

Heat Recovery Steam Generators for Flexibility

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IAGT October 2016*

Overview

- The grids needs flexible power
- HRSG and OTSG Designs
- Supplementary Firing
- Fresh Air Firing Case Study
- Balance of Plant Considerations

The Grid Needs Flexible Power

Changes in Electricity Generation

- Base loaded power plants
 - High fixed costs
 - Low operating costs
 - Nuclear, Coal
 - Large power plants can take days to reach steady state



Source: www.opg.com

Pickering (~3.1GW)



Nanticoke Generating Station (~4GW)

Changes in Electricity Generation

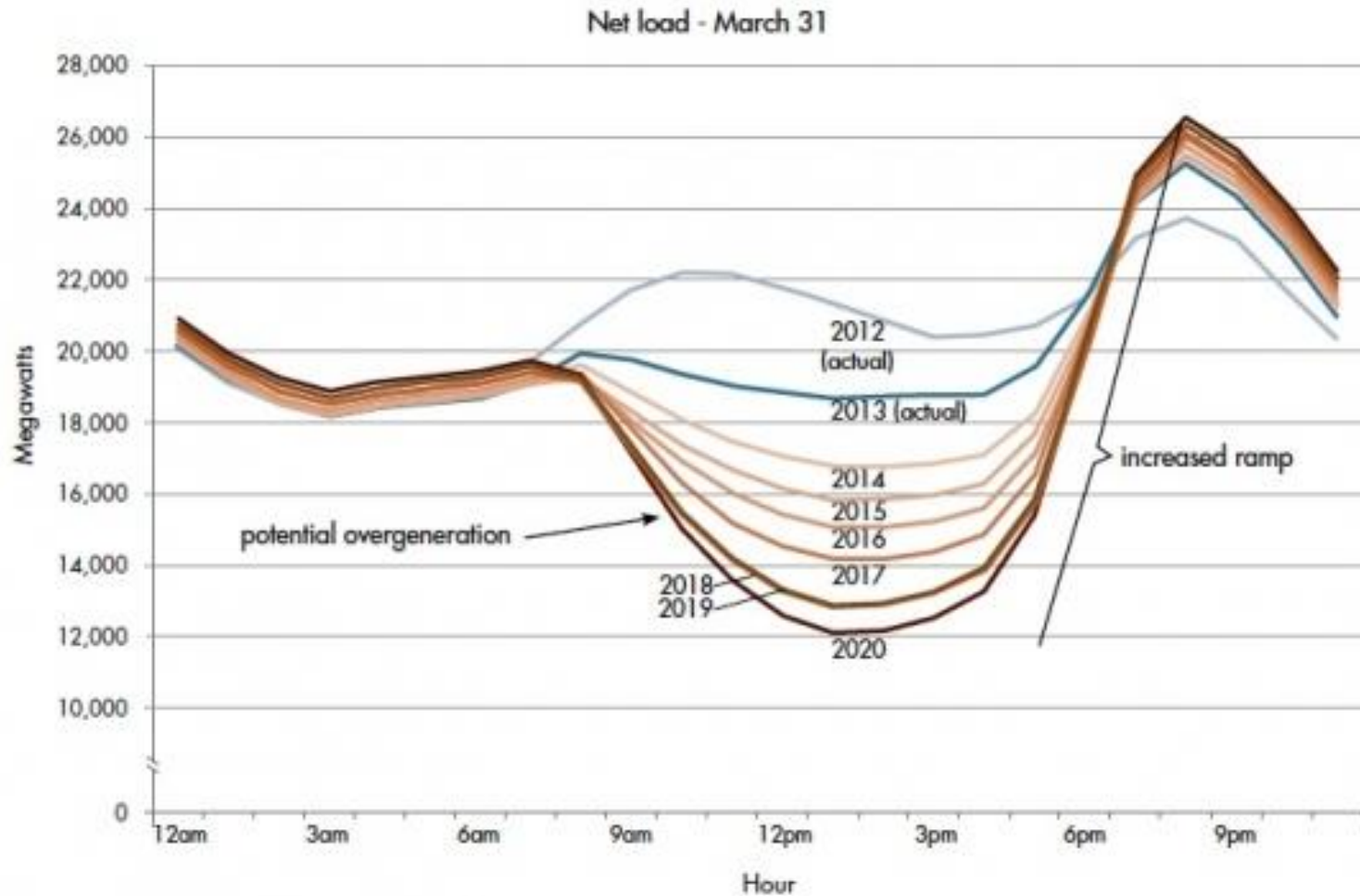
- Peaking Power Plants
 - Simple Cycle Power Plants
 - Combined Cycle Power Plants (CCPPs)
 - Hydroelectric
 - Renewables



Source: www.opg.com

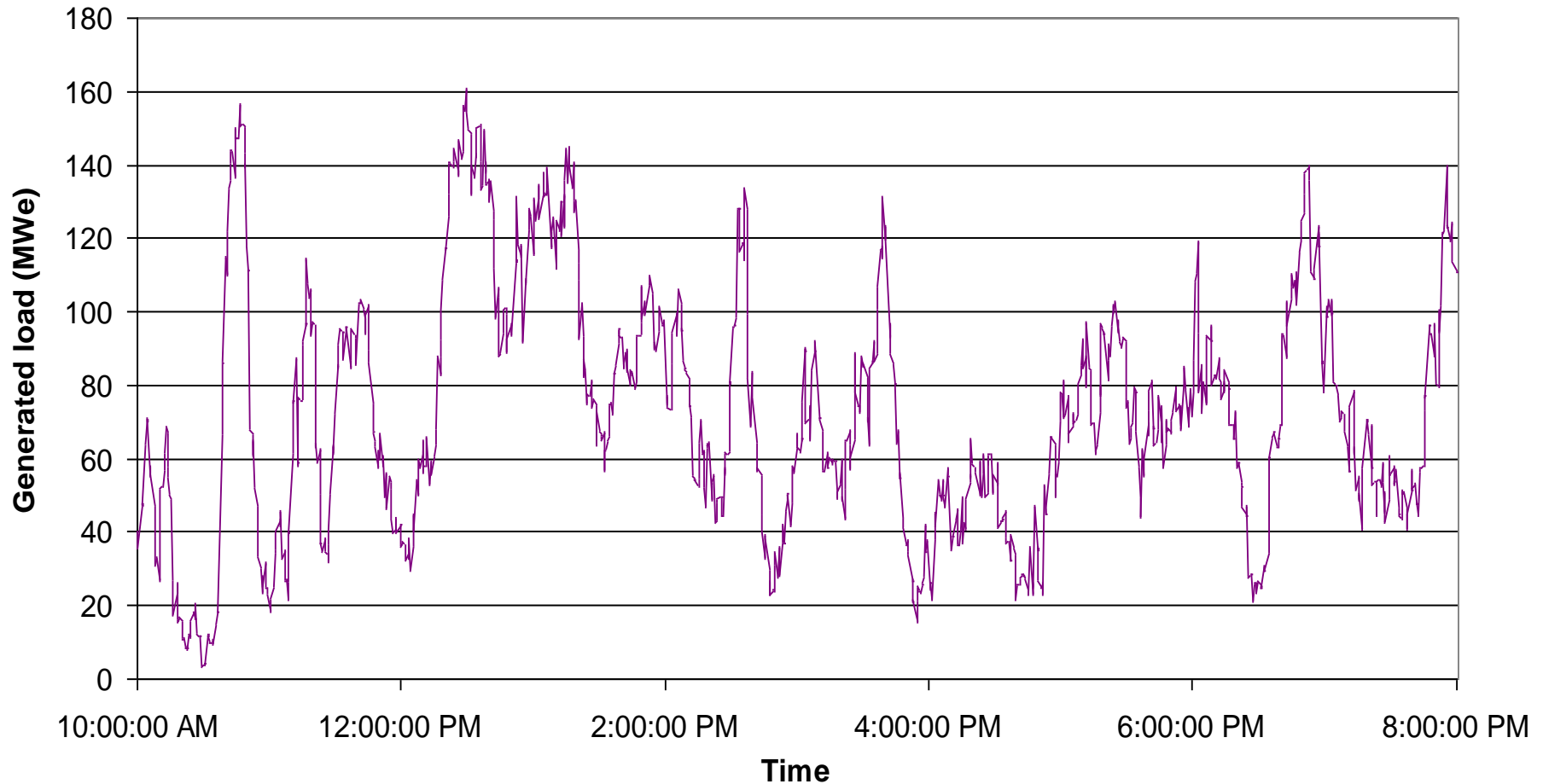


California's "Duck" Curve

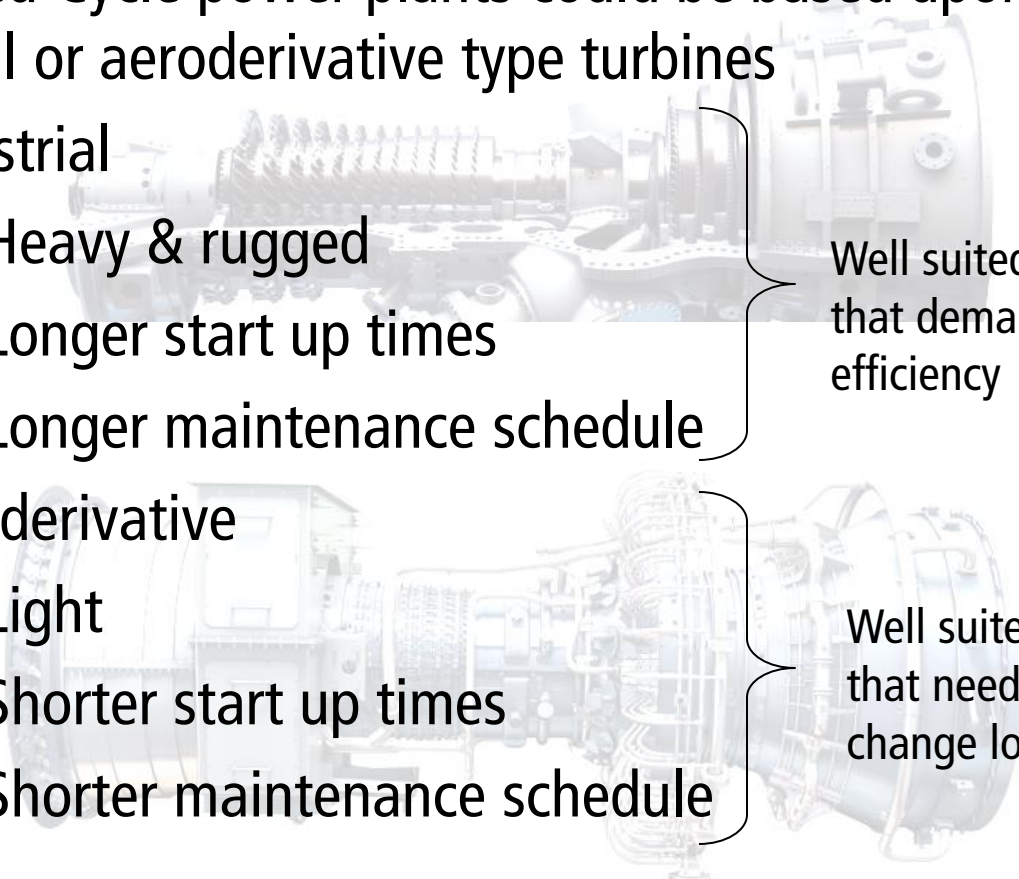


Changes in Electricity Generation

- OTSG-based cycling combined cycle plant loading



Changes in Electricity Generation

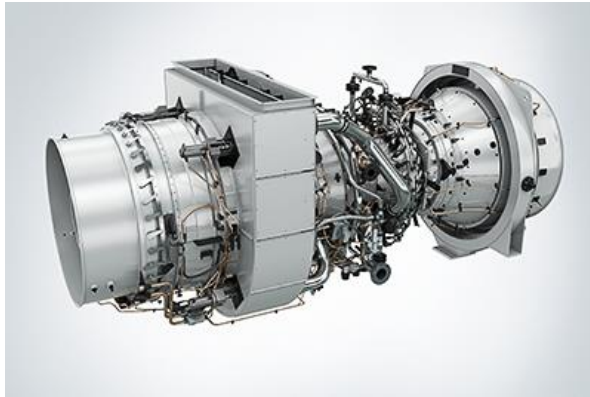
- Combined Cycle power plants could be based upon industrial or aeroderivative type turbines
 - Industrial
 - Heavy & rugged
 - Longer start up times
 - Longer maintenance schedule

