

LH2 release
experiments to
support large scale
Shell projects

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Agenda

01 Background

O2 Experimental Programme

03 Process conditions

04 Pool formation

05 Dispersion

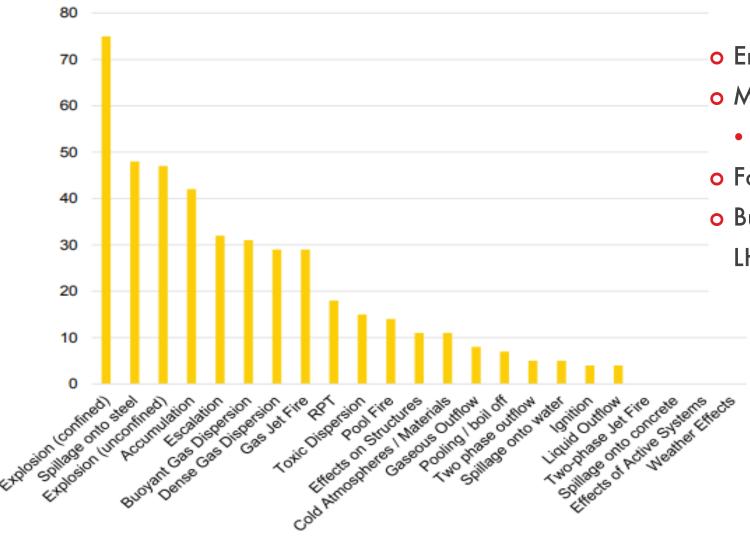
06 Jet Fire

07 Summary

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Further quantification of major hazards required



- Energy transition is driving rapid change
- Many questions raised across industry
 - Especially for Liquid H₂ (LH2)
- Focussed assessment by Shell marine business
- But also unknowns for electrolyser plants,
 LH2 processing and LH2 storage

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Shell H2 experimental programmes

- Urgent demand especially to develop standards
- o JIPs very important but can they answer all the questions?
 - Can be slow to start and generate results
 - Programme is usually a compromise
- Develop dedicated Shell programmes to resolve these urgent questions
 - Is a sustained LH2 pool a credible scenario?
 - Quantify material properties at LH2 temperatures
 - Collaboration with AkzoNobel to test CSP system exposed to LH2
 - Generate dispersion data to confirm predictions for buoyancy
 - Obtain good quality jet fire results
 - Investigate H2 detector performance

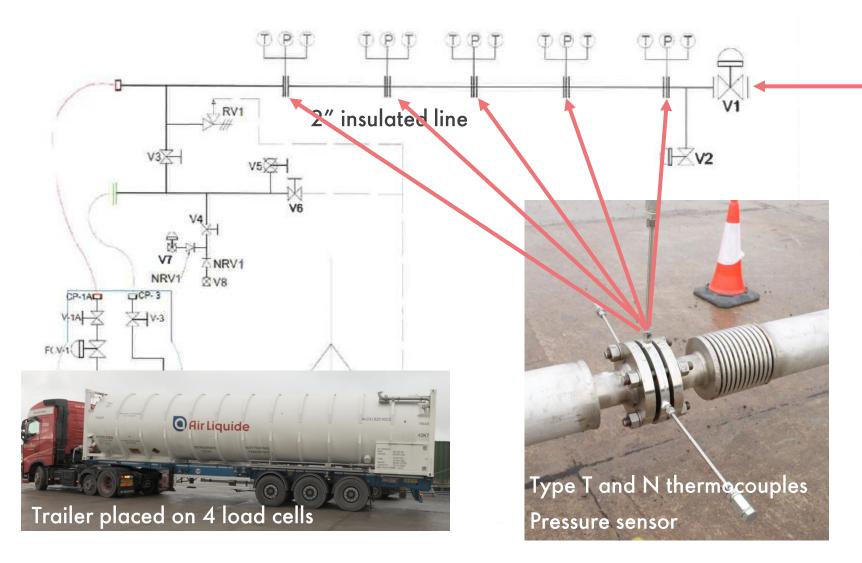
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Experimental programme

LH₂ Supply / Pipe Schematic





Instrument Array - Near Field

- 4 arrays of thermocouples jet impingement measurements
 - 5 Type T thermocouples in each array (cross arrangement)
- 4 Radiometers
 - 30° to horizontal / 120° field of view
 - Positioned 5 m downwind distance and at ±8 and ±12 m perpendicular to release direction
- 8 dynamic pressure transducers (PCB Piezotronics)
 - Similar distance to radiometers



