.0040	0.0045	0.0051	6.0057	0.0063	0.0068	0.0074	-	
44	8.5	0.0001	0.0006	0.0012	0.0018	0.0024	0.0029	0.0035	0.0041	0.0047	0.0053	0.0059	0.0065	0.0071	0.0076		
8.5	8.2	0.0001	0.0006	0.0012	0.0018	0.0024	0.0030	0.0037	0.0043	0.0049	0.0055	0.0061	0.0067	0.0073	MARKET.		
7.8	7.9	0.0001	0.0006	0.0013	0.0019	0.0025	0.0032	0.0038	0.0044	0.0051	0.0057	0.0063	0.0070	0.0078	1000		
7.5	7.6	0.0001	0.0007	0.0013	0.0020	0.0026	0.0033	0.0039	0.0046	0.0053	0.0059	0.0066	0.0072	0.0079			
8.0	7.3	0,0001	0.0007	0.0014	0.0021	0.0027	0.0034	0.0041	0.0048	0.0055	0.0062	0.0066	0.0075	NAME:			
**	6.8	0.0001	0.0007	0.0015	0.0022	0.0029	0.0037	0.0044	0.0051	0.0059	0.0066	0.0074	1800				
16.0	6.2	6.0002	0.0008	0.0016	0.0024	0.0032	0.0040	0.0048	0.0056	0.0065	0.0073	1,000					
11.0	5.6	0.0002	0.0009	0.0018	0.0027	0.0036	0.0045	0.0054	0.0063	0.0071	-						
12.0	3.1	0.0002	0.0010	0.0020	0.0029	6.0039	0.0049	0.0000	8.0069	-							
13.0	4.5	0.0002	0.0011	0.0022	0.0033	0.0044	0.0056	0.0067	0.0076								
14.0	3.9	0.0002	0.0013	0.0026	0.0038	0.0051	0.0064	0.0077	S. Septe								
15.0	3.4	0.0002	0.0015	0.0029	0.0044	0.0009	0.0074	Ames.									

Boiler Requires Service

Before using gas analyser use outside air to purge (20.9 air) Check air intake to flue is at the same level or flue may be brok

Boiler may be NCS or AR





# Working Pressure

**Appliance ON** 



#### **WORKING Pressure**



Gas Valve Inlet Test Point

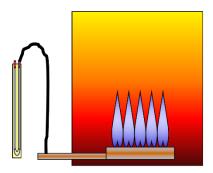
[D]



**1.5mb** 







**Appliance ON** 

Gas	
Mimium pressure loss	
Mimium pressure allowed	
Water	
Minimum water pressure	
Minimum flow rate	

2 min gas flow m <sup>3</sup>	Heat input Kw	Heat input Kw	Answ	er	Answer
	(gross)	(net)			
0.034	10.98	9.89	Boiler Kw (	net)	-
0.036	11.63	10.48	Gas m³/hr		<b>M</b> 3,
0.038	12.27	11.06			
0.040	12.92	11.64		(	Gas
0.042	13.57	12.22		rs	Gas ating
0.044	14.21	12.80			utilig

Kw

M³/hr

#### Gross input gas rate ready reckoner for domestic metric index meters

2 minutes gas flow rate		ate per our		ulated input
m <sup>3</sup>	m <sup>3</sup>	ft <sup>3</sup>	kW	Btu/hr
0.001	0.03	1.06	0.3	1,100
0.002	0.06	2.12	0.6	2,200
0.003	0.09	3.18	1.0	3,300
0.004	0.12	4.24	1.3	4,400
0.005	0.15	5.31	1.6	5,500
0.006	0.18	6.37	1.9	6,600
0.007	0.21	7.43	2.3	7,700
0.008	0.24	8.49	2.6	8,800
0.009	0.27	9.55	2.9	9,900
0.010	0.30	10.61	3.2	11,000

2 minutes gas flow rate		ate per our	Calculated heat input			
m <sup>3</sup>	m <sup>3</sup>	ft <sup>3</sup>	kW	Btu/hr		
0.020	0.60	21.22	6.4	22,000		
0.030	0.90	31.83	9.7	33,000		
0.040	1.20	42.44	12.9	44,000		
0.050	1.50	53.06	16.1	55,000		
0.060	1.80	63.67	19.3	65,900		
0.070	2.10	74.28	22.5	76,900		
0.080	2.40	84.89	25.8	87,900		
0.090	2.70	95.50	29.0	98,900		
0.100	3.00	106.11	32.3	109,800		
0.200	6.00	212.22	64.4	219,700		

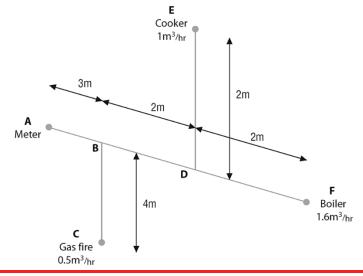
#### Equivalent Length (m) Nominal Pipe Size Bends Fittings Tee A) Tee A) 90<sup>0</sup> Copper 45<sup>0</sup> 90° elbow (Entering Branch) (Exiting Branch) ≤ 15 mm ≤ 15 mm 0.15 0.20 R 1/2 0.40 0.75 1.20 20 mm 22 mm 0.20 0.30 0.60 1.20 1.80 R 3/4 25 mm R 1 28 mm 0.25 0.40 0.80 1.50 2.30 R 11/4 32 mm 35 mm 0.30 0.50 1.00 2.00 3.00 A) Use the largest connection size on the fitting that is not necessarily the branch size

# Gas Pipe sizing

Flow Rate	Hea	it Input		Nominal Pipe Size (mm) A)						
	Gross	Net	8	10	12	15	22	28	35	
(m3/h)	(kW)	(kW)	(6)	(8)	(10)	(13)	(19)	(25)	(32)	
0.25	2.70	2.46	0.2675	0.0710	0.0255	0.0077	0.0014	0.0004	0.0001	
0.50	5.40	4.91	0.8348	0.2188	0.0777	0.0231	0.0040	0.0011	0.0004	
0.75	8.10	7.37		0.4285	0.1514	0.0447	0.0077	0.0022	0.0007	
1.00	10.81	9.82		0.6940	0.2444	0.0719	0.0123	0.0035	0.0011	
1.25	13.51	12.28			0.3553	0.1042	0.0178	0.0050	0.0016	
1.50	16.21	14.73			0.4833	0.1414	0.0240	0.0067	0.0021	
1.75	18.91	17.19			0.6276	0.1832	0.0311	0.0086	0.0027	
2.00	21.61	19.65			0.7877	0.2296	0.0388	0.0108	0.0034	
2.25	24.31	22.10			0.9630	0.2804	0.0473	0.0131	0.0042	
2.50	27.01	24.56				0.3353	0.0565	0.0156	0.0049	
2.75	29.72	27.01				0.3945	0.0663	0.0183	0.0058	
3.00	32.42	29.47				0.4577	0.0769	0.0212	0.0067	
3.25	35.12	31.93				0.5249	0.0880	0.0243	0.0077	
3.50	37.82	34.38				0.5960	0.0998	0.0275	0.0087	
3.75	40.52	36.84				0.6709	0.1123	0.0309	0.0097	
4.00	43.22	39.29				0.7496	0.1253	0.0345	0.0108	
4.25	45.92	41.75				0.8321	0.1390	0.0382	0.0120	
4.50	48.63	44.20				0.9182	0.1533	0.0421	0.0132	
4.75	51.33	46.66					0.1681	0.0462	0.0145	
5.00	54.03	49.12					0.1836	0.0504	0.0158	
5.25	56.73	51.57					0.1996	0.0548	0.0172	
5.50	59.43	54.03					0.2162	0.0593	0.0186	
5.75	62.13	56.48					0.2334	0.0640	0.0200	

Pressure loss to the appliance must be lower then 1mb in total pipe route.
Incorrect sized pipe can lead too poor combustion readings

Pipe	Gas	Pipe	Estimated	Fitting allowance		Corrected	Pressure	Calculated
section	rate	length	Pipe dia			length	loss	pressure loss
	M3/h			Туре	length		Mb/pm	
A – B	3.1	3	22	Elbow x 2	1.2	4.2	0.0880	0.37
B – C	0.5	4	15	Elbow x 3 Tee(exit) x 1 <sub>(22m)</sub>	3	7	0.0231	0.1617



#### **Heating**

Pipe sizing.

#### Fact

Flow rate for heating should be 1m/s, lower sludge can settle, 1.5 can be disruptive, 2.5 can erode pipes, Part L, states flow temperatures should be 55° with a DT of 20°

#### **System** design

Reference:

BS 5449 **BS EN 806** 

Pipe Dia (mm)	Watts
8	1500
10	2500
15	6000
22	13000
28	22000
35	34000

#### **Pipe Flow rates**

= Rad Watts

TD = Temp diff

SHC = Specific Heat

**Low loss header sizing** (m/s)

Kw = Boiler output

SHC = Specific heat

DT = Temperature diff

#### **Bypass setting**

KW / Dt x 4.20

Manufacturers guidelines mini flow & system head



#### Radiator Sizing

TD x 4.186

Kw x 3600 ÷ 1000

SHC x DT

#### **Ventilation heatloss**

V = Room volume m<sup>2</sup>

 $0.33 \times V \times N \times TD = heat loss$ 

N = Air change p/hour

0.33 = Specific heat of air

TD = Temp diff, between -3° + desired room temp

i.e;

living room 1980 3m x 3m x 4m @21

 $0.33 \times 36 \times 1.5 \times 24 = 427.68$ 

In Coastal areas -5 can be used for outside

Room	Category A (Pre 2000)	Category B (2000)	Category C (New build)
Lounge/living room	1.5	1	0.5
Dining/breakfast room	1.5	1	0.5

U-Valves for new build						
Room	U-Value					
Pitched insulated roof	0.20					
Flat roof	0.20					
Walls	0.30					
Internal walls	1.6					
Floors	0.25					
Windows & doors	2					

#### **Correction factors**

Htg flow – htg return = water temp Water temp – desired room temp =

Boiler flow is 70 return temperature is 50, Water mean temperature is 60

Deduct room temperature of 21, equals 39.

39 falls between figures so accurate Calculations are needed.