Well suited to plants that demand base-loaded efficiency
 - Aeroderivative
 - Light
 - Shorter start up times
 - Shorter maintenance schedule

Well suited to plants that need to start up/ change load quickly

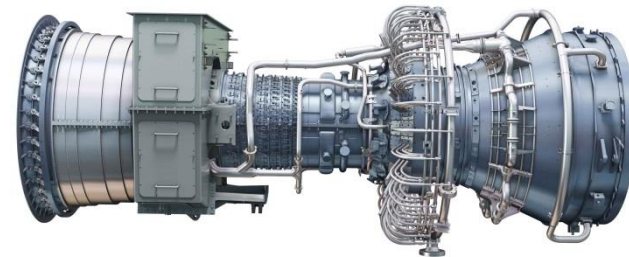
Building a CC with ~50 MW Gas Turbines? Have Fun!

SIEMENS



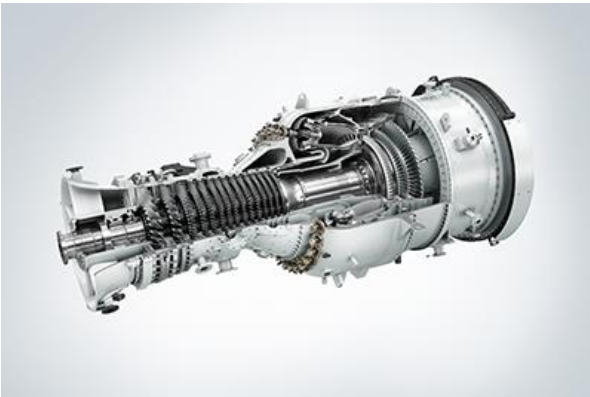
siemens.com

Aero



powergen.gepower.com

Frame



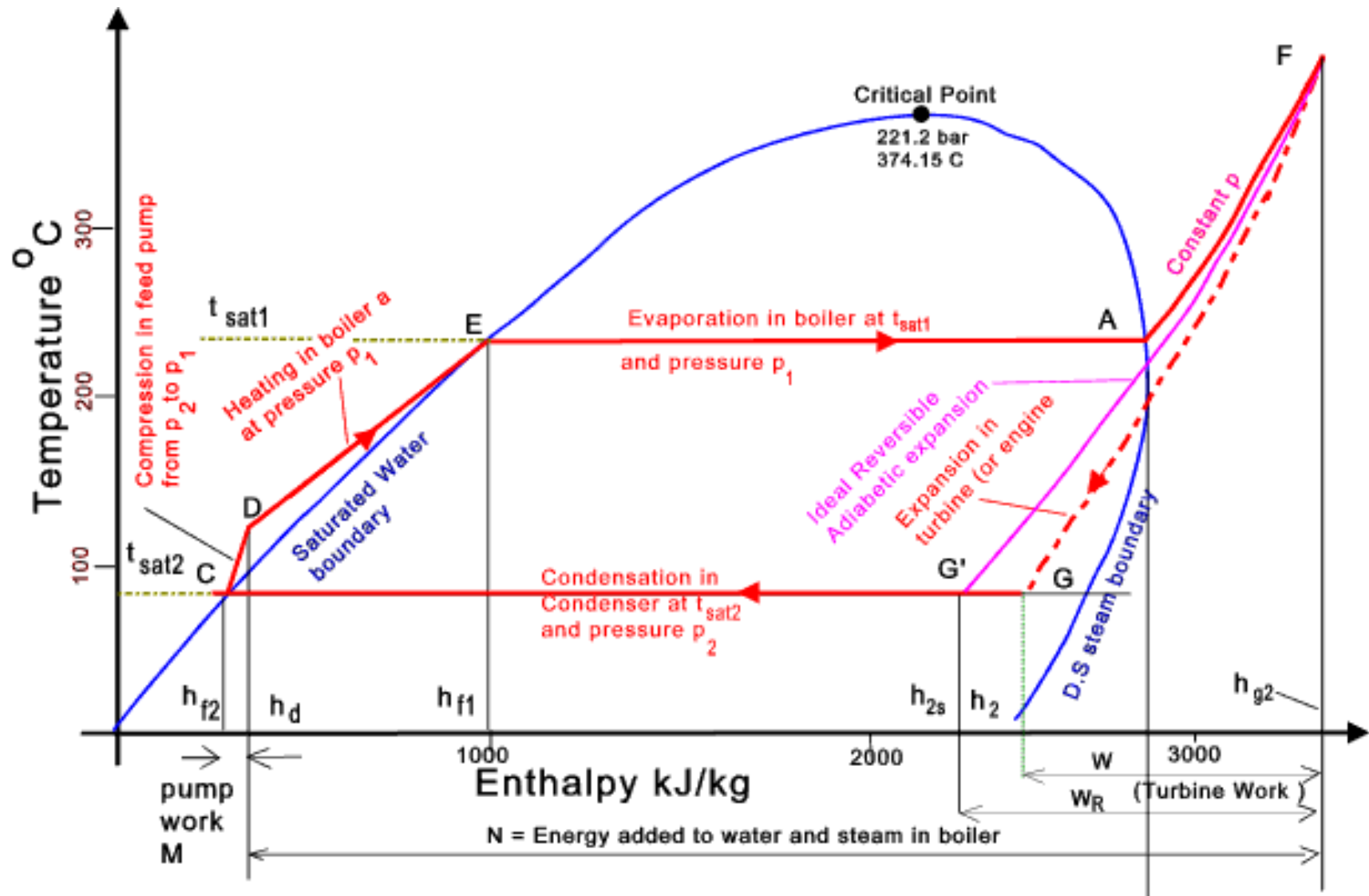
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powergen.gepower.com

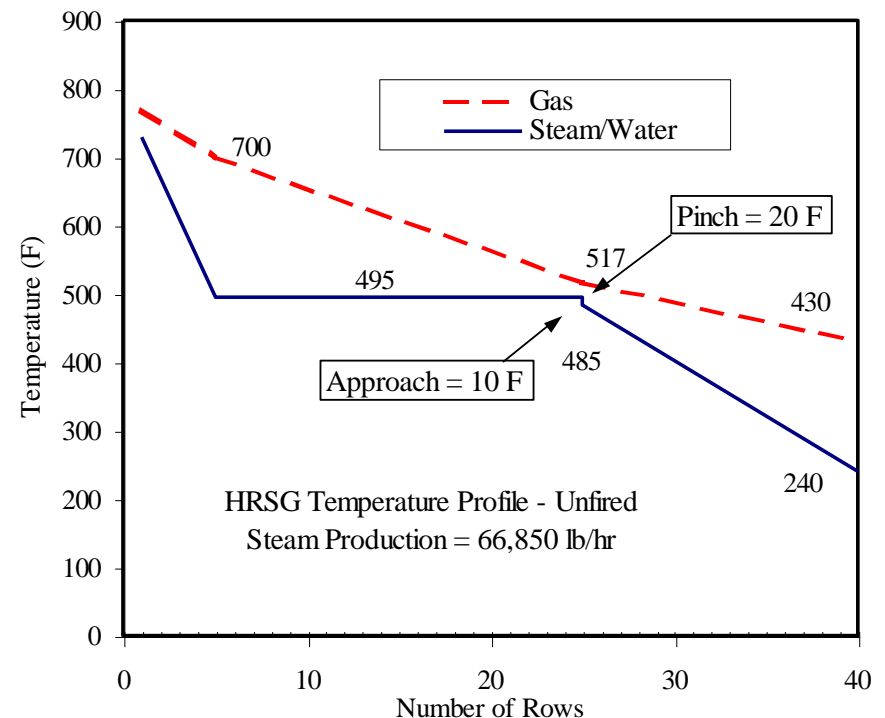
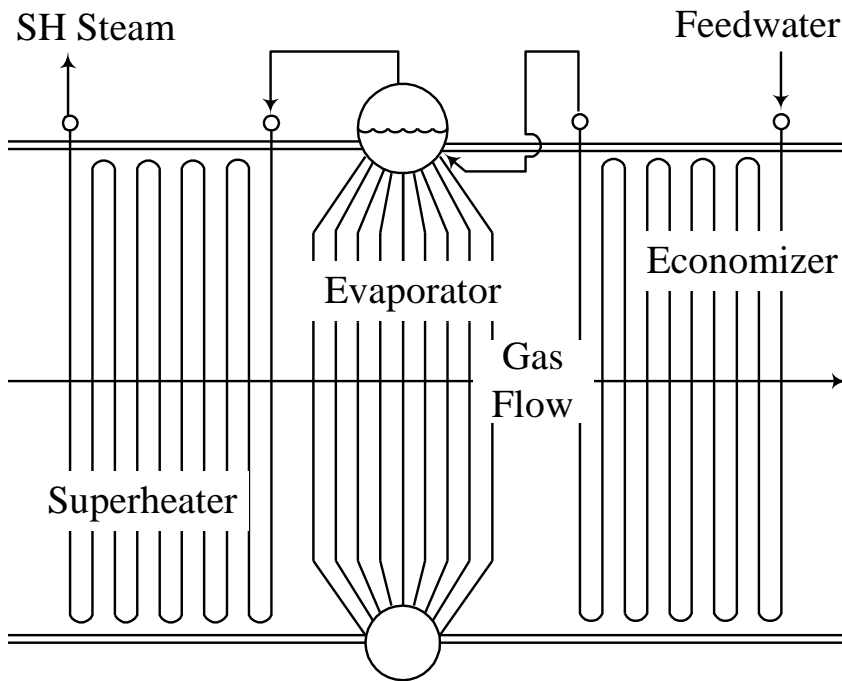
Flexible HRSG Designs