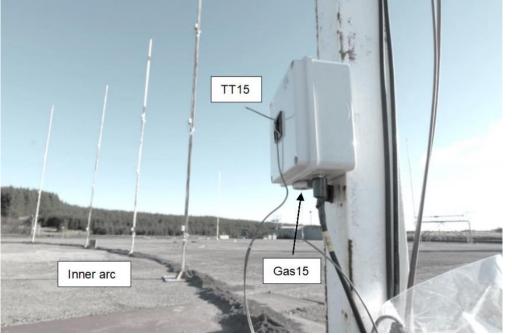




Instrument array - far field

- Two arrays of sensors at 25 and 50 m
- Oxygen depletion and thermocouples at 3 heights up to 8 m
- Ultrasonic detector + five dedicated H₂ detectors





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Experiments

- Approximately 25 releases
 - Each releases about 2-3 mins long
 - Flow rates approximately 0.06 0.91 kg/s
- Range of conditions
 - Orifice size from 5 mm 50 mm
 - Tanker pressure 0.35 3.5 barg
- o Environment
 - Ambient wind speed 1.5 6 m/s
 - Humidity 50 100%
 - Wind direction ±20° along release

- Dispersion
 - Horizontal releases (2 release heights)
 - Pool releases
- o 6 ignited tests with radiometer measurements
- 4 tests filling bunded area
 - Concrete + PFP
 - Different pressure / filling rate
- Jet impingement on I-beam



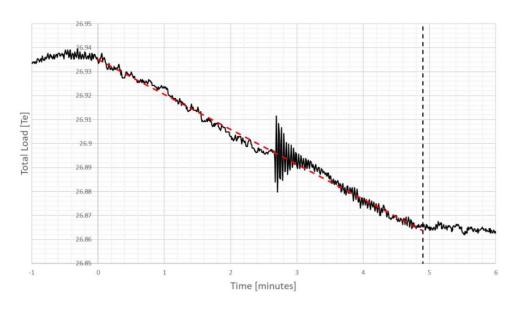
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Process conditions

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Defining the source term

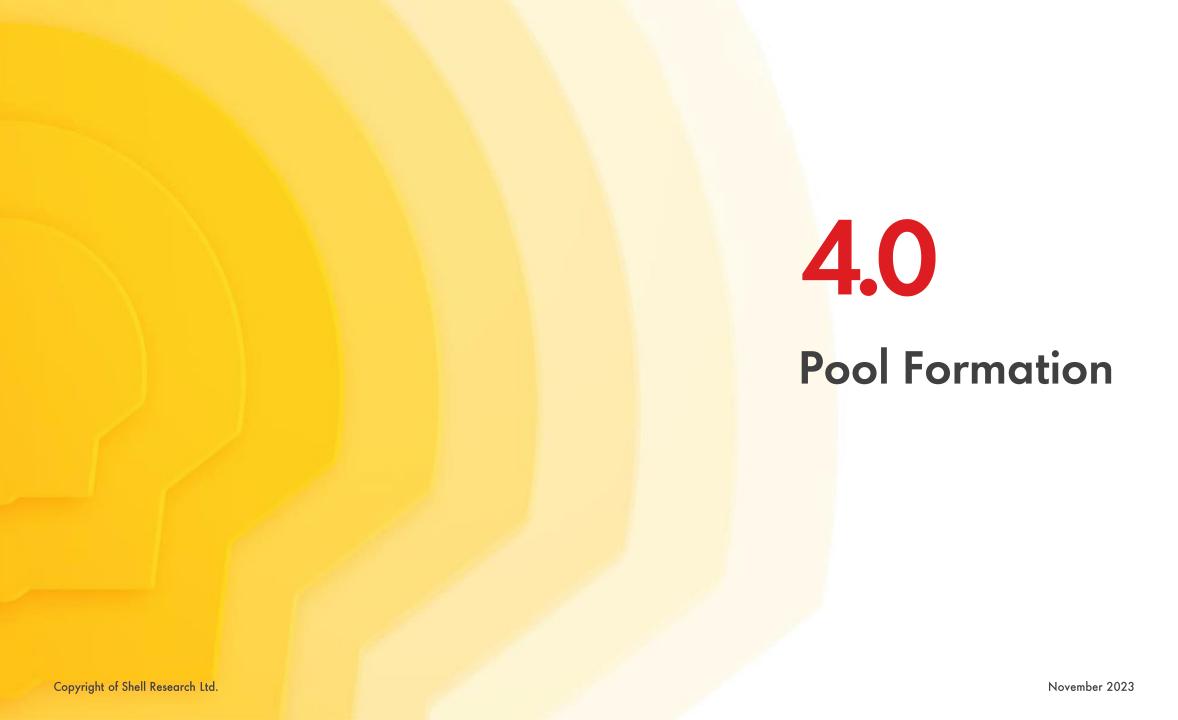
What is coming out of the orifice?