0.748 - 0.629 = 0.119

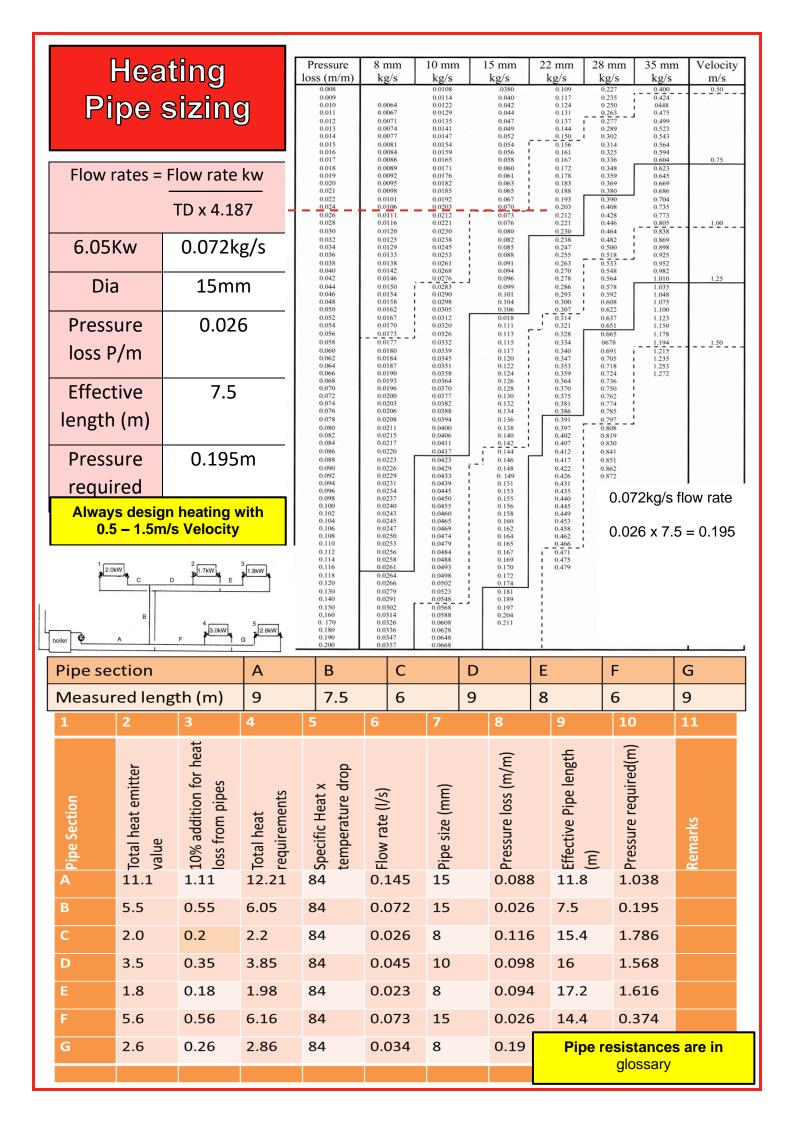
 $\underline{0.119}$  = 0.024 – the figure per  ${}^{\circ}$ C difference

0.748 - 0.024 = 0.748

25	0.406
30	0.515
35	0.629
40	0.748
45	0.872
50	1.000
55	1.132
60	1.267

Further details in Glossary

	Room heat loss										
Surface elemen	t	area (m2)	х	U Valv (W/m2		X	Temp dif (oC)	=	he	esign at loss vatts	Totals
			х			X		=			
			х			х		=			
			х			х		=			
			х			х		=			
			х			x		=			
			х			х		=			
			х			X		=			
				Air he	eat lo	oss					
Air changes (1.5)	x	Room volume (m3)	x	Temp/d (21 + -3		x	Vent factor 0.33	=			
			x			X		=			
Fabric heat loss	5	+	Ai	ir heat los	SS		+ 15%	=			
		+						=			
	<b>Total</b> Add				3			=			
	Heat emitter size										
Flow 70	Flow 70 +			eturn 55 ÷ 2 – Room te		<ul> <li>Room ten</li> </ul>	<b>np</b> 21	=	N	IWT	
		х	÷2					=		•	
M	MWT					CF	correct factor	=		Radiato	or size
		x					=				



Pipe Centres	Conversation factor
100	10
150	6.6
200	5

#### Pipe lengths

#### **UFH facts**

RA = Area of room
PC = Pipe centre
DfM = Distance from manifold x 2
Add 5%

le;

 $RA-24 m2 \qquad \quad PC\ 150 mm \qquad \quad DfM-6 m$ 

24 x 6.6 = 158 158/2 = 79.50 6 x 2 = 12 91.5 + 5% = 95.8m

ie;

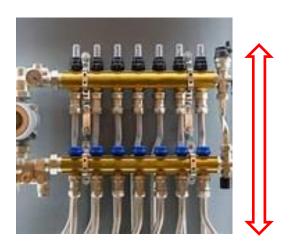
RA - 12<sub>M2</sub> PC - 150<sub>MM</sub> DfM - 6

 $12 \times 6.6 = 79.2m$ DfM = 12m

Sub total = 91.2m + 5%(4.5)

Total = 95.7m

Below is the W/m2 produced from the pipe centres, as you can see 100mm centres provides more heatput



DFM; Distance from manifold

Flow Rate	Friction Loss (kPa/m)						
(L/min)	16mm PE-X	20mm PE-X	25mm PE-X	32mm PE-X			
0.5	0.01	0.00	0.00	0.00			
1	0.04	0.01	0.00	0.00			
2	0.15	0.04	0.01	0.00			
3	0.31	0.09	0.03	0.01			
4	0.53	0.15	0.05	0.02			
5	0.80	0.23	0.08	0.02			
10	2.88	0.84	0.28	0.08			
12	4.04	1.18	0.39	0.12			
14	5.37	1.57	0.51	0.15			
16	6.88	2.00	0.66	0.20			
18	8.55	2.49	0.82	0.24			
20	10.39	3.03	1.00	0.30			
25	15.70	4.58	1.50	0.45			
30	22.00	6.41	2.11	0.63			
35	29.26	8.53	2.80	0.83			
40	37.46	10.92	3.59	1.07			
45	46.58	13.57	4.46	1.33 uri			

30 MWT 18 rtemp	100	150	200	250	300
30	37	34	31	29	26

le, 80 x 0.15 = 1.2

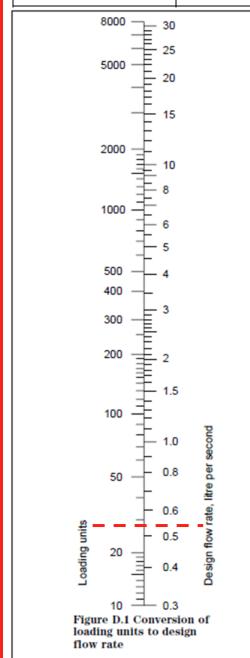
Pipe	Heat output W/m.			
centres(mm)	2			
100	91.4			
150	82			
200	74			
250	66.4			
300	60			
Based on 75mm screed & 45° mean temp				

More UFH Outputs in Glossary

# Hot & Cold Pipe Sizing

#### Below example

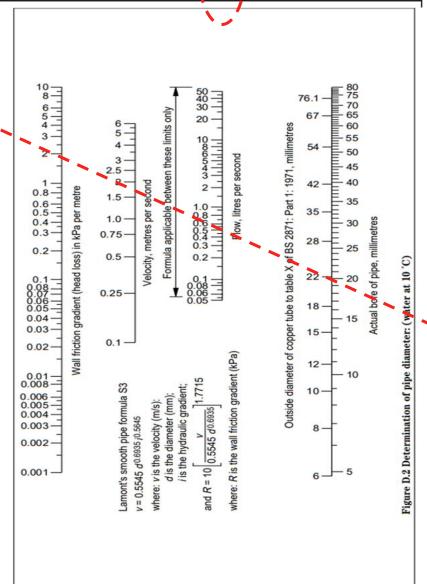
Garden tap x 2	10
Bath x 2	8
Sink	2
Shower	2
Wash basin	1
W/machine	2
D washer	2



Draw-off point	$Q_A$	$Q_{min}$	Loading units			
	l/s	l/s				
Washbasin, handbasin, bidet, WC-cistern	0,1	0,1	1			
Domestic kitchen sink, - washing machine <sup>a</sup> , dish washing machine, sink, shower head	0,2	0,15	2			
Urinal flush valve	0,3	0,15	3			
Bath domestic	0,4	0,3	4			
Taps /garden/garage)	0,5	0,4	5			
Non domestic kitchen sink DN 20, bath non domestic	0,8	0,8	8			
Flush valve DN 20	1,5	1,0	15			
<sup>a</sup> For non domestic appliances check with manufacturer.						

Maximum flow rate velocity 3m/s this prevents water hammer, 27 LU against he chart equals too 5.5l/s & flow rate of 1.7ls which points to 22mm pipe

Table 3.2 — Copper														
Max. load	LU	1	2	3	3	4	6	10	20	50	165	430	1 050	2 100
Highest value	LU			2			4	5 /	8					
d <sub>a</sub> x s	mm	<b>12</b> x	1,0		15 x	1,0		18 x 1,0	22 x 1,0	28 x 1,5	35 x 1,5	42 x 1,5	54 x 2	76,1 x 2
di	mm	10,0			13,0			16,0	20,0	25	32	39	50	72,1
Max length of pipe	m	20	7	5	15	9	7	1	i					



# Hot water demand

#### **Hot water Demand**

#### **Basic**

Demand	Cylinder size	Kw req	Boiler allowed
2 bed, 1 bath	125	7.2	2
3 bed, 1 bath	145	8.4	2.5
4 bed, 1 bath	165	8.4	2.5
4 bed, 1 bath + 1 shower	175	10	2.5
4 bed, 2 bath	225	13	3.0

#### **Calculated formula**

#### **Heat required**

SHC x Kg x Tr =

SHC =

Kg = litres of water

Tr = Temperature rise

**Period** 

SHC x Kg x Tr = 
$$\frac{1}{2}$$

Secs

#### Hot & Cold Pipe sizing (unvented DHW)

Loading units

Appliance	Loading units		
Basin/WC	1		
Sink/Shower/W.machine	2		
Urinal	3		
Bath	5		
Non domestic	8		
Taps/Garden	5		

#### Diameter per Units

LU	1	2	3	3	4	6	10	20	50	165	430
Dia (mm)	15	15	15	15	15	15	22	22	28	35	42

#### **Hot water** ventilation pipe

How to calculate vent pipe height?

150mm standard number 40mm per metre height

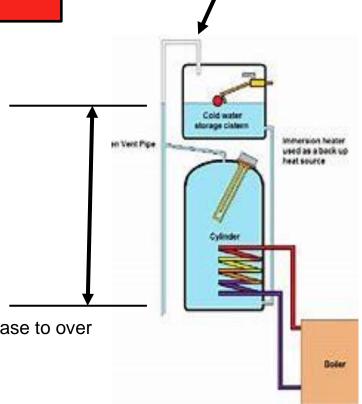
150 + 40 = vent height

Height from cylinder base to over pipe level

ı.e

4m height from cylinder base to over flow pipe

 $4 \times 40 + 150 = 310$ mm



To hot outlets

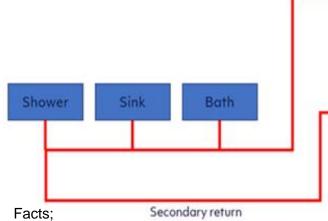
Secondary

circulation

pump

Isolation

valve



- Return pump must be bronze
- Must connect onto cylinder 1/4 from top
- 5°TD from draw off & return
- Minimum return temp 50° within
- Minimum 0.5l/s
- Secondary return must be a minimum 2 x dia smaller then distruption
- Return with more than 15ltres needs expansion vessel
- Pump works on timer

Pipe	15ltr in		
dia	m		
15	107		
22	48		
28	30		

Isolation

Non

return valve

valve

Secondary circulation

Immersion heater

## **Unvented Hot water**

20lpm 1.5 – 3.5 bar

- D2 next dia above D1
- Discharge should be copper
- Terminate 100mm above ground with cage
- Must terminate 3m from plastic surface (gutter/roof sheeting)
- D2 discharges in solvent weld must be clipped every 300mm/labelled with a HepVo valve
- Warning audio light device for disable tennats

Valve Outlet size	Minimum size of discharge D1	Minimum size of discharge D2  (From tundish)	Maximum resistance, expressed as a length of straight pipe	Resistance created by each bend or elbow
G1/2``	15mm	22mm	Up to 9m	0.8m
		28mm	Up to 18m	1m
		35mm	Up to 27m	1.4m
G3/4``	22mm	28mm	Up to 9m	1m
		35mm	Up to 18m	1.4m
		42mm	Up to 27m	1.7m
G1``	28mm	35mm	Up to 9m	1.4
		42mm	Up to 18m	1.7m
		54mm	Up to 27m	2.3m