William Rankine Cycle



HRSG Design

- Basic HRSG Design
 - Economizers / Preheaters
 - Evaporators
 - Superheaters / Reheaters



Fundamentals of Transient Response

The laws of the conservation of mass and energy dictate the transient response of steam generators. Simplified equations are provided below.

$$W_s - S_d = d/dt (W_{in}) \dots\dots\dots (1)$$

$$Q_s - Q_d = d/dt (Q_{in}) \dots\dots\dots (2)$$

where:

W_s – quantity of water supplied to the steam generator

Q_s - quantity of heat supplied to the steam generator

S_d – quantity of steam delivered from the steam generator

Q_d – quantity of heat delivered from the steam generator

W_{in} – quantity of water in the steam generator

Q_{in} – quantity of heat in the steam generator

$$Q_{in} = (M_m C_m t_m + M_w C_w t_w + M_s C_s t_s)$$

M - mass

C – specific heat

m – metal

w – water

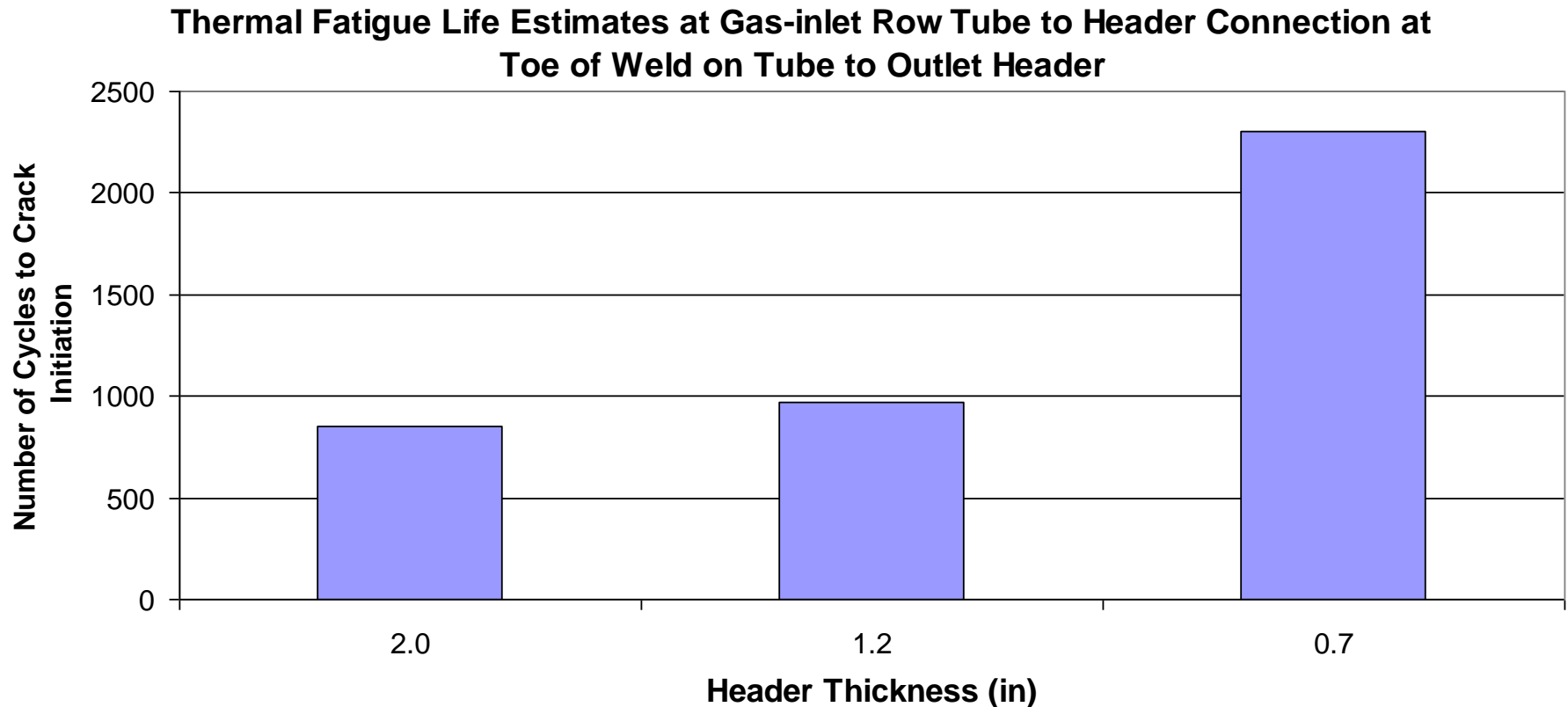
s – steam

Response time is dependant on the water/steam inventory and quantity of heat in the steam generator.



HRSG Design

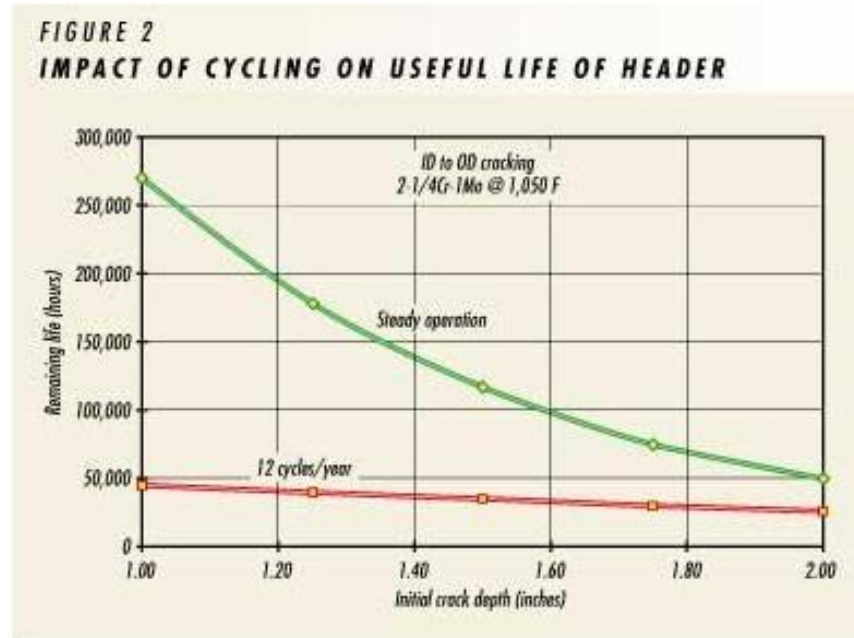
- HRSG design limitations for cycling
 - Thick drums/headers lead to large cyclic thermal stress



Source: Anderson, R. & Pearson, M., Influences of HRSG and CCGT Design and Operation on the Durability of Two-Shifted HRSGs.

HRSG Design

- HRSG operation drawbacks
 - Superheater drain failures during warm starts
 - Slow start up times
 - There are operational means of maintaining drum heat/pressure during a shutdown to minimize thermal cycling



Source: Pijper, A., "HRSGs Must Be Designed for Cycling." Power Engineering, Vol 106, Issue 5.

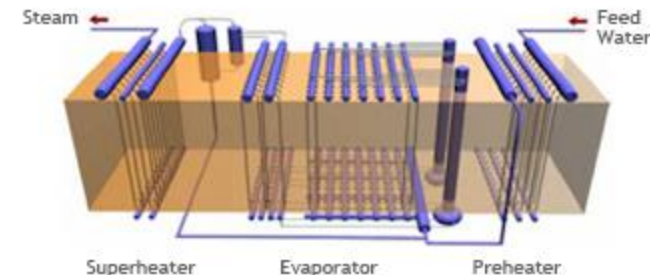
The Industry's Response



- “The HP drum of our DrumPlus™ requires a small wall thickness and nozzle sizes are minimized. As a result peak stresses are significantly reduced.”



- “The startup of a HRSG is limited by the maximum allowable startup saturation temperature rise in the thick HP steam drum (typically in the 2-10° F/minute range).” In reference to the Benson Technology license