Source (°C)	Type N (°C)	Type T (°C)
LIN (-195.95)	-195.95	-196.82
LHe (-268.95)	-301.02	-252.72





Setup of Pool Bund

- Collaboration with AkzoNobel
 - Resilience of Cryogenic Spill Protection (CSP) to LH2
- o Bunded area based upon ISO22899-1 / ISO20088-1
 - Fill one side with LH2
 - Filled area is $1.5 \times 0.75 \text{ m} = 1.11 \text{ m}^2$
 - Max liquid height 250 mm
- Concrete bund (C40)
 - Same bund dimensions
 - Determine boil off rates
- Source for passive dispersion



Liquid H2 pool on Cold Spill Protection



Integrity of CSP System

- No disbondment or visible defects immediately after LH2 testing
- Jet fire testing of this CSP system showed no adverse properties
- o Similar results when box protected with reduced thickness CSP
- AkzoNobel verified that overall response similar to LIN (for same CSP)





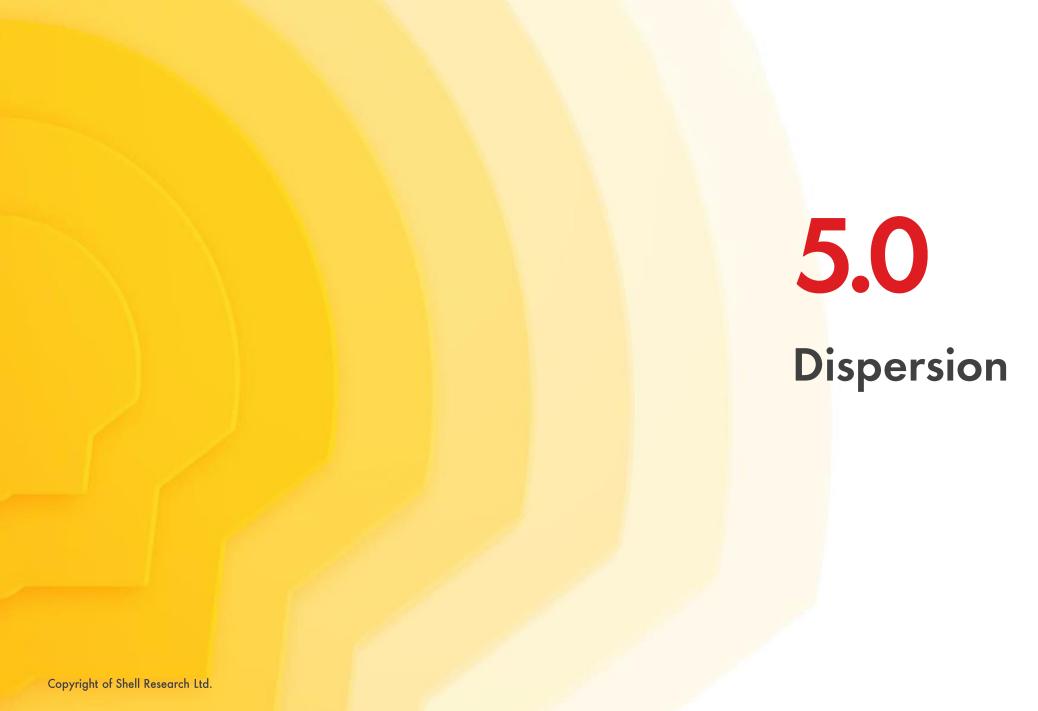


Concrete Bund Test

- Sustained pool formed at
 - Raised pressure 1.0 barg saturation (estimated 0.5 kg/s)
 - 25 mm orifice 570 mm above surface