#### Example:

Current install, cylinder has G1/2` exit, 6 bends on D2 route which is 8m long

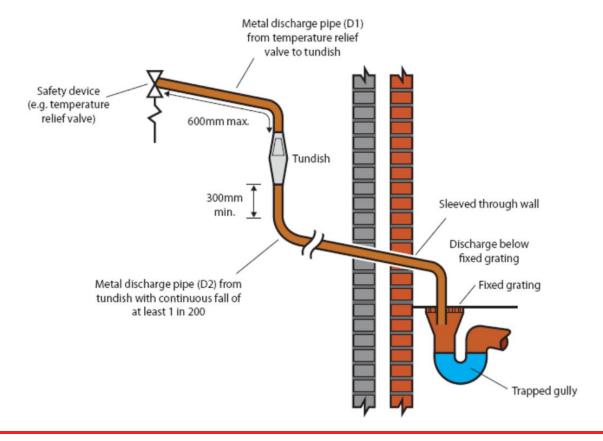
Two options follow;

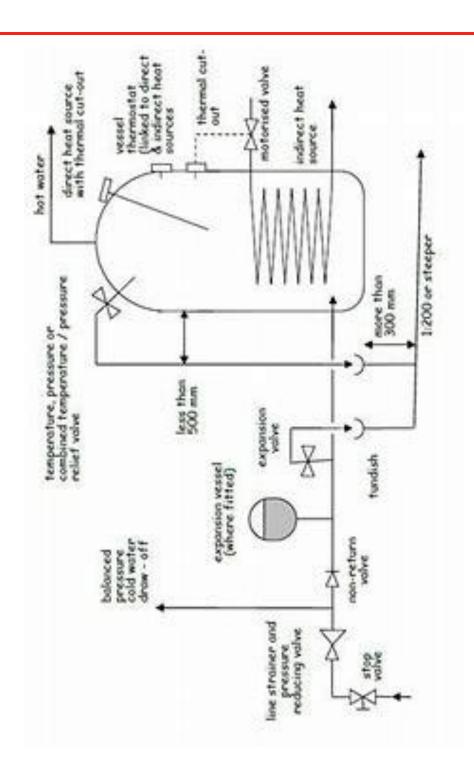
D2 -- 22mm

D1 = 15mm -- D2 22mm 6 x 0.8 + 8 = 12.8m incorrect too long for 22mm

D2 - 28mm

D1 = 15mm - D2 28mm 6 x 1 + 8 = 14m correct for 28mm as actual length is under 18m





#### **Temperature guidelines**

60° daily for 60mins

Showers 43°

Care home 43°

Basin 38 - 41°

Sinks 46 - 48°

Bath 44°

#### Unvented Cylinder safety temperatures

Thermostat 60°

ECO 85°

Energy cut off

(switches electric off to boiler)

Temperature relief valve 95°

(Poopet valve)



Pump pressure adjustment

Pressure on/off adjustment switch

Run time

# Booster pumps

Pump run times

L/m x Run time = flow rate

66l/m x 10 = 660litres



#### **Operating pressures:**

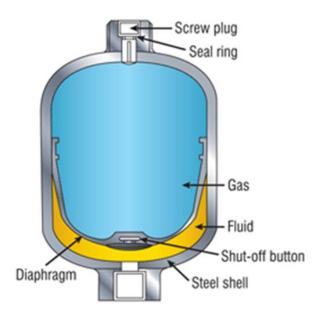
Accumulator operates between P1 and P2

P1 = minimum operating pressure

P2 = maximum operating pressure

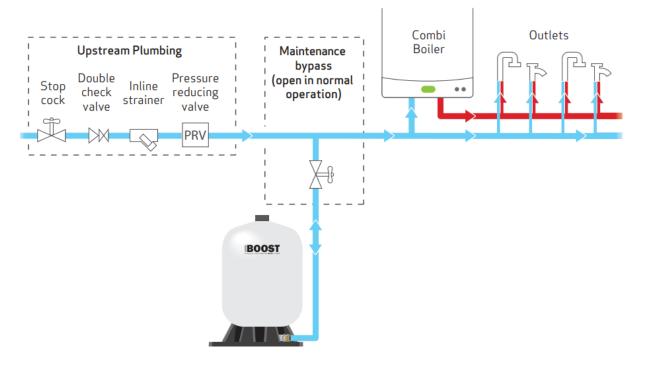
PO = pre-charge pressure (normally 90% of P1)

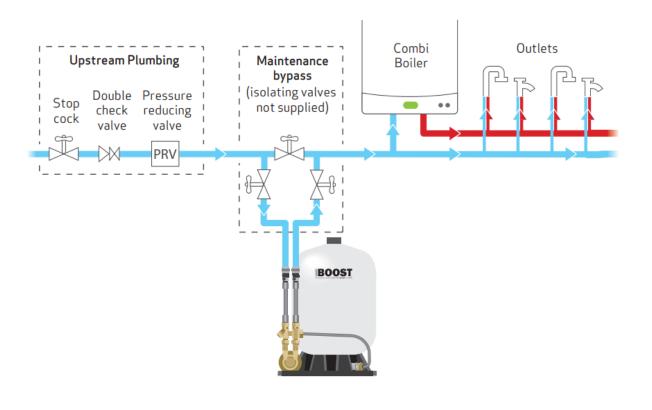
- allows a small amount of water to remain in the vessel at all times
- prevents the bladder collapsing completely during each operating cycle.

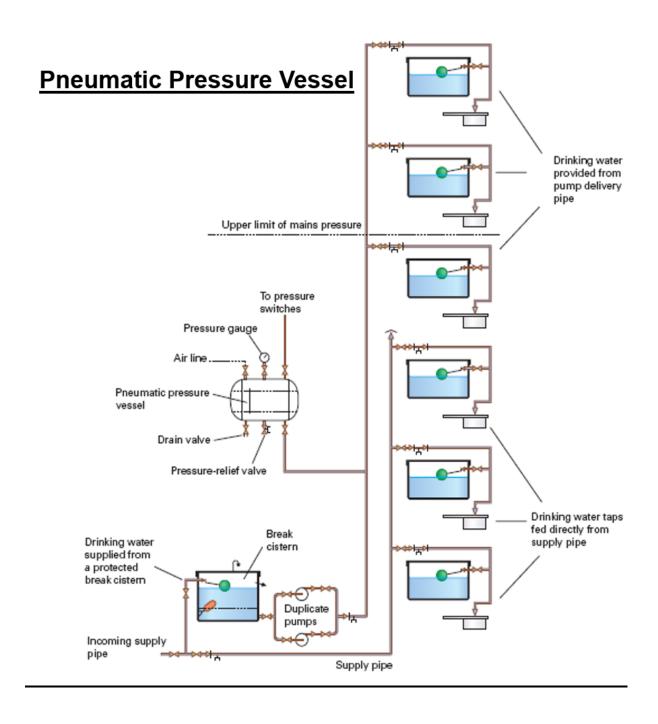


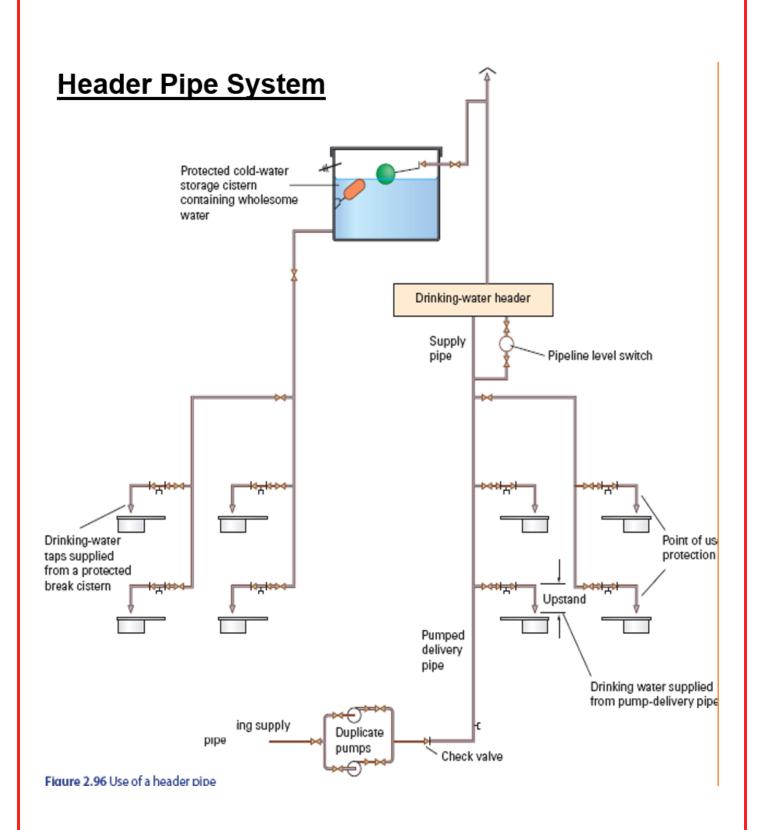
Pre charge in some vessels simulate charging pump

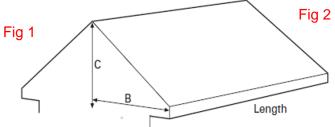
#### Unpumped











For roofs between 10° and 50° pitch, this can be calculated by using the following formula:

 $\underline{C} + B$  × length of roof = effective roof area in m<sup>2</sup>

Тур	e of surface	Effective design area
1	Flat roof	plan area of relevant portion
2	Pitched roof at 30° Pitched roof at 45° Pitched roof at 60°	plan area of portion x 1.29 plan area of portion x 1.50 plan area of portion x 1.87
3	Pitched roof over 70°	elevational area x 0.5

# **Gutter sizing**

or any wall

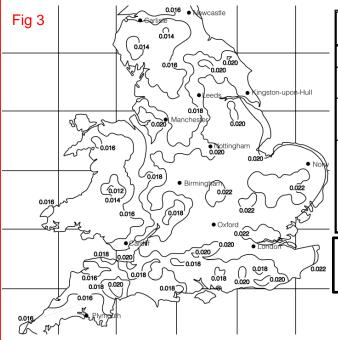


Fig 4	Risk factor
Eaves gutters	1,0
Eaves gutters where water overflowing would cause particular inconvenience, e.g. over entrances to public buildings	1,5
Non-eaves gutters and in all other circumstances where abnormally heavy rain or blockage in the roof drainage system could cause water to spillover into the building	2,0
For non-eaves gutters in buildings where an exceptional degree of protection is necessary, e.g.  - hospital operating theatres - critical communications facilities - storage for substances that give off toxic or flammable fumes when wet - buildings housing outstanding works of art	3,0

Q = Fall (dia 2) R = Rain fall intensity (dia 3) C = Risk factor of dwelling (dia 4) A = area (dia 1)

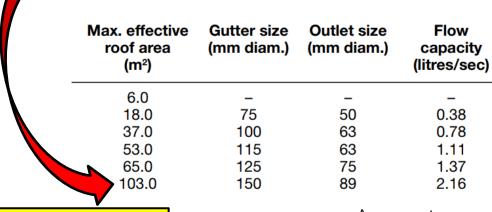
 $A \times Q \times R \times C =$ 

 $1+3 \times 14.5 \times 1.5(fall) = 87$ 

 $87 \times 0.020$  (rain intensity) = 1.74

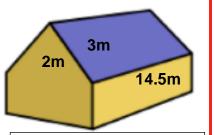
 $1.74 \times 1(Risk factor) = 1.74$ 

Location	Nottingham
Pitch	45
Dwelling	House no risk factor



Ref: Reg H BS 12056

Areas greater than 25m2 needs a Shoe exit



Stop end.

Gutter depth x 50 =

Distance between outlets.