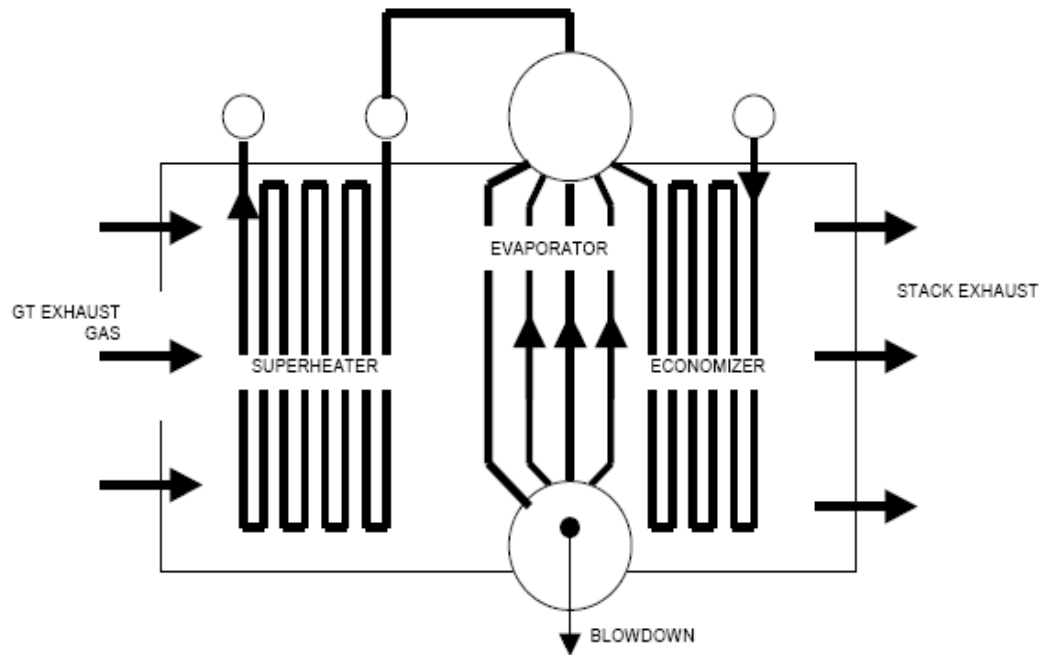


HRSG

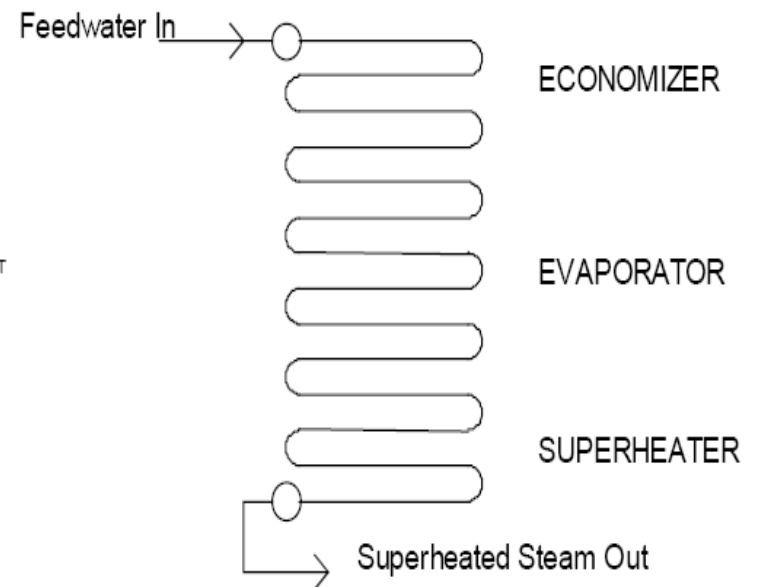
VS

IST OTSG

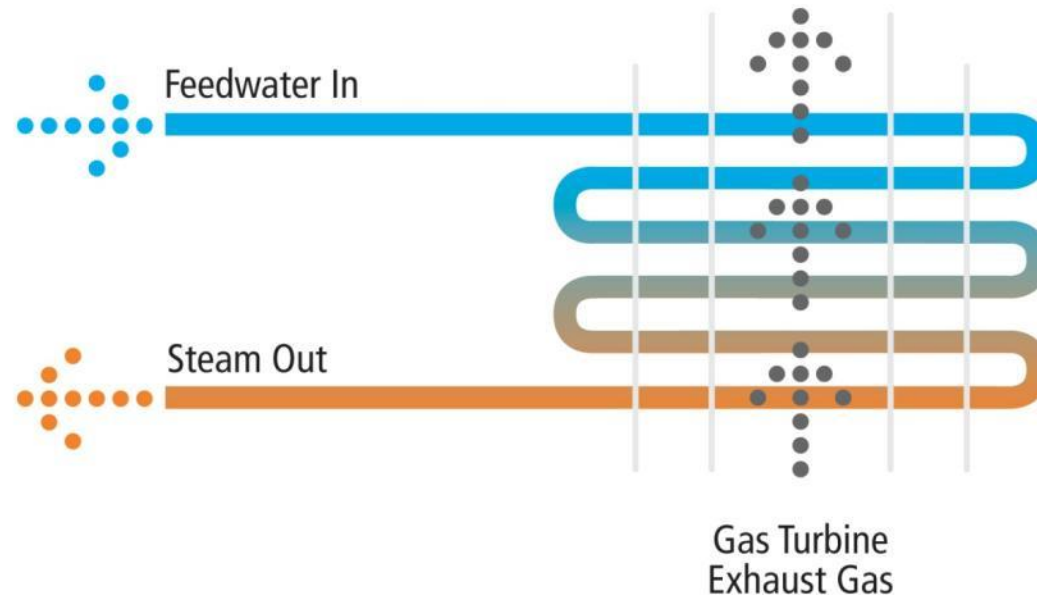
Drum-Type HRSG
Fixed Sections



OTSG Type HRSG
Non Fixed Section

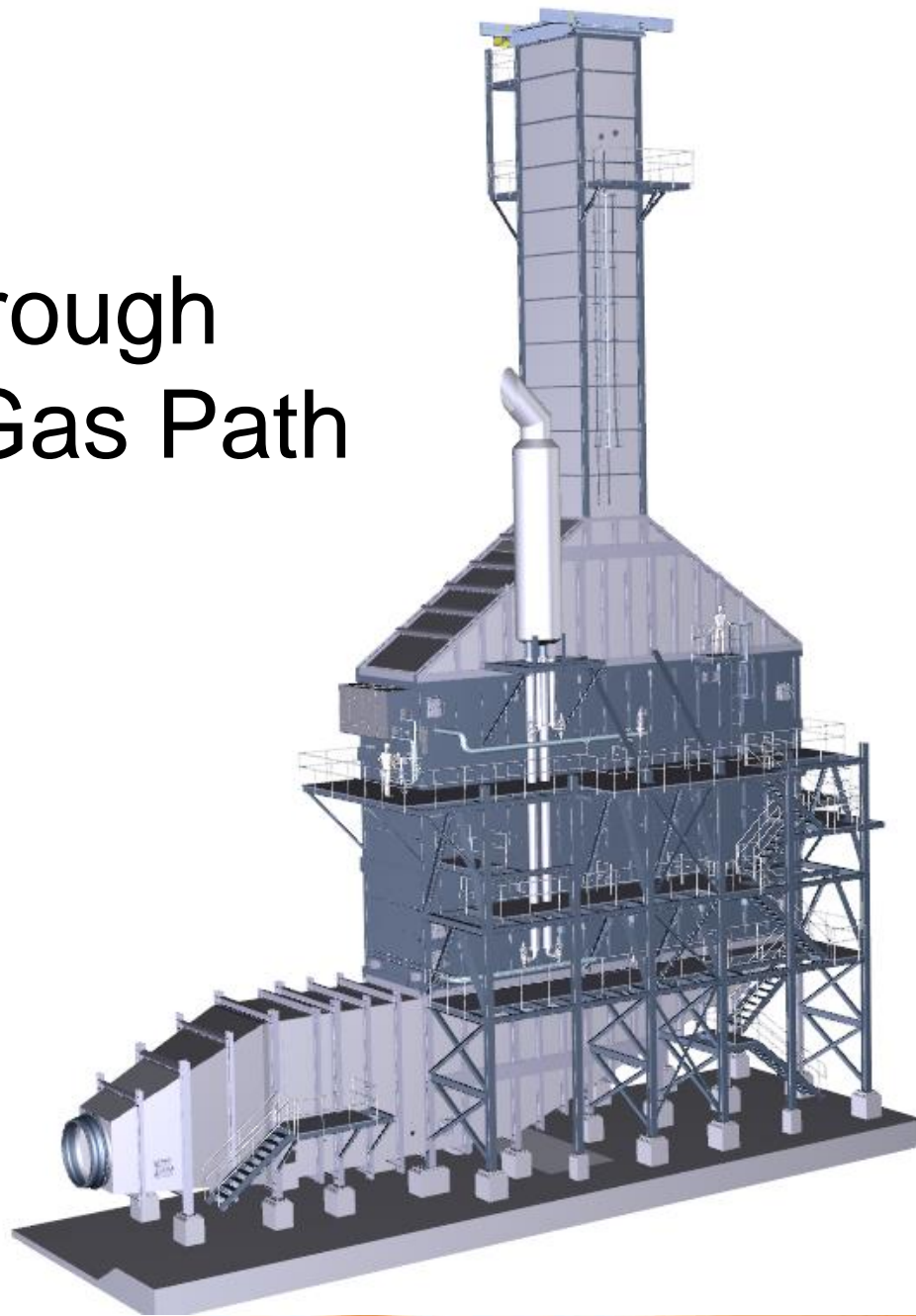


“Drumless” Design



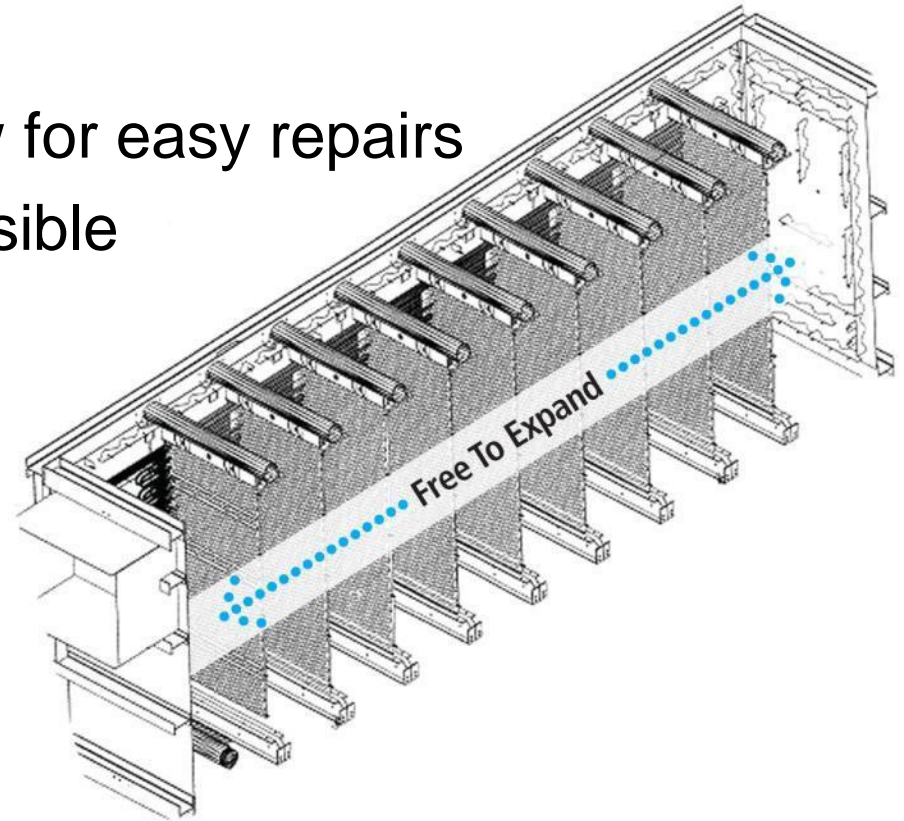
- All tubes thin-walled → low thermal mass → fast cycling
- Compact lightweight pressure bundle
- Simple once through steam path
- Zero Blowdown (no blowdown treatment)