Bund	Pressure (barg)	Nozzle Height (mm)	Regression rate (kg/m²/s)
Thick CSP	0.3	20	0.014
Thin CSP	0.3	20	0.021
Concrete	0.3	20	0.064
Concrete	1.0	570	Unknown

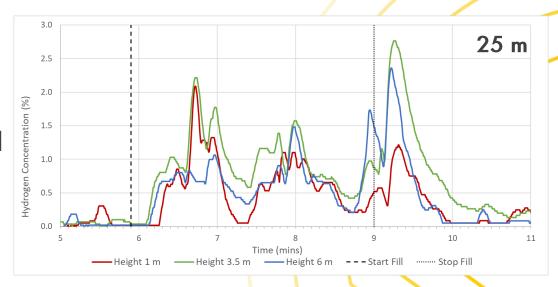


Dispersion From Concrete Bund



Dispersion Results - Concrete Bund @ 1 barg

- Concentration is max value across 5 stands
 - Account for plume meander
 - Concentration peak detected after filling stopped
- o Results @ 25 m
 - Average plume height approximately 3.5 m
- o Results @ 50 m
 - Majority of cloud at 8 m
- Concentrations for pool tests below LFL (4%)
 - At 25 and 50 m





Jet Dispersion

- Results still being analysed
- Some trends on buoyancy





Example of Jet Fire result



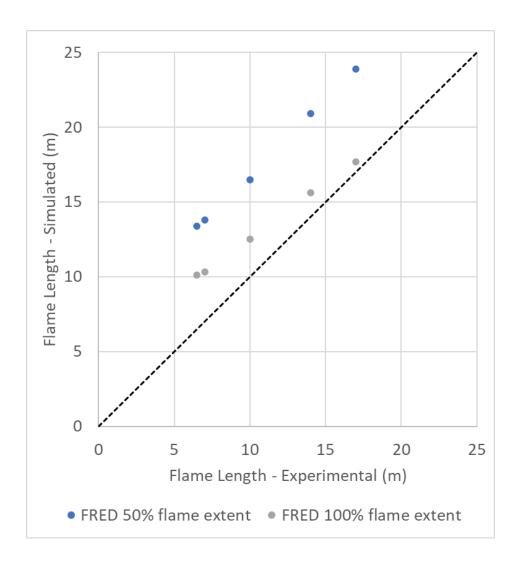


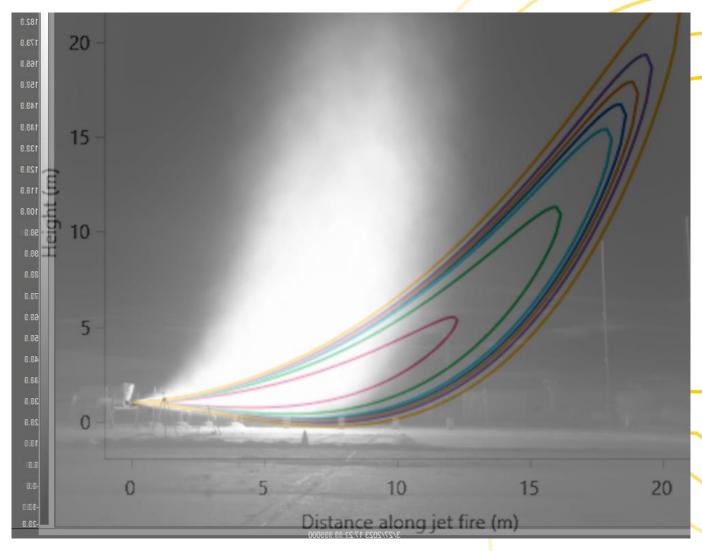
Quantification of Jet Fire Size



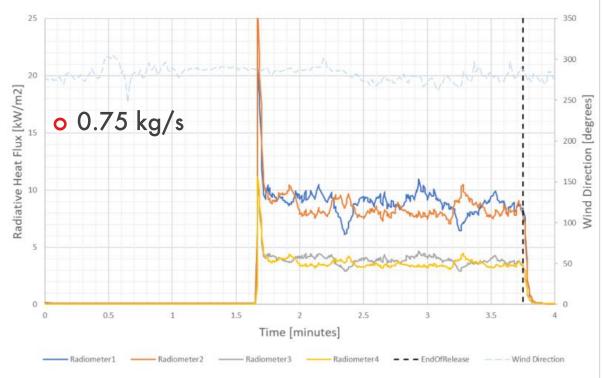
Test ID	Flow Rate	Length (m)	Height (m)
T11	0.24	6.5	6.5
T12	0.27	7	6.5
T16	0.51	10	10
T18	0.75	14	12.5
T21	0.91	17	13