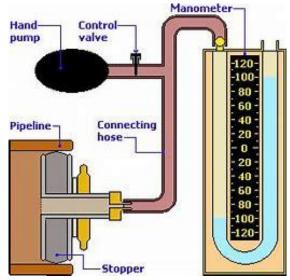
Gutter depth x 100 =

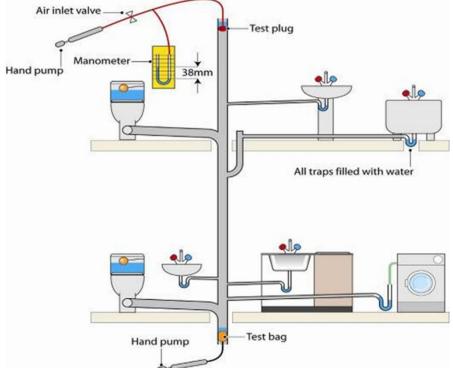
100m gutter 50mm depth

 $100 \times 50 = 5m$ 

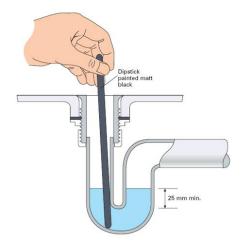
# Drainage testing

- Fill trap seals with water
- Bung ventilation pipe with stop
- Using hand pump charge to 38mm
- Should be no drop after 3minutes





Drainage performance testing



To performance test sanitation, run at least 3 – 4 appliances WC, bath, basin and sink. Once water has drained away, using a dipstick check the trap seals must have at least 25mm water depth, this process should be carried out 3 times

# Heat Pump design

			heatir	g SPF		her emitte	rs		screed		Al	uminium pa	inel	
		Temperature Star Rating	Heating circuit flow temperature °C	GSHP	ASHP	Domestic Fan Convector/Fan- assisted Radiato	Standar d Radiator	Fan Coil Unit	with TILE	with W00D	with CARPET	with TILE	with WOOD	with CARPET
		<del>àààààà</del>	35	4.3	3.6	4.3	6.8	5.0	PS≤300	PS±300	PS≤200	PS≤200	PS≤200	PS≤150
		<b>CACACACA</b>	40	4.1	3.4	3.1	4.3	3.5	PS≤300	PS±300	PS±300	PS≤300	PS≤300	PS≤200
	Room specific heat loss less	that the	45	3.7	3	2.4	3.1	2.6	PS≤300	PS≤300	PS±300	PS≤300	PS≤300	PS±300
	than 30 W/m²	******	50	3.4	2.7	2.0	2.4	2.1	PS≤300	PS≤300	PS≤300	PS≤300	PS≤300	PS≤300
		thinhinh	55	3.1	2.4	1.7	1.9	1.7	PS≤300	PS≤300	PS≤300	PS≤300	PS≤300	PS≤300
		\$	60	2.8	2.1	1.4	1.6	1.5	PS≤300	PS≤300	PS≤300	PS≤300	PS±300	PS≤300
			35	4.3	3.6	4.3	6.8	5.0	PS±300	PS≤100		PS≤100	Reduce	heat loss
	0	than that	40	4.1	3.4	3.1	4.3	3.5	PS≤300	PS≤200	PS≤150	PS≤200		
	Roon specific heat loss 30	****	45	3.7	3	2.4	3.1	2.6	PS≤300	PS≤300	PS≤300	PS≤200	PS≤200	PS≤150
	to 50 W/m²	******	50	3.4	2.7	2.0	2.4	2.1	PS≤300	PS±300	PS≤300	PS≤300	PS≤200	PS≤200
		thinininini	55	3.1	2.4	1.7	1.9	1.7	PS≤300	PS≤300	PS≤300	PS≤300	PS≤300	PS≤300
		***********	60	2.8	2.1	1.4	1.6	1.5	: PS≤300	PS≤300	PS≤300	PS≤300	PS≤300	PS≤300
	Room specific heat loss 50 to 80 W/m <sup>2</sup>		35	4.3	3.6	4.3	6.8	5.0	PS≤100	Parting 1	wat loss		ļ	
		<b>COCCACAC</b>	40	4.1	3.4	3.1	4.3	3.5	PS≤200				Reduce	leat loss
		inininini	45	3.7	3	2.4	3.1	2.6	PS≤300	PS≤100	PS≤100	PS≤150		
		นำนำนำนำนำ	50	3.4	2.7	2.0	2.4	2.1	PS≤300	PS≤200	PS≤150	PS≤200	PS≤100	
		thinininin	55	3.1	2.4	1.7	1.9	1.7	PS≤300	PS≤300	PS≤ 200	PS≤200	PS∉150	PS≤100
educing fabric and/or		rataranana	60	2.8	2.1	1.4	1.6	1.5	PS≤300	PS≤300	PS≤300	PS≤300	PS≤200	PS≤150
entilation heat losses	Room specific	<b>COCCE</b>	35	4.3	3.6	4.3	6.8	5.0				į		
n move a room up to		ininininininininininininininininininin	40	4.1	3.4	3.1	4.3	3.5	PS≤150	Reduce I	eat loss		Reduce	heat loss
ext specific heat loss d, making it easier to	heat loss 80	thinhinhinhinhinhinhinhinhinhinhinhinhinh	45	3.7	3	2.4	3.1	2.6	PS≤200			PS≤100	San Jan Jan Jan Jan Jan Jan Jan Jan Jan J	
achieve a good SPF.	to 100 W/m <sup>2</sup>	inininini	50	3.4	2.7	2.0	2.4	2.1	PS≤250	PS≤100	PS≤100	PS≤150		ļ
		นำนำนำนำนำ	55	3.1	2.4	1.7	1.9	1.7	PS≤300	PS≤200	PS≤150	PS≤200	PS≰100	
1 1		thinhhinh	60	2.8	2.1	2.1	1.6	1.5	PS≤300	PS≤250	PS≤250	PS≤200	PS≤150	PS≤100
		THE PROPERTY OF THE PARTY OF TH	35	4.3	3.6	4.3	6.8	5.0				ļ		
	Room speciofic	****	40	4.1	3,4	3.1	4.3	3.5						
	heat loss 100	THE THE PARTY OF T	45	3.7	3	2.4	3.1	2.6	Red	ce heat to	155	Re	duce heat	loss
	to 120 W/m <sup>2</sup>	inininini inininini	50	3.4	2.7	2.0	2.4	2.1				ļ		
		นา	55	3.1	2.4	1.7	1.9	1.7						
		********	60	2.8	2.1	1.4	1.6	1.5				<u> </u>		
			35	4.3	3.6	4.3	6.8	5.0						
	Room specific	THE THE THE	40	4.1	3.4	3.1	4.3	3.5						
	heat loss 120	THIMMIT I	45	3.7	3	2.4	3.1	2.6	Red	ce heat to	55	Re	duce heat	055
	to 150 W/m <sup>2</sup>	MANAGER	50	3.4	2.7	2.0	2.4	2.1						
		THE THE THE TENT	55	3.1	2.4	1.7	1.9	1.7						
		นำนำนำนำนำ	60	2.8	2.1	1.4	1.6	1.5						
						Ĺ								

# **Buffer Sizing**

 $V = \frac{Q \times t \times 60}{4.18 \times DT}$ 

i.e

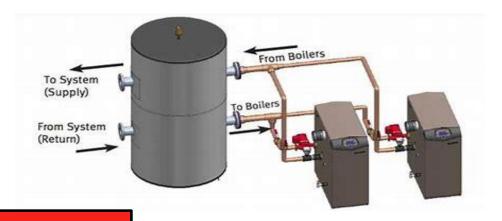
5 x 15 x 60 4.18 x 5 V = tank volume

Q = heat load (5kw)

DT = Delta T (rads 10° / Udfr 5°)

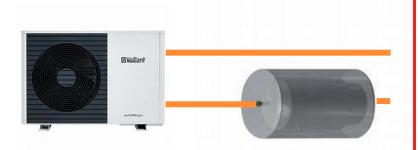
60 = 60 seconds

T = HP compressor starts in hour



# Sizing Volumizers

Volumisers are installed to prevent systems freezing, should the primary pipework be lower than 20l then a volumiser should be installed



0.141	15mm copper
0.311	22mm copper
0.5l	28mm copper
600 x 1000 rad	61

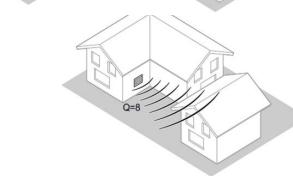
### Heat pump performances with outside temperatures

Output Water 45°C		UNITS	4 kW	6 kW	8 kW	12 KW	15 KW
Outside Air at 0°C	Qh	KW	3.17	4.02	5.11	8.03	9.80
	COP	kW/kW	2.57	2.43	2.42	2.44	2.48
Outside Air at -3°C	Qh	KW	2.93	3.71	4.41	7.39	9.06
	COP	kW/kW	2.42	2.31	2.34	2.32	2.36

# Heat Pump location



Q = 4



### Table 1:

Q = 2

Q rating	4	5	6	8	10	12	15	20	25
2	-20	-21	-23	-26	-28	-29	-31	-34	-36
4	-17	-19	-20	-23	-25	-26	-28	-31	-33
<u>8</u>	-14	-16	-17	-20	-22	-23	-25	-28	-30

Q = 8

#### Table 2:

Restriction	db reduction
Solid barrier between assessment position	-10
Move HP 25cm to be seen from assessment position	-5

### Table 3:

Difference between two noise levels	Correction factor
5	1.2
6	1
7	0.8
8	0.6

**Scenario**; ASHP installed against wall, manufacturers data states 55db, this install is partially covered with wall and the assessment position is 4metres away

Description	Result
1 Manufacturers db	55db
2 Installed against single wall	Q4
3 Distance from wall	4m
4 Db reduction 4m @Q4 (table 1)	-17
5 Brick wall between assessment (table 2)	-5
5 55 + -17 + -5 =	33db
6 MCS approval guide (table 3) 40 – 33 = 7	0.8
7 Final 40 + 0.8 =	41
8 figure is below 42	Permitted

# Heat Pump Sizing

#### **Dwelling 1970 no improvements**

	No improvement to insulation	UPVC/wood Double glazing, + loft insulation	UPVC/wood Double glazing, + loft & cavity wall insulation
1970 to 1995	100 W/m²	85 W/m <sup>2</sup>	70 W/m²
1996 to 2005	80 W/m²	70 W/m <sup>2</sup>	60 W/m²
2006 to 2010	50 W/m²	50 W/m <sup>2</sup>	50 W/m²
New build	40 W/m²	40 W/m²	40 W/m²

Ground floor  $45m_2 + f/floor 45m_2 = 90m_2$ 

 $90 \times 100 = 9$ Kw

After adding improvements Loft insulation & glazing

 $90 \times 85 = 7.65$ Kw



	No improvement to insulation	UP
1970 to 1995	100 W/m²	

			Likely heatin	space ng SPF		size Factor her emitter		Und	erfloor heat screed	ing:		rfloor hea minium pa	
	Temperature Star Rating	Heating circuit flow temperature °C	GSHP	ASHP	Demestic Fan Cenvector/Fan- assisted Radiator	Standard Radiator	Fan Coll Unit	with TILE	with W000	with CARPET	with TILE	with WOOD	with CARPET
	*****	35	4.3	3.6	4.3	6.B	5.0						
	TOTAL COM	40	4.1	3.4	3.1	4.3	3.5						
Room specific	****	45	3.7	3	2.4	3.1	2.6	n-	Jue neat le	SS	Red	uce heat l	SS
eat loss 100 o 120 W/m <sup>2</sup>	that the that	50	3.4	2.7	2.0	2.4	2.1						
	*****	55	3.1	2.4	1.7	1.9	1.7						
	******	60	2.8	2.1	1.4	1.6	1.5						

#### Scenario

Bungalow with 90m² floor area, dwelling heat loss of 10500kw 1980 built located in Humberside.