Once Through Vertical Gas Path

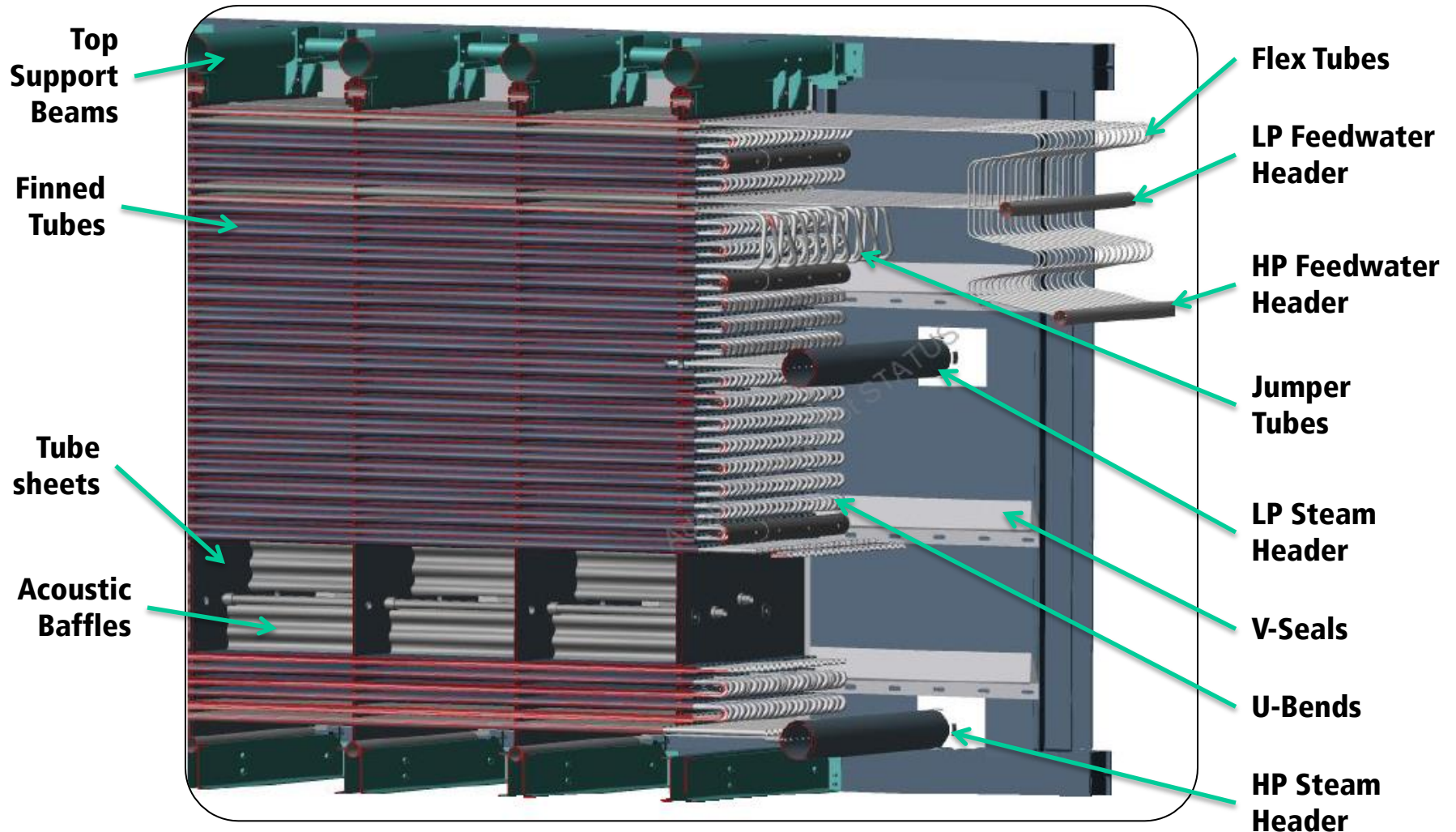


Pressure Module Layout

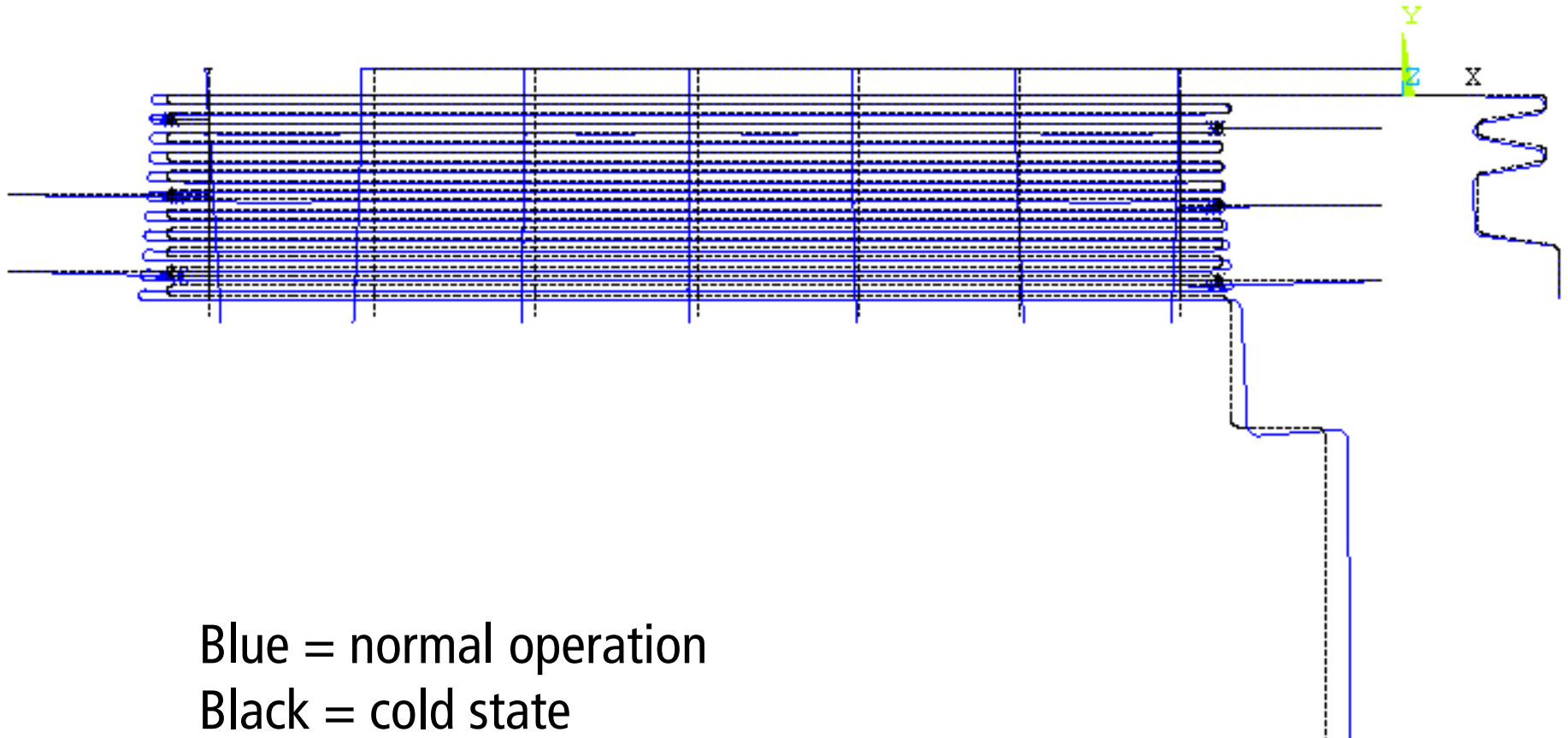
- Tubes held in place by tubesheets
- Entire boiler is designed to freely expand thermally
- Internally insulated casing
- Maintenance cavities allow for easy repairs
- 100% of tube welds accessible



Main Internal Components

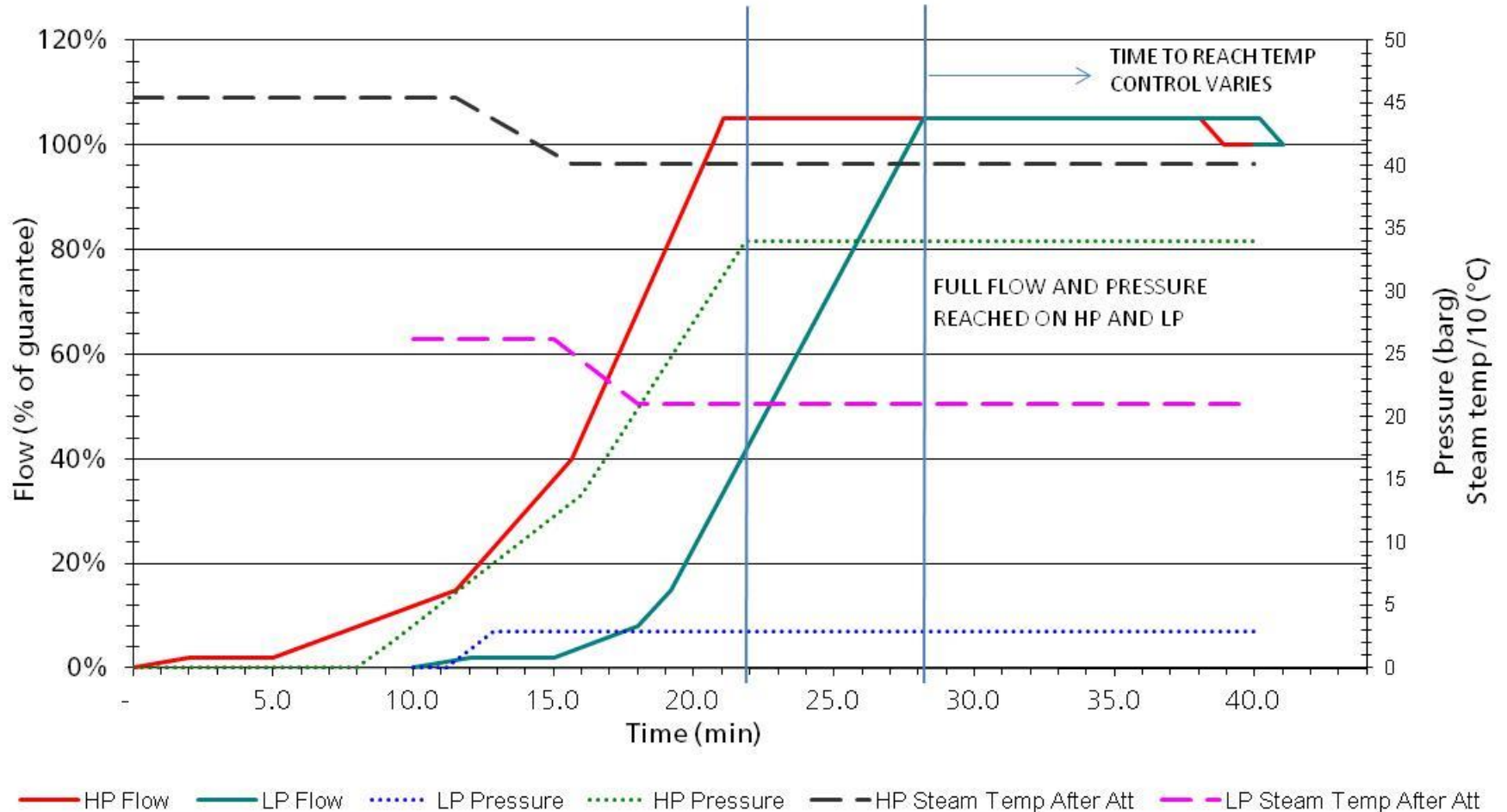


OTSG Bundle Movement



OTSG Start-Up Curve

(Start Permissive approx 12 min from GT ignition without SCR/CO)