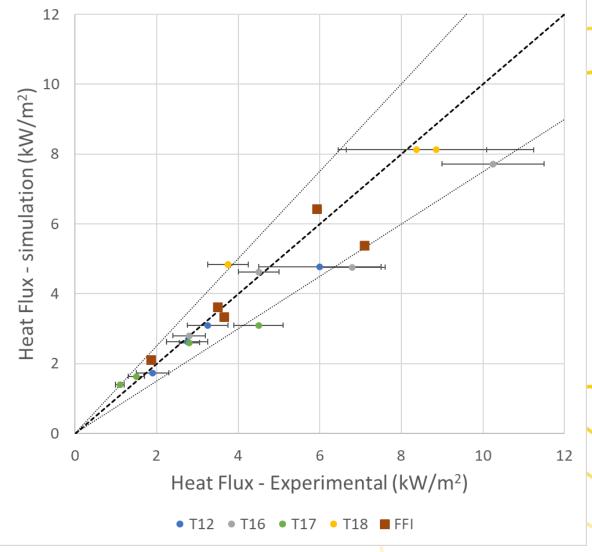
Validation of Jet Fire Model





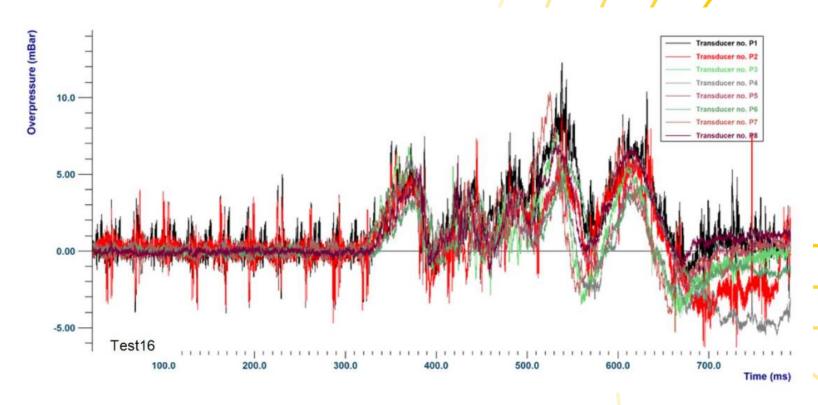
Thermal Radiation





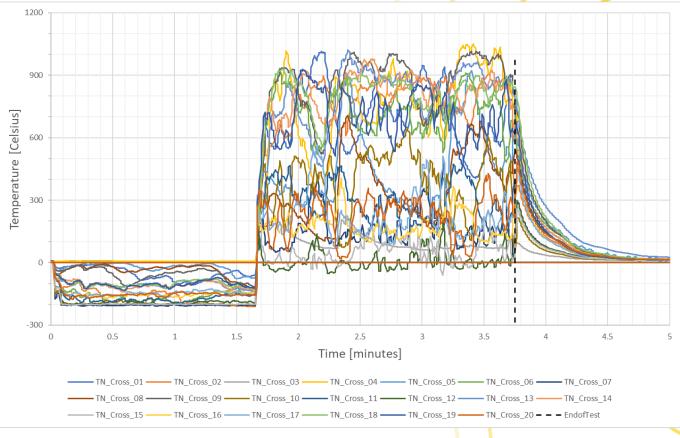
Overpressure

- Overpressure occurred for all ignited jets
 - Max overpressure 4-10 mbar
 - Multiple peaks



Flame Impingement







Summary

- A dedicated experimental programme on large LH₂ releases has started
- A sustained LH2 pool was generated and regression rates calculated
- o An AkzoNobel CSP coating used for marine / offshore deck applications showed no adverse effects
- o Dispersion measurements indicate a transition from dense to buoyant behaviour
- The overpressure following ignition resulted in an OP ≤ 10 mbar
- o Jet Fire results for LH₂ have been quantified (0.25 kg/s to 1 kg/s)
 - LH₂ jet fires have significant buoyancy and standard jet fire models overpredict flame length
 - FRED gives good prediction of overall thermal radiation
- Ongoing work to complete dispersion analysis
- Future work in 2024 is being planned

Q&A



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