Heating system 35 under floor heating system incorporating HPC cylinder  $\frac{10500}{90} = 117 \text{w/m}^2 \text{ heat loss}$ 

## **Sap Calculation methods**

Solar sizing

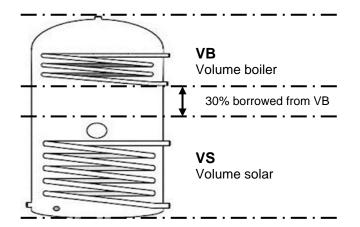
Below table is for new build properties where number of people is unknown

For example 120m<sup>2</sup> TFA equals 111litres VD

The solar VS must be able to hold 80% of the VD

110 x 0.8 = 88.8

88.8litres is lower than the VS volume of 105litres so therefore the cylinder is correct



#### **BSRIA** method

46 + (26 x number of occupants)

For example 3 people

$$46 + 78 = 124$$

$$124 \times 0.8 = 99.2$$

99.2 VS

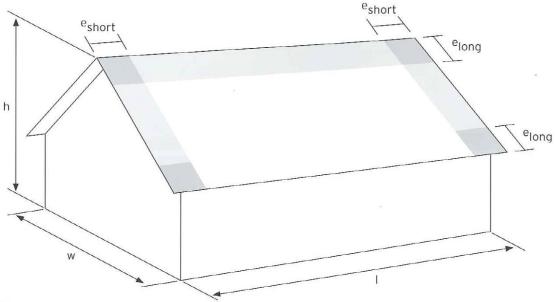
Total Floor area TFA	Assumed Occupancy	Hot water demand
(m2)		(litre/day)
40	1.4	72
80	2.5	100
120	3.0	111
200	3.2	116
300	3.4	121
400	3.6	127

Solar panel sizing

50 litres per panel South facing 30°



Purge for 30mins remove air



#### Key:

- w. Building width
- h. Building height
- I. Building length

Calculate the building width w, building height h and building length I.

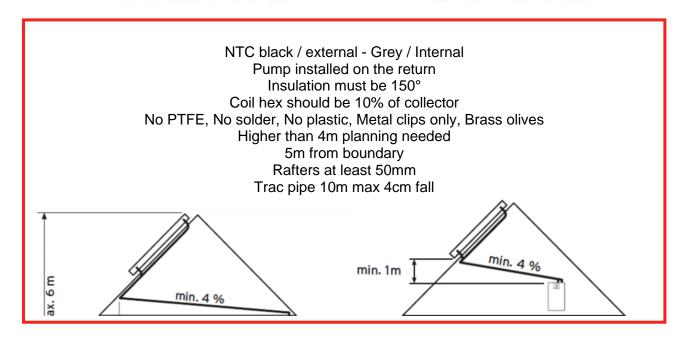
The values for the edge clearances to be observed,  $^{\rm e}$ short and  $^{\rm e}$ long can be found in the following tables.

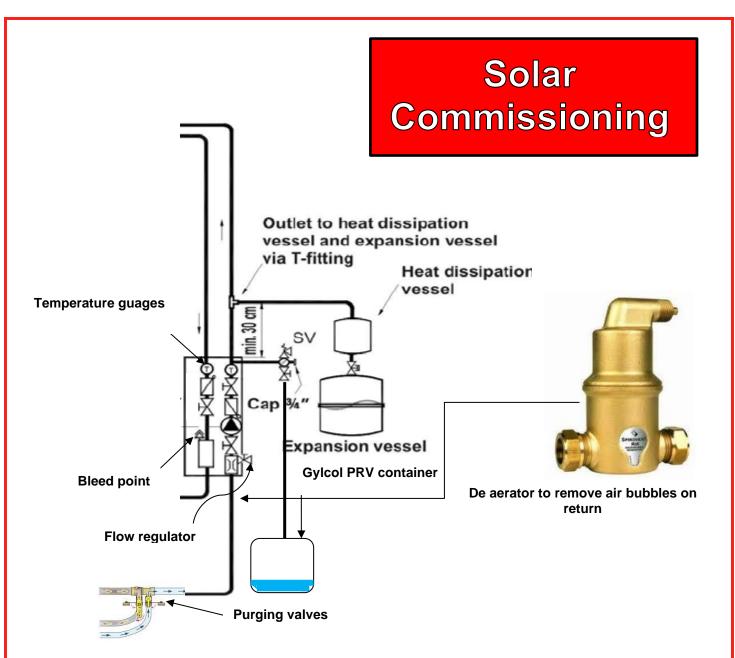
	w				Bui	lding	heigh	nt h	(m)			
	(m)	5	6	7	8	9	10	11	12	13	14	15
	8			//			1.0					
	9						1.0					
(m) w	10						1.0					
	11	1.0					1	.1				
Building width	12	1.0					1.	2				
ding	13	1.0	1.2					1.3				
Build	14	1.0	1.2					1.4				
	15	1.0	1.2	1.4				1.	5			
	16	1.0	1.2	1.4				1.	6			
	17	1.0	1.2	1.4	1.6				1.7			
	18	1.0	1.2	1.4	1.6				1.8			

	1				Bui	lding	heigh	nt h	(m)			
4.0	(m)	5	6	7	8	9	10	11	12	13	14	15
	10			43			1.0				01	
	11	1.0					1.	.1				
(m)	12	1.0					1.	2				
	13	1.0	1.2					1.3				
Building length	14	1.0	1.2					1.4				
ding	15	1.0	1.2	1.4				1.	5			
Build	16	1.0	1.2	1.4				1.	6			
	17	1.0	1.2	1.4	1.6				1.7			
	18	1.0	1.2	1.4	1.6				1.8			
	19	1.0	1.2	1.4	1.6	1.8			1.	9		1
	20	1.0	1.2	1.4	1.6	1.8		-	2	.0		

Edge clearances: <sup>e</sup>short (m)

Edge clearances: elong (m)





#### Servicing

Comissioning	min	max
Flow rate	2l/m	3l/m
Ph levels	7	9
Refractometer	-16	-26
Sanitise	30mins	retest
Flush	30mins	Assess no air bubbles
Pressure	2bar	6bar

#### How to calculate flow rates for solar

Kw x T SHC x TD

Kw amount of energy collector can absorb, Time 1sec SHC fluid gycol 3.9 Temperature difference 6

# Sizing air conditioning units

Calculating air conditiioning required to meet demands,

allow 0.15 per Kw

elements to consider;

- Deduct by 10% if room in shaded area
- Add 10% if in high sun light exposureIf oven in room incase by 1.15Kw
- If more than 2 individuals add 0.18kw pp

(Floor width x Floor length) x 0.15 =

Example room 5.5m by 7.5m, 20 people inside

**Temperature Conversion** 

# **Celsius to Kelvin**

Celsius Kelvin + 273

# **Conversation for Fahrenheit**

Celsius Fahrenheit 
$$(cx 1.8) + 32 =$$

Fahrenheit Celsius 
$$F - 32 \div 1.8 =$$

#### Example

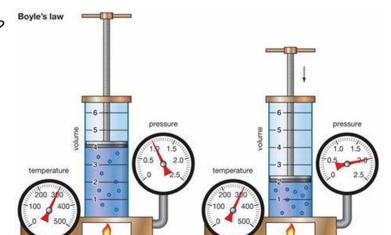
Tyre pressure is 11.41I @44psi,

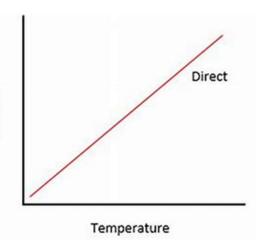
What will the pressure be at 10.66l?

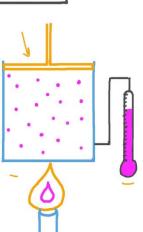
 $P1 \times V2 \div V1 = P2$ 

 $44 \times 11.41 = 47.36$ 

10.6







**Boyes Law** 

Example

275ml @ 25°c what will be the volume at 50 c

Always concert to Kelvin

25 + 273 = 298

50 + 273 = 323

275 = ??? = 88.825 divide by lower T1 for new V1 = 298

298 Multiply 323

#### Example

A vessel is 250k in temperature with volume of 3.5l, when the vessel temperature is increased to 400k what will be the new volume?

Volume

# Chillers

Calculate the amount of heat that must be removed from 500 kg of poultry that is to be stored at -18°C if it is to enter the refrigerated space at 7°c.

Specific heat of poultry before freezing = 3.18 kj/kg KSpecific heat of poultry after freezing = 1.55 kj/kg KLatent heat of fusion (hfg) = 246 kj/kgFreezing temperature of poultry = -2.75°c

QT = hSB + hSA + hL

Where:- QT = Total heat.

hSB = sensible heat before freezing

hSA = sensible heat after freezing

*hL* = *Latent heat* 

QSB = sensible heat before freezing

 $QSB = m \times sp.ht \times td$ 

 $QSB = 500 \times 3.18 \times (7 - (-2.75))$ 

 $QSB = 5L00 \times 3.18 \times 9.75$ 

 $QSB = kg \times kj/kg K \times K$ 

 $QSB = 500 \times 3.18 \times 9.75 = 15502.5 \text{ kj}$ 

QSA = sensible heat after freezing (sensible heat is adding heat)

 $QSA = m \times sp. ht. \times td$ 

 $QSA = 500 \times 1.55 \times (-2.75(-18))$ 

 $QSA = 500 \times 1.55 \times 15.25$ 

 $QSA = kg \times kj/kg K \times K$ 

 $QSA = 500 \times 1.55 \times 15.25 = 11818,75 \text{ kj}$ 

QL = Latent heat after freezing (heat that doesnt change)

QL = m x hfg

QL = kg x kj/kg

 $QL = 500 \times 246 = 123000 \text{ kj}$ 

QT = QSB + QSA + QLT =

QT = 15502.5 + 11818.75 + 123000 = 150321.25 kj

# Air conditioning

Solar gain = radiation

Heat gain = room generated

Heat gain (w) =  $(Area m_2) x (U valve W/m_2 K) x (Sat - Int temp)$ 

- All testing should confirm with BSEN 378
- New or old system
- Refrigeration type
- New systems x 1.43
- Old systems x 1.1
- LP temperature 320
- HP temperature 550 ( water cooled 430)
- If needed remove drier
- Nitrogen can cause suffocation

Existing ( c )	New ( c )	Side
1.1 x 55	1.43 x 55	HP
1.1 x 32	1.43 x 32	LP
1.1 x 32	1.43 x 43	Water cooled

#### CALCULATION OF STRENGTH TEST = $1.1 \times PS$

**EXAMPLE** 

HIGH SIDE (Air cooled condenser)

55°C on R407F = 26.16 Bar

26.16 Bar × 1.1 = 28.78 Bar on the high side

LOW SIDE (Heat exchanger exposed to indoor ambient)

27°C on R407F = 11.07 Bar

11.072 Bar × 1.1 = 12.18 Bar

High Side Strength Test Pressure = 28.78 Bar

Low Side Strength Test Pressure = 12.18 Bar

REMEMBER: The high side test pressure could exceed the rating of the pressure relief valves (PRV's). If this is the case, then they should be removed and plugged for the strength test procedure.