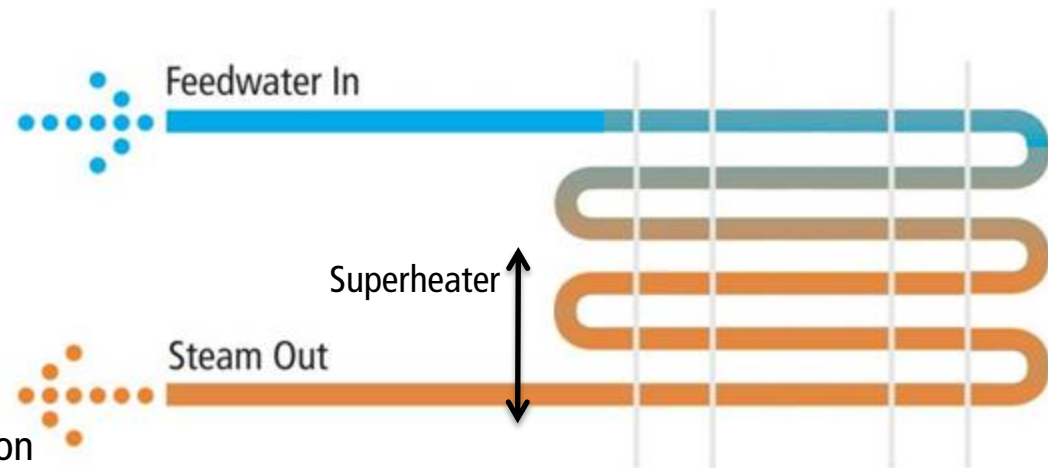


Turndown and Flexibility



Normal Operation

- 2+ rows of economizer section
- 1 row of superheated steam



Turndown Operation

- 1-2 rows of economizer section
- 3+ rows of superheated steam

Supplementary Firing

Supplementary Firing

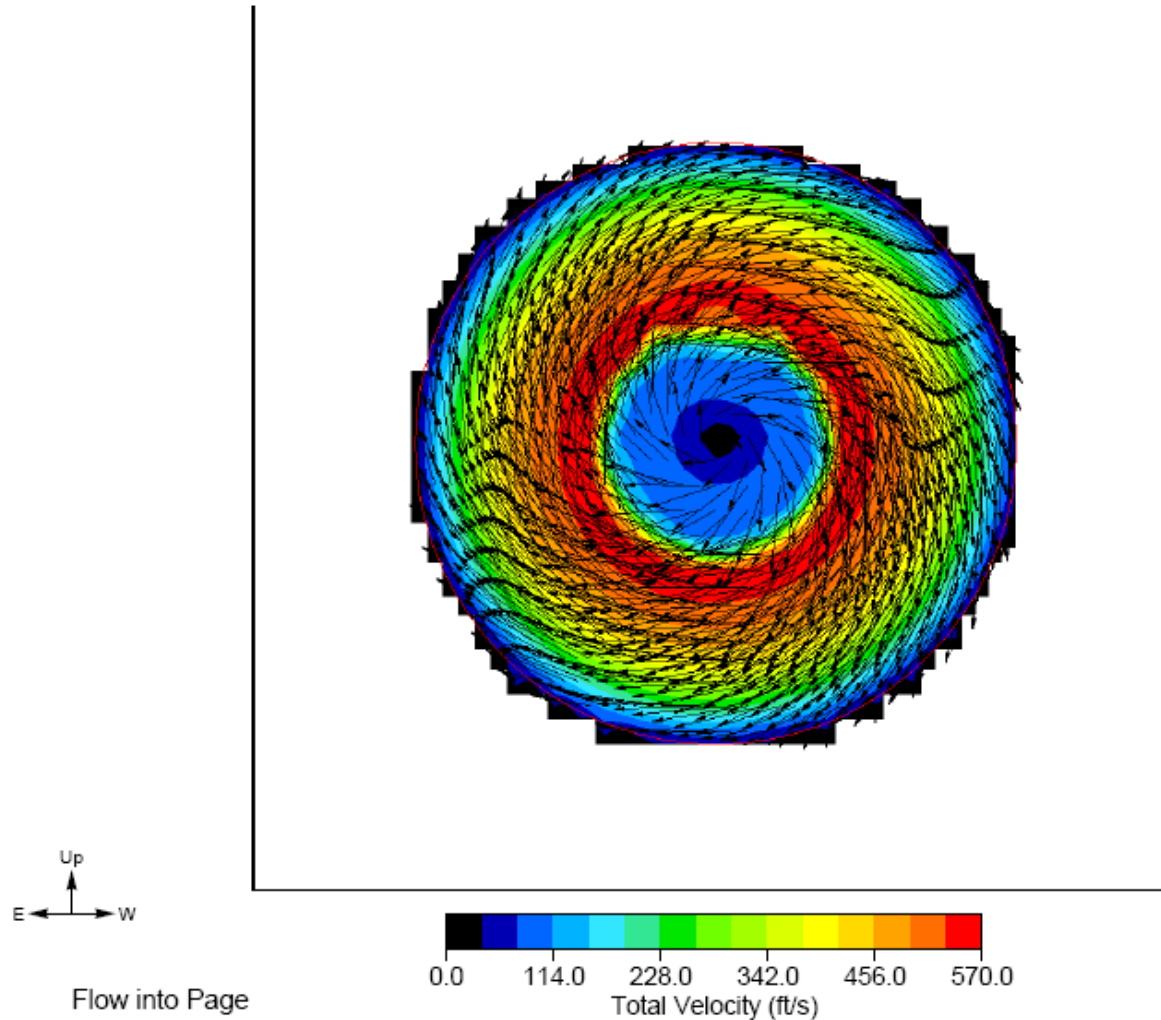
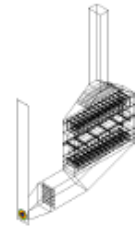
- Combust natural gas (or liquid fuel) in the TEG path to add to the available energy for heat recovery
- Common in cogen applications where the value of the steam exceeds the cost of additional fuel burned
- Natural gas is piped through “runners” and distributed by nozzles across the width of the duct.
- Scope consists of runners, gas distribution manifold, fuel handling skid, and auxiliary blower skid



Supplementary Firing – Velocity Distribution

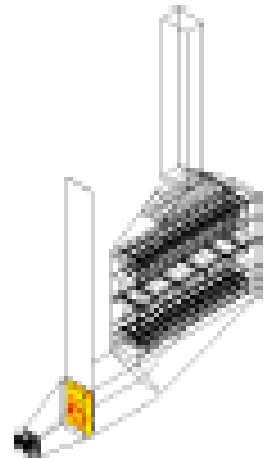
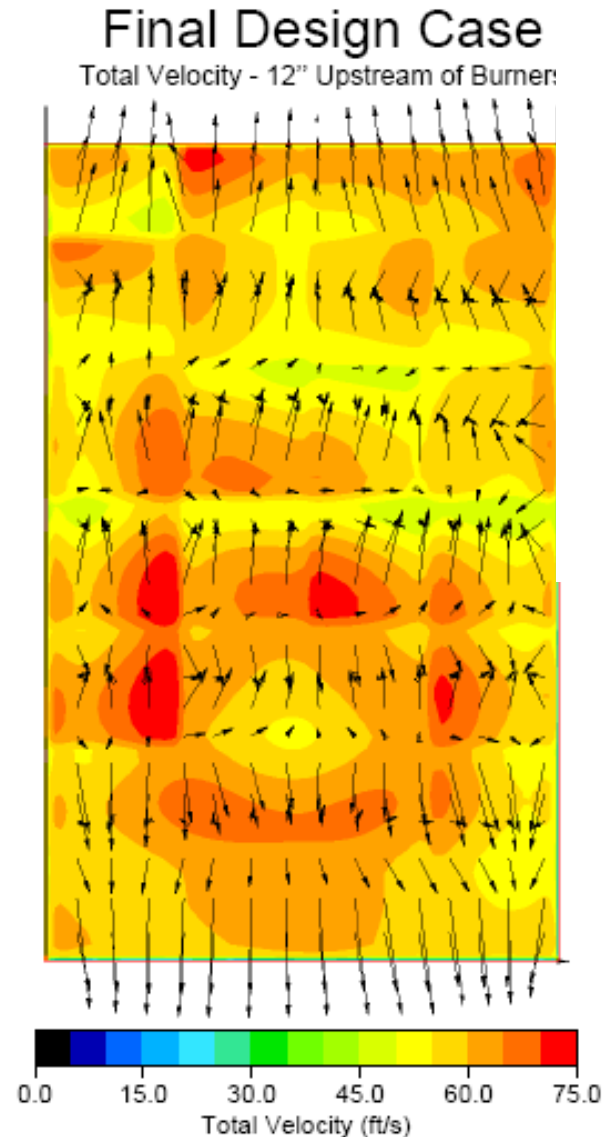
Final Design Case

Total Velocity - OTSG Inlet



Supplementary Firing – Velocity Distribution

- Distribution Grid + Flow Straightener
 - Flatten velocity profile and remove swirl
- Target 75 ft/s normal operation
 - 35 ft/s minimum
- $\pm 10\%$ of average free stream velocity after distribution grid
- Burner duct length provision
 - 1.5x flame length
- Burner duct liner material
 - 409SS, 304SS, 316SS, Piro Block

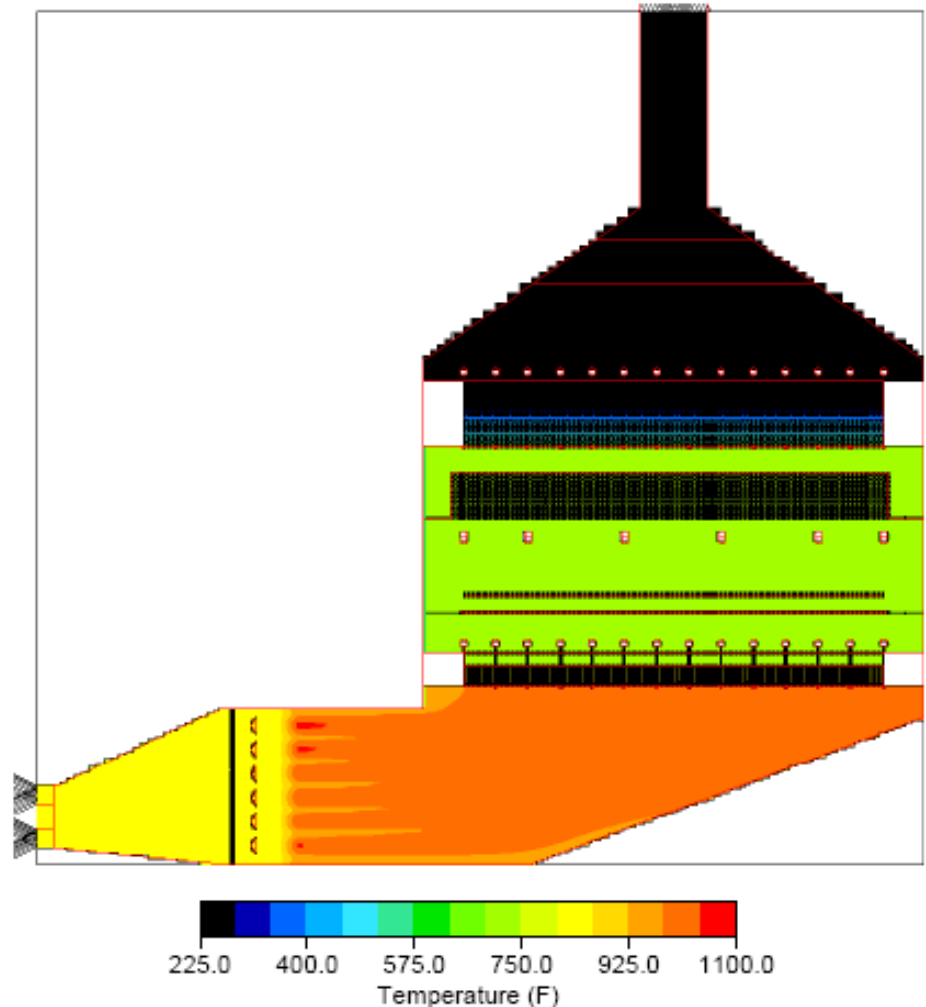


Supplementary Firing – Velocity Distribution

Final Design Case

Temperature - Centreline of OTSG

- Typical temperature distribution guarantee $\pm 10\%$ of the average temperature given a particular velocity profile input guarantee
- Typical heat release from a burner runner is 3 MMBtu/hr per linear foot
 - Increase total heat release by wider duct or more runners (taller duct)
- Duct size is driven by a balance between space required for runners (heat release) and the 75 ft/s target



Module Material Considerations in Fired Applications

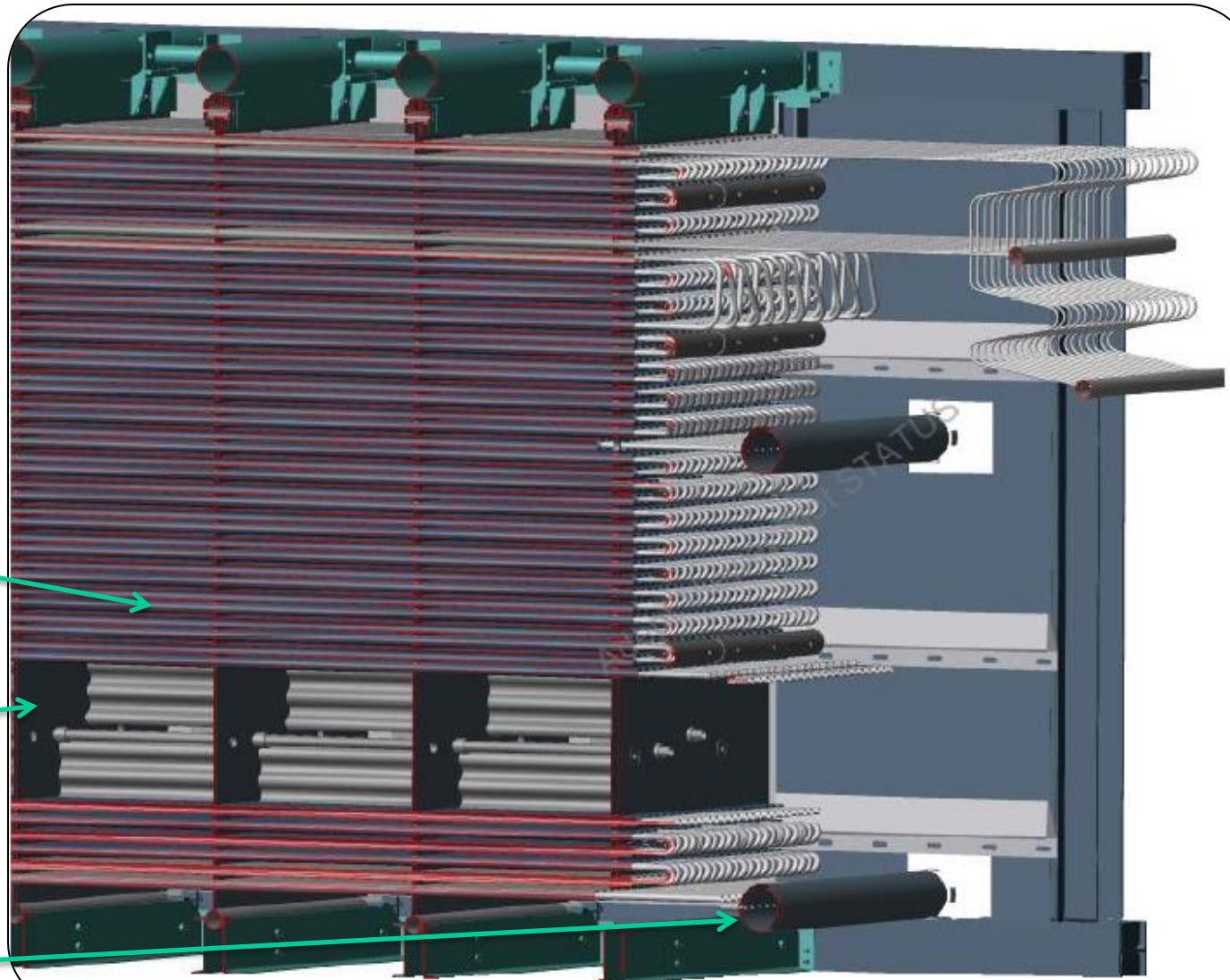
Fin Material

Tubesheets

<1050 F – Chromoly
1050 – 1400 F – 347SS
1400 – 1500 F – NO6617

Steam Headers

P22 or P91



Fin Material Considerations

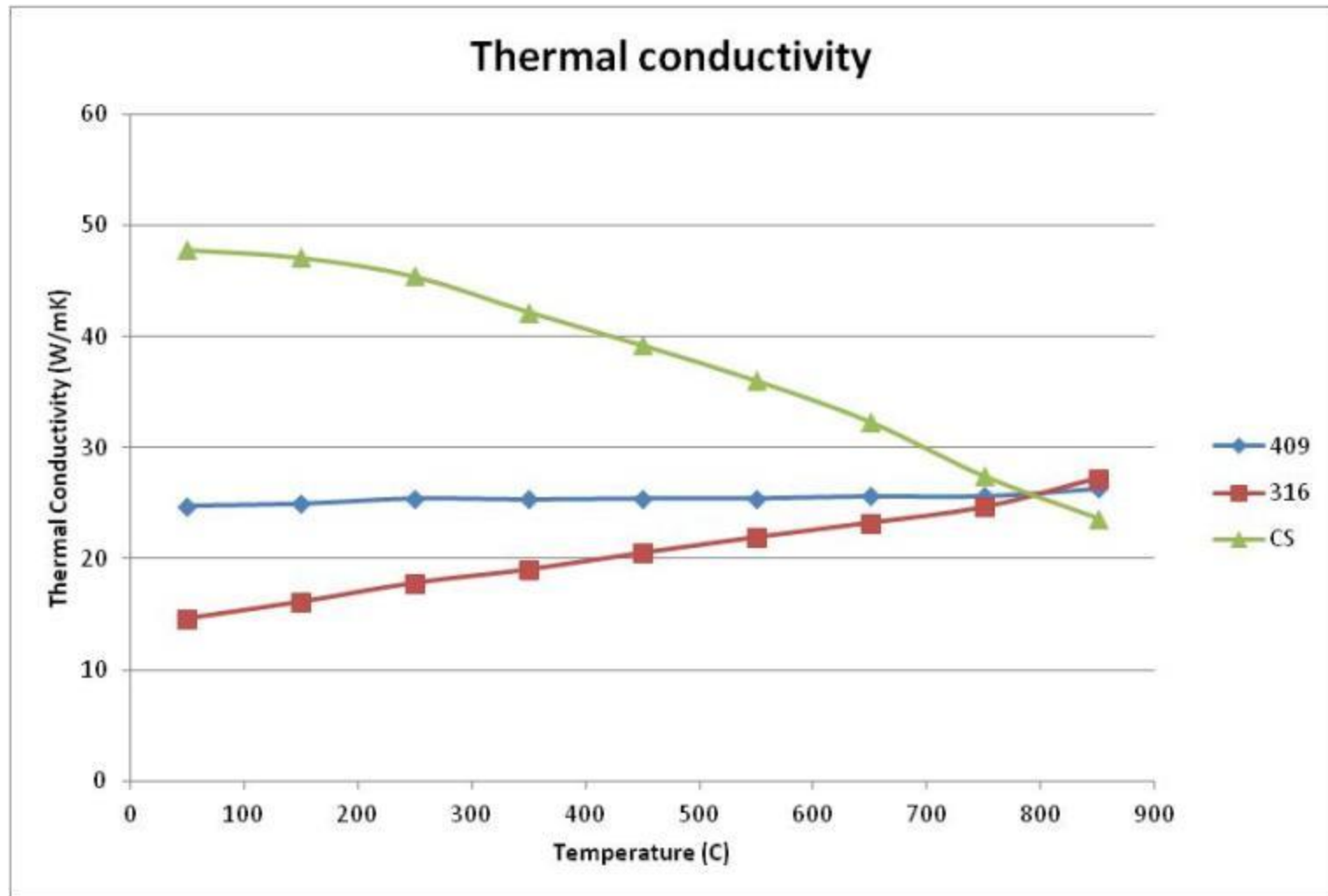
Design Limits

CS < 454 C

409SS < 593 C

316SS < 871 C

Corrosive duty must be considered as well



Fresh Air Firing – Case Study

The image displays three architectural drawings of a building, likely a school or institutional structure, with a focus on mechanical and structural details.

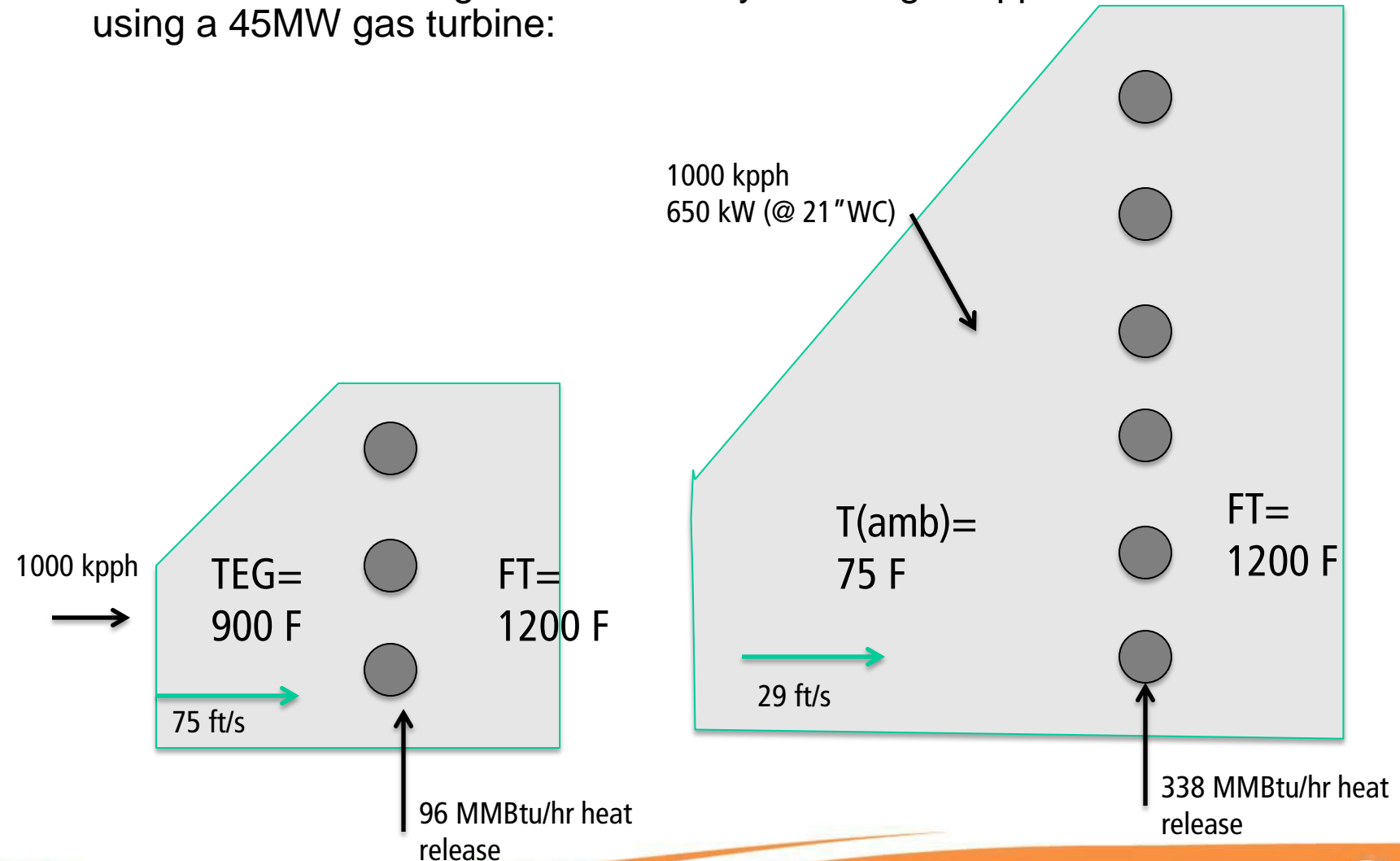
- PLAN VIEW (Top):** Shows a longitudinal section of the building. It includes a central corridor (labeled "CORRIDOR") and various rooms. The drawing is color-coded with green, yellow, and purple. Dimensions and annotations are provided throughout.
- SECTION VIEW (Middle):** A cross-section of the building, showing the roof, walls, and floor. It includes a detailed view of a window or door (labeled "WINDOW") and a section of the roof (labeled "ROOF"). The drawing is color-coded with green, yellow, and purple. Dimensions and annotations are provided throughout.
- DETAIL VIEW (Bottom):** A close-up view of a specific part of the building, showing a window or door (labeled "WINDOW") and a section of the roof (labeled "ROOF"). The drawing is color-coded with green, yellow, and purple. Dimensions and annotations are provided throughout.