# **Leak Check Report**

Site Name and address		Date	
		Leak checked by	
		Company Name	
Location of plant		Equipment Model	
Refrigerant Type	Single / Blend	Refrigerant Qty (kg)	

# Condenser

Calculated Discha	arge Pressure (I	bar)		
Calculated Discha (°c) (using pressure read		ire		
Discharge Pressure (bar)	Condensing Temperature (°c)	Liquid Line Temperature (°c)	Air On Temperature	Air Off Temperature
Temperature Difference			23	

# Evaporator

Calculated Su	ction Pressure	(bar)		
Calculated Su (°c) (using pressure	ction Tempera	ture		
Suction Pressure (bar)	Evaporating Temperature (°c)	Suction Temper (°c)	 Air On Temperature (°c)	Air Off Temperature (°c)
Temperature Difference				

	Safet	y group
Higher Flammability	A3	В3
Lower	A2	B2
Flammability	A2L*	B2L*
No flame Propagation	A1	B1
	Lower Toxicity	Higher Toxicity

<sup>\*</sup>A2L and B2L are lower flammability refrigerants with a maximum burning velocity of ≤ 10 cm/s

## Refrigerants Safety Data

Products and equipment	Minimum Frequency
Hermetic System with GWP< 10 of CO2	Not Required
System with GWP = 5 TONES of CO2	Once every 12 months
System with GWP = 50 TONES of CO2	Twice every 12 month
System with GWP = 500 TONES of CO2	Four Times every 12 month
∘ Leak Testing	

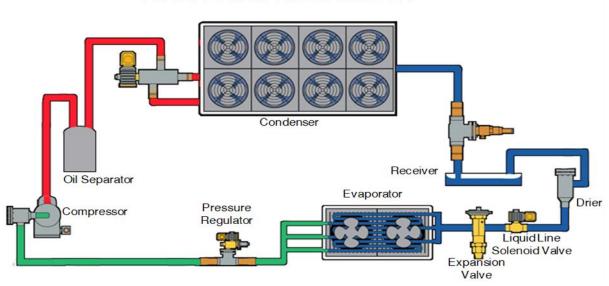
System Below 3 kg Semi Hermetic and 6 kg Hermetic (If labelled correctly) do not require leakage testing under this article until 1/1/2017

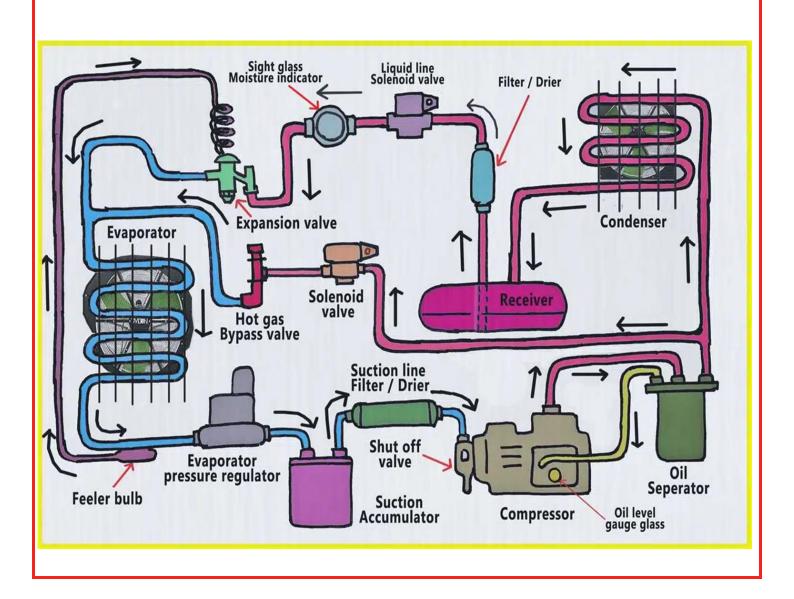
Products and equipment	Minimum Frequency
System with GWP = 5 TONES of CO2	Once every 24 months
System with GWP = 50 TONES of CO2	Once every 12 months
System with GWP = 500 TONES of CO2	Once every 6 months

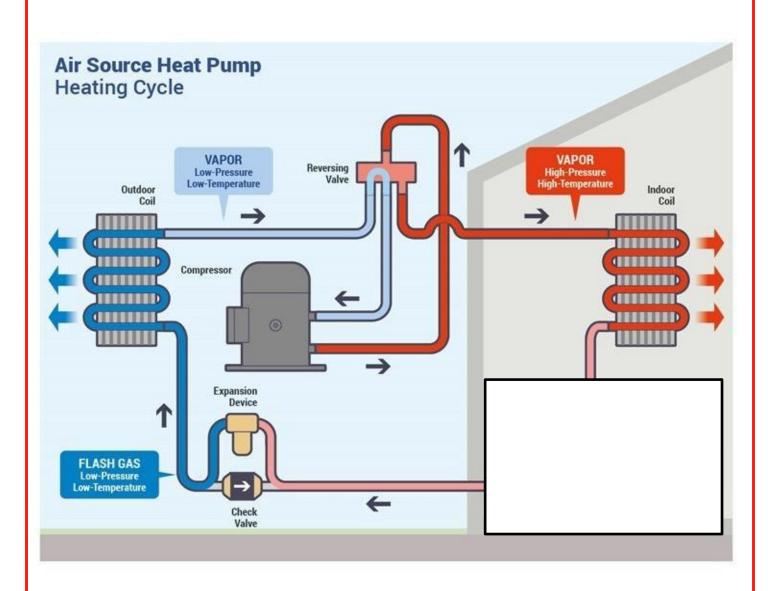
Leak Testing with leak detection system installed

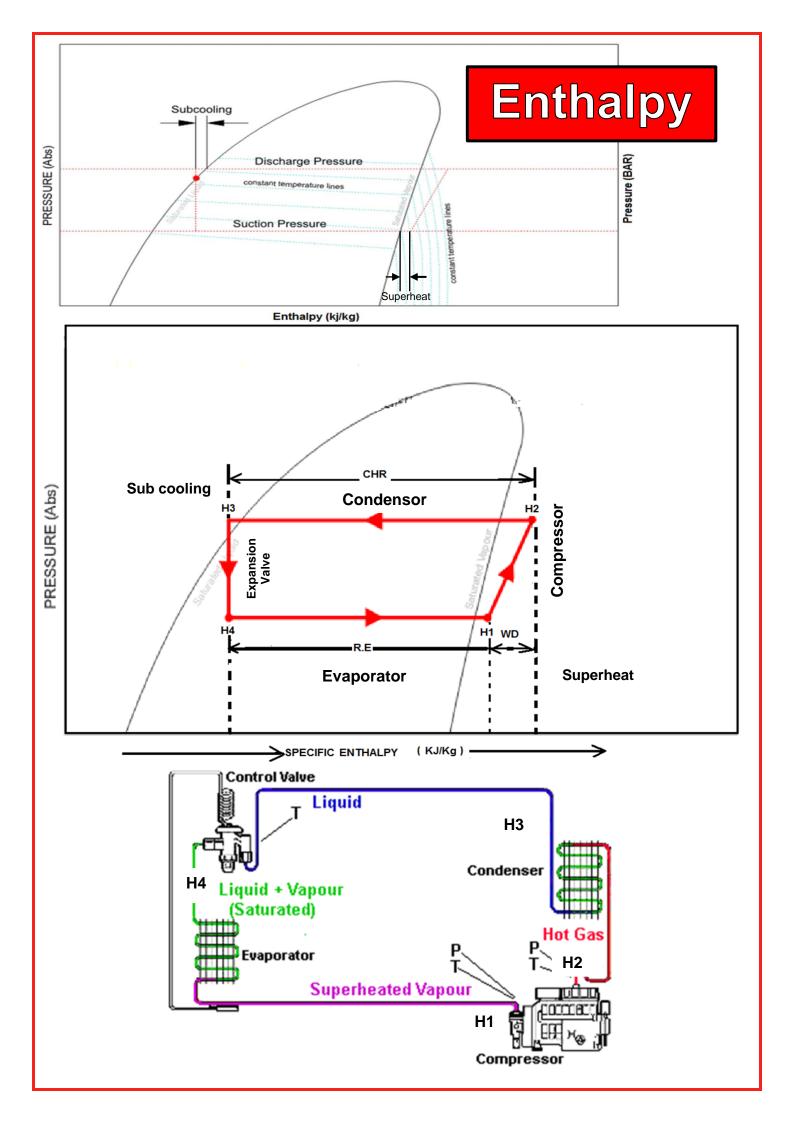
Operators of the equipment containing fluorinated greenhouse gases in quantities of 500 tonnes of CO2 equivalent or more, shall ensure that the equipment is provided with a leakage detection system which alerts the operator or a service company of any leakage. Leak Check Minimum Mass of Refrigerant

#### A REFRIGERATION CIRCUIT









# **Enthalpy**

Mass Flow Rate of Refrigerant (m) = Cooling duty / (H1 – H4)

Measured in kg/s

Work Done by Compressor  $= (H2 - H1) \times m$ 

Measured In kw

Condenser capacity measured =  $(H2 - H3) \times m$ 

In kw

Refrigeration Effect measured =  $(H1 - H4) \times m$ 

In kw

Volume Flow Rate (v) measured = Specific volume x m

In m<sup>3</sup>/s

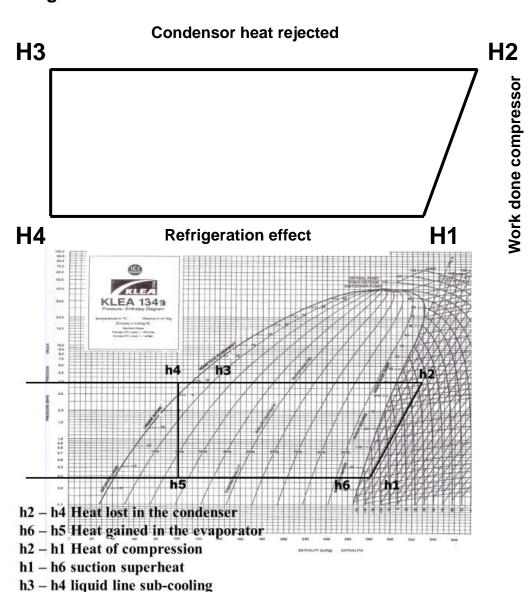
Coefficient of Performance (COP) = Refrigeration effect

No units(simply a ratio) (H1 – H4) / work done (H2 – H1)

#### Refrigerant flow rates

Kw = 10Kw = 0.05Kg/s

HRE 200kg



# Compressor testing



Above: Remove compressor casing

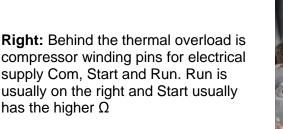
Left: Pull off wiring harness



Right: Thermal overload, reset may need pressing instances of overheating, the ohms reading should be lower than 0.3Ω

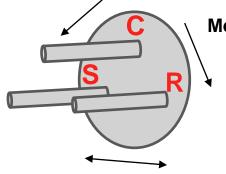


**Left:** Relay, soft compressor start, Resistance should be lower than  $0.3\Omega$ 





Measure  $\Omega$  C to S



Measure Ω C to R

Compressors can fail due to low oil levels, overheating from refrigeration pressures, lack of cooling water from condense and fan failure

Measure  $\Omega$  S to R which should be equal to CS + CR

Tc = condensing temperature
Ta = ambient temperature
te= evaporating temperature
tei = air inlet to the evaporator

TDc = Tc - Ta TDe = tei - te

For air cooled condensers :
Hot climates ----- TDc = 6 to 8°C
Normal climates ----- TDc = 8 to 10 °C
cold climates ----- TDc = 12 to 15 °C

# TEV sizing formula

Ta 32 Te -35

39.4k

#### JEHS-1400-B4-L-3 EVI

Amount of Sub-cooling (K)							
Ta\Te	e -40 -35 -30 -25 -20						
27	38.8	37.3	35.8	34.3	32.8		
32	41.3	39.4	37.6	35.8	34.0		
35	42.7	40.7	38.7	36.7	34.6		
38	44.2	42.0	39.7	37.5	35.3		
43	46.6	44.1	41.5	39.0	36.5		

# Glossary

Building Regs approved document J: Combustion appliances & fuel storage systems Building Regs approved document F: Ventilation

The Water Supply (Water Fittings) Regulations 1999

The Gas Safety (Installation and Use) Regulations 1998

The IET 18th Edition Wiring Regulations BS 7671.