The drawings are color-coded and include numerous annotations and dimensions, providing a detailed view of the building's structure and mechanical systems.

- 

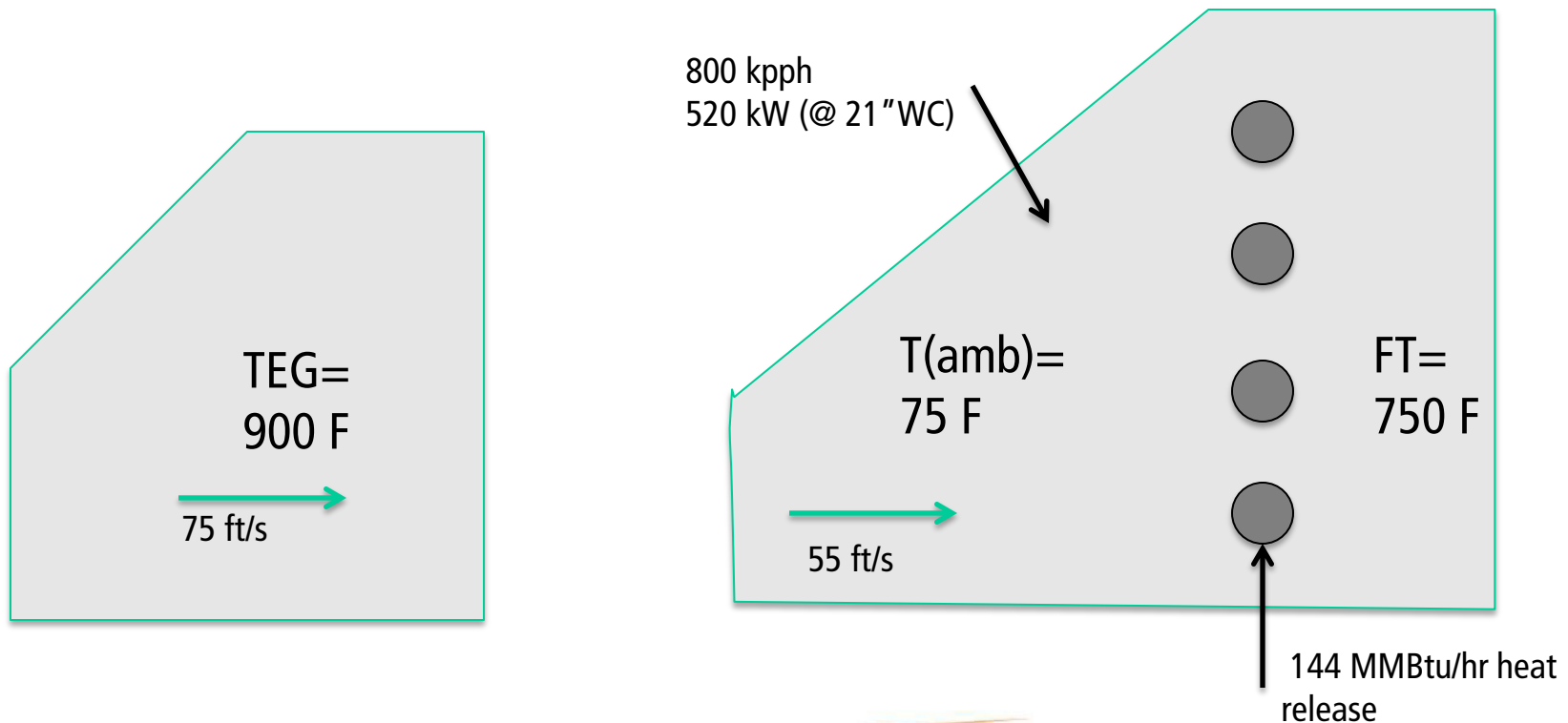
Fresh Air Firing

- Consider the following FAF case study for a cogen application using a 45MW gas turbine:



Fresh Air Firing

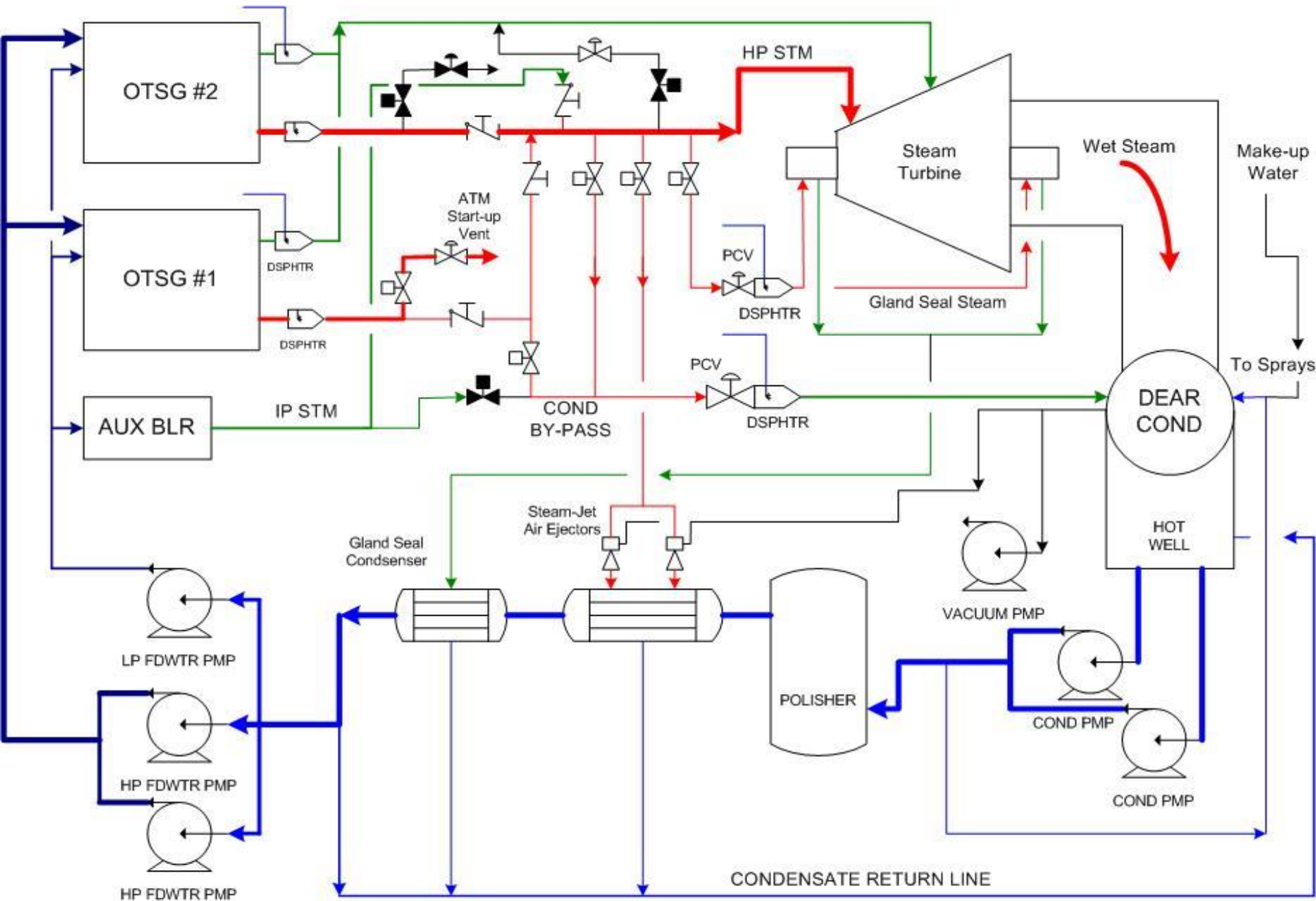
- Conclusion: Managing the flu gas velocity and peak heat release in FAF mode is a considerable challenge. The capital investment and parasitic load associated with the fan often pushes projects toward direct fired aux boilers.
- The compromise:
 - Generate partial steam supply in the FAF case (70 – 80% of unfired capacity)



Balance of Plant Considerations

OPTIMAL STEAM LOOP B.o.P.:

1. Maintain Condensate Loop Vacuum during overnight shutdowns (requires auxiliary boiler)
 - Fastest start due to STG thermal gradient, gland steam, and water chemistry
2. ST- Condenser should be spec'd for part load operation (larger vacuum pumps)
 - Allows gas removal from condensate in turndown modes
3. Dedicated ST Condenser By-passes
 - Minimize water consumption during frequent starts and multi-unit configurations



OPTIMAL OTSG CC PLANT
CONFIGURATION

Fastest Ramping CC in the World

Escatron

Tecnicas Reunidas SA, Zaragoza, Spain

- 4x LM6000 & 4x OTSGs
- Duct fired to 1088 F
- Load ramp from 50% to 100% in 100 seconds



Thank you for your time