British Standards for designing central heating systems include:

BS EN 12828: Heating systems in buildings. Design water-based heating systems

BS EN 12831: Heating systems in buildings Method for calculation of design load.

BS EN 442: Radiators and convectors. Technical specifications and requirements.

#### Other correction factors for radiators

Radiator connection factor	f2
Top and bottom same end (TBSE)	1.00
Top and bottom opposite end (TBOE)	1.05
Bottom opposite end (BOE)	0.96

Enclosure factor	F3
Fixed on plain surface	1.00
Shelf over radiator	0.95
Fixed in open recess	0.90
Encased in cabinet with front or top grille	0.70 or 0.80

Paint finish factor	F4
Oil or water based paint	1.00
Metallic based paint	0.85

#### Desired room temperatures

Room	Room Temperature <sup>o</sup> C
Living Room	21
Dining Room	21
Bedsitting room	21
Bedroom	21
Hall and Landing	21
Kitchen	21
Bathroom	22
Toilet	21
Unheated (including floor)	10

calculating ventilation heat loss:

#### Category A

Air change rates for older existing buildings (pre 2000)

#### Category B

Air change rates for modern buildings (2000 or later) with double glazing and regulatory minimum insulation

Category C
New buildings (constructed after 2006) complying with all current Building Regulations

Room	Category A	Category B	Category C
Lounge/living room	1.5	1	0.5
Dining/breakfast room	1.5	1	0.5
Kitchen	2	1.5	1.5
Hall	2	1	0.5
Cloaks/WC	2	1.5	1.5
Utility room	3	2	0.5
Study	1.5	1.5	0.5
Bedroom	1	1	0.5
Bedroom with ensuite bath	2	1.5	1
Internal room or corridor	0	0	0
Landing	2	1	0.5
Bathroom/shower room	3	1.5	1.5
Storeroom	1	0.5	0.5

# Softline temperature table

#### **TEMPERATURES**

Factors for differences between mean water temperature and room temperature in °C and °F other than 50°C (90°F)

	°C	0	F
5	0.050	10	0.057
10	0.123	20	0.142
15	0.209	30	0.240
20	0.304	40	0.348
25	0.406	50	0.466
30	0.515	60	0.590
35	0.629	70	0.721
40	0.748	80	0.858
45	0.872	90	1.000
50	1.000	100	1.147
55	1.132	110	1.298
60	1.267	120	1.454
65	1.406	130	1.613
70	1.549	140	1.776
75	1.694	-	-

#### Other correction factors for radiators

Radiator connection factor	f2
Top and bottom same end (TBSE)	1.00
Top and bottom opposite end (TBOE)	1.05
Bottom opposite end (BOE)	0.96

Enclosure factor	F3
Fixed on plain surface	1.00
Shelf over radiator	0.95
Fixed in open recess	0.90
Encased in cabinet with front or top grille	0.70 or 0.80

Paint finish factor	F4
Oil or <u>water based</u> paint	1.00
Metallic based paint	0.85

# **Heating pipe resistances**

Fitting description	Equivalent length of straight pipe in metres			es	
Pipe diameter (copper)	10mm	15mm	22mm	28mm	35mm
Straight valves	0.5	0.5	0.6	0.6	0.8
Angle valves	2.0	2.0	4.5	6.0	N/A
Press fit/ capillary elbow	1.7	1.4	1.3	1.3	1.2
Tee branch (press fit)	1.7	1.5	1.5	1.7	2.0
Tee branch (capillary)	0.6	0.7	1.0	1.3	1.5
Radiator heat emitter	Assume 1 metre pipe per metre of radiator length				

# Cylinder heat loss

Norminal Capacity (litres)	Standing heatloss			
	Per day (kwh/24hr)	Per year (kwh/365d)		
120	1.24	453		
150	1.43	522		
170	1.54	562		
210	1.89	690		
250	2.07	756		
300	2.36	961		
Tested to BS EN 12897 : 2016 stored 20 heated to 60				

# Gas rating chart

Time taken for 1 complete revolution of meter test dial (1ft <sup>2</sup> )		Gas flow rate		Calculated heat input	
min	sec	ft³/hr	m³/hr	kW/hr	BTUs/hr
10	0	6.000	0.168	1.80	6146.15
9	55	6.050	0.169	1.82	6197.80
9	50	6.102	0.171	1.83	6250.32
9	45	6.154	0.172	1.85	6303.74
9	40	6.207	0.174	1.86	6358.09
9	35	6.261	0.175	1.88	6413.37
9	30	6.316	0.177	1.90	6469.63
9	25	6.372	0.178	1.91	6526.88
9	20	6.429	0.180	1.93	6585.16
9	15	6.486	0.182	1.95	6644.49
9	10	6.545	0.183	1.97	6704.89
9	5	6.606	0.185	1.98	6766.40
9	0	6.667	0.187	2.00	6829.05
8	55	6.729	0.188	2.02	6892.88
8	50	6.792	0.190	2.04	6957.90
8	45	6.857	0,192	2.06	7024.17
8	40	6.923	0.194	2.08	7091.71
8	35	6.990	0.196	2.10	7160.56
8	30	7.059	0.198	2.12	7230.76
8	25	7.129	0.200	2.14	7302.36
8	20	7.200	0.202	2.16	7375.38
8	15	7.273	0.204	2.18	7449.88
8	10	7.347	0.206	2.21	7525.90
8	5	7.423	0.208	2.23	7603.48
8	0	7.500	0.210	2.25	7682.69
7	55	7.579	0.212	2.28	7763.56
7	50	7.660	0.214	2.30	7846.15
7	45	7.742	0.217	2.32	7930.52
7	40	7.826	0.219	2.35	8016.72
7	35	7.912	0.222	2.38	8104.81
7	30	8.000	0.224	2.40	8194.87
7	25	8.090	0.227	2.43	8286.94 8381.11
7	20	8.182	0.229	2.46	8477.45
7	15	8.276	0.232	2.51	8576.02
7	10	8.372	0.234	2.54	8676.92
7	5	8.471	0.237	2.57	8780.21
7	0	8.571	0.243	2.60	8886.00
6	55	8.675	0.246	2.64	8994.36
6	50	8.780 8.889	0.249	2.67	9105.41
6	45	9.000	0.252	2.70	9219.22
6	35	9.114	0.255	2.74	9335.92
6	30	9.231	0.258	2.77	9455.61
6	25	9.351	0.262	2.81	9578.41
6	20	9.474	0.265	2.84	9704.45
6	15	9.600	0.269	2.88	9833.84
6	10	9.730	0.272	2.92	9966.73
6	5	9.863	0.276	2.96	10103.26
6	0	10.000	0.280	3.00	10243.58
5	55	10.141	0.284	3.04	10387.86
5	50	10.286	0.288	3.09	10536.26
5	45	10.435	0.292	3.13	10688.96
5	40	10.588	0.296	3.18	10846.13
5	35	10.746	0.301	3.23	11008.0
5	30	10.909	0.305	3.28	11174.8
5	25	11.077	0.310	3.33	11346.7
5	20	11.250	0.315	3.38	11524.0
5	15	11.429	0.320	3.43	11706.9
5	10	11.613	0.325	3.49	11895.7
5	5	11.803	0.330	3.54	12090.7
5	0	12.000	0.336	3.60	12292.3
4	55	12.203	0.342	3.66	12500.6
4	50	12.414	0.348	3.73	12716.1
4	45	12.632	0.354	3.79	12939.2
4	40	12.857	0.360	3.86	13170.3
4	35	13.091	0.367	3.93	13409.7
4	30	13.333	0.373	4.00	13658.1

Time taken for 1 complete revolution of meter test dial (1ft <sup>3</sup> )		omplete clution of er test dial		Calculated heat input		
min	sec	ft³/hr	m³/hr	kW/hr	BTUs/hr	
4	25	13.585	0.380	4.08	13915.81	
4	20	13.846	0.388	4.16	14183.42	
4	15	14.118	0.395	4.24	14461.53	
	-		0.403	4.32	14750.76	
4	10	14.400		4.41	15051.79	
4	5	14.694	0.411		15365.37	
4	0	15.000	0.420	4.50		
3	55	15.319	0.429	4.60	15692.30	
3	50	15.652	0.438	4.70	16033.43	
3	45	16.000	0.448	4.80	16389.73	
3	40	16.364	0.458	4.91	16762.23	
3	35	16.744	0.469	5.03	17152.04	
3	30	17.143	0.480	5.15	17560.43	
3	25	17.561	0.492	5.27	17988.73	
3	20	18.000	0.504	5.40	18438.45	
3	15	18.462	0.517	5.54	18911.23	
3	10	18.947	0.531	5.69	19408.89	
3	5	19.459	0.545	5.84	19933.46	
3	0	20.000	0.560	6.00	20487.16	
2	55	20.571	0.576	6.18	21072.51	
2	50	21.176	0.593	6.36	21692.29	
	45	21.818	0.611	6.55	22349.63	
2	40	22.500	0.630	6.76	23048.06	
2		The state of the s		6.97	23791.55	
2	35	23.226	0.650		24584.60	
2	30	24.000	0.672	7.21	The second secon	
2	25	24.828	0.695	7.45	25432.34	
2	20	25.714	0.720	7.72	26340.64	
2	15	26.667	0.747	8.01	27316.22	
2	10	27.692	0.775	8.31	28366.84	
2	5	28.800	0.806	8.65	29501.52	
2	0	30.000	0.840	9.01	30730.75	
1	55	31,304	0.877	9.40	32066.87	
1	50	32.727	0.916	9.83	33524.45	
1	45	34.286	0.960	10.29	35120.85	
1	40	36.000	1.008	10.81	36876.90	
1	35	37.895	1.061	11.38	38817.79	
1	30	40.000	1.120	12.01	40974.33	
1	25	42.353	1.186	12.72	43384.58	
_	-		1.260	13.51	46096.12	
1	20	45.000	1.344	14.41	49169.19	
1	15	48.000	-		52681.28	
1	10	51.429	1.440	15,44	The second secon	
1	5	55.385	1,551	16.63	56733.69	
1	0	60.000	1.680	18.01	61461.49	
0	58	62.069	1.738	18.63	63580.86	
0	56	64.286	1.800	19.30	65851.60	
0	54	66.667	1.867	20.01	68290.55	
0	52	69.231	1.938	20.78	70917.11	
0	50	72.000	2.016	21.62	73753.79	
0	48	75.000	2,100	22.52	76826.87	
0	46	78.261	2.191	23.50	80167.17	
0	44	81.818	2.291	24.56	83811.13	
0	42	85.714	2.400	25.73	87802.13	
0	40	90.000	2.520	27.02	92192.24	
0	38	94.737	2.653	28.44	97044.46	
0	36	100.000	2.800	30.02	102435.82	
		105.882	2.965	31.79	108461.46	
0	34		The second second second	33.78	115240.30	
0	32	112.500	3.150		122922.9	
0	30	120.000	3.360	36.03	The second secon	
.0	28	128.571	3.600	38.60	131703.20	
0	26	138.462	3.877	41.57	141834.2	
0	24	150.000	4.200	45.03	153653.7	
0	22	163.636	4.582	49.13	167622.2	
0	20	180.000	5.040	54.04	184384.4	
0	18	200.000	5.600	60.04	204871.6	
0	16	225.000	6.300	67.55	230480.6	
0	14	257.143	7.200	77.20	263406.4	
0	12	300.000	8.400	-	307307.4	
U	1.6.	360.000	10.080		368768.9	

## **Gas Pipe sizing chart**

Based on straight actual length with 1mb droppage from both ends

use 0.5m for a bend & 0.3m for a machine bend

	Length of	pipe (m)						
	3	6	9	12	15	20	25	30
mm (OD)	Discharg	e (m <sup>3</sup> /hr)						
8	00.29	00.14	00.49	00.07	00.05	-	-	-
10	00.86	00.57	00.50	00.37	00.30	00.22	00.18	00.15
12	01.50	01.00	00.85	00.82	00.69	00.52	00.41	00.34
15	02.90	01.90	01.50	01.30	01.10	00.95	00.92	00.88
22	08.70	05.80	04.60	03.90	03.40	02.90	02.50	02.30
28	18.00	12.00	09.40	08.00	07.00	05.90	05.20	04.70
35	32.00	22.00	17.00	15.00	13.00	11.00	09.50	08.50

## **Underfloor heating**

Underfloor heating Outputs W/m2

# Overlay™ and Overlay™ Lite Solid Floor



Mean water temperature °C	Pipe spacing mm	Output W/m²	Surface floor temperature °C
40	150	61.0	25.8
45	150	68.0	26.3
50	150	79.0	28.1
55	150	101.0	30.1
60	150	124.0	32.0



Mean water temperature °C	Pipe spacing mm	Output W/m²	Surface floor temperature °C
40	100	60.9	25.7
45	100	76.2	27.0
50	100	91.6	28.3
55	100	95.0	28.6
40	200	50.8	24.9
45	200	63.6	26.0
50	200	76.3	27.0
55	200	77.0	27.2
40	300*	42.8	24.2
45	300*	53.6	25.1
50	300*	64.3	26.0
55	300*	66.7	26.9

# **Suspended and Floating Floor**



Mean water temperature °C	Pipe spacing mm	Output W/m²	Surface floor temperature °C
40	225/300	31.7	23.1
45	225/300	40.2	23.9
50	225/300	49.2	24.7
55	225/300	50.0	24.8
60	225/300	52.3	25.0

# **MHP System**



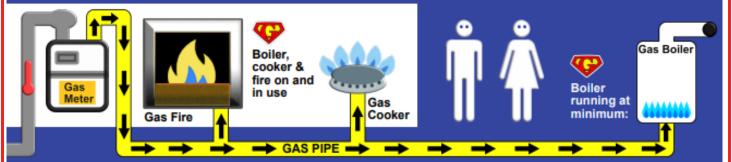
Mean water temperature °C	Pipe spacing mm	Output W/m²	Surface floor temperature °C
40	90	52.0	25.0
45	90	64.0	26.0
50	90	76.0	27.0
55	90	100.0	29.0
60	90	124.0	31.0

Credits: Paul Hull (founder of The Gas Safety Superheroes)

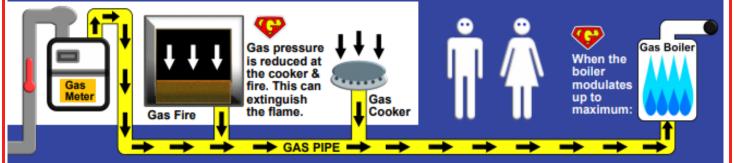
# THE GAS SAFETY SUPERHEROES THE DANGERS OF AN UNDERSIZED GAS PIPE:

If a gas pipe is undersized, the way a new boiler draws gas through the gas pipe from the gas meter can lead to problems with the boiler and other gas appliances in the property.

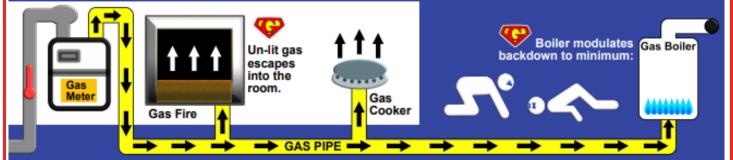
Undersized gas pipes can contribute to incomplete combustion that can produce carbon monoxide.



If the gas pipe is not large enough, you could draw the flame off the cooker, fire or both through reduced pressure, and then end up with un-lit gas escaping from the cooker burners & gas fire when the boiler modulates down again.



Exposure to extremely high levels of natural gas can cause loss of consciousness or even death. if a natural gas leak has occurred and is severe, oxygen can be reduced, causing dizziness, fatigue, nausea, headache, and irregular breathing.

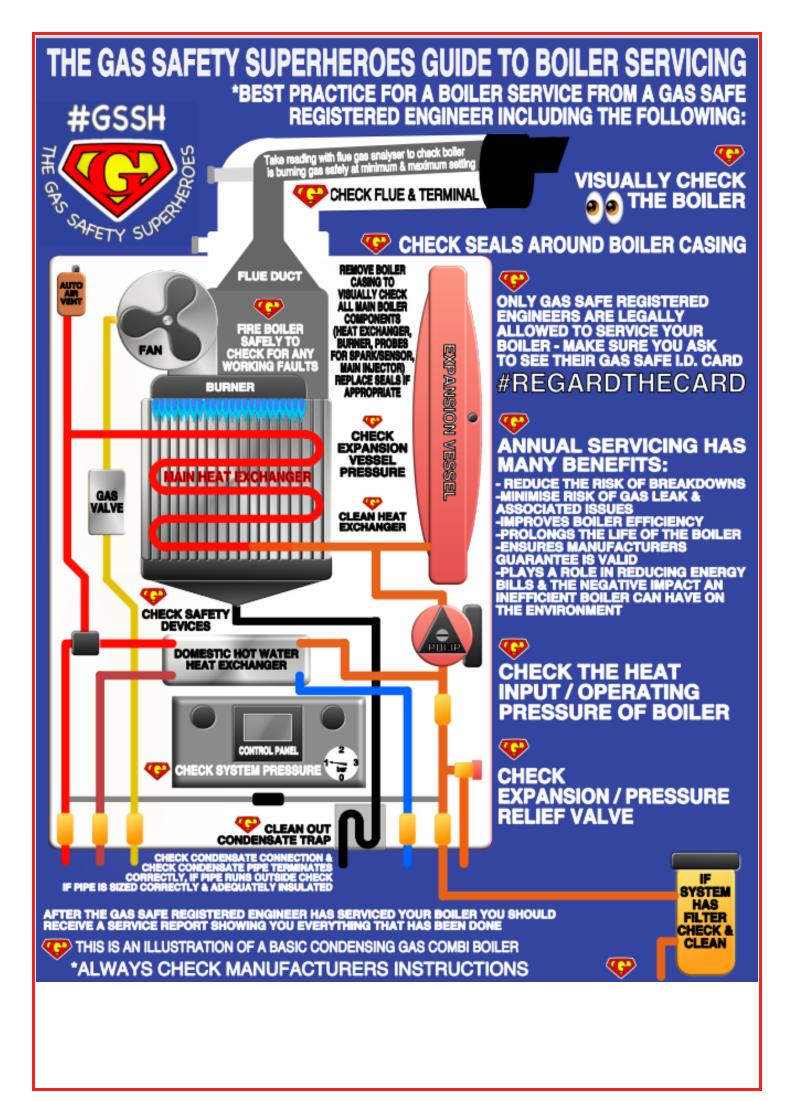


When natural gas fills a room, it just takes one spark for an explosion that can destroy a home and end lives. Smell Gas? To report a gas or carbon monoxide emergency call the National Gas Emergency Service 24 hours a day on 0800 111 999





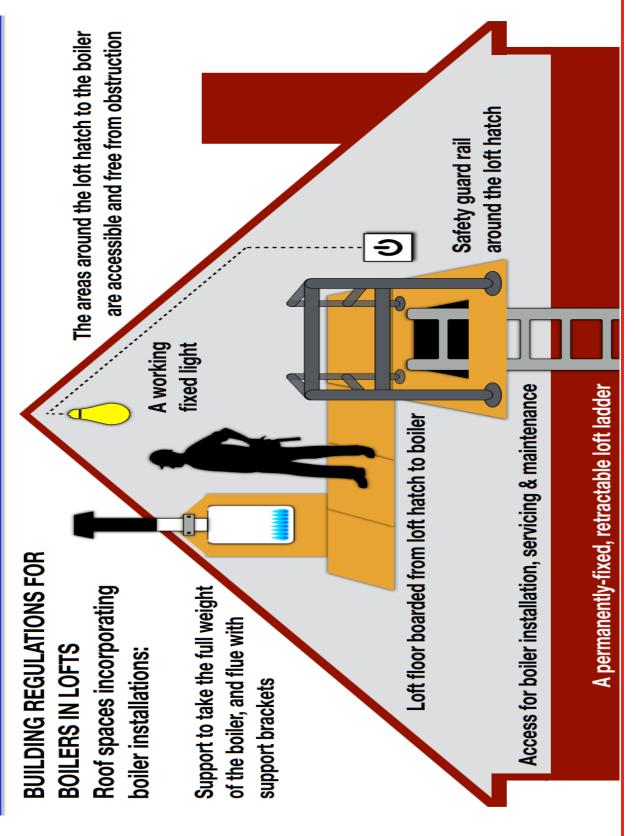
If your gas pipe has only 15mm diameter pipe coming straight off your gas meter or is a long distance in 15mm pipe to your gas appliances then it is possible you need to upgrade your gas pipe. If you are unsure if you actually need to upgrade your gas pipes, contact your local Gas Safe Registered engineer to carry out an assessment (and quote if necessary).





# THE GAS SAFETY SUPERHEROES







# THE GAS SAFETY SUPERHEROES

#### BOILER AND FLUE GAS ANALYSER TECHNICAL SUPPORT PHONE NUMBERS AND WEBSITES:

BOILER: ALPHA HEATING INNOVATION	0344 871 8760 https://www.alpha-innovation.co.uk/installers
BOILER: ARISTON	0333 240 7777 https://www.ariston.com/uk/
BOILER: ATAG	0800 254 5065 http://atagheating.co.uk/installer/
BOILER: BAXI	0344 871 1545 https://www.baxi.co.uk/trade
BOILER: BIASI	01922 714 636 http://www.biasi.co.uk/
BOILER: FERROLI	0330 205 0005 https://www.ferroli.co.uk/
BOILER: GLOW-WORM	01773 828 300 https://www.glow-worm.co.uk/trade/
BOILER: IDEAL	01482 498 663 http://idealboilers.com/installer/
BOILER: INTERGAS	01527 888 000 https://www.intergasheating.co.uk/installer/
BOILER: KESTON	01482 443 005 http://www.keston.co.uk/
BOILER: MAIN	0344 871 1545 https://www.mainheating.co.uk/
BOILER: NAVIEN	020 3598 2020 https://navienuk.com/
BOILER: POTTERTON	0344 871 1545 http://www.potterton.co.uk/
BOILER: RAVENHEAT	0113 252 7007 https://ravenheat.co.uk/
BOILER: SIME	0345 901 1114 http://sime.co.uk/installers/
BOILER: VAILLANT	0344 693 3133 https://www.vaillant.co.uk/for-installers/
BOILER: VIESSMANN	01952 675 070 https://www.viessmann.co.uk/
BOILER: VOKERA	0844 391 0999 http://www.vokera.co.uk/
BOILER: WORCESTER BOSCH	0330 123 3366 https://www.worcester-bosch.co.uk/

FLUE GAS ANALYSER: ANTON	01923 274 730	https://www.anton-group.com/index.htm
FLUE GAS ANALYSER: KANE	0800 059 0800	https://www.kane.co.uk/
FLUE GAS ANALYSER: TESTO	01420 358 123	https://www.testo.com/en-UK/
FLUE GAS ANALYSER: T.P.I.	01293 530 196	https://www.tpieurope.com/